

# Intra-catalyst Reductant Chemistry in Lean NO<sub>x</sub> Traps: A Study on Sulfur Effects

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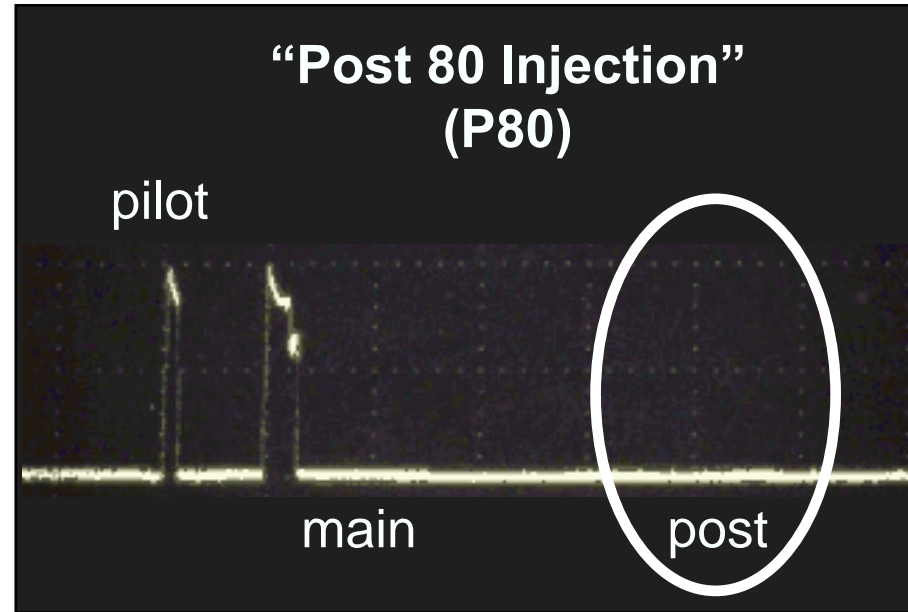
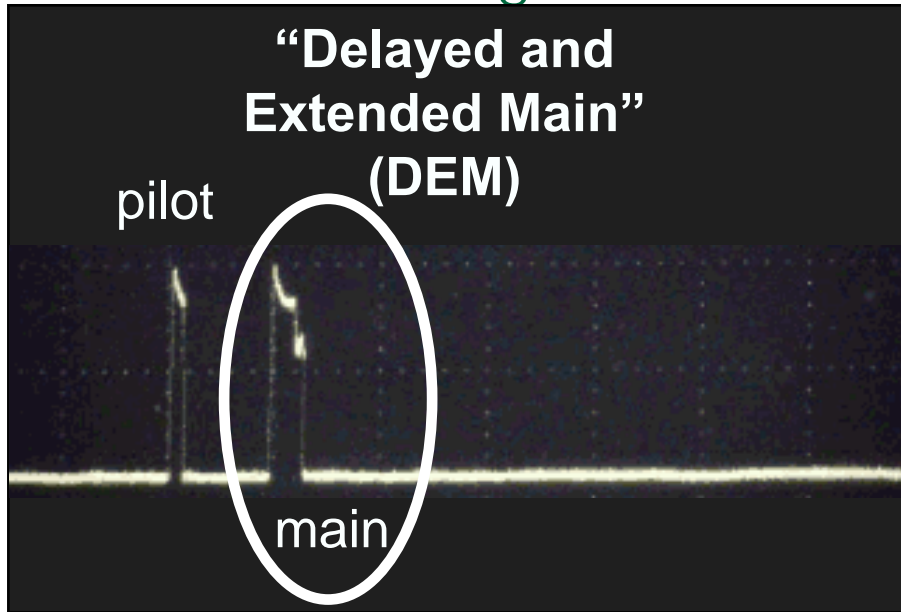
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**Program Managers: Ken Howden, Gurpreet Singh, Kevin Stork**

# Study Focus Area: Sulfur Effects on Reductant Utilization by Lean NOx Trap Catalysts

- **Lean NOx Trap (LNT) catalysts are effective at reducing NOx from diesel engines but need...**
  - **Periodic “regeneration” (rich exhaust) with suitable reductants**
  - **Durability against negative sulfur effects**
    - **Sulfur degrades performance over time by poisoning NOx sites**
    - **deSulfation (high temperature clean up) recovers lost site activity**
- **ORNL has studied regeneration chemistry on a light-duty diesel engine platform with in-cylinder combustion techniques**
  - **Intra-catalyst sampling has been applied to characterize reductant utilization [SAE 2006-01-1416, SAE 2005-01-3876, SAE 2004-01-3023]**
- **Study presented here focuses on the effects of sulfur on intra-catalyst chemistry during in-cylinder regeneration**

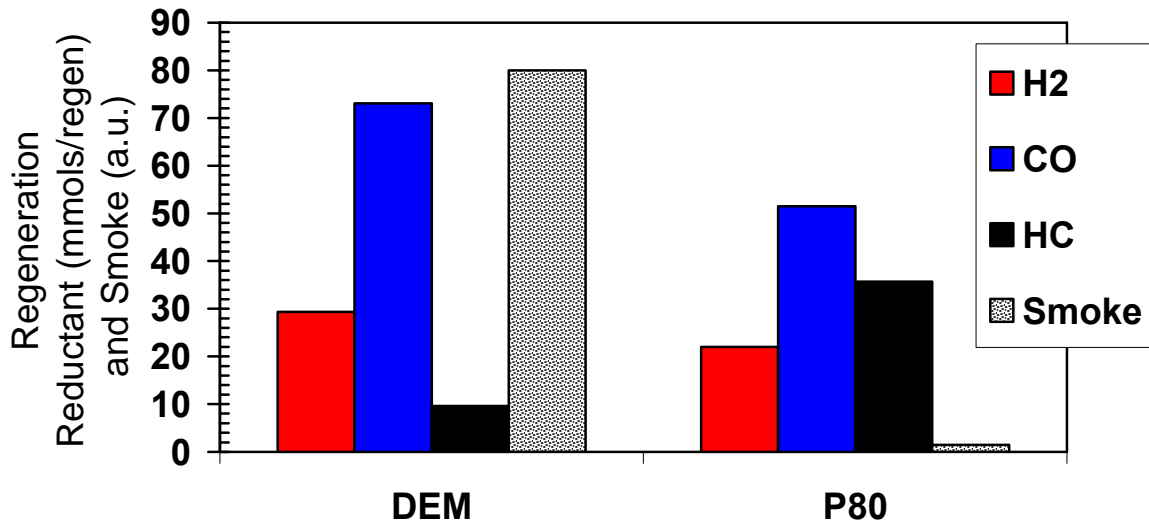
# Two engine control strategies for achieving intermittent rich combustion for regeneration of LNT



## Two LNT Regeneration Strategies Chosen Based on Difference in Chemistry

- **Delayed and Extended Main (DEM):**
  - Throttle for reduced air flow
  - Extra fuel injected near main injection timing to achieve rich conditions
- **Post 80 Injection (P80):**
  - Throttle for reduced air flow
  - Extra fuel injected after main injection later in cycle to achieve rich conditions

# Two engine control strategies for achieving intermittent rich combustion for regeneration of LNT

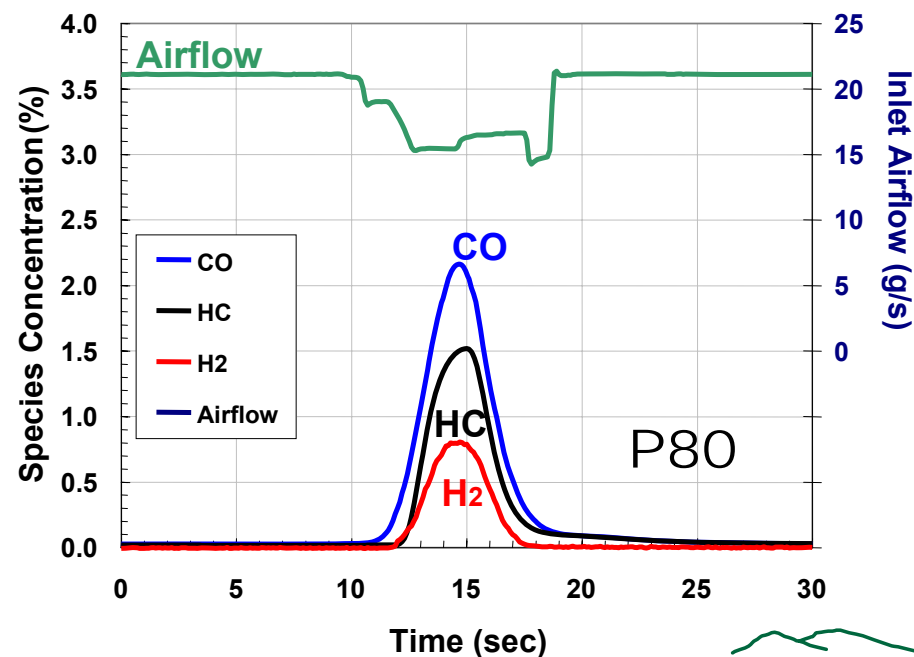
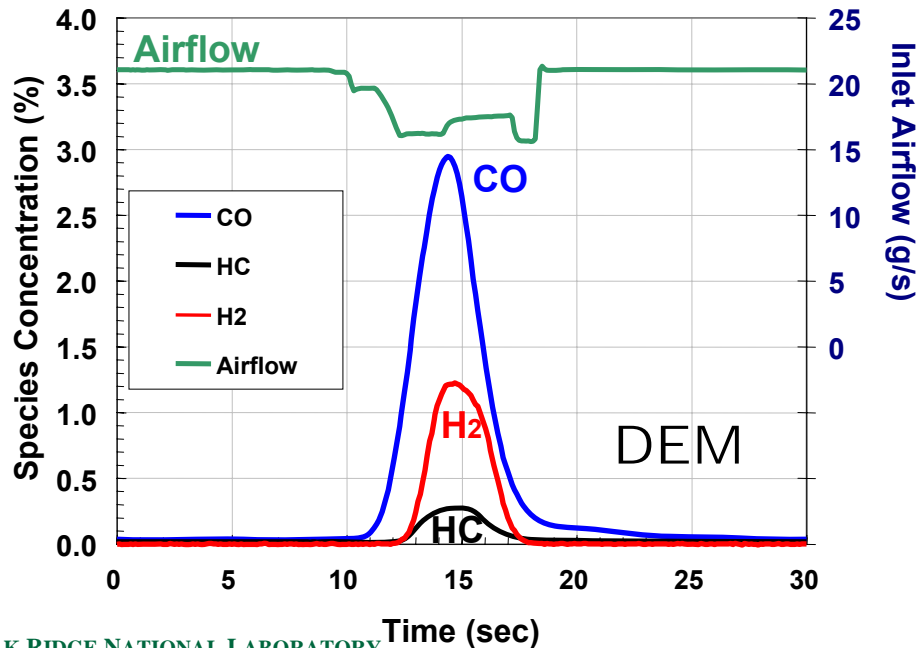


