



Next Generation Three-Way Catalysts for Future, Highly Efficient Gasoline Engines

Christine Lambert

Ford Research and Advanced Engineering

9-June-2016

Project ID: PM067



Timeline

- Start Date: 1-Oct-2014
- End Date: 30-Sept-2017
- Status: ~ 50% complete

Budget

- Total funding: \$1,690,470
 - DOE share: \$752,376
 - Contractor share: \$338,094
 - Additional ORNL \$600,000
- Funding in FY 2015
 - \$301,228 (+ ORNL \$600,000)
- Funding in FY 2016
 - \$257,494

Barriers

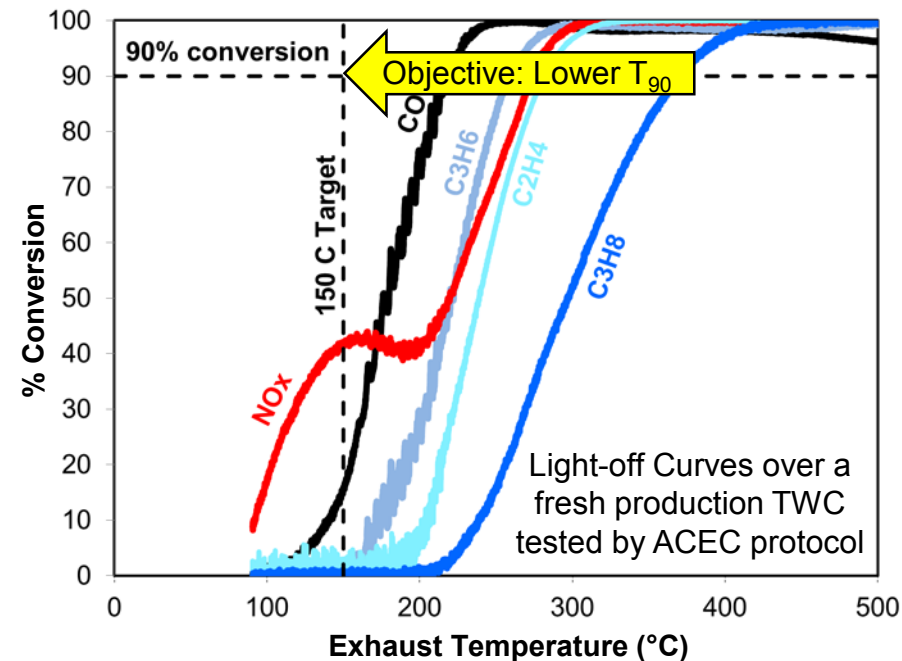
- Long lead times for materials commercialization
- Cost

Partners

- Ford Motor Company
- Oak Ridge National Lab
- University of Michigan

➤ Overall Objective

- Develop new three-way catalysts and/or catalyst systems capable of achieving durable 90% activity [HC, CO, NOx] at 150°C.
 - Today's automotive three-way catalysts (TWCs) become highly efficient only when exhaust temperatures reach 250-400°C.
 - The next generation of engines will be more efficient and thus produce cooler exhaust at low load conditions
 - *TWC activity will be required at lower temperatures to satisfy strict emission standards with the next generation of automobiles.*



➤ Current Budget Year Objectives

- Identify/characterize new materials, and predict performance and costs.
- Identify/capitalize on synergies between various catalyst materials within and between partners



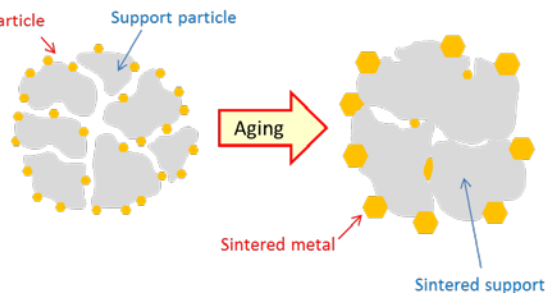
Milestone	Status
Confirm Reactor Comparability <ul style="list-style-type: none"> • Cross lab comparisons and test protocol were confirmed 	Completed Nov. 2015
Commercial vs. New Material Performance – Status (BP1) <ul style="list-style-type: none"> • Tested and compared commercial TWC material to new materials developed in-house 	Completed Nov. 2015
Down-select Promising Materials/Confirm Synthesis and Characterization Path(s) <ul style="list-style-type: none"> • Agreed to keep all material synthesis pathways active through this budget period 	Completed Oct. 2015
Confirm Test Protocols and Down-select Criteria <ul style="list-style-type: none"> • Agreed on test protocol and laboratory systems to allow cross-lab comparisons. 	Completed Oct. 2015
Confirm Benchmark State of the Art TWC <ul style="list-style-type: none"> • Agreed no new benchmarking was necessary. 	Completed Oct. 2015
Commercial vs. New Material Performance – Status (BP2) <ul style="list-style-type: none"> • Evaluations of new materials made in house and comparison to the commercial TWC material will continue throughout project as new materials show promise. 	Ongoing
System Model Assessment – Status <ul style="list-style-type: none"> • New assessments will be completed as necessary. 	Mar. / Jun 2016
Cost Model Assessment – Status <ul style="list-style-type: none"> • New assessments will be completed as necessary. 	Sept. 2016
Down-Select Promising Catalysts <ul style="list-style-type: none"> • Determine which catalysts and/or catalyst materials should be carried over into Budget Period 3. 	Sept. 2016

- Identify strategies to improve precious metal dispersion and promote activity
- Make and characterize new materials, and predict performance and costs
- Leverage cross-laboratory analytical capabilities

Oxide overlayer on oxide support

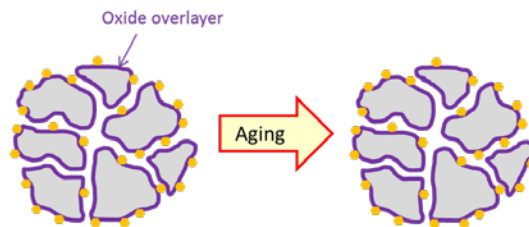
Challenge:

Prolonged exposure to high temperature automotive exhaust gases leads to sintering of both active metal and support, leading to loss of activity

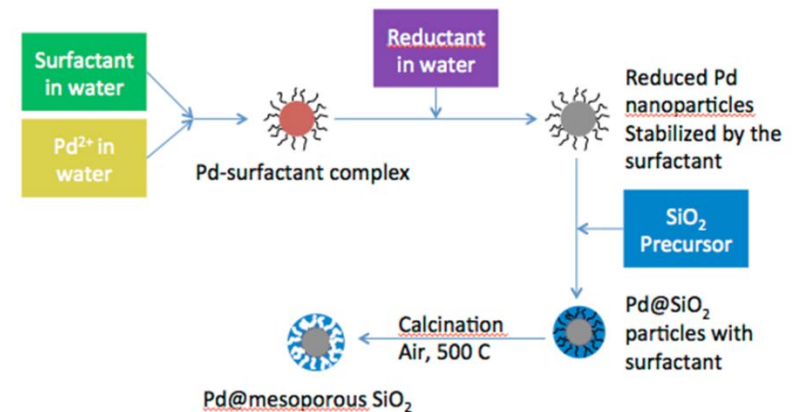


Approach:

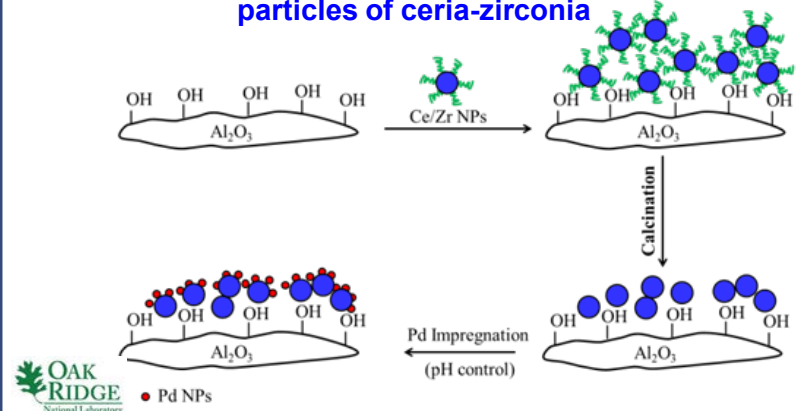
Overcoat a high surface area oxide with a second oxide layer to reduce sintering and promote precious metal activity



One-pot synthesis of Pd@SiO₂ core-shell catalyst



Improved dispersion and enhanced low temperature activity on using nanophase particles of ceria-zirconia





Ford Motor Company



- Modified Support Materials
 - Use novel, high surface area, layered oxides as precious metal supports
- Cost and Performance Models
 - Estimate finished catalyst costs; predict vehicle tailpipe performance.

