

Engineering an Adsorbent-Based Hydrogen Storage System: *What Have We Learned?*

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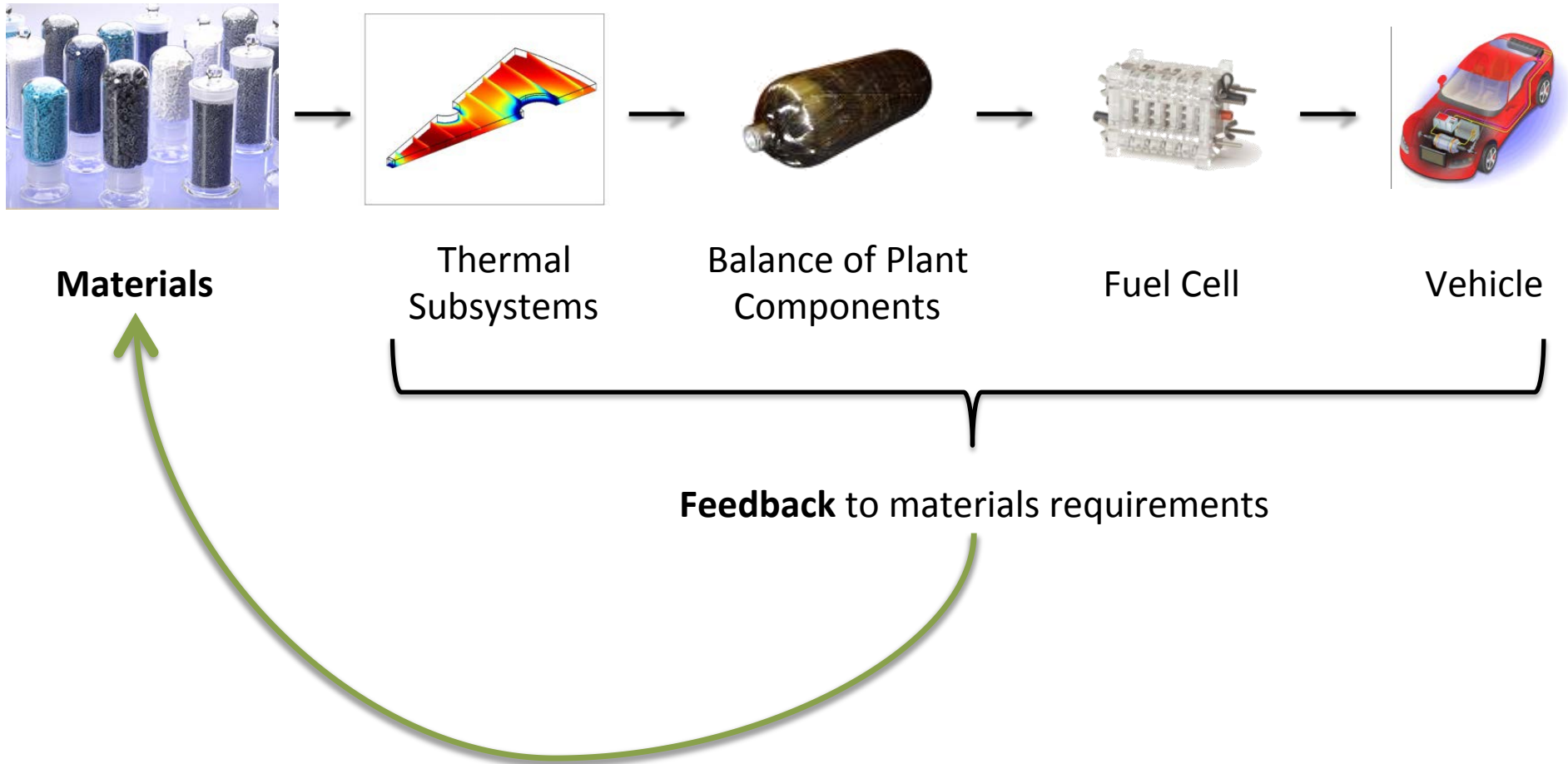
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Overview

- For the past 5 years the HSECoE has been developing hydrogen storage systems based on adsorbent, metal hydride, and chemical hydride media
- As we near the Center's conclusion, we seek to translate insight gained from the Center to the materials development community
- This presentation summarizes:
 1. Lessons learned in the development of a MOF-5-based storage system
 2. Materials properties needed to achieve DOE targets
(Adsorbent Acceptability Envelope)

Engineering *around* an **imperfect** material can guide development of an optimal material



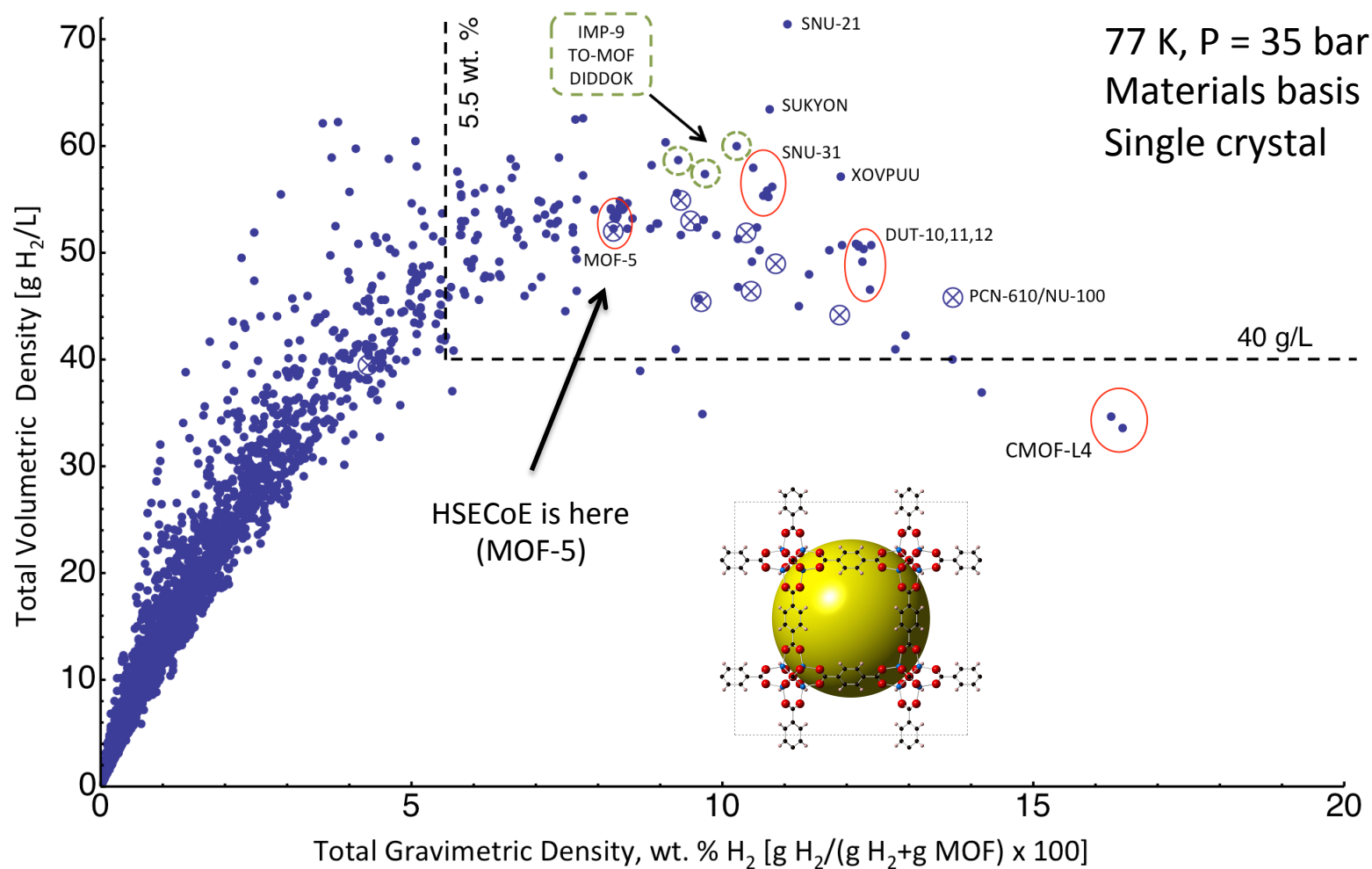
HSECoE Goals – Adsorbent System

- Model, design, and construct an adsorbent-based hydrogen storage system that has the potential to meet DOE 2017 targets.
- Reveal design tradeoffs, e.g.:
 - Gravimetric vs. volumetric density
 - Capacity & cost vs. fill time
 - Pros/cons of various HX designs
- Guide materials development by identifying materials properties that most strongly impact system performance.

Part 1: HSECoE Highlights

MOF-5 Selected as Baseline Adsorbent

Good combination of volumetric and gravimetric density;
Available in large quantities (BASF)



System Performance Metric

The Center developed a multivariable approach to measure design tradeoffs. This model was used to rank various system concepts.