- **Delayed and Extended Main (DEM):**

- High H<sub>2</sub> and CO
- Low HC
- High PM

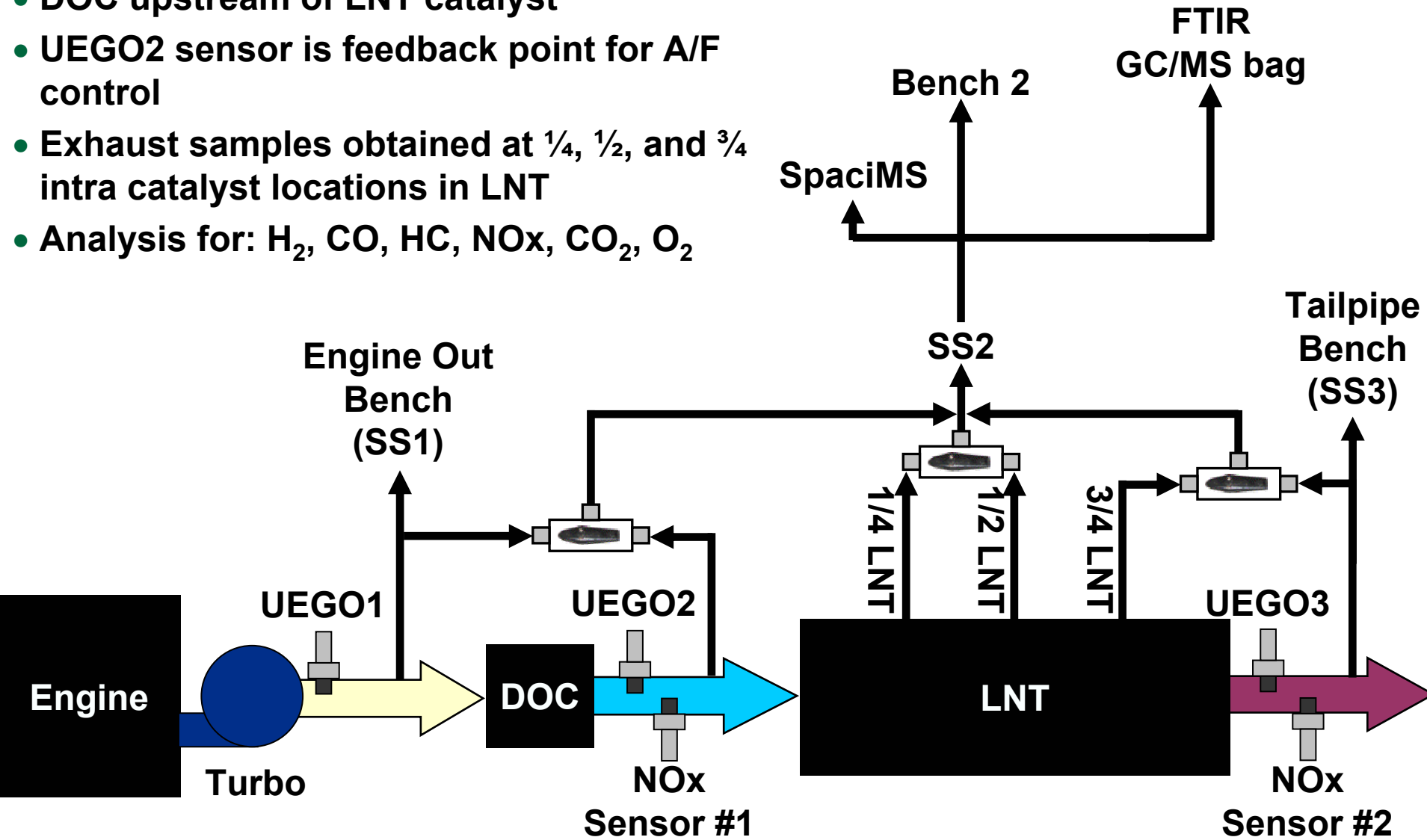
- **Post 80 Injection (P80):**

- Moderate CO and H<sub>2</sub>
- High HC
- Low PM

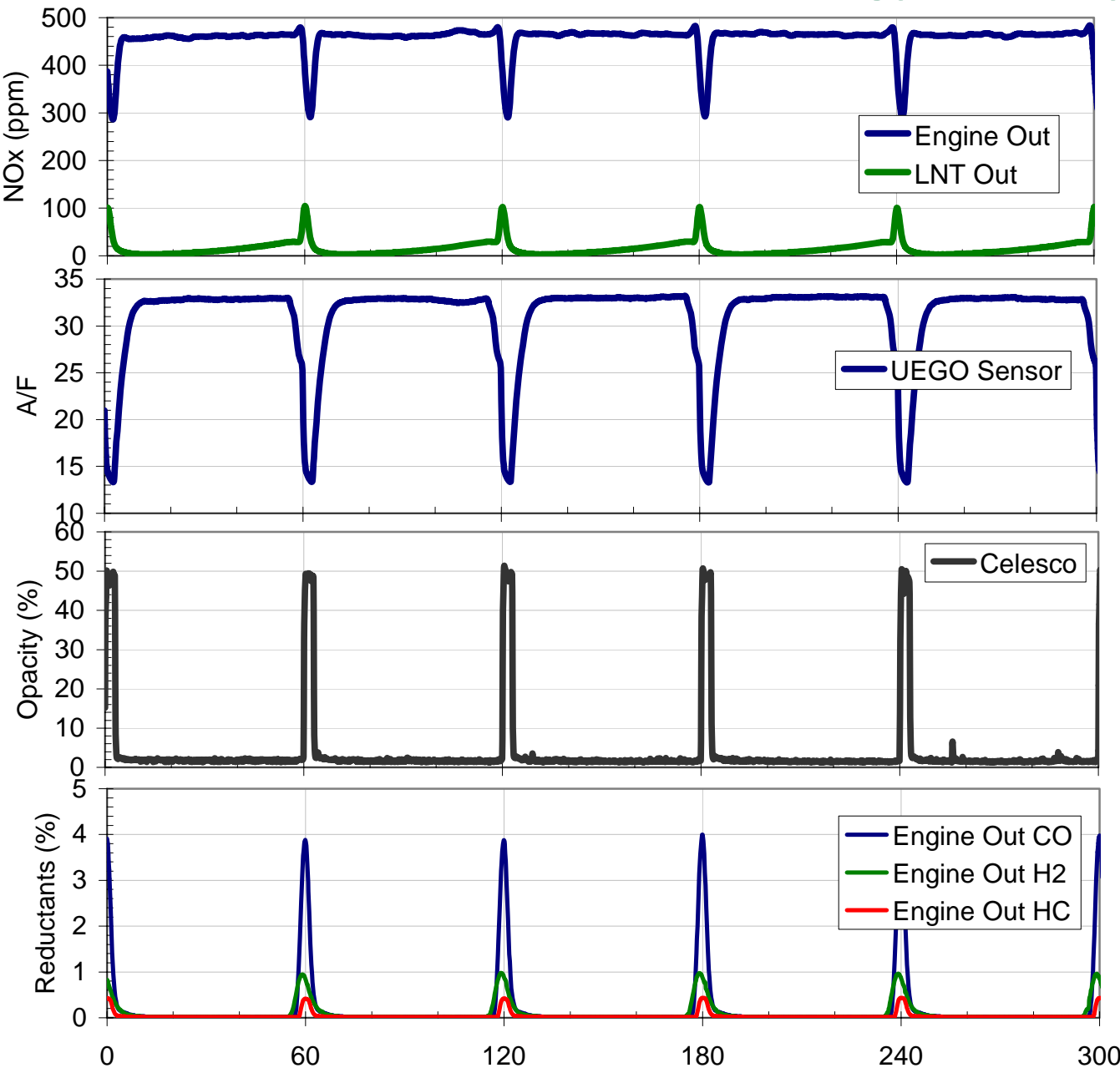


# Experimental setup allows full exhaust species characterization throughout the catalyst system

- DOC upstream of LNT catalyst
- UEGO2 sensor is feedback point for A/F control
- Exhaust samples obtained at  $\frac{1}{4}$ ,  $\frac{1}{2}$ , and  $\frac{3}{4}$  intra catalyst locations in LNT
- Analysis for:  $H_2$ , CO, HC, NO<sub>x</sub>, CO<sub>2</sub>, O<sub>2</sub>