Oak Ridge National Laboratory



- Modified Support Materials
 - Investigate modification of supports for thermal stability, adherence of metal to the support, and tailoring the metal-support interactions for optimal catalytic performance.
- Ternary Oxide Development as PGM Substitute
 - Investigate the functionality of low-PGM or PGM-free, ternary-oxide catalyst systems, starting with CuO-CoO-CeO (CCC).

University of Michigan



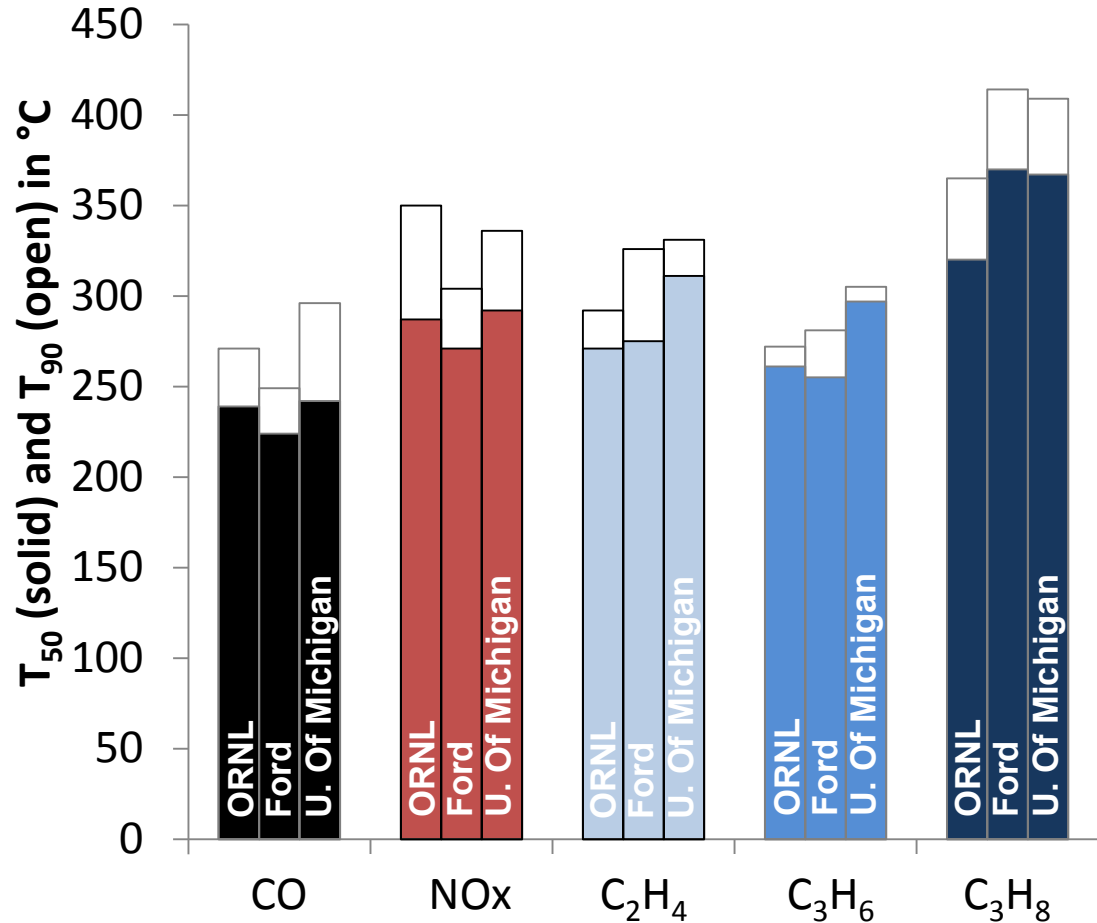
- Core-Shell Model Catalysts (incl. monolith cores)
 - Investigate catalyst architectures containing a core-shell conformation composed of a metal nanoparticle surrounded by a metal oxide shell.
 - Synthesis will begin with silica, alumina, and ceria-zirconia-based model catalyst systems

Accomplishments



“Round Robin” confirmed reactor similarities with aged modern TWC

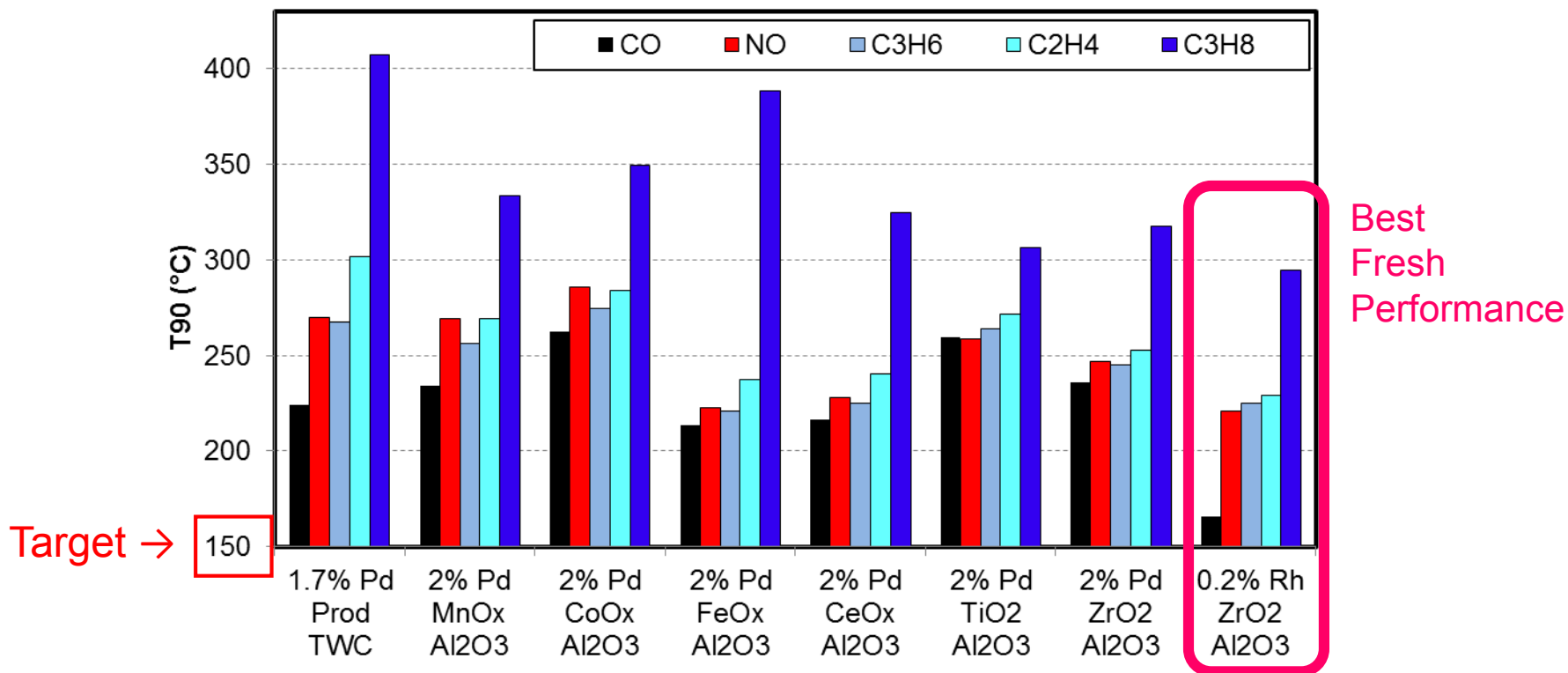
- TWC aged by Ford
 - 50h 4-mode durability
 - 960°C max bed temperature
- Evaluated at all partner organizations using protocol developed by ACEC tech team
- Good agreement at each research lab even though sample weights range from 0.1 to 2.0 g



ACEC stoich protocol:

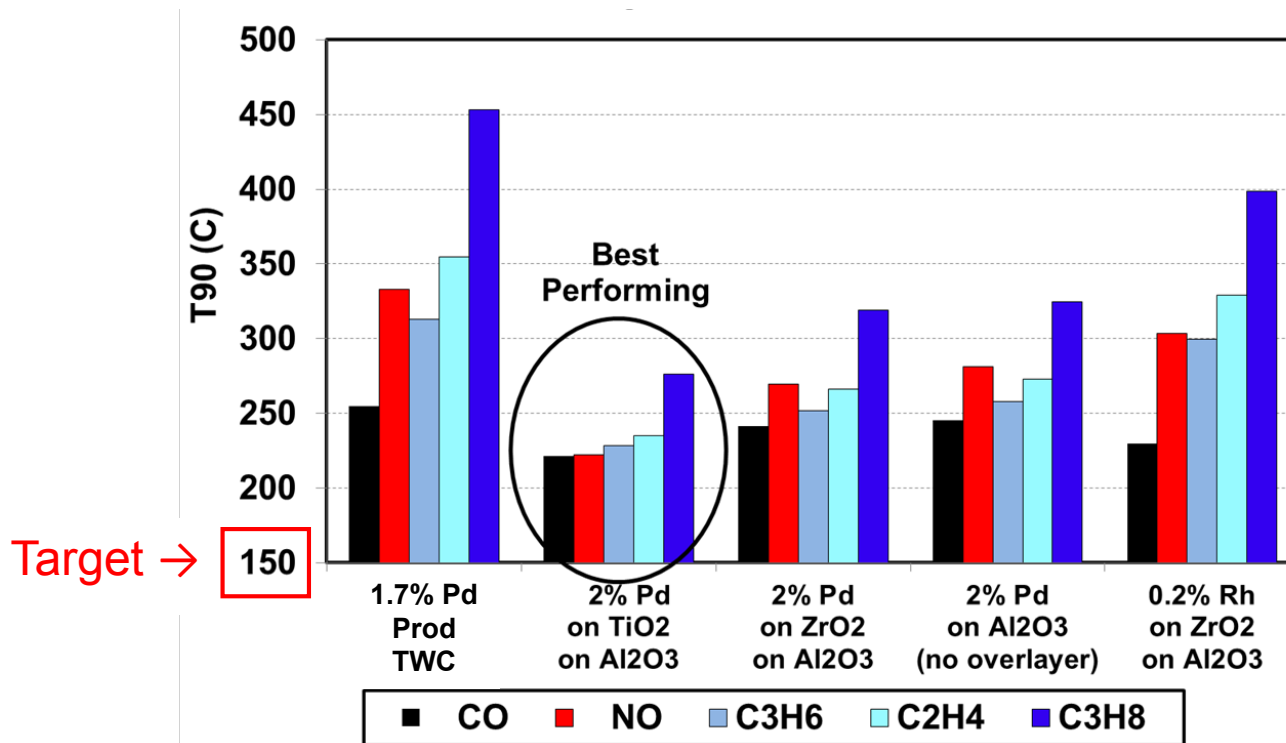
[H ₂ O] = 10%	[O ₂] = {stoichiometric}	[CO ₂] = 5%	[NO] = 1000ppm
[CO] = 5000ppm	[C ₃ H ₈] = 150ppm	[C ₃ H ₆] = 500ppm	[C ₂ H ₄] = 525ppm
[H ₂] = 1700ppm	N ₂ or Ar Balance	0.2 – 3.4 slm flow	0.1 – 2.0 g crushed monolith

Performance of Catalysts in the Fresh State



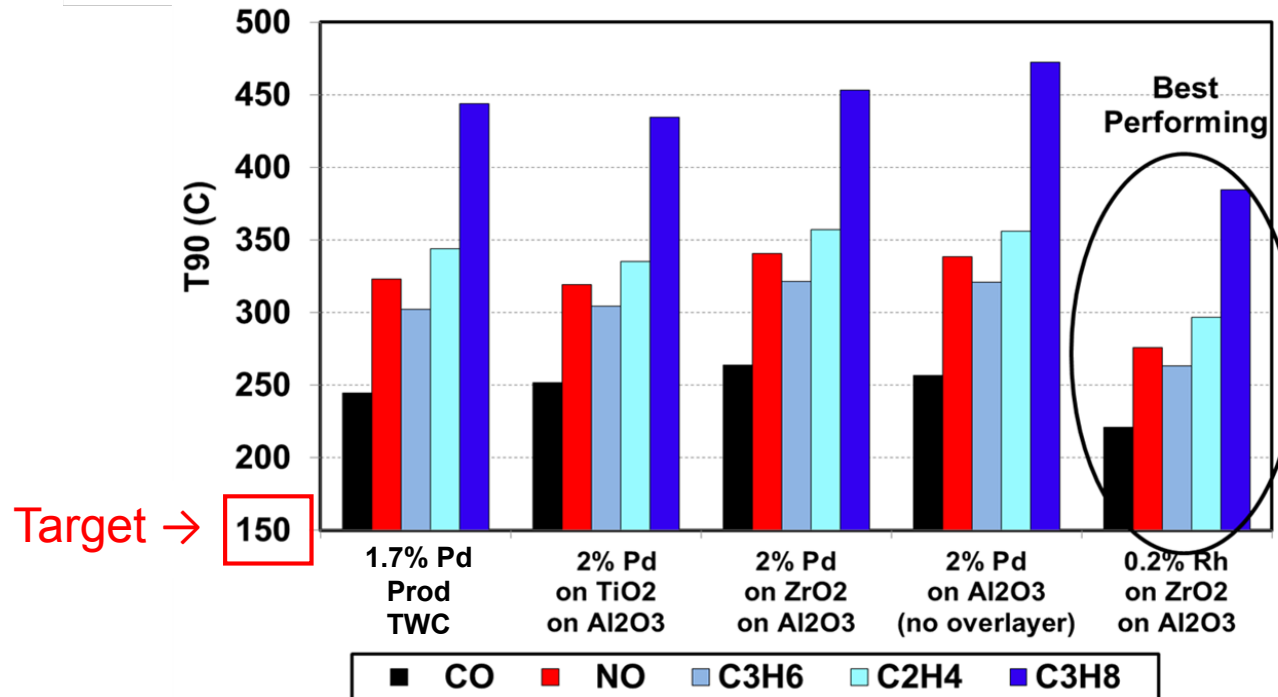
- Fresh production TWC does not satisfy the T90 target of 150°C for any exhaust gas
- Some of the overlayers with 2% Pd outperformed the production TWC
- The Rh on ZrO₂ overlayer had the best fresh performance
 - Fresh CO T90 near program target

Performance After 950°C Oven Aging in Air/H₂O



- All of the over-layer formulations had better performance than the production TWC after lean aging at 950°C
- The 2% Pd on TiO₂ overlayer provided the best performance
 - Performance *improves* after lean aging!

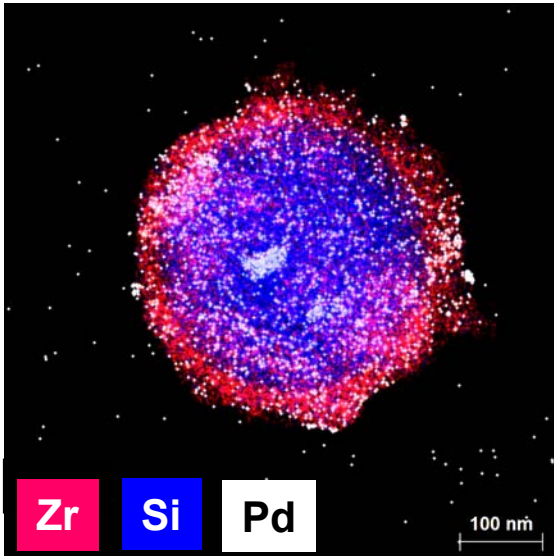
Catalyst Results After 4-Mode Aging 960°C max



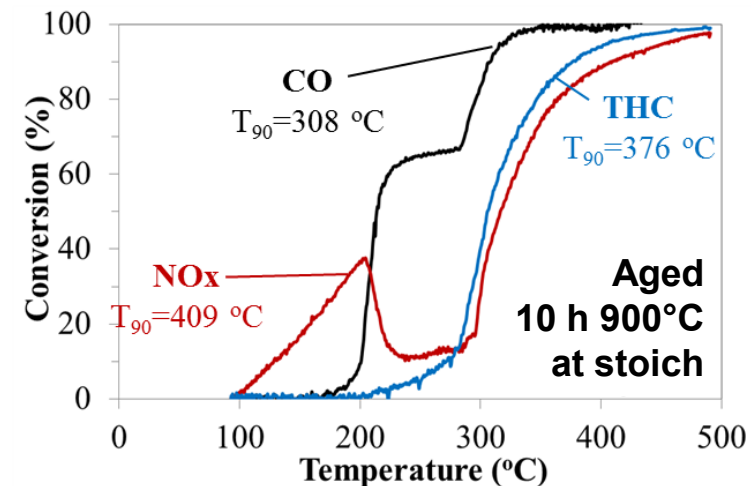
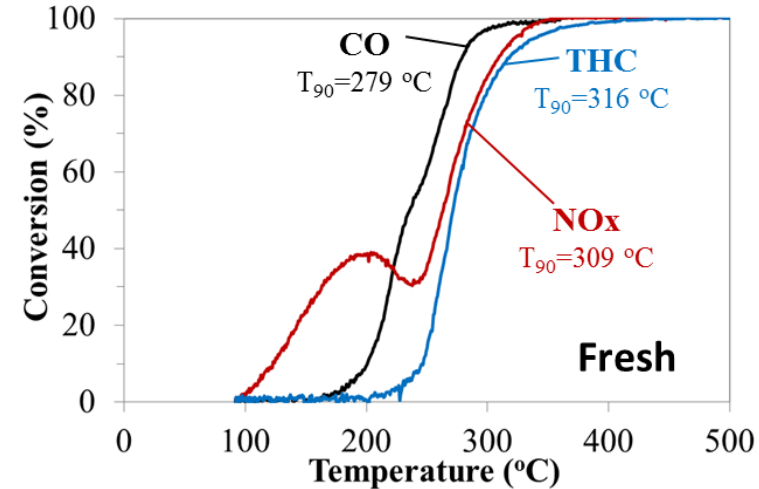
- After 4-mode aging, the 0.2% Rh on Zr over-layer provided the best performance
- Lean aging not appropriate for catalysts intended primarily for stoichiometric operation