○ System Score = Gravimetric Score + Cost Score + Volumetric Score

○ Gravimetric Score

$$= S_{GD\%} (I_{FE} \times C_{GFE} + I_{DR} \times C_{GDR} + I_{VA} \times C_{GVA} + I_{VC} \times C_{GVC})$$

○ Cost Score

$$= S_{C\%} \times I_{VC} \times C_{CVC}$$

○ Volumetric Score

$$= S_{VD\%} \times I_{VDR} \times C_{VDR}$$

$S_{GD\%}$ = % gravimetric density system target from 2017 target

$S_{C\%}$ = % system cost target from 2017 target

$S_{VD\%}$ = % volumetric density system target from 2017 target

I_{FE} = 11.3= importance rating for fuel economy (vehicle level)

I_{DR} = 5.5= importance rating for driving range (vehicle level)

I_{VA} = 3.4= importance rating for vehicle acceleration (vehicle level)

I_{VC} = 19.2= importance rating for vehicle cost (vehicle level)

C_{GFE} = 0.03= correlation % change in gravimetric density for fuel economy (% system to % vehicle)

C_{GDR} = 0.03= correlation % change in gravimetric density for driving range (% system to % vehicle)

C_{GVA} = 0.04= correlation % change in gravimetric density for vehicle acceleration (% system to % vehicle)

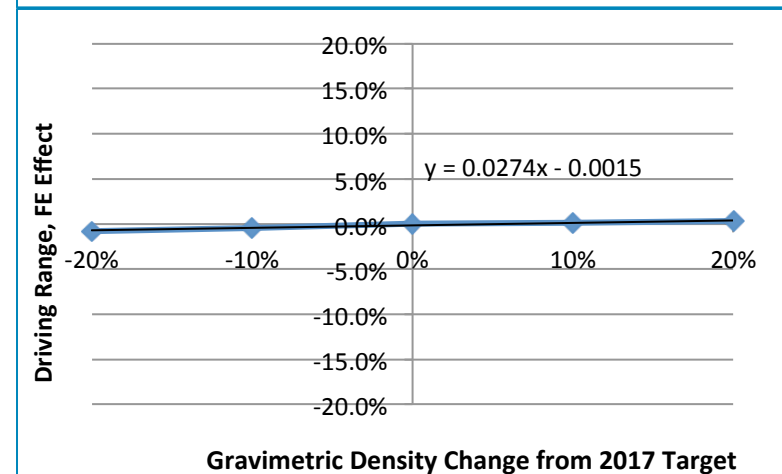
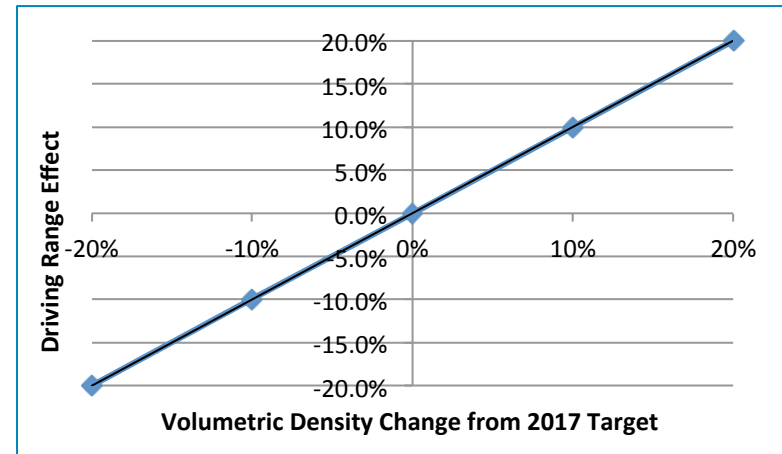
C_{GVC} = 0.1= correlation % change in gravimetric density for vehicle cost (% system to % vehicle)*

C_{CVC} = 0.15= correlation % change in cost for vehicle cost (% system to % vehicle)

C_{VDR} = 1= correlation % change in volumetric density for driving range (% system to % vehicle)

* this correlation value is a placeholder and needs to be confirmed with further analysis

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Rapid System Design Tool

Narrowed space of possible designs to 4 “systems of interest.”

Approach – From over ½ Billion combinations... down to 4 Systems

Over ½ Billion Possible System Combinations:

- Internal heat exchangers (all options) (x45)
- Tank types (x6)
- L-to-D ratios (x3)
- LN₂ inner wall chiller (x2)
- Hemispherical vs. oblate endcaps (x2)
- Pressure vessel only vs. full design (x2)
- Material types (with volume-% changes) (x87)
- Media packing density (x10)
- Full tank pressure (x12)
- Full tank temperature (x7)
- Empty tank temperature (x4)

Perform a
parametric
study

Option #1	Option #2	Option #3	...	Option N
1	1	1	...	1
2	1	1	...	1
⋮	⋮	⋮	⋮	⋮
N ₁	1	1	...	1
1	2	1	...	1
2	2	1	...	1
⋮	⋮	⋮	⋮	⋮
N ₁	N ₂	N ₃	...	N _N

Eliminate unrealizable
system options and
combinations of options

62 Million Reasonable Systems Combinations:

- Internal heat exchangers (all options) (x31)
- Tank types (x2)
- L-to-D ratios (x3)
- LN₂ inner wall chiller (x2)
- Hemispherical vs. oblate endcaps (x2)
- Pressure vessel only vs. full design (x1)
- Material types (with volume-% changes) (x29)
- Media packing density (x5)
- Full tank pressure (x12)
- Full tank temperature (x6)
- Empty tank temperature (x8)

Filter the
Results

Final 4 Systems:

- Three flow-through cooling with resistance HX options:
 - HexCell with powder MOF-5
 - HexCell with 0.32 g/cc compacted MOF-5 pellets
 - Helical coil with powder MOF-5
- One isolated-LN₂ cooling with isolated-H₂ heating option:
 - MAT1 with 0.32 g/cc compacted MOF-5 pucks

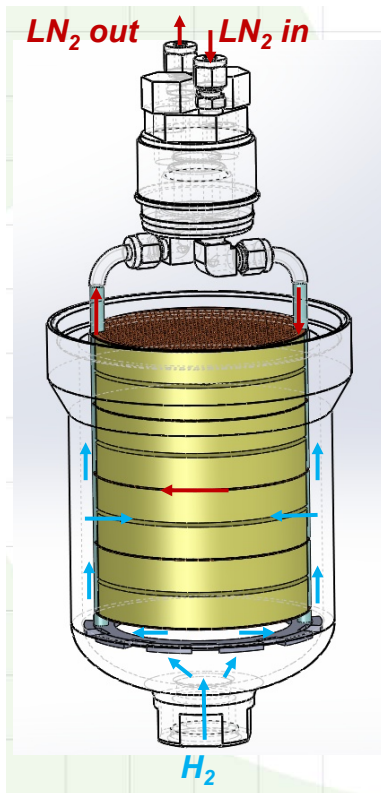
David Tamburello, SRNL

System Prototypes

Two system prototypes are being built and tested in the final phase of the HSECoE

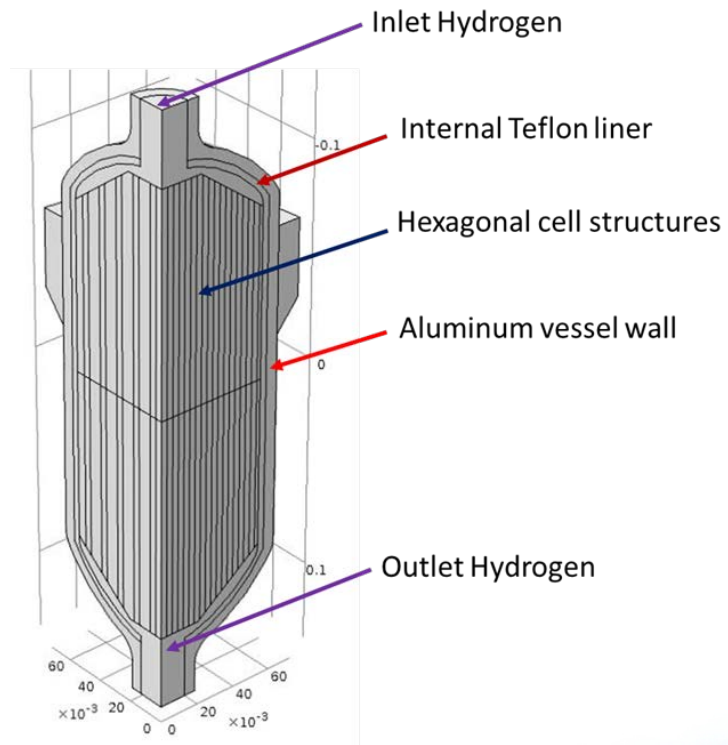
MATI*

Densified media
Isolated cooling/heating flow



Hex-Cell

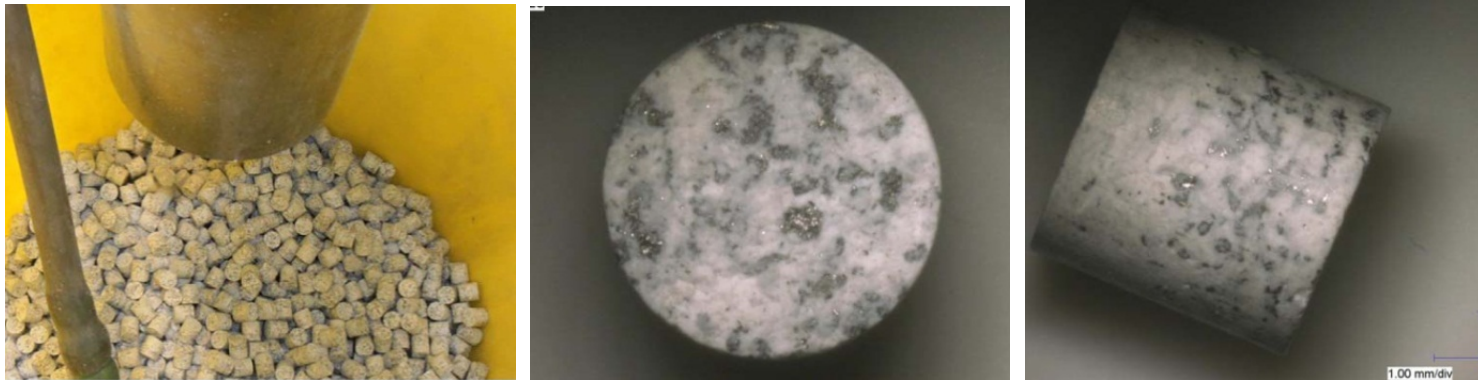
Powder media
Flow-through cooling + resistive heating