# Exhaust Speciation: DEM Strategy, 60s Cycle (DEM, 60s)

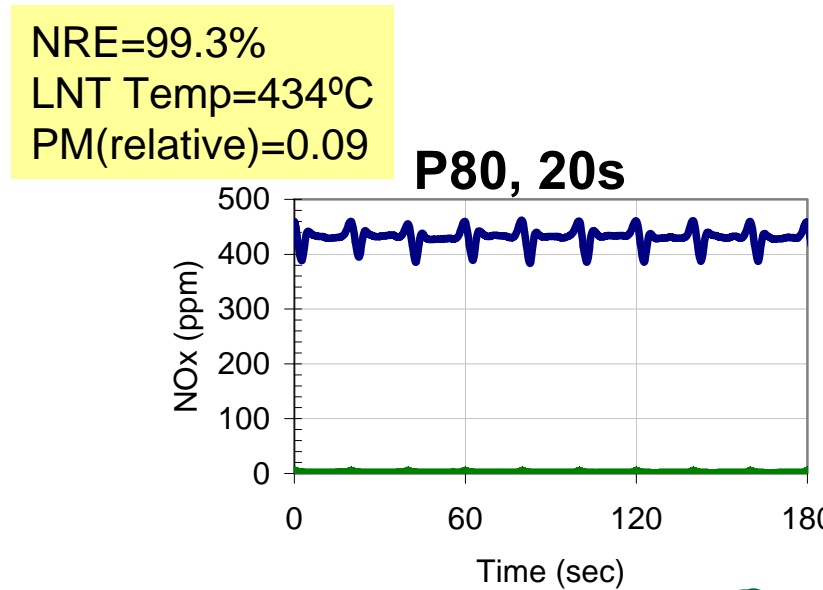
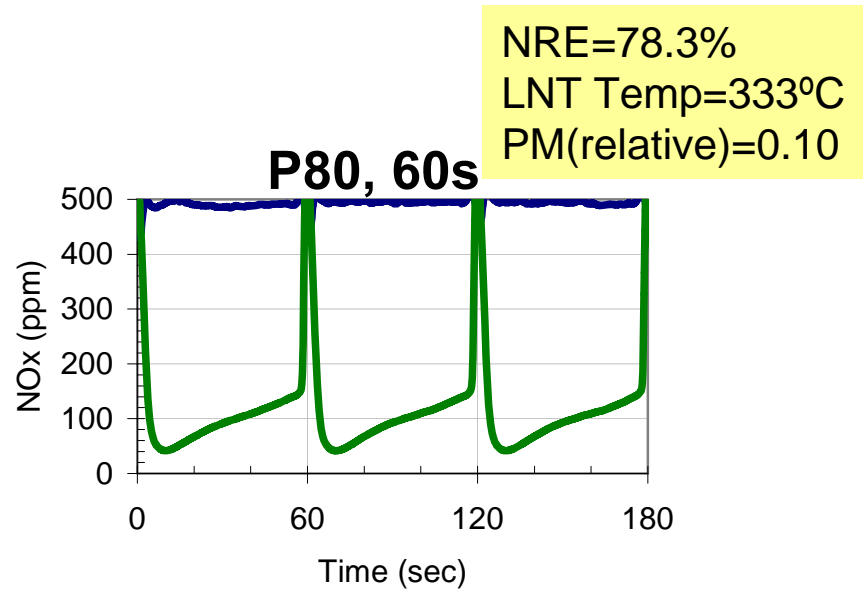
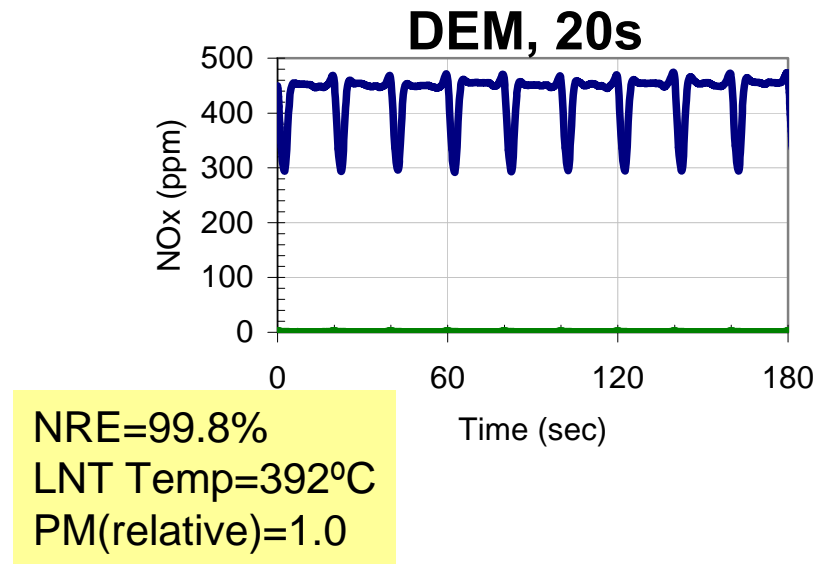
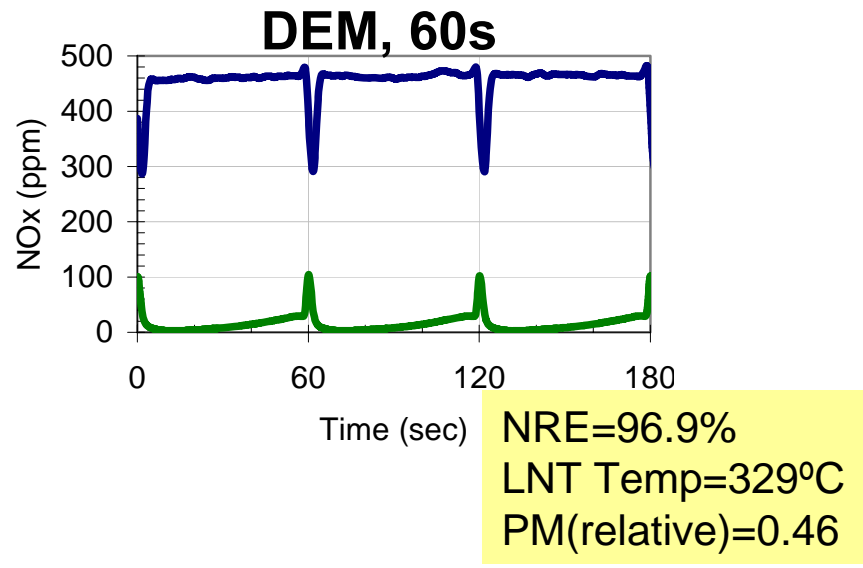


## DEM, 60s

- NOx Reduction Efficiency (NRE)=96.9%
- Mean LNT Temp=329°C
- Minimum A/F=13.5
  
- 60 second Cycle:
  - 57 seconds Lean
  - 3 seconds Rich

# Strategy and Cycle Time Combinations in Study

— Engine Out  
— LNT Out



# Catalyst chemistry characterized under sulfated and desulfated conditions

## Sulfation procedure

- **Degreened in air**
- **BP15 fuel**
- **1% bottled SO<sub>2</sub> at 3.4slpm**
- **Three loading states (fuel S + bottled S)**
  - **3.06g S ≈ 2888 miles**
  - **5.63g S ≈ 5319 miles**
  - **9.63g S ≈ 9087 miles**
- **Full characterization done at each loading state**

## Desulfation procedure

- **Engine based desulfation**
  - **Target 700°C / 14AFR**
  - **Fixed boost to 0kPa**
  - **Use RPM to control airflow**
  - **Control catalyst inlet AFR using in-pipe injection**
- **20 minute desulfation event**

### Fuel loading

Fuel Flowrate	0.6 g/s
Fuel Economy (assumed)	45 mi/gal
BP 15 Sulfur Content	0.0015%
Fuel Density	0.143 gal/lb
Miles per gram S	944 mi/g
grams S /min	0.00054 g/min

### Bottle loading

Molecular Weight of S	32.06 g/mol S
1% SO <sub>2</sub> flowrate	3.4 slpm
SO <sub>2</sub> concentration	1.00%
S flowrate	0.0486 g/min

	state 1	state 2	state 3
1% SO <sub>2</sub> Injected (min)	28	45	60
Injected S (g)	1.35	2.18	2.92
Cumulative Engine S (hrs)	52.8	64.9	98.0
Cumulative Engine S (g)	1.71	2.10	3.18
Running Total S (g)	3.06	5.63	9.63
Equivalent miles	2888	5319	9087



