# The Role of Hydrogen in the 21<sup>st</sup> Century BioEconomy

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## Outline

- The Need for Hydrogen in BioEconomy Biofuels Bioproducts
- Renewable Hydrogen Production Pathways
- Waste to Hydrogen Concept
- Integration of Hydrogen Production and Biorefinery
- Path to Carbon-Negative Economy or Circular Economy
- Broader impact
  - Water-Energy Nexus
  - Resource recovery: P, N, metals, water



### Hydrogen in Biomass to Biofuels Pathways

- Biomass contains 35-40% oxygen
- Deoxygenation requires significant amount of reductant to preserve carbon and minimize CO<sub>2</sub> release
- Typical hydrogen sources
  - Natural gas
  - Electricity (derived from fossil?)
- Increasing availability of renewable hydrogen sources solar, wind, biomass
- Smart ways to incorporate these sources into the biorefinery are needed!



# **Hydrogen for Bioproducts**

- Aromatics
  - High yields of aromatics from biomass are possible via Integrated Catalytic Pyrolysis:
    - Bio-oil + Hydrogen -> Aromatics (Hydrogenation) (Vispute et al.)
    - 46% reduction in coking, 36% higher yield of aromatics and olefins
  - Lignin to aromatics
    - Better use of carbohydrates after separation from biomass
    - Yields of aromatics better than from biomass feedstock
    - Potential to generate cyclohexane
- Longer chain fatty acids
  - Elongation of VFAs using H2
- Alcohols
  - Butanol
- Diols

Glycerol to 1,3-PDO, Succinic acid to 1,4-BDO for the U.S. Department of Energy

Brown et al., Biofpr, 2017 Vispute et al., Science 2010,



#### Hydrogen Source Plays an Important Role in Pathway Risk Determination (Zhao et al., 2017, Biofpr)

Pathways	Feedstock	Energy input	Energy output	Source
High T fasification and Fischer Tropsch	Corn Stover	Biomass, natural gas, electricity	Gasoline, diesel, electricity	Swanson et al. (2010)
Low T gasification Fischer Tropsch	Corn stover	Biomass, natural gas, electricity	Gasoline, diesel, electricity	Swanson et al. (2010)
Fast Pyrolysis and hydroprocessing	Corn stover	Biomass, hydrogen, electricity	Gasoline, diesel, electricity	Bittner et al (2015), Brown et al., (2013)
High Temperature Liquefaction	Hybrid poplar	Biomass, natural gas, electricity	Gasoline, diesel, heavy oil, electricity	Zhu et al. (2014)
Indirectly heated gasification and Acetic acid synthesis	Hybrid poplar	Biomass, CO, H2, electricity	Ethanol, Electricity	Zhu and Jones (2009)
Directly heated gasification and Acetic acid synthesis	Hybrid poplar	Biomass, natural gas, CO, H2, electricity	Ethanol, Electricity	Zhu and Jones (2009)
Methanol to Gasoline	Hybrid poplar	Biomass, electricity	Gasoline, electricity, liquefied petroleum gas	Zhu et al., (2012)

# The Vibe of the US Transportation Industry

- The new movement towards Electrification
- Natural gas based transportation energy (electricity, CNG, LNG, etc.)
- Liquid biofuel industry still in infancy
- Renewable biogas from lignocellulosics Significant contribution to RFS2
  - 42.2 million gallons-equivalent of cellulosic biofuels 98.5% as liquefied renewable natural gas
- Strategies for making biomass-derived fuels economically competitive are needed



# Waste to H<sub>2</sub> to Biofuels and Chemicals Pathways

- Waste sources
  - Biorefinery
    - Pyrolysis aqueous phase (up to 20% carbon potential loss)
    - Fermentation effluent (fermentation byproducts + remaining 5-10% sugars)
    - Stillage (concentrated effluent), Lignin
  - Bioproducts industry
  - Food waste
    - Households, restaurants, food processing, bakeries, groceries
  - Breweries and wineries
  - Paper and pulp industry
  - Municipal waste
    - Food component (30-40%)
    - 40% of all purchased food ends up in trash can



# **Technologies for H<sub>2</sub> Production**





# **Microbial Electrolysis Cell Technology**

- Conversion of Waste to hydrogen
- Anode: Degradable organics to electrons, protons and CO<sub>2</sub>
- Cathode: Proton reduction to hydrogen at applied potential of 0.3-1V.
- Uses electroactive biofilms with broad specificity and activity for biomass-derived components