Densification of Powders

MOF-5 powders can be formed into pellets & pucks without binder

GW0117 – pellets 6x6 mm, 5 +/- 0.1% ENG, .391 g/cc with $\sigma = .013$ g/cc

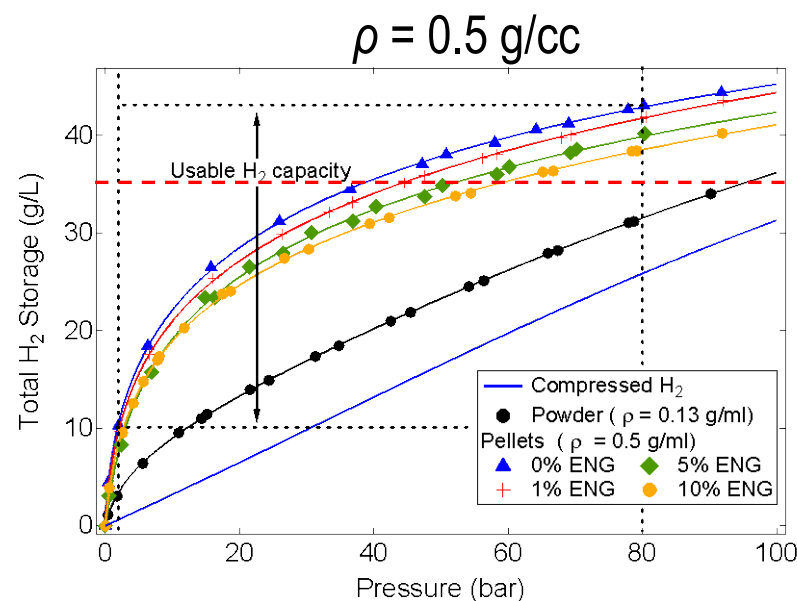
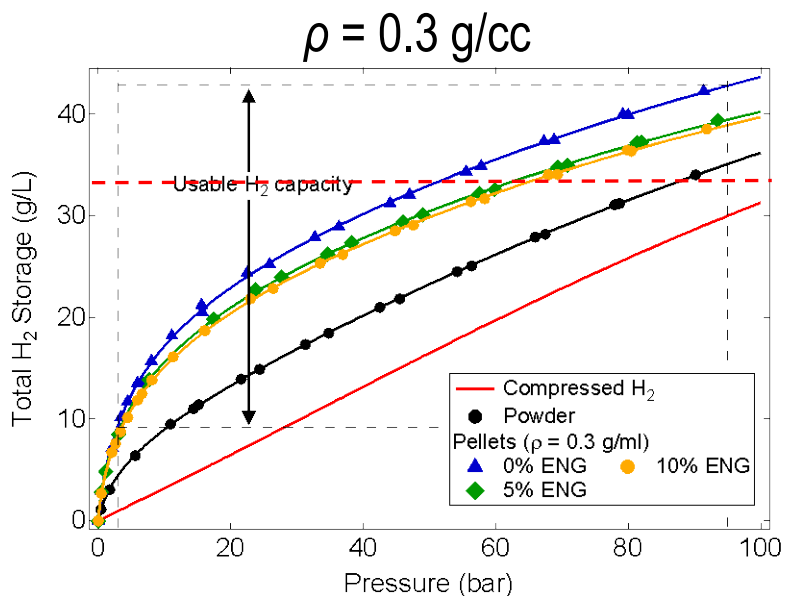


Pucks: \varnothing 5 cm x 1.5 cm

ENG layering + pins

Improved Volumetric Density in MOF-5 Pellets

Monoliths have > 50% improvement in volumetric hydrogen density.
 Practical upper limit to density = ~0.5 g/cc (plastic deformation)



- Note: All curves currently assume skeletal densities of 2 g/cc and 100% packing efficiency.

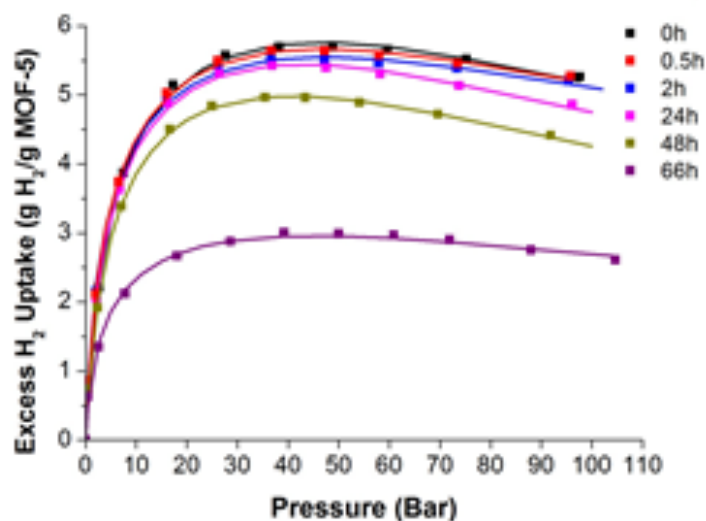
Powder 5-60 bar & 80 K	0.3 g/cc + 5% ENG 5-60 bar & 80 K	0.3 g/cc + 5% ENG 5-60 bar & 80-160 K	0.5 g/cc + 5% ENG 5-60 bar & 80 K	0.5 g/cc + 5% ENG 5-60 bar & 80-160 K
20 g/l	22 g/l	31 g/l	22 g/l	34 g/l
<i>60% packing efficiency:</i>				
	20 g/l	26 g/l	21 g/l	27 g/l

Stability: Robustness to Air-Exposure

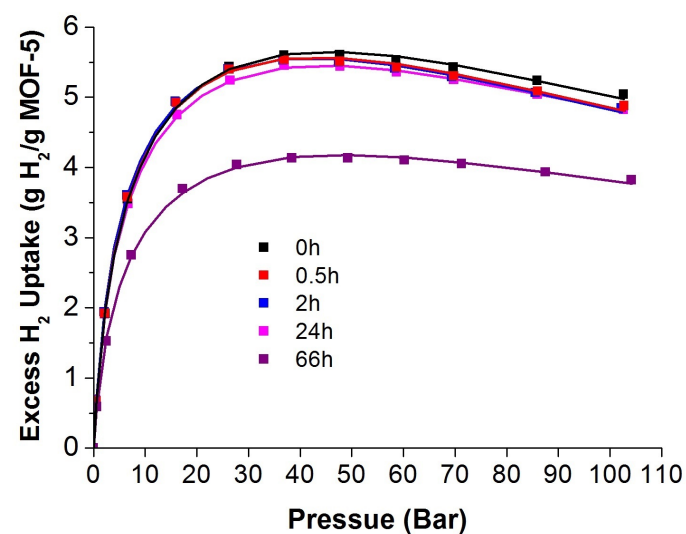
Exposure tests show that MOF-5 undergoes limited capacity degradation in humid environments for exposure times up to 2 hours