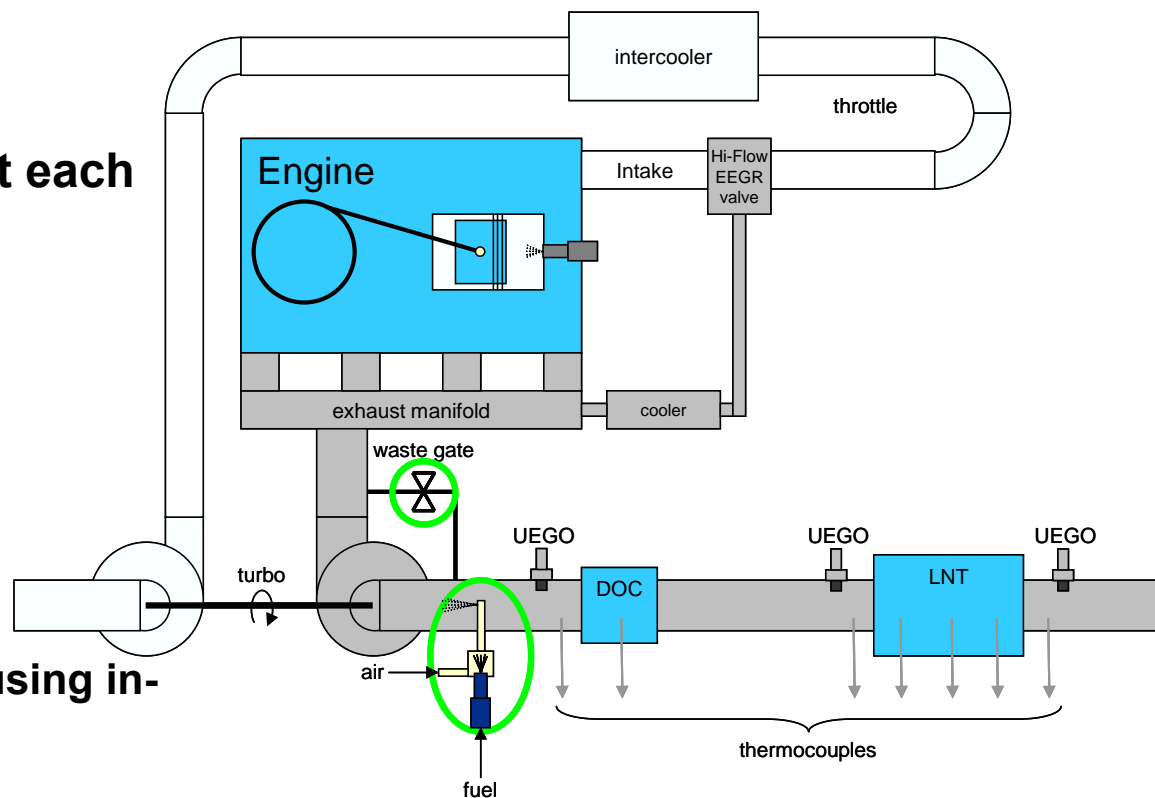
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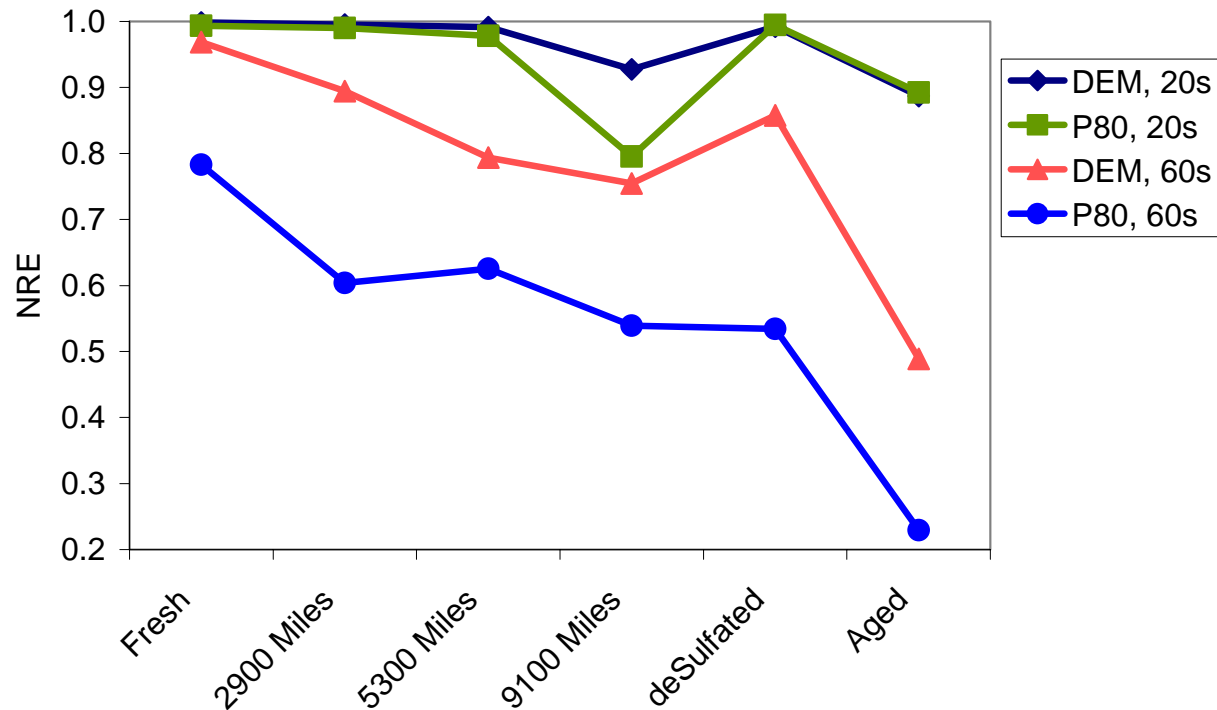
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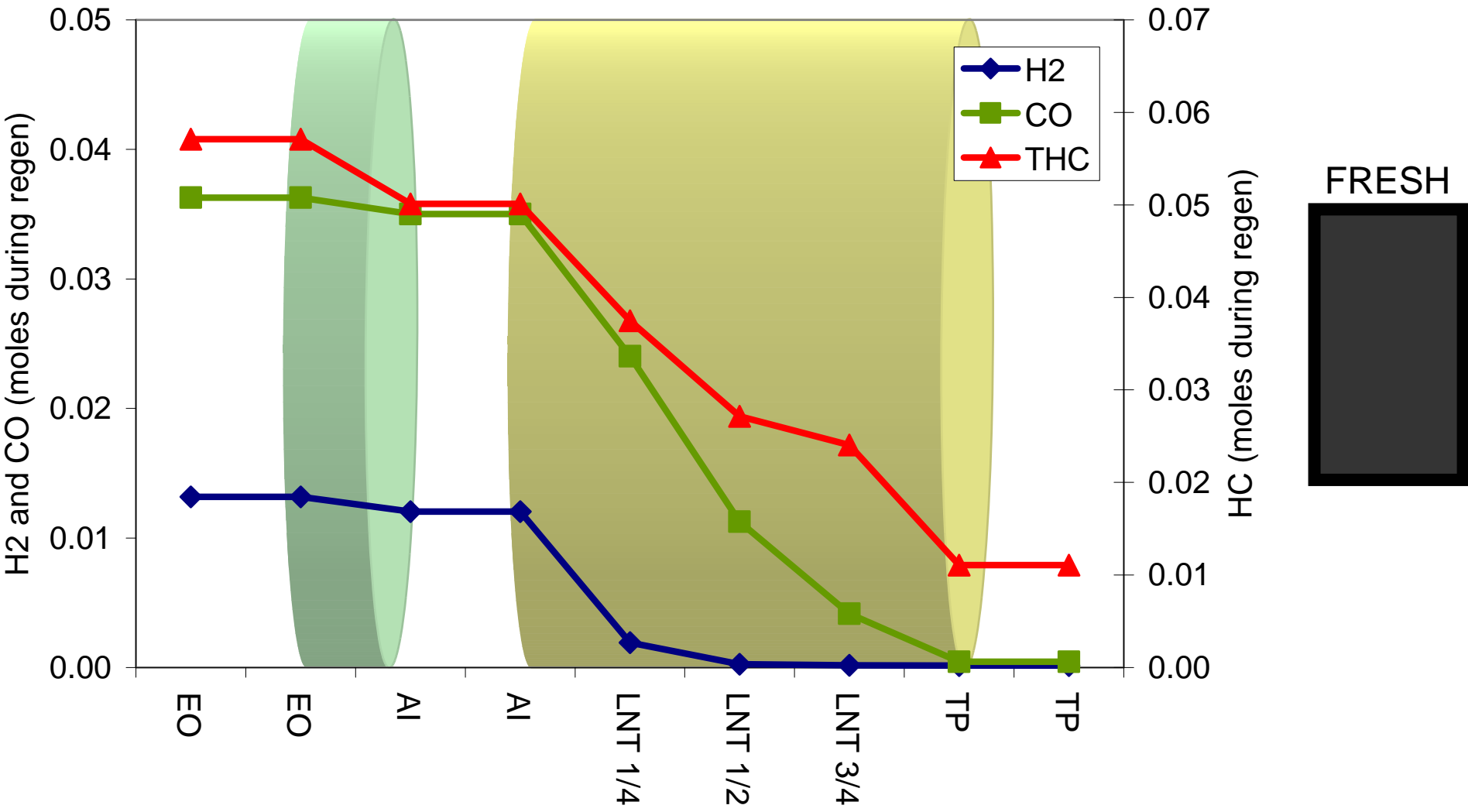


# S/deS Effect on Strategy Performance

- **P80 strategies (Higher in HCs, Lower H<sub>2</sub>/CO) appear to degrade more with S/deS; Why???**