Goal: Improve ZrO_2 surface area through deposition on SiO_2 core

- Previous lean data suggested Pd/ ZrO_2 was promising
- Coat a SiO_2 with ZrO_2 shell then add 1% Pd
- Pd particles are on ZrO_2 shell, but initial deposition has poor dispersion → improvements underway

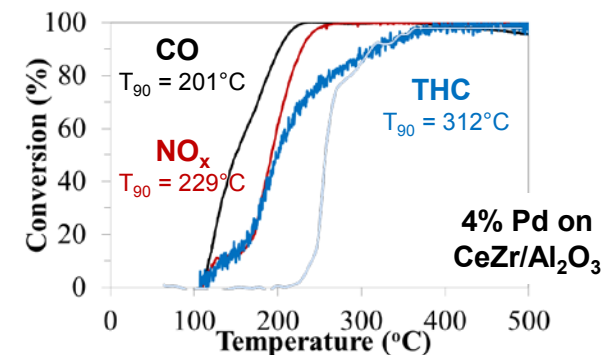
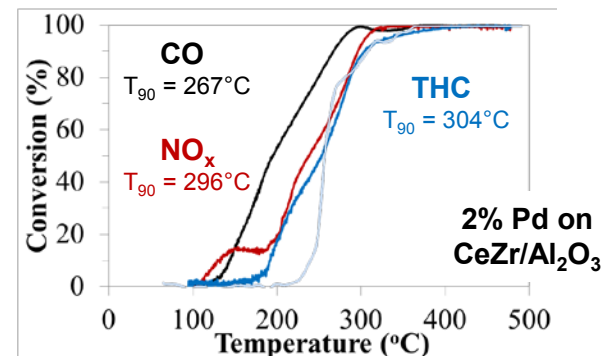
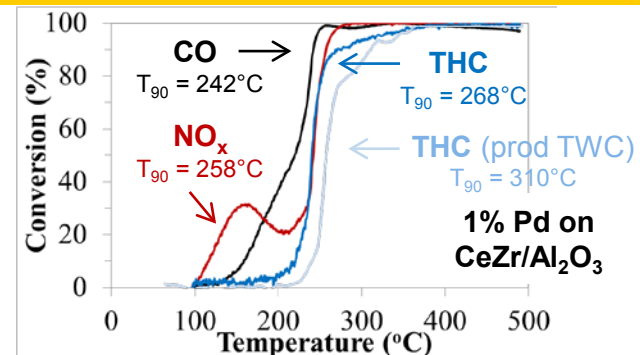
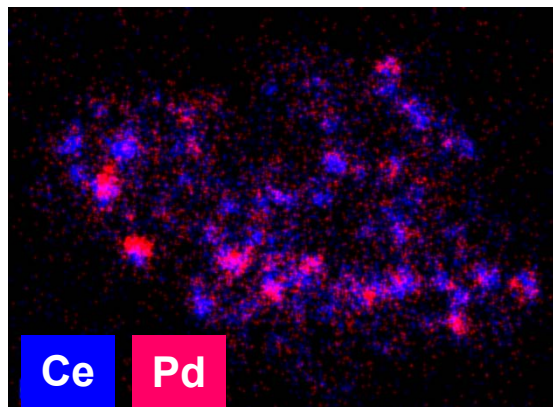
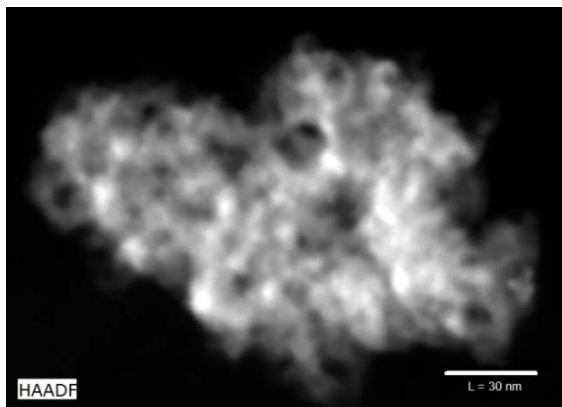


Elemental maps while rotating a fresh sample $\pm 40^\circ$ (TEM).



Enhanced activity through deposition of well defined nanoparticles of Ce-Zr with targeted deposition of Pd

- Dispersion of Ce-Zr nanoparticles on Al_2O_3
- Targeted deposition of Pd on nanoparticles on Ce-Zr
 - TEM used to confirm both nanoparticles and targeted deposition

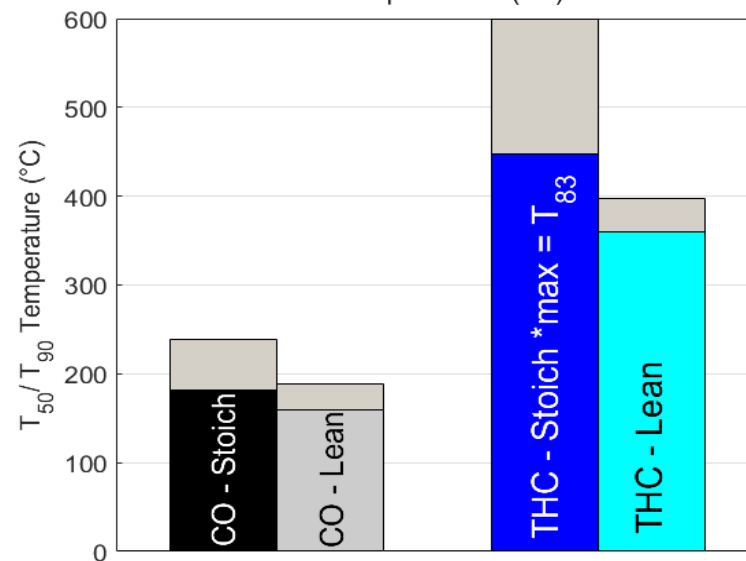
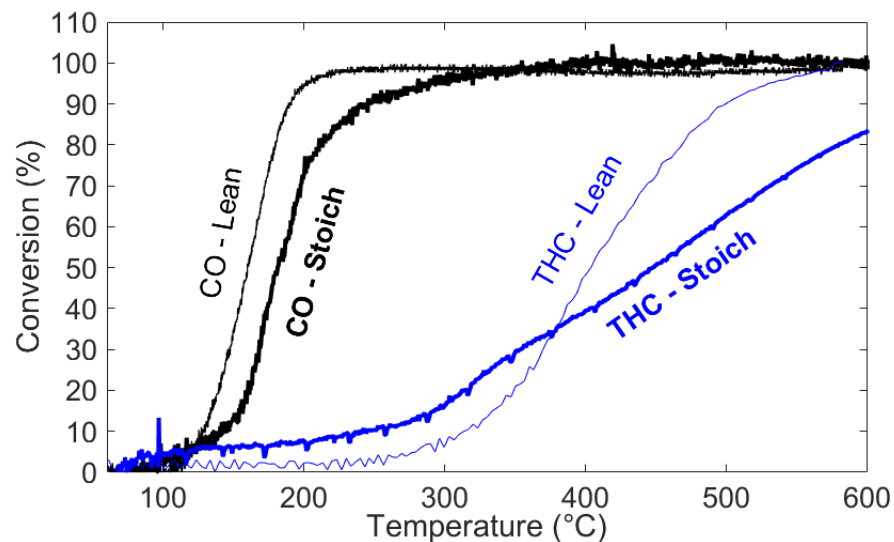