Relative humidity = 45 %

Powder, $\rho = 0.13 \text{ g/cm}^3$

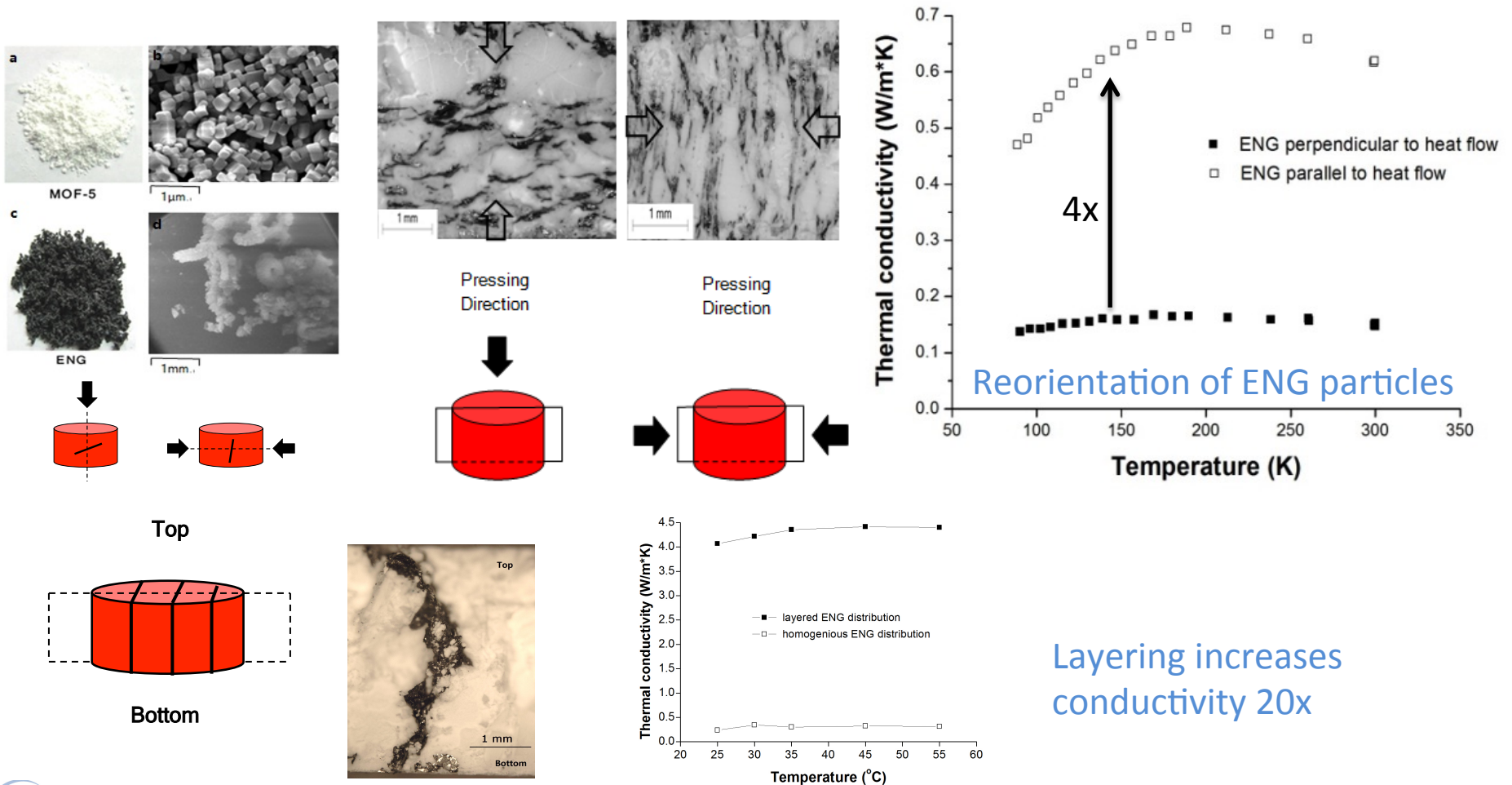


Pellets, $\rho = 0.37 \text{ g/cm}^3$



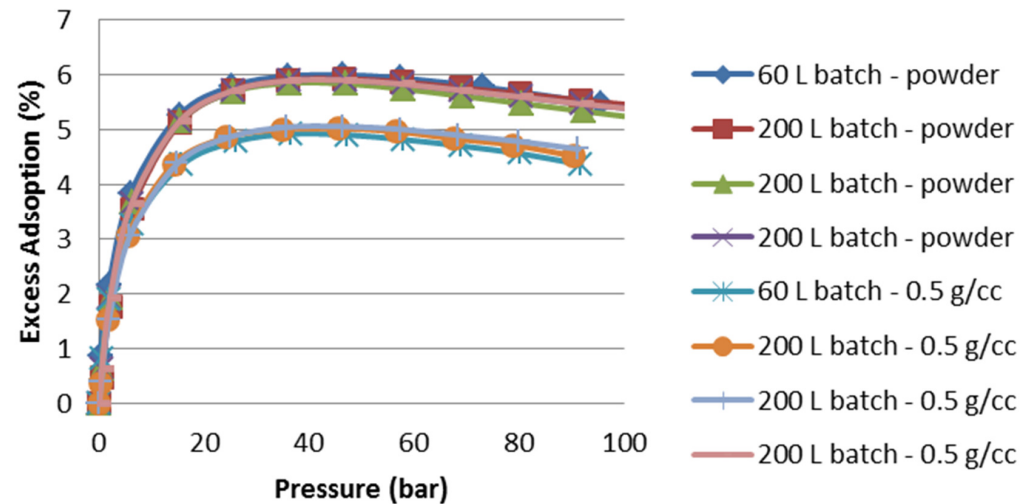
Thermal Conductivity

Reorientation and layering of ENG additions can dramatically improve the low conductivity of MOF-5



Scale-up of MOF-5

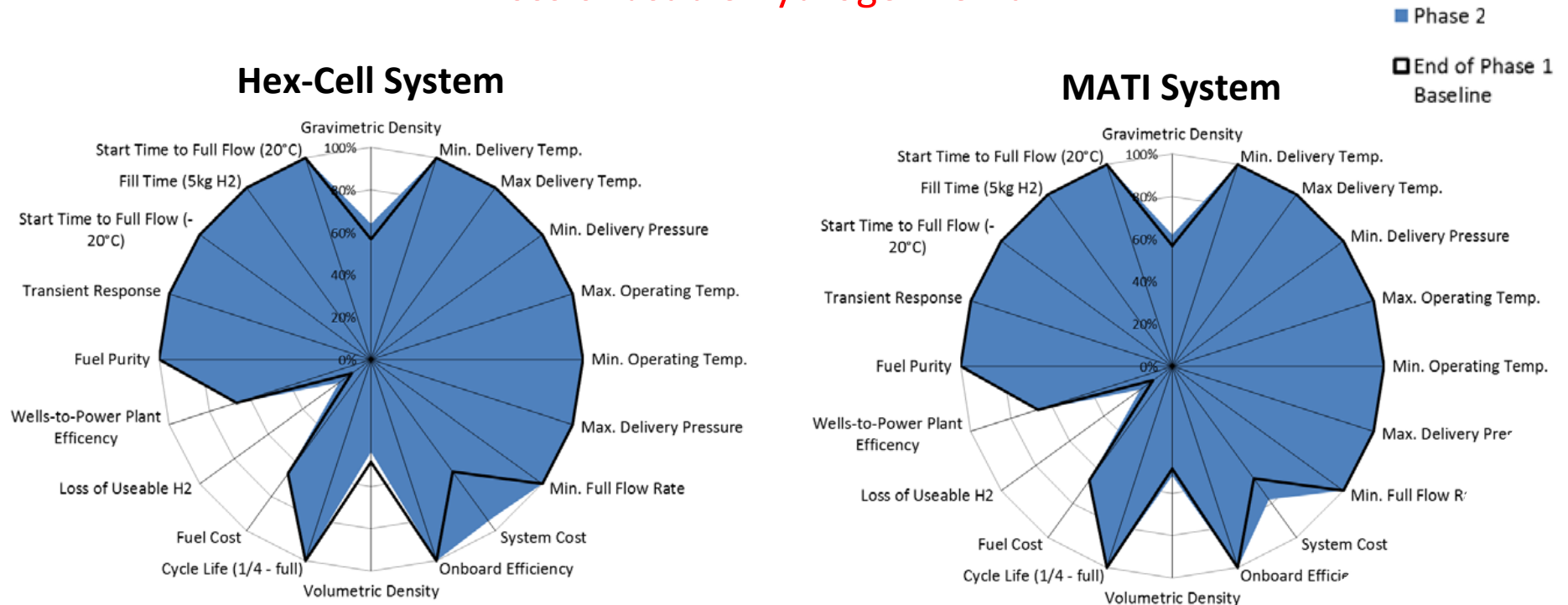
MOF-5 manufacturing process has delivered ~9.3 kg of material.
Performance confirmed to be within 10% of lab-scale material



Batch Code	Reactor Size [L]	Amount [kg]	BET [m ² /g]	LSA [m ² /g]	Zn [wt%]	C [wt%]	Crystal size* [μm]	Particle size** [mm]
GP0372	200	3.1	2937	3838	32	37	0.2-2.0	
GP0374	200	3.5	2870	3794	34	37	0.2-2.0	
GP0375	200	3.2	2955	3896	34	37	0.2-2.0	
GP0378	Mix	9.3	2937	3877	30	37	0.2-2.6	0.1-1.3
GP0326	60	1	2905	3891	34	37	0.2-3.0	0.1-1.4
Scale-Up Difference:			1%	.4%				7%
Reference GW0116	7	.14	2680	3547			0.2-2.0	

System Design Improvements

The center has identified lower cost designs, but limitations in capacity and loss of usable hydrogen remain



Phase 1 system: AX-21 powder, **Type 3 CF tank, 200 bar, 80 K**



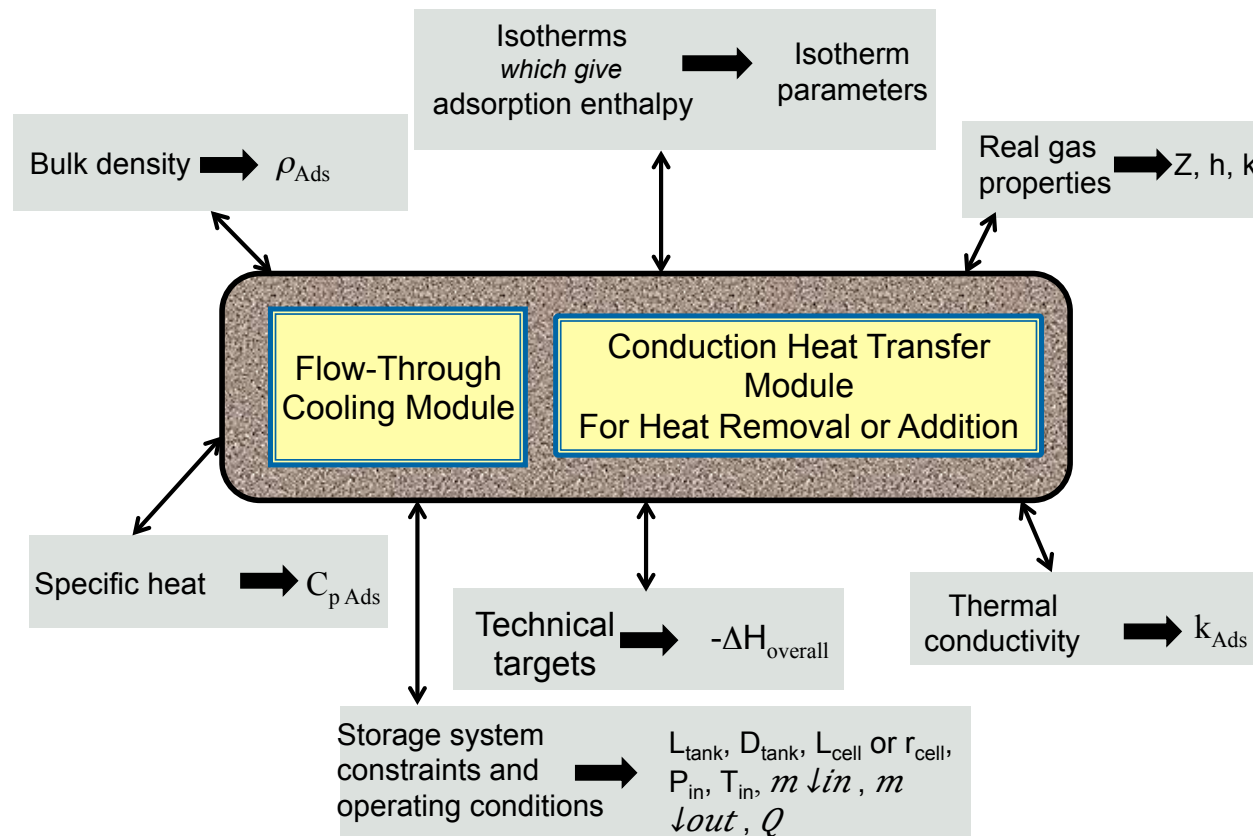
Lower pressure → lower cost,
heavier tank → comparable capacity!