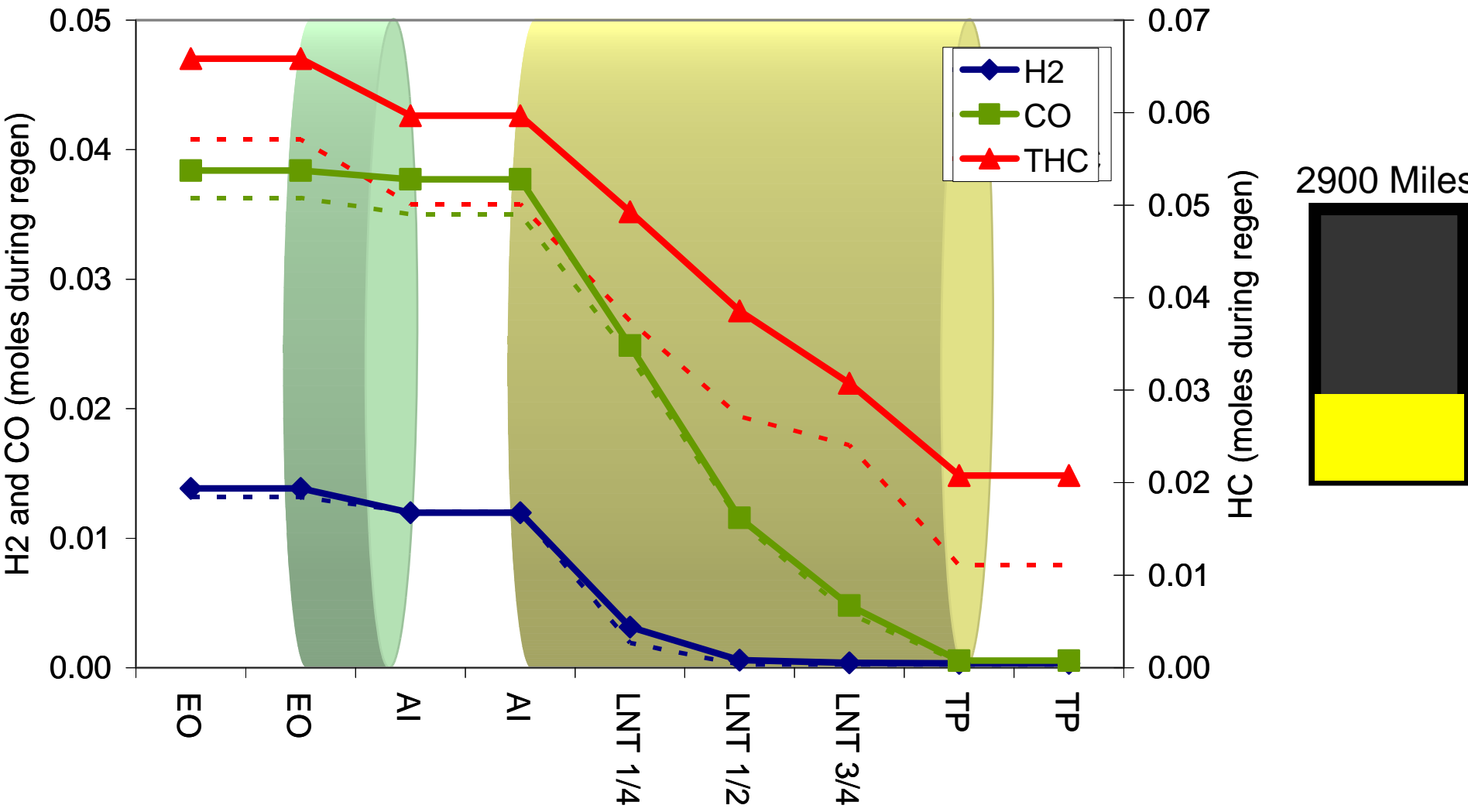


# Small downstream shift in reductant utilization with S exposure



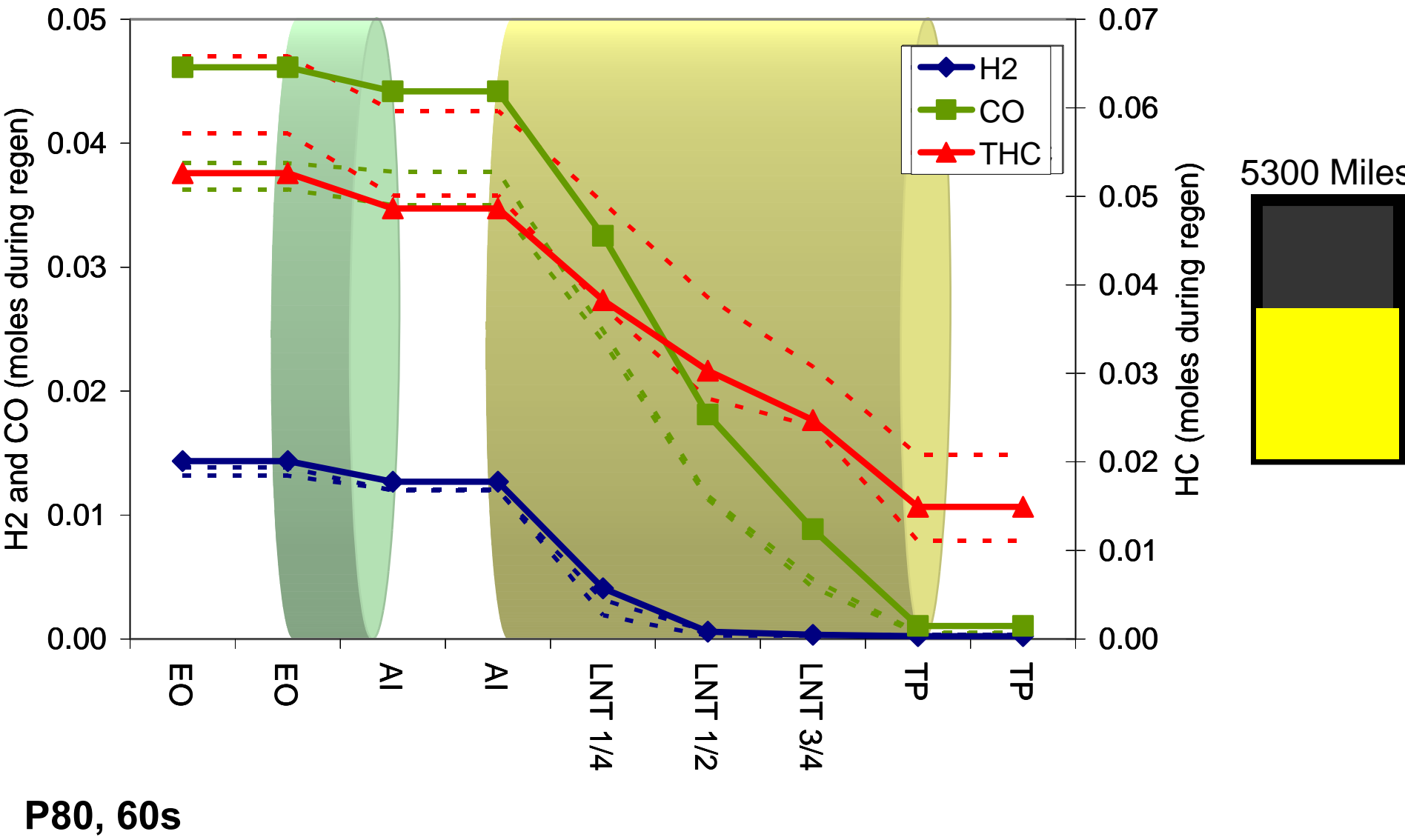
P80, 60s

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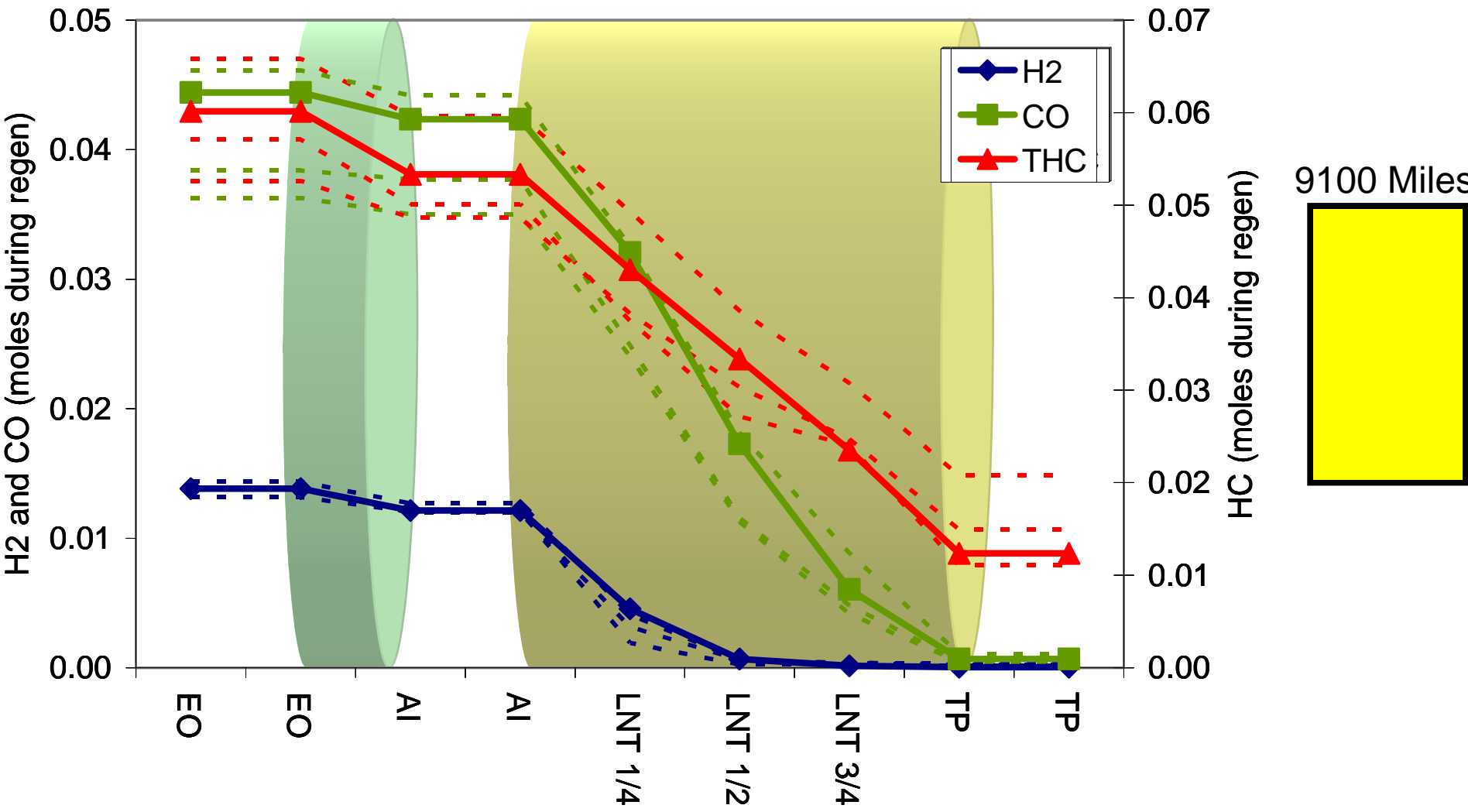