Ternary Oxide as PGM substitute shows promise, but only for CO

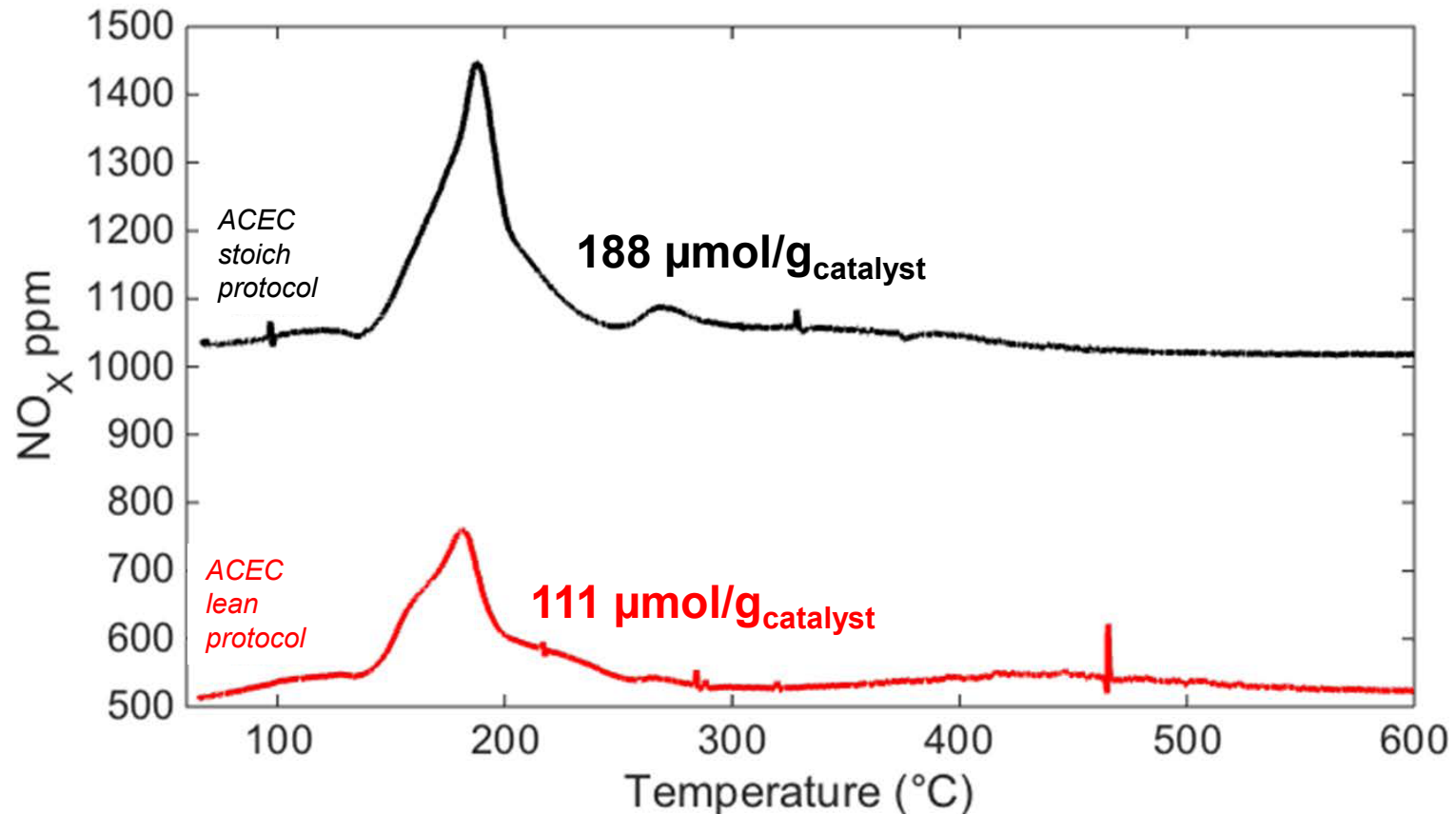
- CuO-Co₃O₄-CeO₂ (CCC) catalyst has shown inhibition resistance for lean CO oxidation
- Also a good CO oxidation catalyst under stoichiometric conditions
- CCC is clearly poor for HC and NO and can only be considered as a “specialist” for CO

Continuing work

- CCC catalyst as a CO oxidation “specialist”; use less PGM in system
- New Formulations:
 - Increase surface area, Cu content, and Cu-Ce interface active site
 - Improve the already good CO oxidation activity

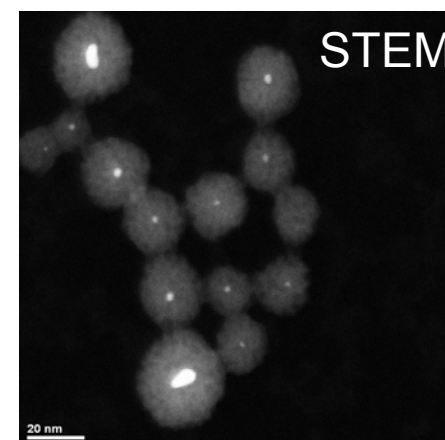
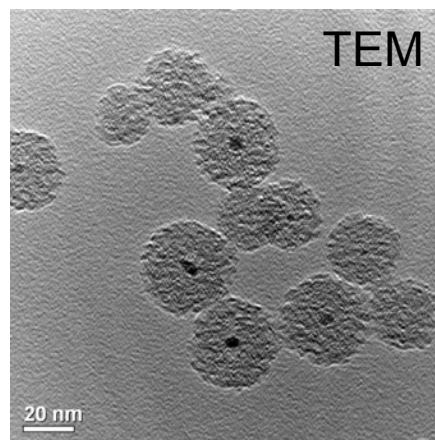
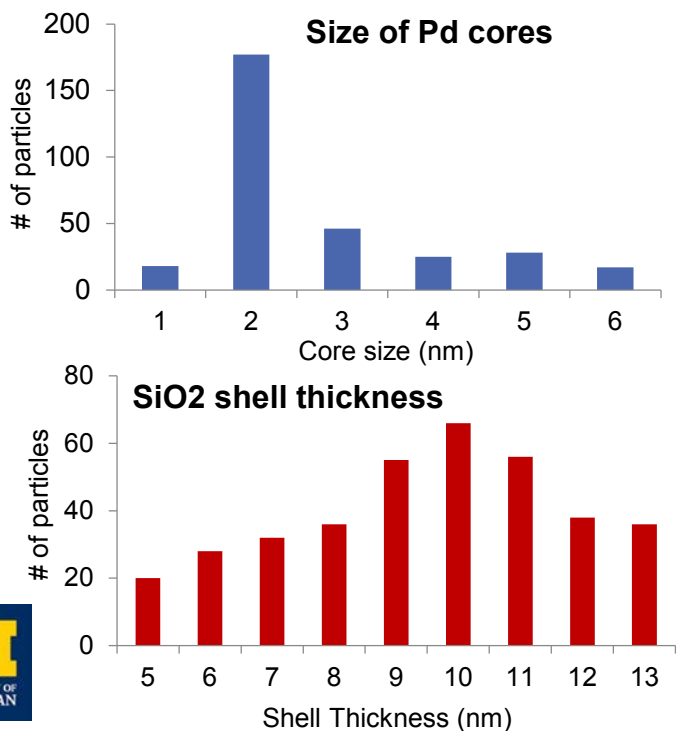
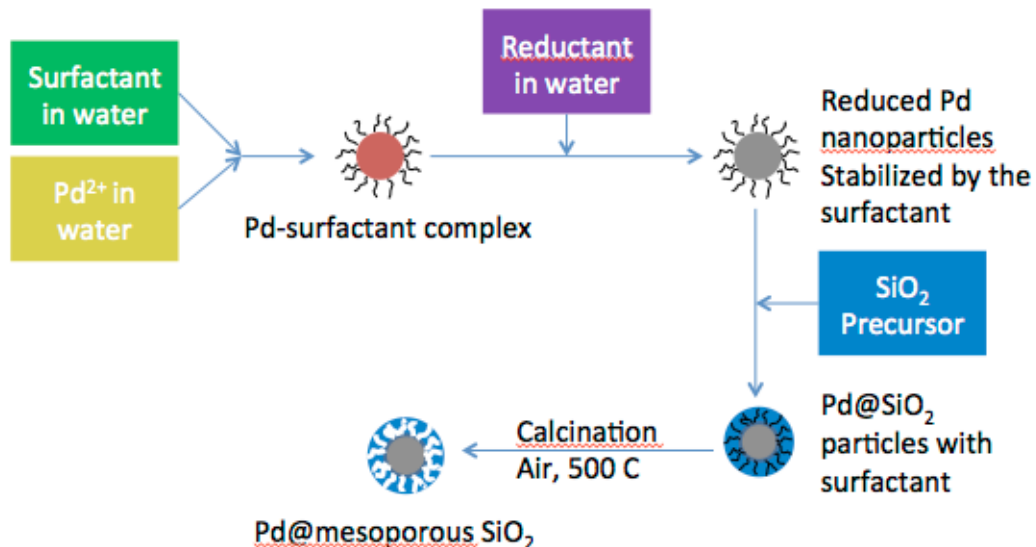