Final system: MOF-5, **Type 1 Al tank, 100 bar, 80K**

Part 2: Adsorbent Acceptability Envelope

Adsorbent Acceptability Envelope

Leverages knowledge gained by HSECoE in modeling, characterization, and construction of adsorbent system



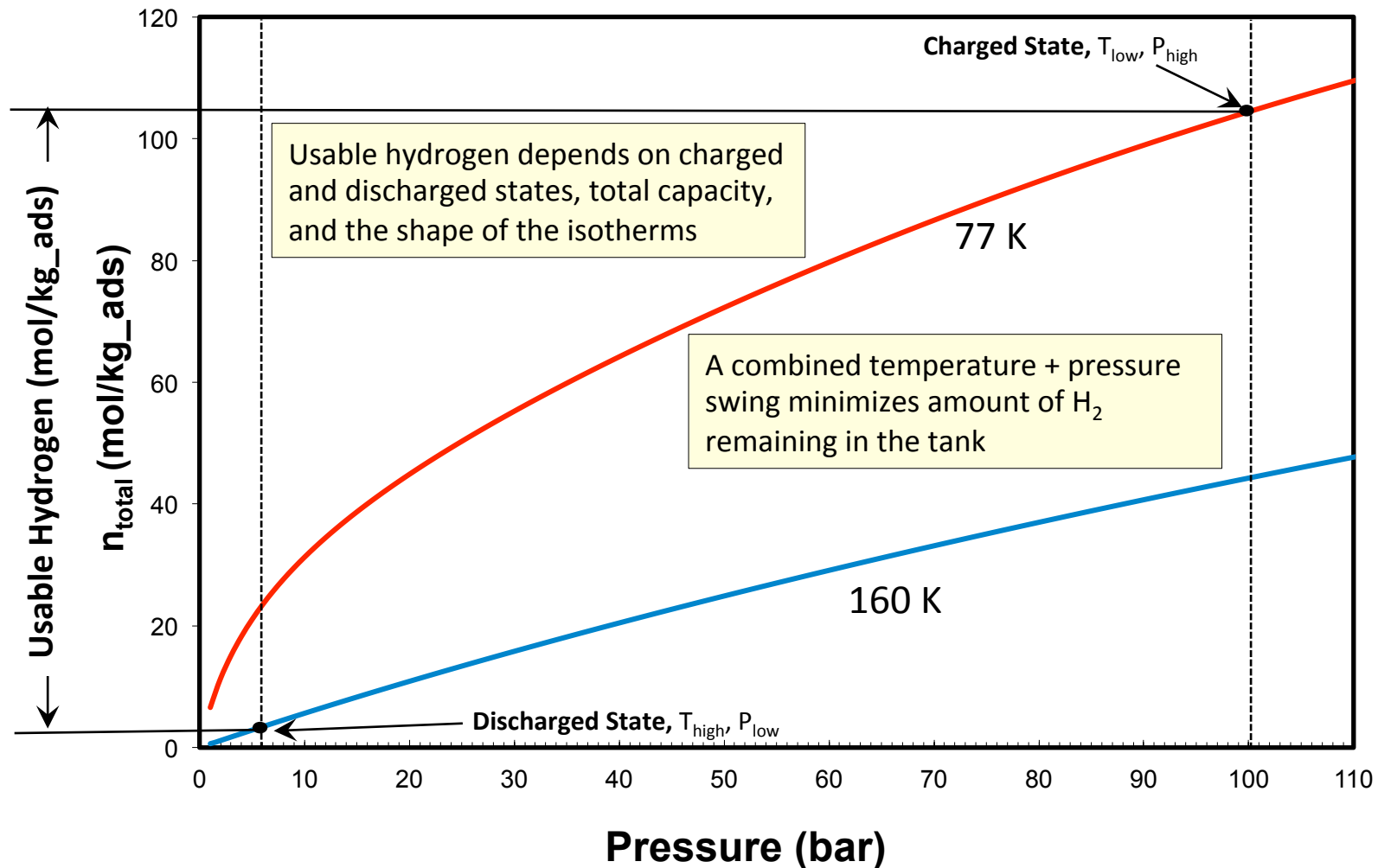
Overview

Goal: Identify coupled adsorbent and storage vessel properties that can meet 700 bar and DOE targets

- Accomplished by:
 - Use of isotherms that yield necessary amount of **usable** hydrogen (not just total)
 - Depends on final (empty) and initial (full) states
 - Determined through numerical variation of isotherm parameters
 - Can also determine parameters that **optimize** usable hydrogen
 - Isotherms also determine enthalpy of adsorption
 - Requires knowledge of bulk, crystal, and skeletal densities
 - OR bulk density, inter-particle porosity, and intra-particle porosity

Definition: Usable Hydrogen

Determined using a temperature + pressure swing from
 $T_{\text{low}}, P_{\text{high}}$ to $T_{\text{high}}, P_{\text{low}} = 5 \text{ bar}$



UNILAN Isotherm

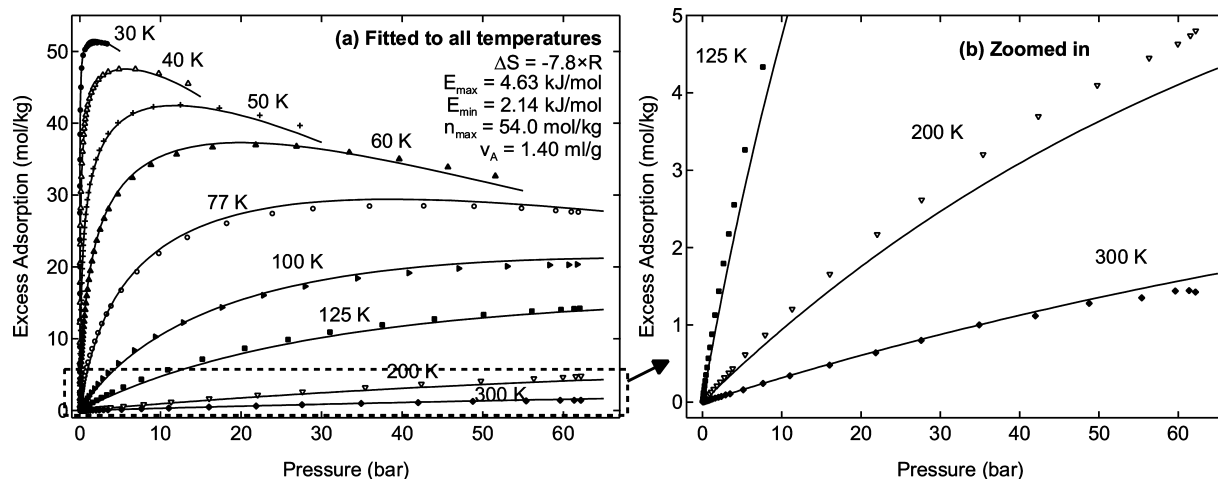
UNILAN model provides an accurate description of the MOF-5 experimental data, requiring only five parameters to predict uptake across a wide temperature range

$$n_a = \frac{n_{max}RT}{(E_{max} - E_{min})} \ln \left(\frac{e^{-\Delta S_0/R} + \frac{P}{P_0} e^{E_{max}/RT}}{e^{-\Delta S_0/R} + \frac{P}{P_0} e^{E_{min}/RT}} \right)$$

$$n_{Total} = n_a + c(V_v - V_p)$$

$$n_{Usable} = n_{Total}(T_{chg}, P_{chg}) - n_{Total}(T_{disch}, P_{disch})$$

E_{max} and E_{min} = The maximum and minimum values of $-\Delta H_0$ ($|\Delta H_0|$ is the isosteric heat) [J/mol]. $-\Delta H_0$ is uniformly distributed between E_{min} and E_{max} .