P80, 60s

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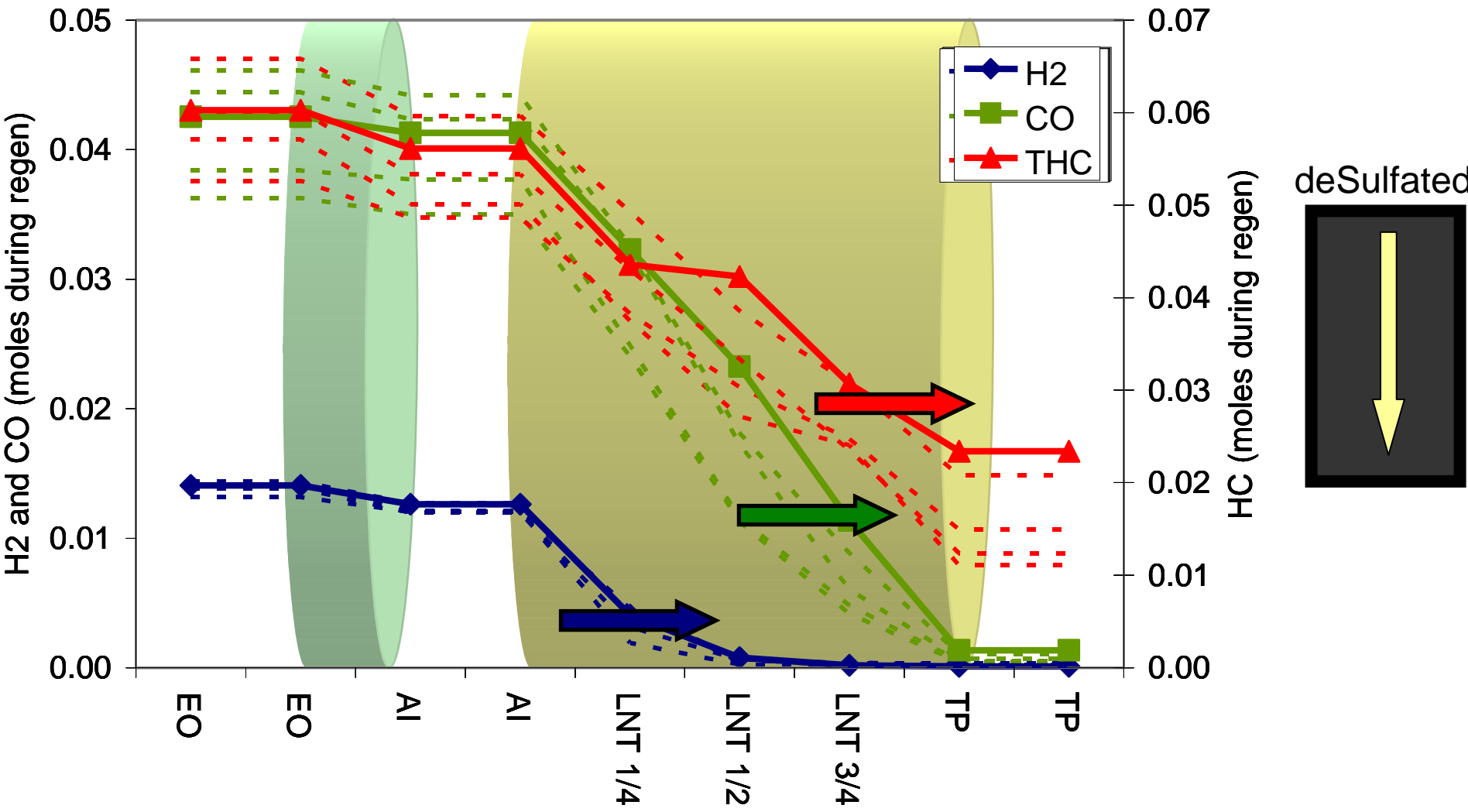


