

### A Novel Flash Ironmaking Process

**DE-EE0005751** 

American Iron and Steel Institute/University of Utah 09/01/2012 - 8/31/2015

Joseph Vehec, American Iron and Steel Institute

U.S. DOE Advanced Manufacturing Office Peer Review Meeting Washington, D.C. May 6-7, 2014







- Develop a new ironmaking process w/ significant reduction in energy consumption and CO<sub>2</sub> generation
- Blast furnace requires pelletization and/or sintering of iron ore concentrate
- Consumes large amounts of energy and carbon → CO<sub>2</sub> emissions
- Alternative ironmaking processes must have:
  - Large production capacities (e.g., ~1,000,000 tpy of iron)
  - Use the main raw material (i.e., iron ore) with minimal pretreatment





# **Technical Approach**

#### **Current practice**

- Blast furnace (BF) produces >90% iron for steelmaking
- BF needs large capital investments
- High energy consumption in raw materials preparation and CO<sub>2</sub> emissions
- Use of special coals for cokemaking

#### **New Approach – A Novel Flash Ironmaking Process**

- Direct use of iron concentrate (~30 μm)
  - Bypass pelletizing and sintering
- Use of inexpensive, abundant natural gas [or hydrogen, coal gas]
  - No cokemaking required
  - Lower energy consumption
  - Less CO<sub>2</sub> emissions
- Rapid reaction rate and favorable Net Present Value (NPV)





### **Technical Approach**

 Install, commission & conduct test on a new large bench reactor at the University of Utah



- Multidisciplinary team:
  - American Iron and Steel Institute
    - ArcelorMittal USA
    - The Timken Company
    - United States Steel Corporation
  - University of Utah (Lead Research Organization)
  - Berry Metal Company (Bench reactor fabrication)





# Transition and Deployment

Project Objectives	Kinetic Feasibility  Technology Road Map (2005-2007)	Proof of Concept at Lab Scale  AISI CO <sub>2</sub> Breakthrough (2008-2011)	Process Validation/ Scale-up Innovative Manufacturing Initiative (2012-2015)	Industrial Pilot TBD (2016+)
Experimental Apparatuses	Ceramic Reactor  Alumina Honeycomb High-Temperature Furnace  Heating Elements  Powder Collector & Filter			Approaches  1. Large scale 75-100k tpy  2. Modest-scale: 10-25k tpy  3. Expand U of Utah work: Similar to bench reactor but larger
Funding	Federal, \$350k <b>Industry, \$150k</b> Total, \$500k	Federal, \$ 0 Industry, \$ 4.8million Total, \$4.8million	Federal, \$ 7.1million Industry, \$ 1.8million Total, \$8.9million	\$10 – 75million Funding TBD







## **Transition and Deployment**

- Benefits steel users and steel-related industry
- U.S. Steel industry would be the end user
- To be used to produce iron as a raw material for steelmaking resulting in:
  - Direct use of iron ore concentrate
  - Low capital cost
  - Scalable to large capacities
  - Avoidance of cokemaking
- Commercialization through licensing & royalty
- Sustainable as a more energy efficient and green ironmaking step







- If successful, iron will be produced at a lower cost, using less energy, and emitting less CO<sub>2</sub>
- Potential energy savings: ~3.5 GJ/ton Fe vs. avg. BF
- CO<sub>2</sub> emission: Less than 36% vs. avg. BF process

Metric	H <sub>2</sub> -based process	Reformerless natural gas process	Blast Furnace process
Energy Requirement (GJ/ton of hot metal)	11.3	14.5	18.0
CO <sub>2</sub> emission (tons/ton of hot metal)	0.04	1.02	1.60

NPV for standard case (15 year period): \$401M (2010)/(1 M tpy) Natural gas cost: \$5/M (2010) BTU HHV





# Project Management & Budget

Task	Description	Milestones			
Lask		Key Inputs	Criteria	Date	
1	Bench Scale Reactor	Go/No Go Decision # 1:		1/31/2015	
	Installation	Operating Temperature	1400°C		
	Commissioning	Solid feed rate	>1 kg/hr		
		Operation time	>6 hr		
2	Testing Program	Go/No Go Decision # 2:		7/31/15	
	_ Existing lab flash reactor	Metallization	95%		
	Drop-tube reactor	Min. amt. reducing gas	3.ox		
	Bench reactor	Go/No Go Decision # 3:		1/31/16	
	_ CFD model	Metallization	95%		
		Min. amt. reducing gas	1.5X		
		Milestone # 4:		7/31/16	
		Metallization	95%		
		Solid feed rate	>5 kg/hr		
3	Industrial pilot reactor				
	Design				
	Cost estimate				
4	Program Administration			1/31/17	

Total Project Budget		
DOE Investment	\$7,120,000	
<b>Cost Share</b>	\$1,780,000	
Project Total	\$8,900,000	







- Fabricated New bench reactor and ancillary equipment
- Designed/fabricated main burner key component
- Prepared site for bench reactor installation
- Achieved 80-95% metallization in existing lab reactor\*
- Fuel/reductant: Hydrogen
  - •[Natural gas tests are planned]
- Reaction time: 4-6 seconds
- Temperature: ~1200°C
  - •[less than 1300°C in bench reactor]



\*Different from New Bench Reactor with respect to the size and material of construction, which limits the operating temperature. Solid feed rate is limited ( $\sim 0.5 \text{ kg/hr}$ ).







## Results and Accomplishments

- Measurement of reduction kinetics with natural gas using existing Lab reactor (2014)
- Computational Fluid Dynamic model development (2014-2016)
- Installation of new bench reactor (1Q15)
- Testing with new bench reactor (2015-2016)
- Industrial pilot plant design (2016)