Assumptions and Operating Scenarios

The approach uses an assumed set of operating conditions and system architecture

System Architecture

- Flow through (Hex-cell)

- Type 1 Al vessel
- 5:1 Length:diameter
- Internal HX = 20% mass
- 5.6 kg usable H₂ stored
- 1" MLVI
- LN₂ jacket
- MOF-5 like adsorbent
- 181 kg/m³ powder

Scenario 1: Cryo System

$$\begin{aligned}T_{\text{low}} &= 77 \text{ K} \\P_{\text{high}} &= 100 \text{ bar} \\T_{\text{high}} &= 160 \text{ K} \\P_{\text{low}} &= 5 \text{ bar}\end{aligned}$$

Scenario 2: Ambient System

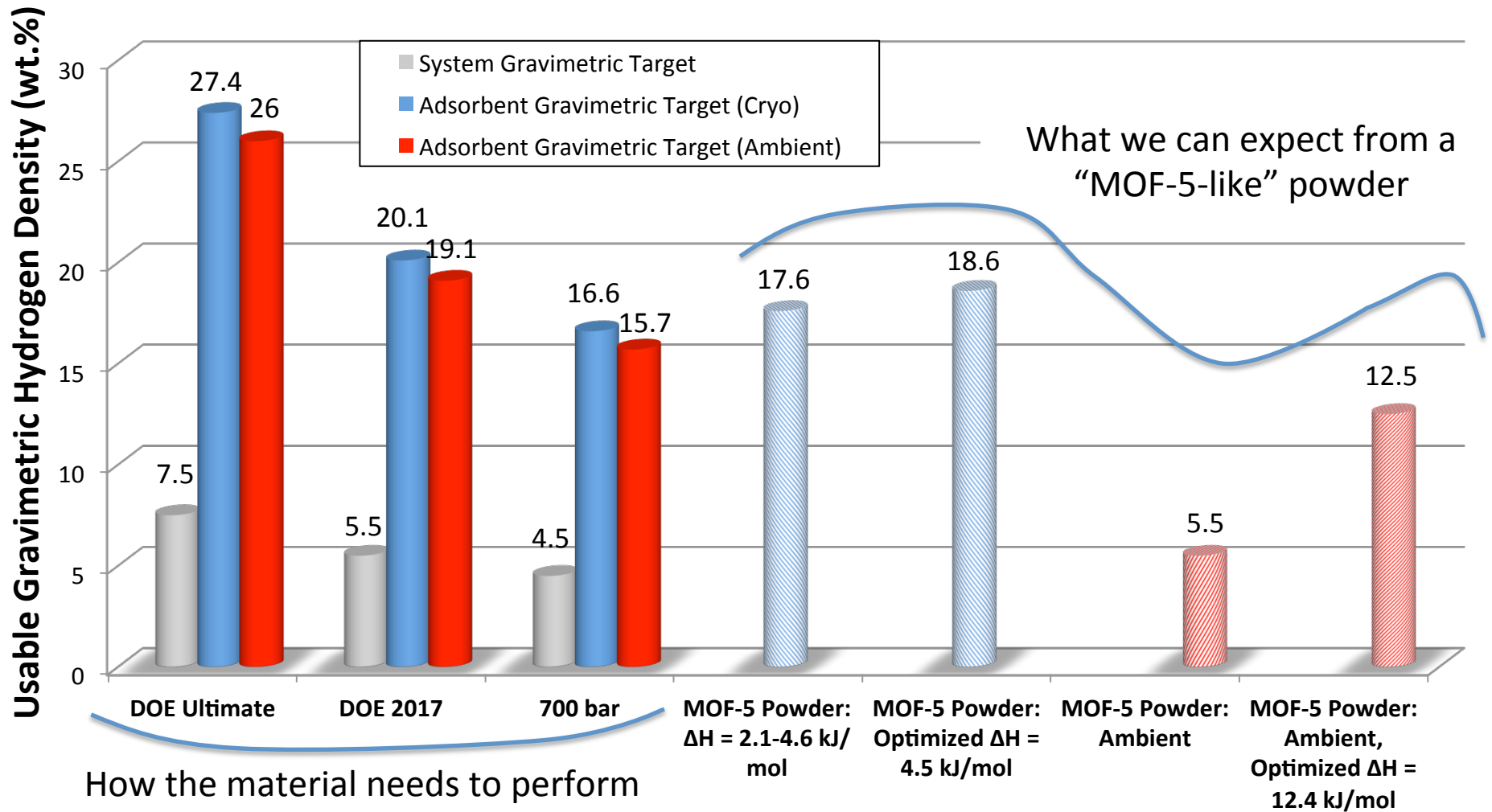
$$\begin{aligned}T_{\text{low}} &= 230 \text{ K} \\P_{\text{high}} &= 100 \text{ bar} \\T_{\text{high}} &= 400 \text{ K} \\P_{\text{low}} &= 5 \text{ bar}\end{aligned}$$

Procedure

1. Set initial (full) and final (empty) T, P conditions
2. Fix entropy change, ΔS , to nominal value for MOF-5
3. Set value for bulk density of adsorbent, ρ_{bulk} (181 kg/m³ MOF-5 powder)
4. Back-calculate materials capacity targets based on system targets & system mass + volume
5. Numerically determine required isotherm parameters with respect to usable hydrogen
 - Optimize n_{max} , E_{max} , and E_{min} in UNILAN model to meet target values (at adsorbent level)
 - Convert isotherm parameters to gravimetric and volumetric H₂ densities (at adsorbent level)
6. Repeat steps 3-5 for different operating scenarios and materials densities

Materials Capacity Targets – Gravimetric

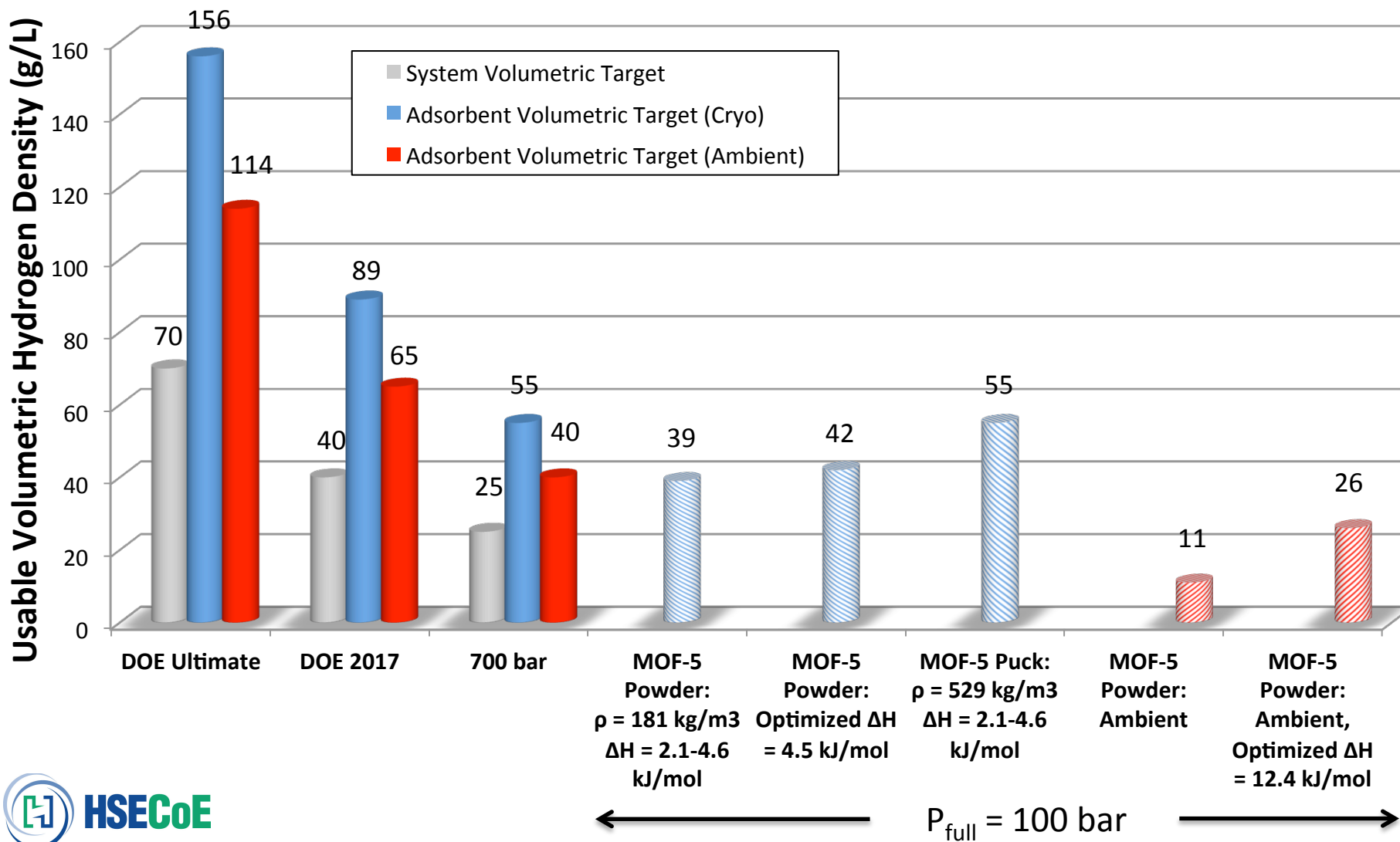
A powder MOF-5-like system can surpass 700 bar in gravimetric density at low-T