# Small downstream shift in reductant utilization with S exposure



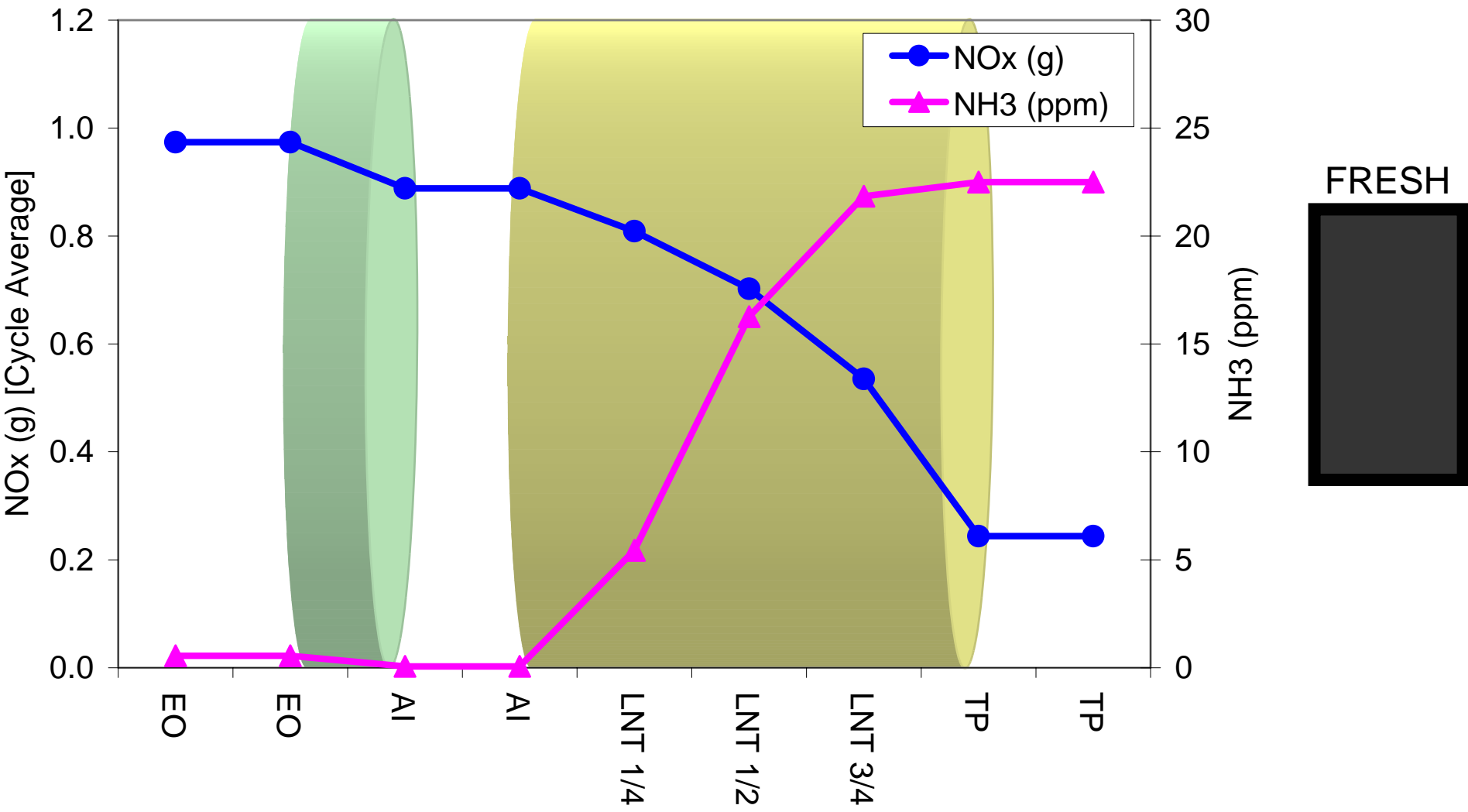
P80, 60s

# Small downstream shift in reductant utilization with S exposure



P80, 60s

# Significant changes observed in N<sub>2</sub> selectivity with S/deS

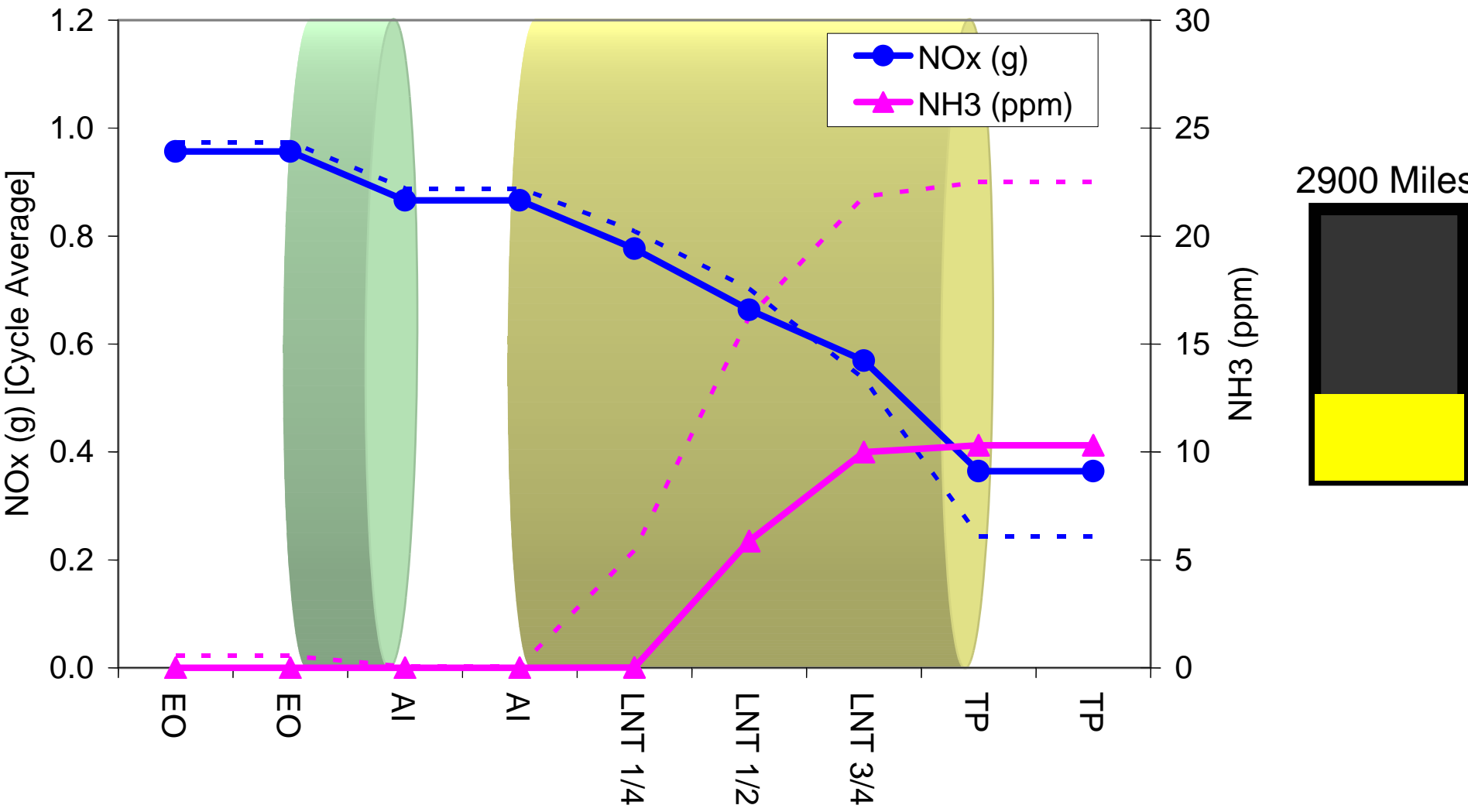


**P80, 60s**

Note: NH<sub>3</sub> and NOx not in same units. EO NOx ~ 500ppm



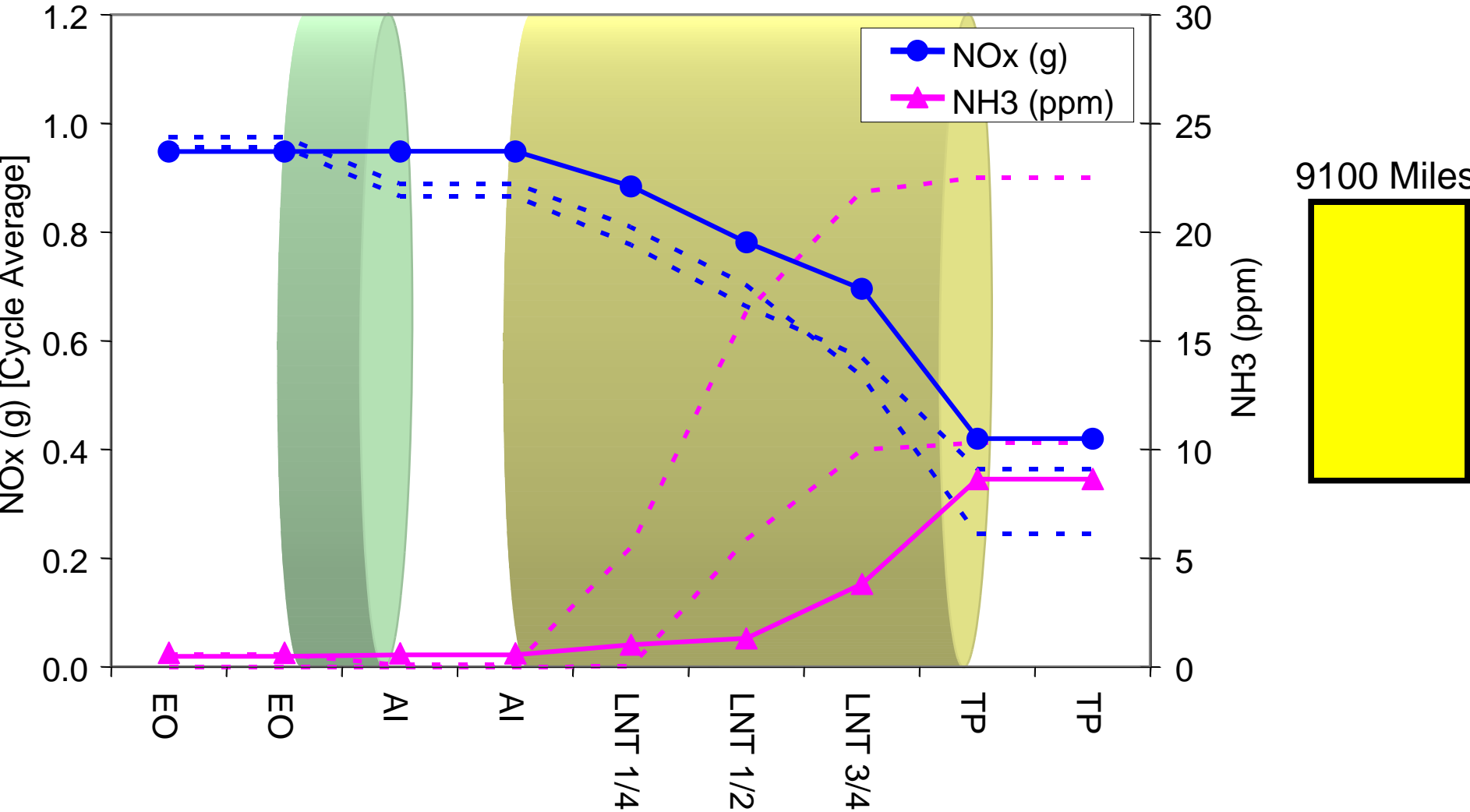
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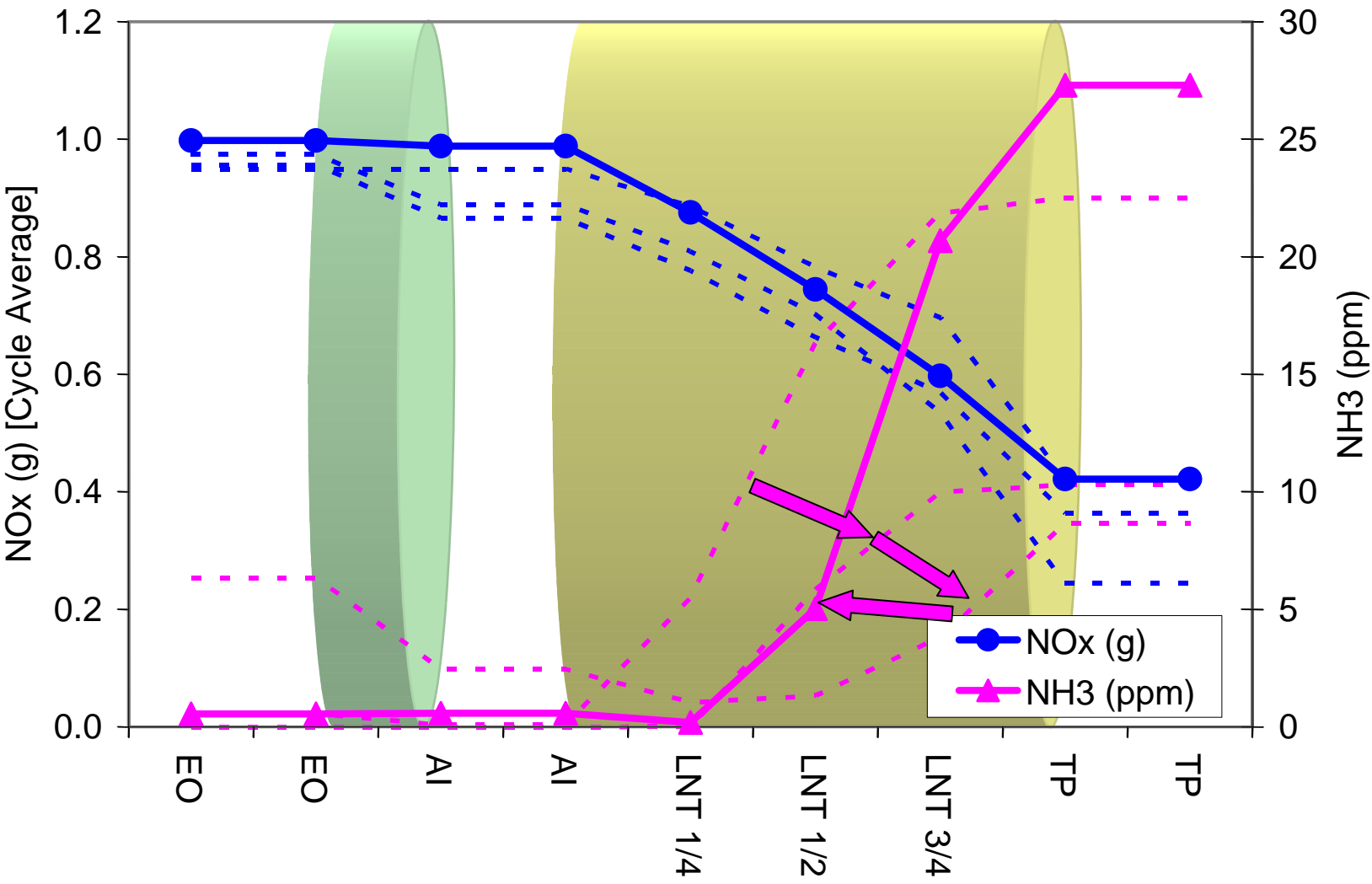
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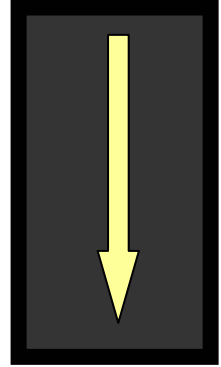
**P80, 60s**

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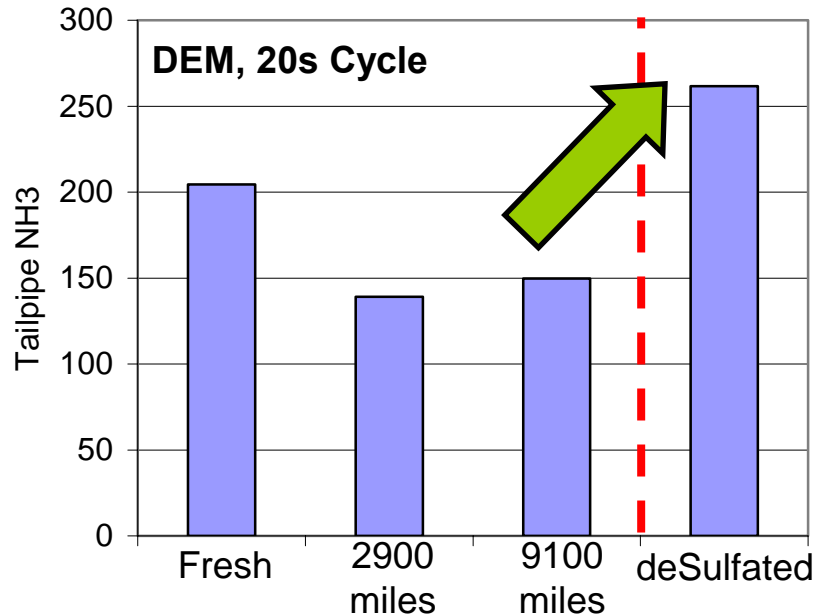
deSulfated



