



### LanzaTech

Integration of CO<sub>2</sub> Electrolysis with Microbial Syngas Upgrading to Rewire the Carbon Economy

WBS# 5.1.3.101 3/7/20192019 BETO Peer Review  $CO_2$  Session PI - Michael Resch, PhD.

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## **Project Overview**



To incentivize <u>BioEnergy</u> with <u>CO<sub>2</sub></u> <u>Capture</u> and <u>Sequestration</u> (BECCS) we will investigate key gas-to-fuels **process integration hurdles** 

## **Project Goals**

### Goal

• Integration of CO<sub>2</sub> flue gas electrolysis with syngas fermentation

### Outcome

- Determine the impact of varied flue gas compositions on electrolyzer efficiency, lifetime, and specificity
- Examine the relationship of electrolyzer produced syngas upon biocatalytic conversion metrics (conversion efficiency and rate)
- Identify key TEA and LCA drivers
  - max electricity cost for process viability
  - carbon intensity of integrated process
  - feedstock inventory requirements

### **Relevance to Industry**

 By producing valuable products out of CO<sub>2</sub> this project will incentivize CCU to realize carbon circular economy opportunities

### **Quad Chart Overview**

### Timeline

- Start Date: 10/1/2018
- End Date: 9/30/2021
- 8% Complete

	FY 18 Costs	Total Planned Funding (FY 19- Project End Date)		
DOE Funded	\$56k (proposal writing)	\$1.444k		
Project Cost Share*	\$0	\$860k		

•**Partners:** Dioxide Materials (\$100k cost share and \$334k BETO funding), 3M (\$760k cost share), LanzaTech (no cost partner)

### **Barriers addressed**

Ct-A Defining metrics around feedstock quality

Ct-D Advanced bioprocess development Ct-H Gas Fermentation Development

#### Objective

Evaluate and overcome key process hurdles associated with the integration of electrocatalytic  $CO_2$  conversion and biological syngas upgrading, in order to achieve economically-viable, sustainable conversion of biopower-derived flue gases to fuels and chemical intermediates.

#### **End of Project Goals**

- Run the CO<sub>2</sub> electrolyzer integrated to a bioreactor to determine the CO inventory needed to maintain carbon requirements of the bioreactor.
- Determine the minimum and maximum CO concentration that can maintain the microorganism production rate or maintain a revivable dormant state, as well as determine robustness of microorganism
- Determine the minimum electricity cost and carbon intensity of the process.

# **Project Overview**

### <u>History</u>

• Awarded at the start of FY19 as a competitive Biopower Lab Call proposal for Topic 7 *Innovative research to enable economic and impactful biopower with carbon capture in the United States* 

### <u>Goal</u>

- To incentivize BECCS we will investigate key flue gas-tofuels process integration hurdles such as:
  - CO<sub>2</sub> concentration
  - Flue gas contaminates
  - Scaling the integration of the two technologies
  - Biocatalyst performance

## Leveraging Work at NREL



## Leveraging Work at NREL

**2.3.2.102** Biogas to Liquid Fuels and Chemicals using Methanotrophic Microorganisms



## Approach - Management





# **ENREL** LanzaTech

### Task 1 - Liu (DM) CO<sub>2</sub> Electrolyzer performance optimization

Design and fabricate a carbonand energy-efficient CO<sub>2</sub> electrolyzer with optimized functionality on biopowerderived effluent gas streams. Task 2 - Guarnieri

### Gas fermentation Process Development and Strain Optimization

Define microbial and gas fermentation requirements to maximize the carbon uptake and conversion efficiencies. Task 3 - Resch

### Analysis and Integration of Combined CO<sub>2</sub> electrolysis with gas fermentation

Integrate technologies to increase the carbon efficiencies of BECCS and other industrial processes by creating valuable products from waste gas sources.

### **Technical Approach**

Integration of CO<sub>2</sub> electrolysis with gas fermentation

## CO<sub>2</sub> Electrolysis

### $CO_2$ + electricity $\rightarrow CO + \frac{1}{2}O_2$

### $2OH^- \rightarrow H_2O + 2e^- + \frac{1}{2}O_2$



### $CO_2 + H_2O + 2 e^- \rightarrow CO + 2OH^-$

The DM/3M Team's Effort: Converting CO<sub>2</sub> Electrolysis From A Laboratory Curiosity To Real Technology

# **Biological Conversion of Syngas**

Diversity of Clostridia autoethanogenum

#### **Rigorous Development and Modeling Enabled Wide Range of Feedstock**



Any combination or interpolation of these can be used for ethanol production with only a change in operating conditions

LanzaTech

No Carbon Left Behind™

## 2 – Approach (Technical)

### **Critical Success Factors**

- Identify flue gas contaminants and toxicity to electrolyzer catalysts
- Flue gas contaminants toxic to electrolyzer membranes
  - Implement gas clean-up strategies
- Poor biocatalyst conversion rate
  - Generate variants with enhanced CO conversion capacity via random and targeted mutagenesis.