$P_{full} = 100$ bar

Materials Capacity Targets – Volumetric

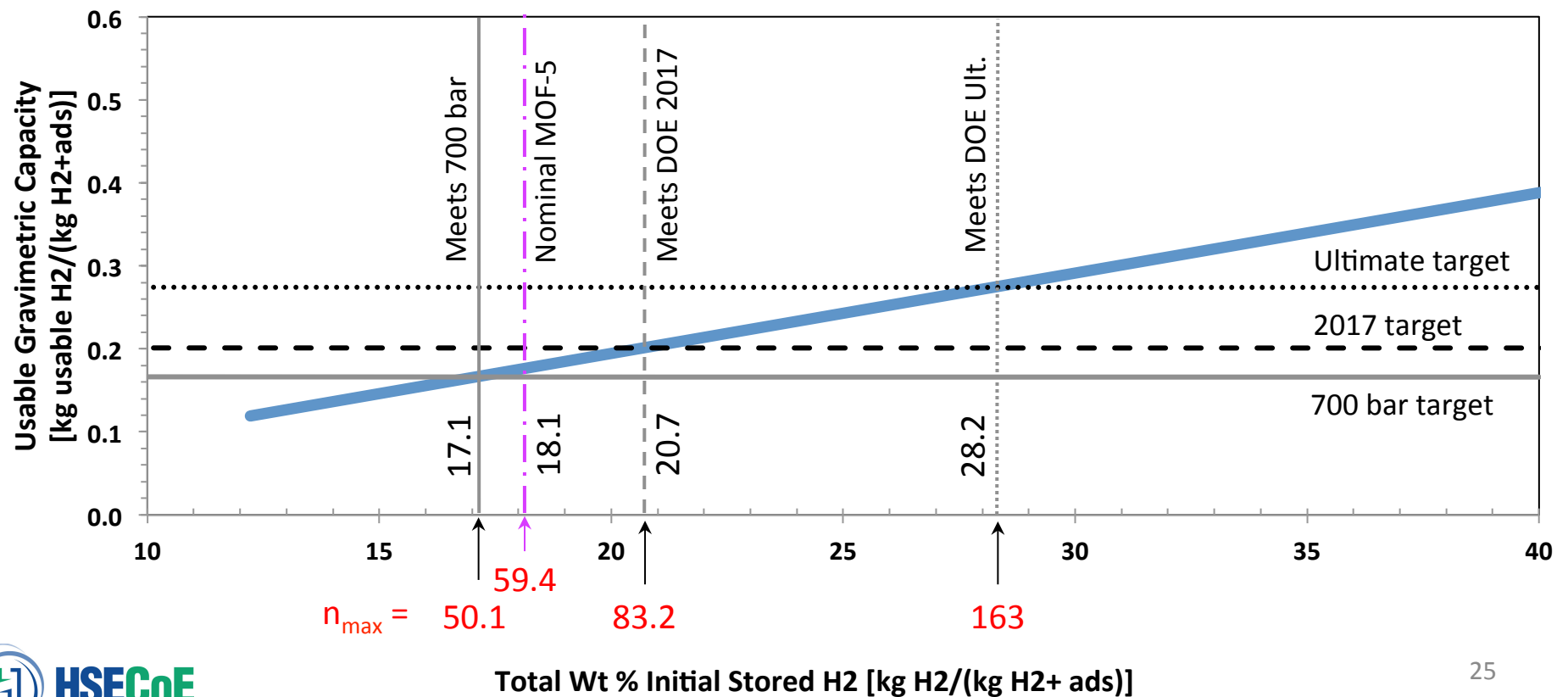
A powder-based system falls short in volumetric H₂ density



Parametric Dependence on Number of Adsorption Sites

Vary number of adsorption sites (n_{max}) while keeping all other adsorbent properties constant

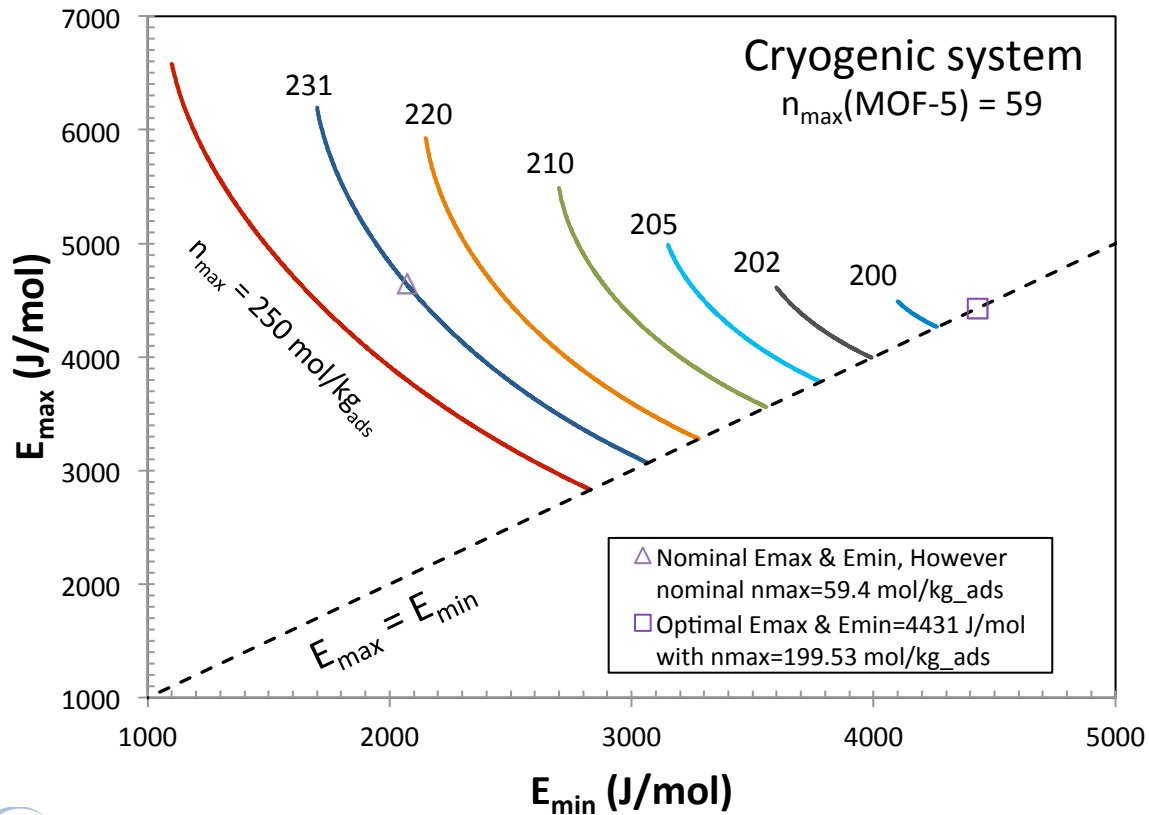
MOF-5 can surpass 700 bar on a gravimetric basis at cryogenic conditions.
However, reaching the DOE 2017 target will require a 14% improvement in capacity.



Parametric Dependence on Adsorption Sites *and* ΔH

Many combinations of ΔH and n_{\max} can in principle satisfy targets
 However, meeting volumetric targets with a powder system requires very large n_{\max}