CCC also shows the ability to store and release NO_x at low temperatures



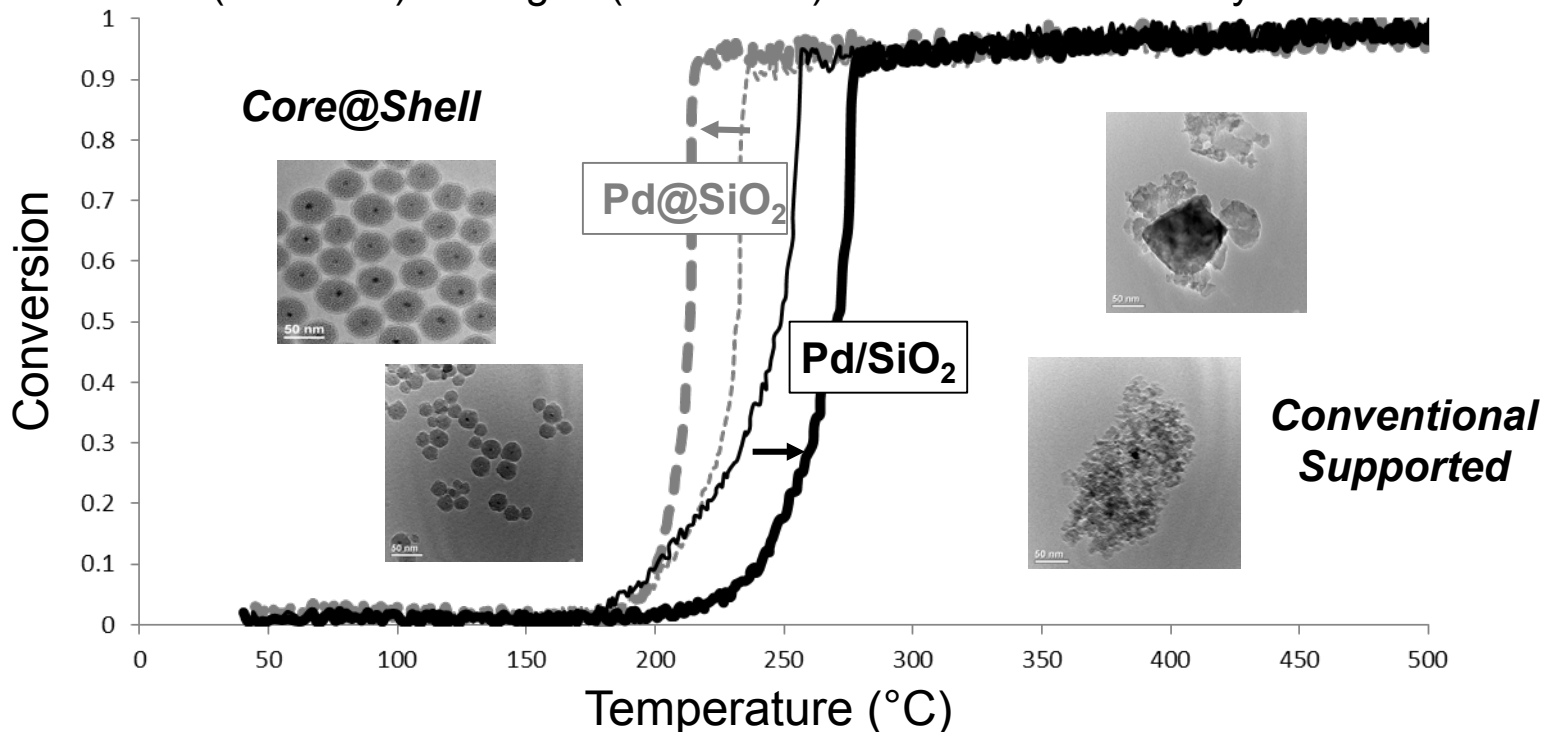
One-Pot Synthesis of Pd@SiO₂ Core@Shell Catalyst

- 1) Core@shell by flame spray pyrolysis
- 2) Simple 1-pot synthesis of core@shell
- 3) Now being extended to other shell oxides (e.g., Pd@TiO₂, Pd@SiO₂-CeO₂)



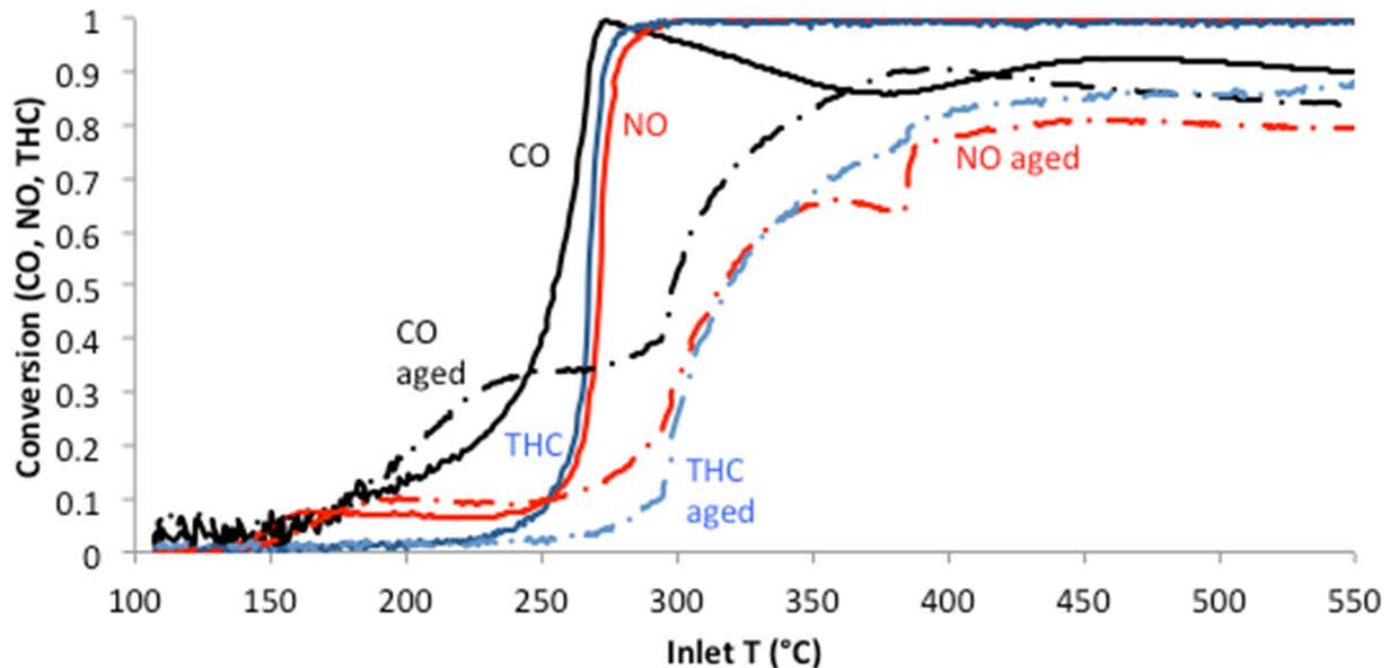
Activity Comparison by CO Oxidation Probe Reaction

- Feed: 1% CO, 1.5% O₂, balance N₂, 400ml/min flow, 60 mg sample
 - Fresh (thin lines) and aged (thick lines) at 850°C for 4 h in dry air



- New synthesis route leads to thermally stable Pd@SiO₂ core shell catalyst
- Pd@SiO₂ is better dispersed after aging at 850°C
- Pd@SiO₂ shows improved light-off behavior after aging at 850°C

Test Results for Hydrothermally Aged Pd@SiO₂ Core@Shell Catalysts



Feed: Full mix, 212 ml/min total, 5% water; 60 mg fresh Pd@SiO₂ (solid line); 60 mg aged Pd@SiO₂ (dotted line); aging in air at 800°C for 10 h with 6% water