#### <u>Pathway</u>: Organics + water $\rightarrow$ electrons + protons (anode ) $\rightarrow$ H<sub>2</sub> (cathode)

Borole, A. P., <u>US Patent</u> 7,695,834, UT-Battelle, USA, **2010.** Borole, A. P., <u>US Patent</u> 8,192,854 B2 UT-Battelle, USA, **2012.** Borole, A. and A. J. Lewis (2016) Provisional Patent Appl. No.: 62/351,322, <u>UT Battelle, LLC.</u> Borole, A. P. and C. Tsouris (2009). <u>US Patent 8,597,513 B2.</u> USPTO. USA, UT-Battelle, LLC. Borole, A. P., et.al., 2009, <u>Biotechnol for Biofuels</u>., *Controlling accumulation of fermentation inhibitors in biorefinery process water using Microbial Fuel Cells*, 2, 1, 7. Borole, A. P., et al., 2011, <u>Energy Environ. Sci., Electroactive biofilms: Current status and future research needs 4: 4813-4834.</u> Borole, A. P., et al., <u>Environ Sci Technol.</u> 2013, 47, 642. Borole, A. P., et al., <u>Bioresour. Technol.</u> 2011, 102, 5098. Borole, A. P., et al., <u>Biochem. Eng. J.</u> 2009, 48, 71.



# **Hydrogen Production from Waste**

### • Waste/Biomass sugars (glucose) to H<sub>2</sub>:

	Process scheme	Theoretical yield	Observed yield	Free energy change (for H <sub>2</sub> -producing step)	Overall observed energy yield	Comments
1	Hypothetical H <sub>2</sub> production	12				
2	Hexose to ethanol to H <sub>2</sub> via autothermal reforming	10	9.5	–265 <sup>ª</sup> kJ/mole	~83%	Prohibitive catalyst (Rh) cost <sup>10</sup>
3	Dark-light fermentation: Glucose $\rightarrow$ acetate $\rightarrow$ H <sub>2</sub>	8	7.1	+164 kJ/mole	59.2%	Limited by light penetra- tion and cost <sup>39</sup>
4	Methanogenesis-steam reforming	8	6.0	+261 kJ/mole	50.5%	Mature technology components <sup>9,40</sup>
5	MEC	12	8.2	+104.6 kJ/mol	64%	Nascent technology 3,30

<sup>a</sup> Processes 3–5 require energy input for the hydrogen-producing step, but this step is energy yielding in process 2. While the hydrogen producing reaction is energy-yielding, energy input is required for production of ethanol from hexose.

# Microbial electrolysis is a high efficiency, high yield, practical alternative available for hydrogen production.

<u>Biofuels, Bioproducts & Biorefining</u> "Improving energy efficiency and enabling water recycle in biorefineries using bioelectrochemical cells." Borole, A. P. (2011). **5**(1): 28-36.



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Presentation name

# **Hydrogen Production Costs**

\$/ba H2	<b>EERE [17]</b>		Literature [19], [14].
\$/ Kg 112	2011 status	2015 Target	
Wind + Electrolysis	4.10	3.00	6.64
PV-Electrolysis			6.18 <sup>†</sup>
Biomass gasification	2.20	2.10	4.63
Biomass pyrolysis			3.80
Solar thermal	NA	14.50	
Photoelectrochemical cell	NA	17.30	
Photobiological	NA	9.20 (2020 Target)	
Nuclear thermal splitting of water			1.63
Natural gas reforming			1.03
Coal gasification			0.96
Microbial electrolysis	NA	12.43 <sup>§</sup>	5.40 <sup>‡</sup> < 4.00 (ORNL study)
Reforming of bio-derived liquids <sup>*</sup>	6.60	5.90	
2. Bio-oil aqueous phase [3]	31.84	3.00 <sup>£</sup> (2017 Target)	

Table 1. Comparison of cost of hydrogen production [17], [19]. The costs reported in last column are based on 2003 \$, except for MEC. \* Based on projected future technology

<sup>§</sup> Derived from [20]. A cost of \$5.18 was deduced from the reported hydrogen production cost of \$12.43, which was for production of substrate via fermentation. The FCTO MYPP reports cost of electrodes for MEC (\$ $300/m^2$ , 2015 target), however, does not give estimated cost of hydrogen production. It assumes a hydrogen production rate of 1 L-H<sub>2</sub>/L-reactor-day (2015 Target).