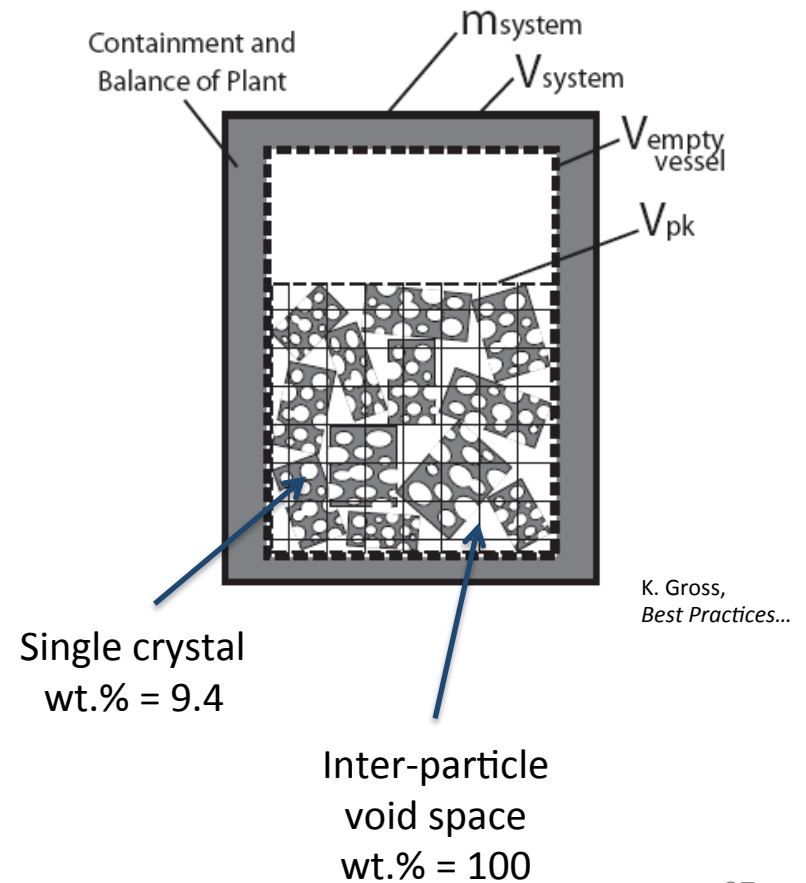
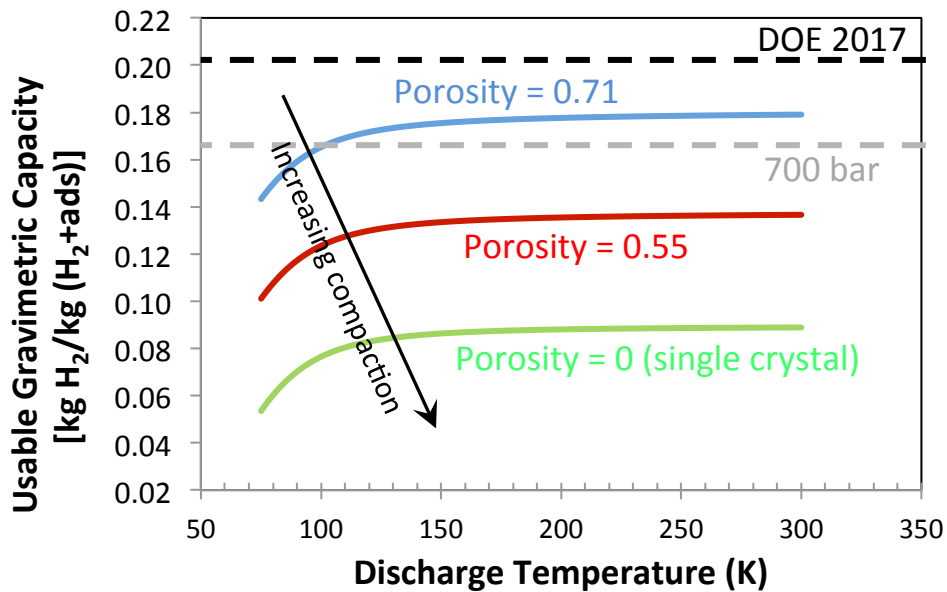
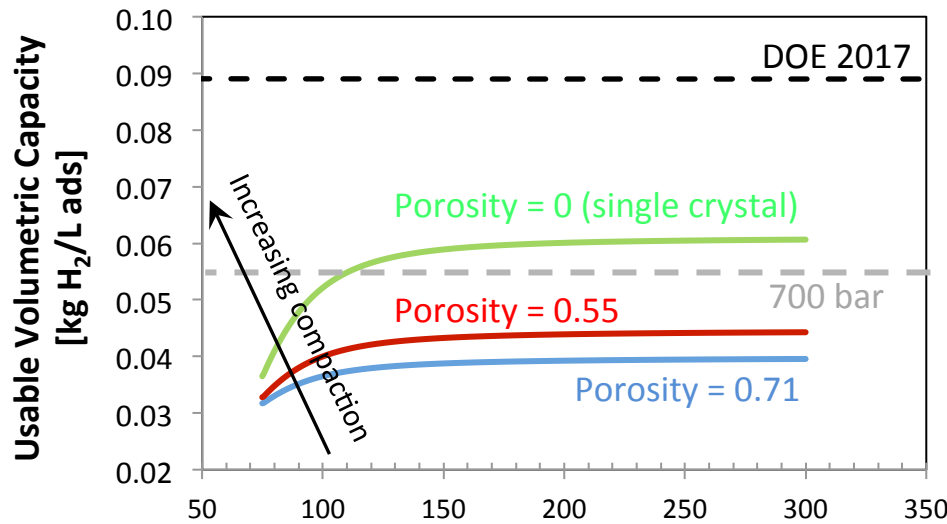
Combinations Which Meet DOE 2017 Volumetric Targets



- Each curve represents an adsorbent having a combination of binding sites (n_{\max}) and ΔH which would meet the DOE 2017 volumetric target
- Adsorbents having adsorption site heterogeneity ($E_{\min} \neq E_{\max}$) generally require more adsorption sites to meet target
- Large $E_{\max} = E_{\min}$ can meet target with smaller n_{\max}

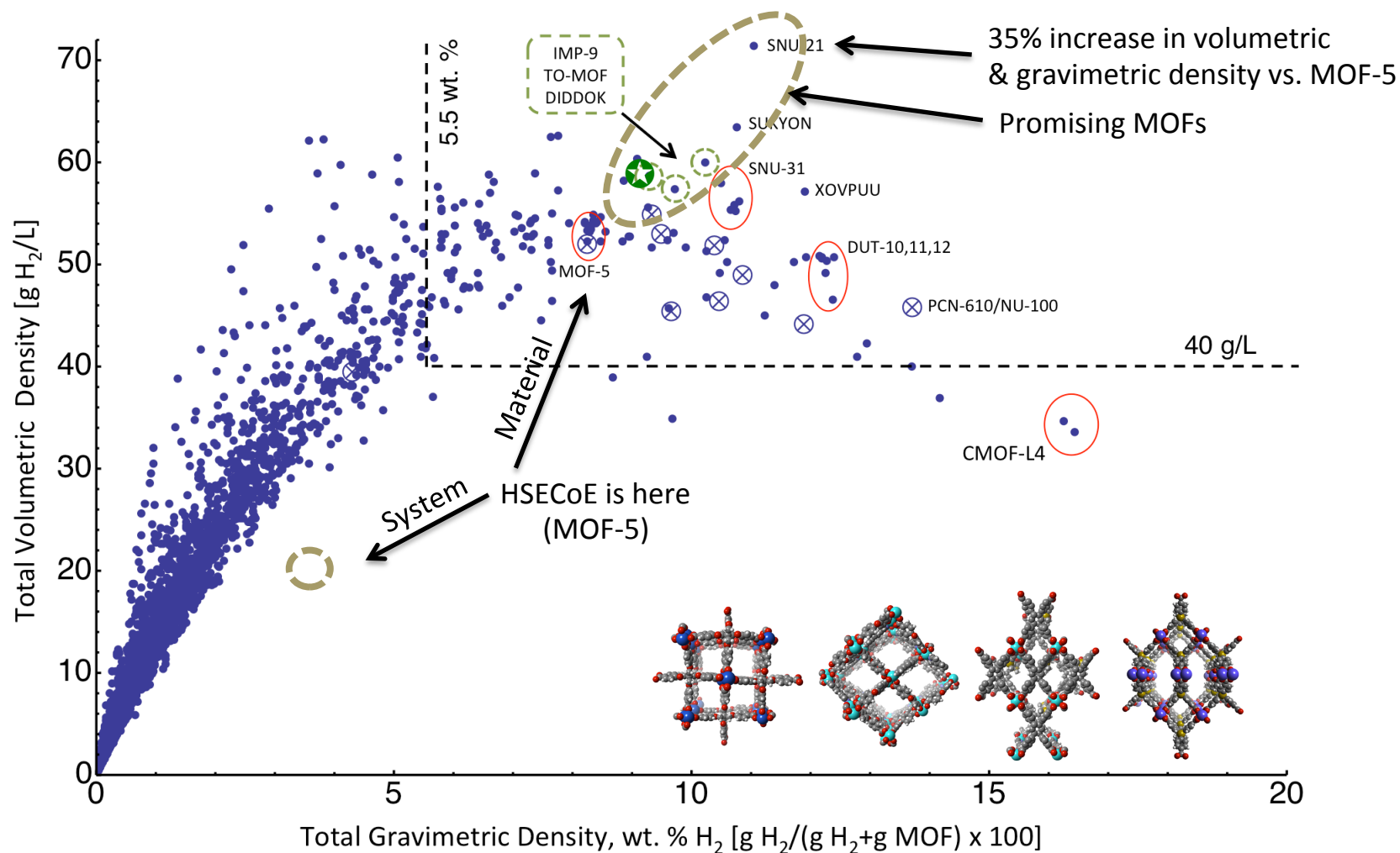
Gravimetric/Volumetric Tradeoff

Compaction can be used to increase volumetric density; however, it will come at a loss to gravimetric density arising from closure of inter-particle voids



Alternative Adsorbents?

MOF-5 is a good baseline, but higher-performing alternatives exist



Summary of Materials Requirements

...for a powder-based adsorbent, $P_{\max} = 100$ bar

System	System-level Targets		Materials-level targets		Notes
	Usable Gravimetric (wt.%)	Usable Volumetric (g/L)	Usable Gravimetric (wt.%)	Usable Volumetric (g/L)	
DOE Ultimate	7.5	70	27.4	156	Cryo-system
			26.0	114	Ambient system
DOE 2017	5.5	40	20.1	89	Cryo-system
			19.1	65	Ambient system
700 Bar	4.5	25	16.6	55	Cryo-system
			15.7	40	Ambient system

Concluding Remarks (1)

- The Adsorbent Acceptability Envelope has been developed to assess viability of hypothetical hydrogen adsorbents
 - Quantifies the amount of usable hydrogen stored
 - Formulated in terms of isotherm parameters and materials density
 - Applied to a powder-based, flow-through system designed by HSECoE
 - Cryogenic and ambient operating conditions explored
 - Extensions: Additional analysis of ambient-T and densified systems
- An advanced adsorbent may be able to surpass the performance of 700 bar compressed systems
 - Such a system could be attractive from an efficiency (low-P, 100 bar) and cost standpoint (metal tank) even though it would not meet DOE targets
- Achieving the DOE 2017 or Ultimate targets remains a daunting challenge

Concluding Remarks (2)

- Trade-off between volumetric and gravimetric density
 - Densification of powders can be helpful, but should be balanced with losses in gravimetric density and plastic deformation (pore collapse)
 - Achieving high surface area alone is insufficient
 - Materials research should focus on adsorbents that circumvent this tradeoff; high gravimetric and volumetric densities must be achieved *simultaneously*
- Adsorbent stability is important, but should be assessed based on likely/moderate failure modes:
 - E.g.: Withstand limited exposure to humid environments during assembly
- Low thermal conductivity of adsorbents can be overcome with engineering approaches

Acknowledgements

HSECoE Team

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Hydrogen Storage Engineering

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