## 2 – Approach (Technical)

### **Potential Challenges**

- Electrolyzers unable to reach 200 mA/cm<sup>2</sup> at high selectivity on low concentration  $CO_2$ 
  - Build a larger electrolyzer to meet needs of fermenter.
  - Increase CO<sub>2</sub> concentration into electrolyzer
- Flue gas contaminants toxic to electrolyzer membranes
  - Implement gas clean-up strategies
- Poor biocatalyst conversion rate
  - Generate variants with enhanced CO conversion capacity via random and targeted mutagenesis.

### Progress

Integration of CO<sub>2</sub> electrolysis with gas fermentation

## Lab Set-up Progress



- Safely Integrate electrolysis with CO gas fermentation at NREL
- Scale matching and gas compatibility
- ✓ P&ID
- ✓ Electrical
- ✓ Hazard Review
- Lab Set up

- Integration
- Industrial flue gas analysis

# Investigating Industrial Flue Gas



### Relevance

# Industrial Relevant CO<sub>2</sub> Feedstocks

F	Process	CO <sub>2</sub> concentration in gas stream % by vol.	Number of sources	Emissions	% of total CO <sub>2</sub> emissions	Cumulative total CO <sub>2</sub> emissions (%)	Average emissions/source (MtCO, per source)	
(	CO, from fossil fuels or :	(						
F	Power							
	Coal	12 to 15	2,025	7,984	59.69	59.69	3.94	
	Natural gas	3	985	759	5.68	65.37	0.77	
	Natural gas	7 to 10	743	752	5.62	70.99	1.01	
	Fuel oil	8	515	654	4.89	75.88	1.27	
	Fuel oil	3	593	326	2.43	78.31	0.55	
	Other fuels <sup>a</sup>	NA	79	61	0.45	78.77	0.77	
	Hydrogen	NA	2	3	0.02	78.79	1.27	
Ν	Natural-gas sweetening							
Bioenergy Fermentation			3 to 8			213		
			100			90		
_	Other processes	1174	07	10	0.12	20.22	U.1/	
F	Petrochemical industry							
	Ethylene	12	240	258	1.93	98.85	1.08	
	Ammonia: process	100	194	113	0.84	99.70	0.58	
	Ammonia: fuel combustion	8	19	5	0.04	99.73	0.26	
	Ethylene oxide	100	17	3	0.02	99.75	0.15	
(	Other sources							
	Non-specified	NA	90	33	0.25	100.00	0.37	
			7,584	13,375	100		1.76	
(	CO <sub>2</sub> from biomass <sup>e</sup>							
	Bioenergy	3 to 8	213	73			0.34	
	Fermentation	100	90	17.6			0.2	

Gale et.al. IPCC Special Report on Carbon dioxide Capture and Storage. (2005)

## Compositions of Biopower Facility Flue Gas

Biopower from biomass could include Combustion, Co-firing, Gasification, Pyrolysis, and Anaerobic Digestion

- 1. Gasifier from waste wood to power 1.5 gen facility
  - ~65% N
  - 14-17% CO<sub>2</sub>
  - ~2% O<sup>2</sup>
  - 15-30 ppm VOCs
  - 30 PPM NO<sub>x</sub>
  - VSCs
- 2. Fermenter Flue Gas Composition
  - 99%+ CO<sub>2</sub>
  - ~51000 #/hr CO<sub>2</sub>
  - Minimal O<sub>2</sub>
  - VOC and VSCs

## **BETO Conversion Relevance**



- This project supports BETO **Conversion R&D** Portfolio which focuses on earlystage technology R&D.
- Use low carbon renewable electricity to catalytically reduce  $CO_2$  into CO intermediate and upgrade into biofuels and bioproducts, to enable BECCS.



Supports BETO's mission to "develop industrially relevant, transformative, and revolutionary **bioenergy technologies** to enable **sustainable, domestically produced biofuels**, bioproducts, and **biopower** for a prosperous nation."