P80, 60s

Note: NH<sub>3</sub> and NOx not in same units. EO NOx ~ 500ppm

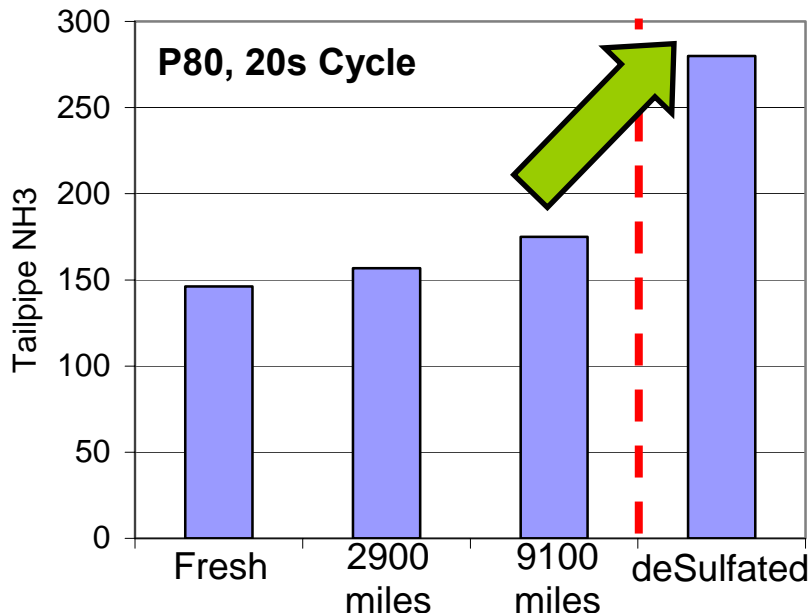
# NH<sub>3</sub> formation increases after deSulfation



- NH<sub>3</sub> formation after deSulfation was higher for all cases

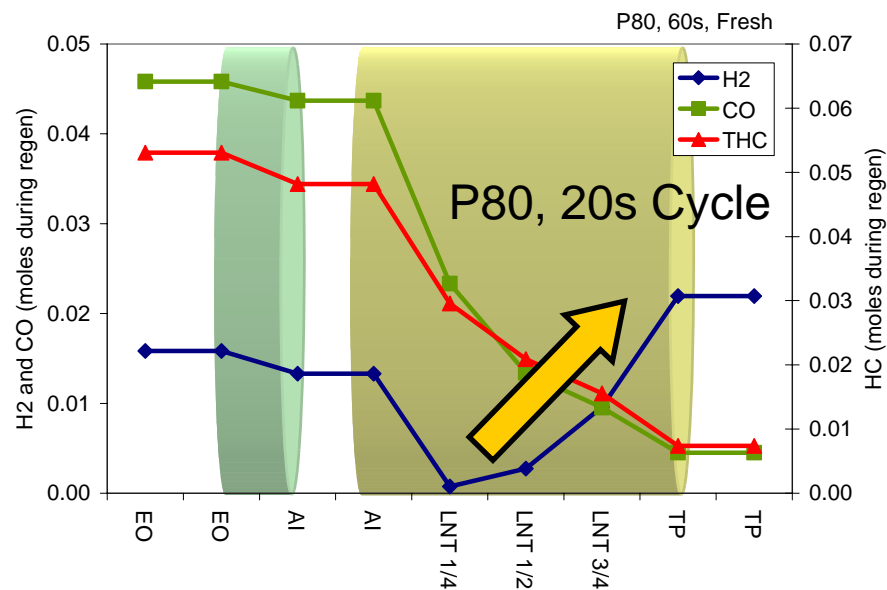
## Potential causes:

- Sintering of Sorbate
  - suspect thermal sintering of sorbate may be the cause of higher NH<sub>3</sub>
  - Castoldi et. al. Report NH<sub>3</sub> formation corresponds with higher sorbate loading (bulk crystallites)
    - L. Castoldi, I. Nova, L. Lietti, P. Forzatti, "Catalysis Today" 96 (2004), pp. 43-52
- Change in Reductant:NOx ratio
  - CLEERS, Pihl, and other work on N<sub>2</sub> selectivity show NH<sub>3</sub> increases with increasing Reductant:NOx ratio
    - Pihl, et.al. SAE 2006-01-3441

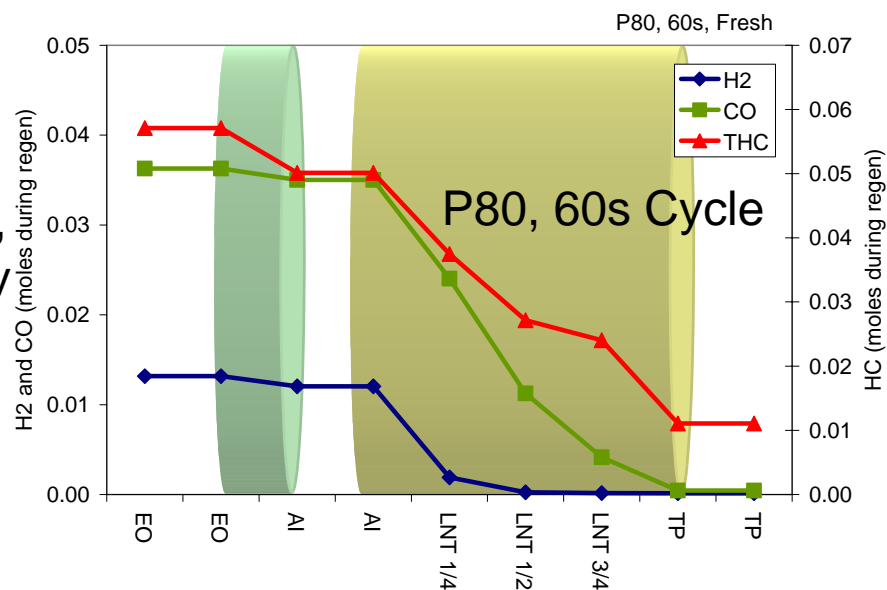


# H<sub>2</sub> Produced In Catalyst During 20s Cycles

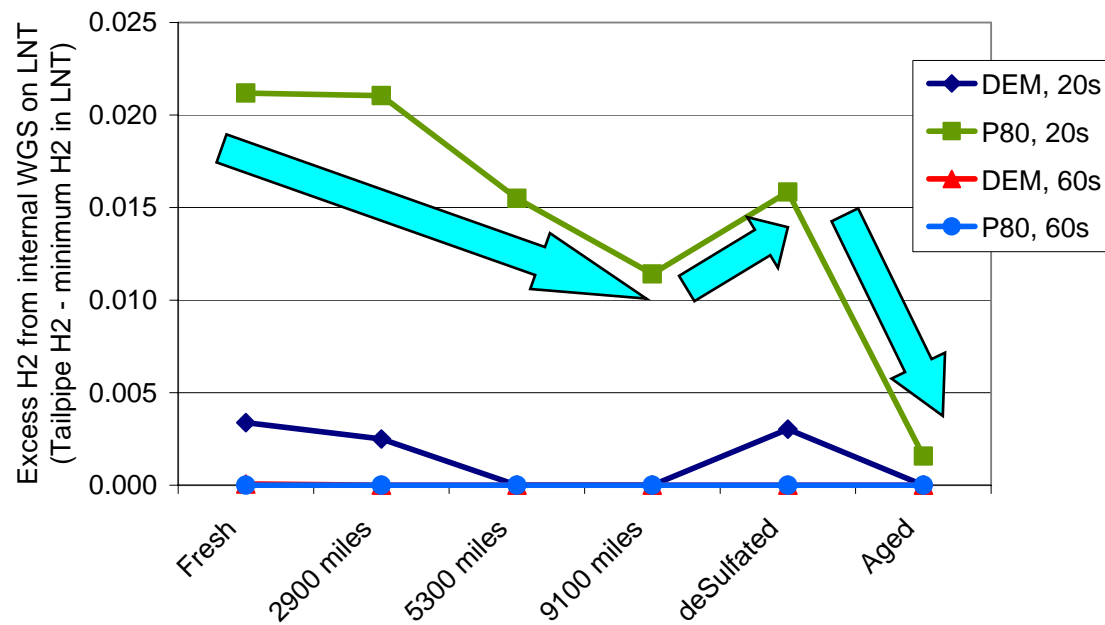
- In 20s cycles, H<sub>2</sub> observed being created in catalyst most likely from reforming reactions (water-gas shift, etc.)



- Same process may occur in 60s data, but H<sub>2</sub> may be consumed immediately for NO<sub>x</sub> reduction



# Catalytic H<sub>2</sub> production: Effect of S/deS



- Increase in catalytic-produced H<sub>2</sub> greater for P80 strategy
- H<sub>2</sub> production degrades with S/deS aging
- LNT performance may degrade more rapidly for strategies that depend on catalyst utilizing HCs from engine

# Summary

- **In general, reductant utilization in LNT moved downstream only slightly with S/deS**
  - Process is consistent; optimism for modeling
- **NH<sub>3</sub> formation increased after deSulfation process**
  - Regeneration control strategies must adjust accordingly with age
- **Strategies with high HC and low H<sub>2</sub>/CO (P80) may depend on catalytic H<sub>2</sub>/CO production for regeneration**
  - S/deS degradation of catalytic H<sub>2</sub>/CO production may have greater degradation impact on the effectiveness of P80-like strategies
- **Preparing Paper for SAE Fall Powertrain and Fluids Conference**