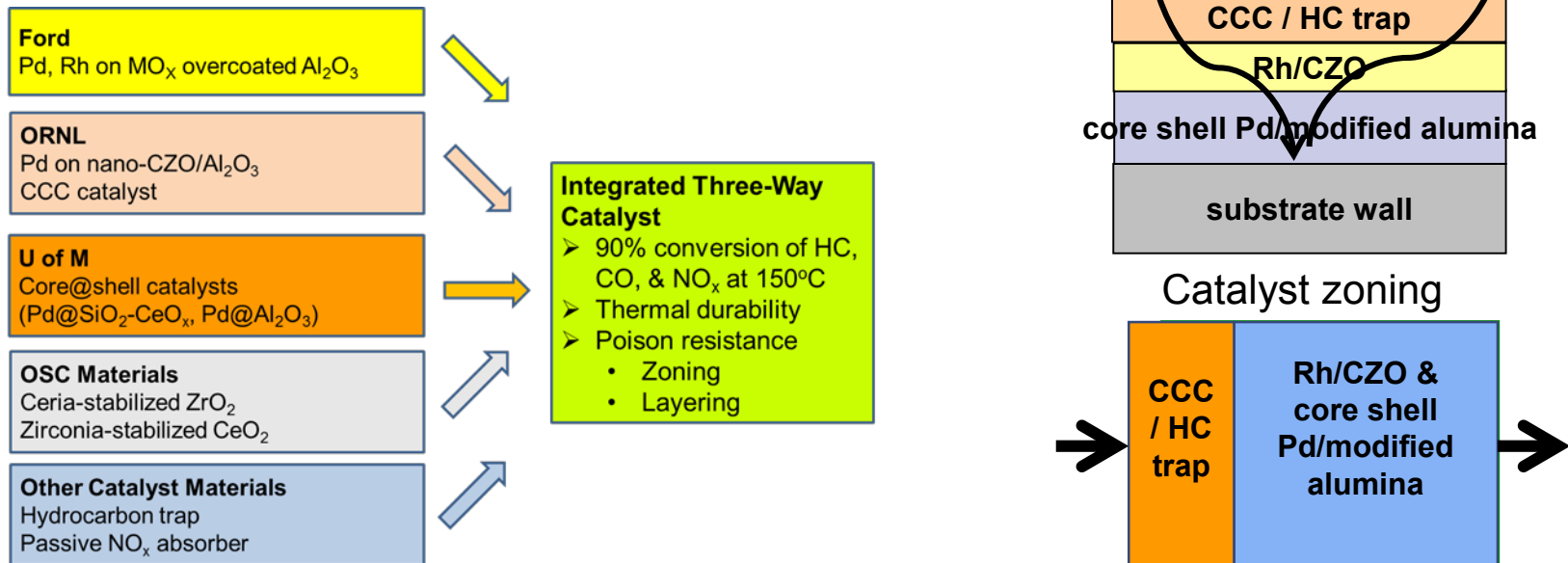
- Simple one-pot synthesis for Pd@SiO₂ core-shell catalyst has been developed
- Core-shell catalyst shows better activity than supported Pd/SiO₂ catalyst
- Pd@Al₂O₃ and Pd@CZO will be more hydrothermally durable



- Long lead times for materials commercialization
 - Use materials with known, high stability in automotive exhaust
 - Use commercially available support materials as a base and add new materials onto base to support metals in novel ways
 - Combine novel materials into a complete catalyst
 - Partner with major automotive catalyst supplier in third year

- Cost
 - Develop stable, high surface areas for better metal dispersion
 - Balance PGM within system to take advantage of lower costs when possible
 - Investigate base metals as PGM substitute
 - Fewer processing steps are desirable

- Identify and capitalize on synergies between various catalyst materials
- Demonstrate full aging (hydrothermal-chemical) and performance from coated monolith cores using most promising materials
- Identify system solutions and estimate vehicle performance and cost





- This project has not been previously reviewed

- Relevance: TWC materials required to be active at lower temperatures to satisfy strict emission standards with the next generation of automobiles
- Approach: Make and characterize new materials, and predict performance and costs; leverage cross-laboratory analytical capabilities
- Collaboration: Full collaboration between Ford, UM, and ORNL
- Technical Accomplishments
 - Commercial TWC “round robin” was used to demonstrate reactor-to-reactor compatibility amongst all three partners
 - Overlayers of metal oxides on high surface area alumina successfully resulted in equal or better TW performance in aged state, most notably Pd/TiO₂/Al₂O₃ and Rh/ZrO₂/Al₂O₃
 - Pd on zirconia shell and ceria-zirconia nanoparticles showed some promise; more work needed
 - Ternary base metal oxides = “CO specialist”; also stores NO_x at low temperatures
 - Successful demonstration of one-step core@shell synthesis; pursuing additional shell materials with improved stability during aging
- Future work: continue towards shorter lead times for materials commercialization and lower costs



Research and
Advanced Engineering

Technical Backup

ACEC Test Protocols

1 gram of powder

3.6 L/min of flow (30K hr^{-1})

Evaluated on powder reactor with

525 ppm C_2H_4

500 ppm C_3H_6

150 ppm C_3H_8

1000 ppm NO

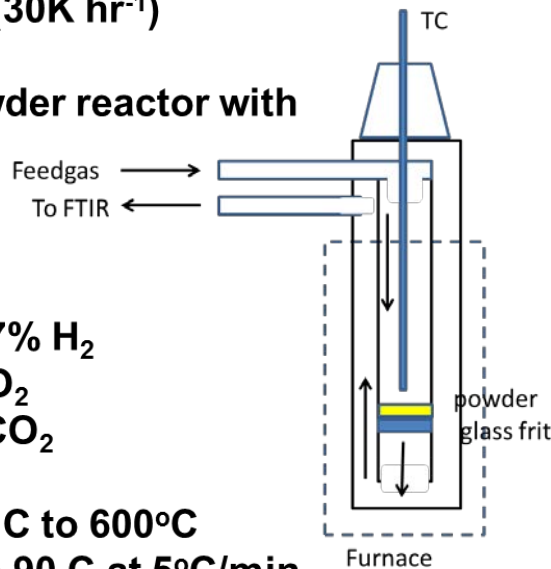
0.5% CO + 0.17% H_2

0.69 to 0.74% O_2

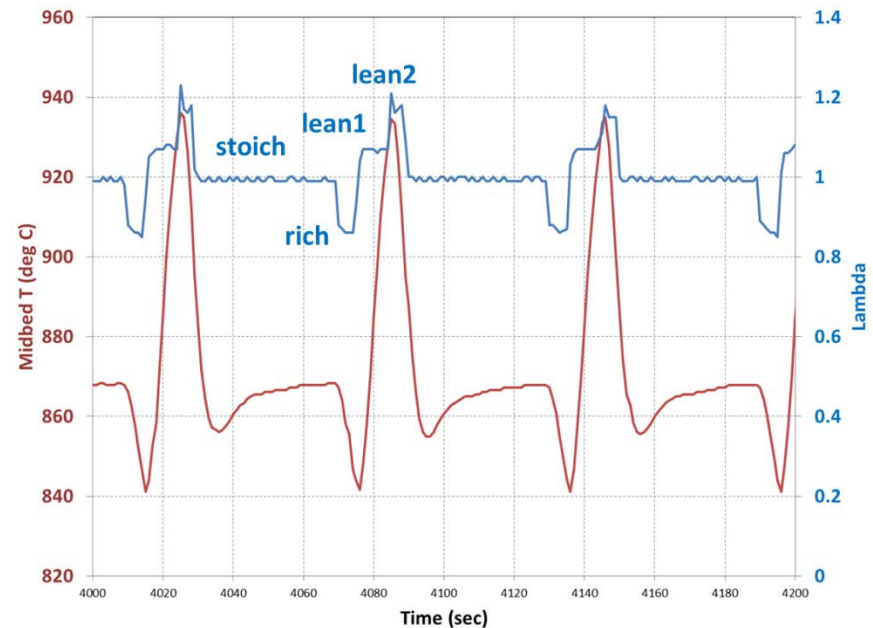
10% H_2O and CO_2

Ramp up from 70 C to 600°C
and back down to 90 C at 5°C/min

Inlet TC recorded and used for control



Four Mode Aging Cycle
Repeated on pulsating flame
combustor for 50 h

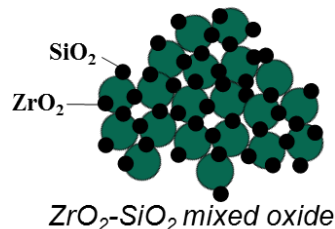
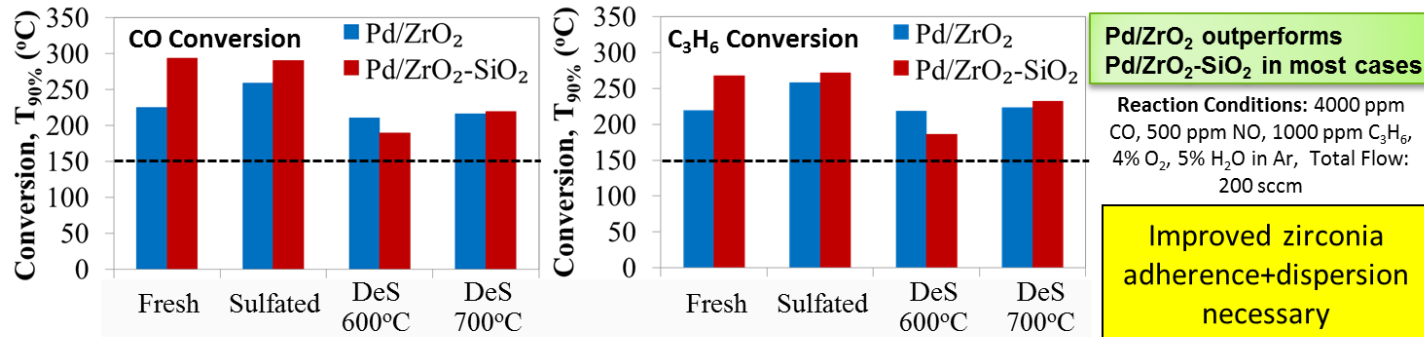