Also directly supports BETO's strategic goal to *enable* use of *America's abundant biomass and waste resources* for advanced biofuels, biopower, and bioproducts by:

- Identifying and developing biofuel pathways and innovative end uses;
- Completing applied R&D on complex, real world systems, and integrating engineering processes for promising new advanced bioenergy technologies;
- While maintaining or enhancing economic, environmental and **social sustainability**.

# Preliminary TEA



Current SOT and impacts of electricity price and electrolyzer capital costs to minimum ethanol selling price (MESP).

### **Future Work**

Integration of CO<sub>2</sub> electrolysis with gas fermentation

## **Electrolytic Gas Stream Evaluation**

### Goal:

1. Identify filtration, purification, and concentration impacts upon performance metrics for electrolyzer output stream composition as well as biocatalyst performance.

#### Approach:

- 1. Establish integrative electro-biocatalytic fermentation capacity.
- 2. Evaluate gas streams from diverse points sources; conduct off gas analyses to establish conversion efficiencies on varied CO<sub>2</sub> concentrations and trace compositions.
- 3. Define biocatalyst growth capacity and productivity in 0.1-5L gas fermenters as a function of input gas composition.
- 4. Develop smart control systems to maximize performance.

**Systems Integration (3/31/20):** Set-up an integrated 25 cm<sup>2</sup> CO<sub>2</sub> electrolyzer feeding syngas into a 2-5L gas fermenter and run for 24 hours



# Strain Engineering

#### Goals:

- 1. Generate a minimal *Clostridia autoethanogenum* genome with maximal fitness (growth rate, carbon efficiency, flux to product)
- 2. Adapt strain(s) to electrolysis-derived syngas stream(s).

#### Approach:

- 1. Generate a genome-wide transposon library.
- 2. Conduct next-gen sequencing to define insertional frequency and essential genes.
- 3. Chemostat+adapted evolution on top-candidate strain variants.



9/30/2019 Generate and screen >1,000 biocatalyst variants for enhanced conversion.



# Summary

- **1. Overview** This project will determine the viability of converting CO<sub>2</sub> into fuels and chemicals
- 2. Approach Integration and optimization of electrolysis with gas fermentation
- **3.** Technical Accomplishments/Progress/Results Establishing core capabilities at NREL
- **4. Relevance** Innovative research to enable economic and impactful biopower with carbon capture in the United States
- 5. Future work
  - Evaluate Biopower flue gas streams
  - Electrolyzer compatibility and scaling
  - Strain Engineering and assimilation improvements
  - Electrolysis and gas fermentation integration
  - Identification of key technical hurdles for industrial applications

#### Team Members:

NREL: Michael Guarnieri Holly Rohrer

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**3M:** Laura Nereng Chris Thomas

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### Thank You

#### www.nrel.gov

**Publication Number** 

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## **Project Milestones**

- **Kickoff Meeting (Q1):** Establish lab set-up, safety requirements, tech transfer, and partner deliverables. Identify two industrial biopower flue gas streams and quantify chemical composition.
- Establish cultivation capacity (Q2): Establish and demonstrate mid-throughput, 0.1-5L batch and chemostat cultivation capacity for CO gas fermentation
- **TEA/LCA Baseline (Q3):** Provide overall integrated process concept, process conditions and parameters for major unit operations, and support analysis team data for TEA and LCA studies to establish a baseline for the current state-of-the-technology.
- **Biocatalyst and Protein Engineering. (Q4):** Generate and screen >1,000 biocatalyst variants for enhanced conversion.
- Electrolyzer fabrication and operation. (12/31/2019): Using a CO<sub>2</sub> 25 cm<sup>2</sup> electrolyzer, we will accomplish continuous operation on an influent gas stream with <50% CO<sub>2</sub> content to identify baseline. Identify filtration, purification, or concentration impact upon performance metrics for electrolyzer output stream composition as well as biocatalyst performance on varying syngas mixtures needed on each gas stream input to maintain 100 hours of performance of the CO<sub>2</sub> electrolyzer and bioreactor.
- Systems Integration (3/31/20): Set-up an integrated 25 cm2 CO<sub>2</sub> electrolyzer feeding syngas into a 2-5L gas fermenter and run for 24 hours
- Process Integration (9/30/21): Run the CO<sub>2</sub> electrolyzer integrated to a bioreactor to determine the CO inventory needed to maintain carbon requirements of the bioreactor. Determine the minimum and maximum CO concentration that can maintain the microorganism production rate over a 100-hour test period. Determine the minimum electricity cost and carbon intensity of the process.