<sup>‡</sup>Derived from [14]-*Chemsuschem* **2012,** *5*, (6), 1012-1019. Cost projected using future cost of electrode materials.

\* For conversion of bio-derived liquids to hydrogen via steam reforming.

<sup>£</sup> The target of \$ 3/kg of hydrogen production from bio-oil aqueous phase has been reported to be very difficult to meet [3].

### Microbial Electrolysis of Pyrolysis Aqueous Phase



#### Potential to generate hydrogen as intermediate for liquid fuel.

Borole & Lewis, Provisional Patent Appl. No.: 62/351,322, <u>UT Battelle, LLC.</u> submitted June 2016 Lewis, A. J., et al. (2015). "Hydrogen production from switchgrass via a hybrid pyrolysis-microbial electrolysis process." <u>Bioresource Technology **195**: 231-241.</u>



#### DOI: 10.1039/07 SE000001

# **Hydrogen Production Metrics for MEC**

	Targetsforcommercialconsideration	June 2017		
Hydrogen production rate	>20 L H <sub>2</sub> /L-reactor-day	11.7 L/L-anode-day for bio-oil aqueous phase		
Anode current density, A/m <sup>2</sup>	20	14 for BOAP		
Anode CE	>90%	60-79%		
Applied voltage	< 0.6 V	0.9V		
Cathode CE	>90% at 0.6V or less	87-96%		
Potential Efficiency	>60%	NA Demonstrated high		
Resistance	$< 80 \text{ m}\Omega \text{ m}^2$	NA performance in terms of H vield		
Capital costs*	<\$2000/m <sup>3</sup> reactor	NA and productivity.		
Performance and efficiency metrics for MEC development.				

\* The costs reported are for n<sup>th</sup> reactor. The reduction in cost will come from improvements in MEC anode performance and use of non-Pt cathode electrode.

13 Managed by UT-Battelle for the U.S. Department of Energy Lewis, A. J., et al. (2015). <u>Bioresource Technology **195**</u>: 231-241. <u>Borole & Lewis (2017), Sustainable Energy & Fuels,</u> DOI: 10.1039/C7SE00060J Lewis, et al., 2017, Microbial Biotechnology, DOI: 10.1111/1751-7915.12756



# **Microbial Electrolysis for Chemicals**

Type of BES	Cathode	Product
	substrate	
MEC	Biomass - protons	Hydrogen
MFC	Oxygen	Electricity
BES	Glycerol	1,3-Propanediol
BES H <sub>2</sub> +	Succinic Acid	1,4-Butanediol
BES	Acetate	Ethanol
BES	Oxygen	Hydrogen peroxide
MEC	Ag run-off/ Wastewater	Phosphate fertilizer/Struvite
MEC	Urine/Wastewater	Ammonia



- H<sub>2</sub> evolution at cathode can improve yields of high value products synthesized via electrosynthesis.
- Borole, A. P., Bioelectrochemical Biorefining, a book chapter in
  Bioenergy & Biofuels, CRC Press, 2017



### **Beyond Current Hydrogen Sources / Applications**



### Integrating the Biomass Resource... $\rightarrow$ Enables A Holistic BioEconomy

Future Hydrogen Energy Systems Integrated with Biomass



for the U.S. Department of Energy

Presentation name

### **Process Optimization via Intensification**



17 Managed by UT-Battelle for the U.S. Department of Energy Borole, A. P., 2015, Sustainable and Efficient Pathways for Bioenergy Recovery from Low-value Process Streams via Bioelectrochemical Systems in Biorefineries." <u>7(9): 11713-11726.</u>



# Conclusion

- Waste to Hydrogen Technologies Need to be Implemented
- Value proposition for chemicals as well as biofuels production
- MEC Potential game-changing technology
- Pros vs. anaerobic digestion Direct H<sub>2</sub> production, minimize fugitive CH<sub>4</sub> release
- Cons Nascent technology
- Hydrogen can play a significant role in bioeconomy
  - Extracting value out of waste
  - Providing a necessary reagent to generate high-value products
  - Introducing tunability in processes requiring hydrogen by diverting electrons from solar/wind to fuels & products



### **BioElectrochemical bioRefining** (The BER Laboratory)



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<u>Environ Sci Technol</u> Conversion of residual organics in corn stover-derived biorefinery stream to bioenergy via microbial fuel cells. **47**(1): 642-648. Borole, A. P., C. Hamilton, et al. (2013).