Synthesis of Layered Oxide Supported Catalysts

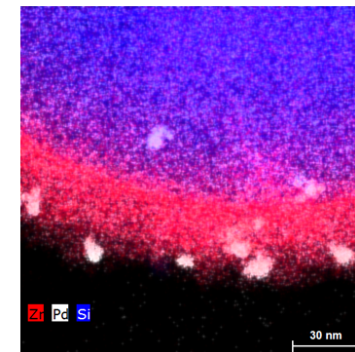
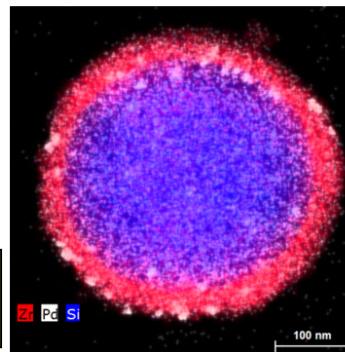


Lean-based study is motivation of new synthesis of $\text{SiO}_2@\text{ZrO}_2$ core@shell improves ZrO_2 coverage of SiO_2

- Approach: optimize support for Pd catalysts by combining high acidity of ZrO_2 with high surface area of SiO_2 ; coated SiO_2 with ZrO_2
- ZrO_2 coating introduces surface acidity
 - High acidity: benefit on HC oxidation vs. high basicity: high sulfur adsorption
 - Pd/ZrO_2 has both strong acidic and basic sites, while Pt/Si has neither



New technique developed to form a monolayer shell of ZrO_2 on a SiO_2 core

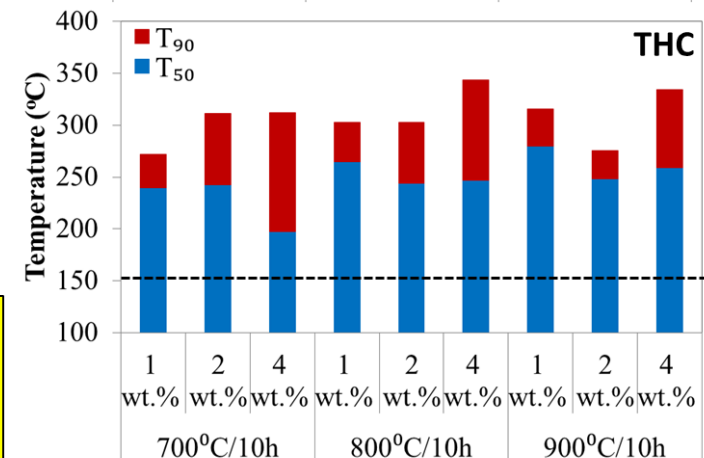
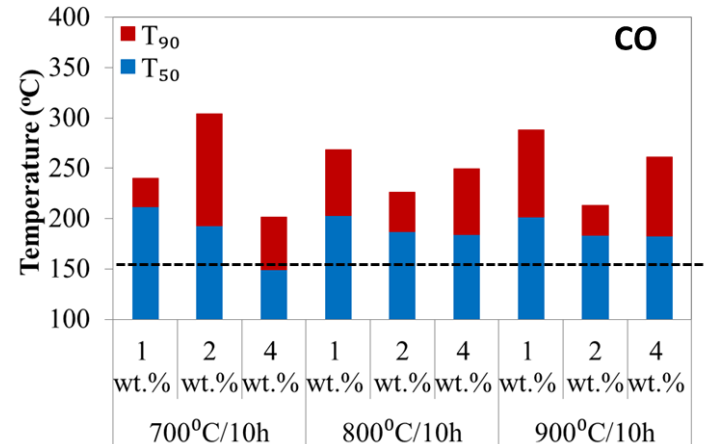


Improved CO and THC conversion over the 2 wt.% Pd/CeZr-Al₂O₃ catalysts after aging at 900°C for 10 hours

- 1 and 4 wt.% Pd/CeZr/Al₂O₃ catalysts deactivate after hydrothermal aging at 800 and 900 °C.
- **HT aging at 800°C:** improved performance of the 2 wt.% Pd/CeZr/Al₂O₃ catalyst for both CO and THC conversion.
- **HT aging at 900°C:** 2 wt.% Pd/CeZr/Al₂O₃ catalyst has the lowest T_{50,90}'s compared to the 1 and 4 wt.% Pd/CeZr/Al₂O₃, indicating that it is the most durable catalyst at elevated temperatures.

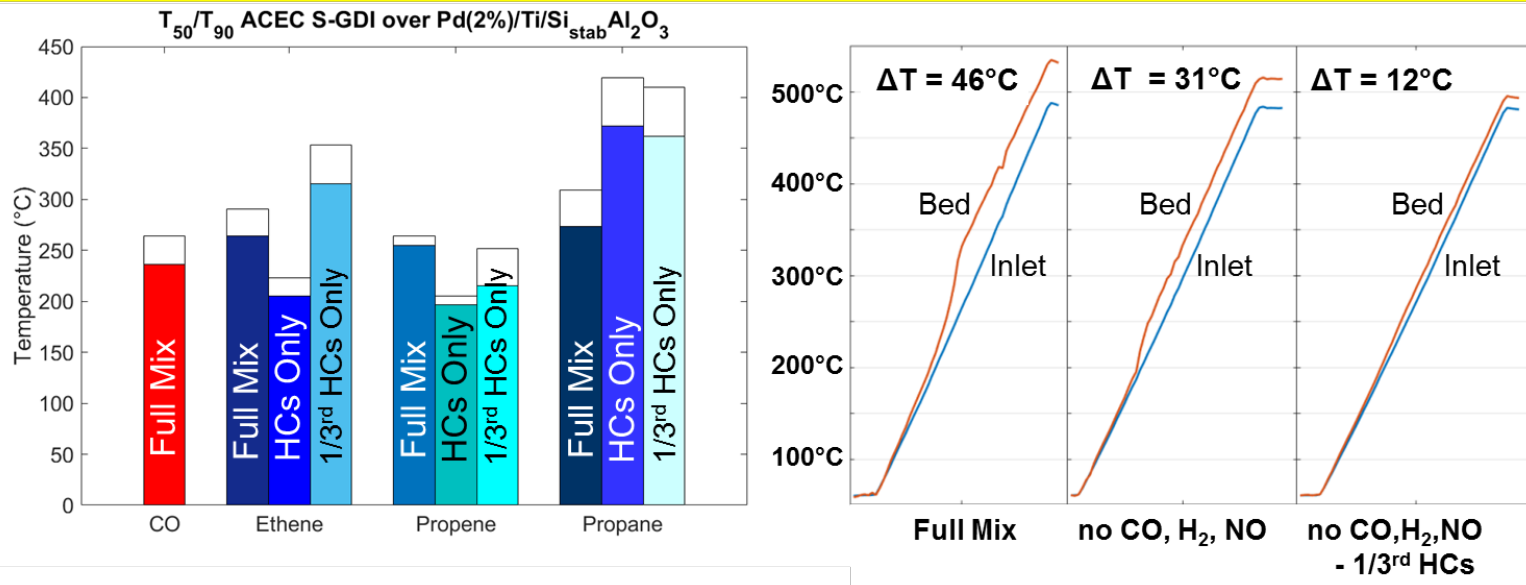
ACEC protocol (S-GDI)

100 mg cat. / flow: 333 sccm / water bath: 60°C
 CO₂:13%, O₂: Stoic - 0.05%, H₂O: 10%, CO:0.5%, NO:0.10%,
 H₂: 0.167%, C₂H₄: 0.0525%, C₃H₆: 0.05%, C₃H₈: 0.015%, Ar
 balance



Exotherm Effects Significant

Sequential tests were conducted to determine the effect of varying exotherm and conditions on overall performance.



The streams were: Full S-GDI Mixture, S-GDI (CO and NO removed), and S-GDI (CO and NO removed, 1/3rd Hydrocarbons by ppm). Results:

- CO and NO are a significant inhibitor to Ethene and Propene performance – Performance increased significantly with the removal of CO.
- Exothermic effects can drastically increase Ethene and Propene performance – Performance decreased with the removal of 2/3rd hydrocarbons and subsequent loss of exotherm.