

Combination & Integration of DPF-SCR Aftertreatment

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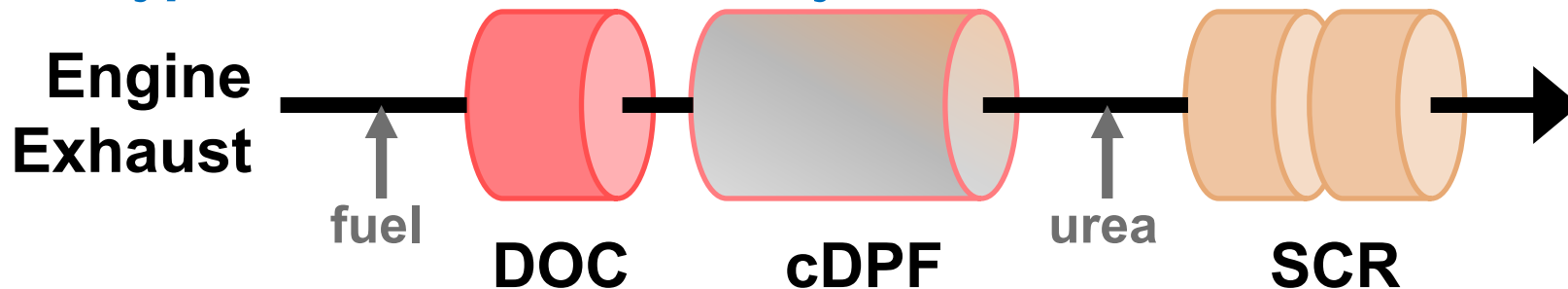
BASF:

Patrick Burk

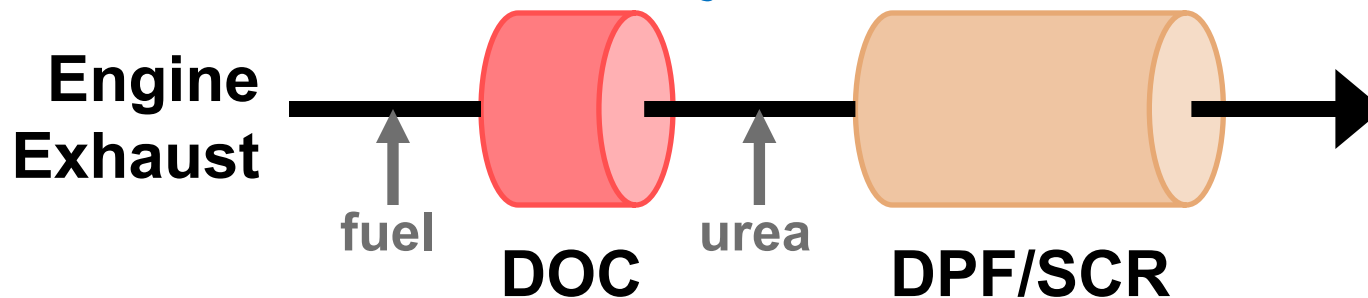
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Integrating DPF & SCR functionalities for reducing cost and volume of engine after-treatment

Typical HDD EPA 2010 Layout



Possible Future HDD Layout



OBJECTIVE: Fundamentally understand the integration of SCR & DPF technologies for HDD to provide a pathway to the next generation of emissions control systems

- CRADA with PACCAR, working closely with DAF Trucks

▶ *Highly* evolving field of work (mostly LDD, some HDD); this effort focused on:

1. Optimizing SCR catalyst wash coat
2. Facilitating passive soot oxidation

▶ BASF (HD Systems Development)

- Providing SCR catalyst (Cu/Z) expertise
- Washcoating, manufacturability

▶ Corning

- Developmental UHP cordierite

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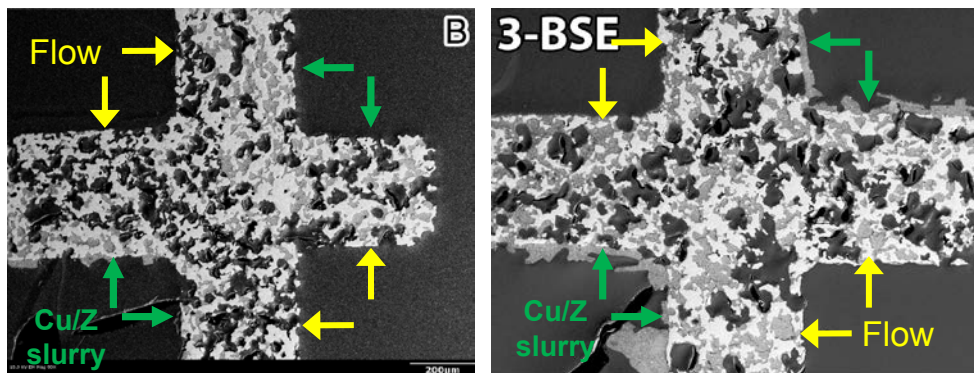
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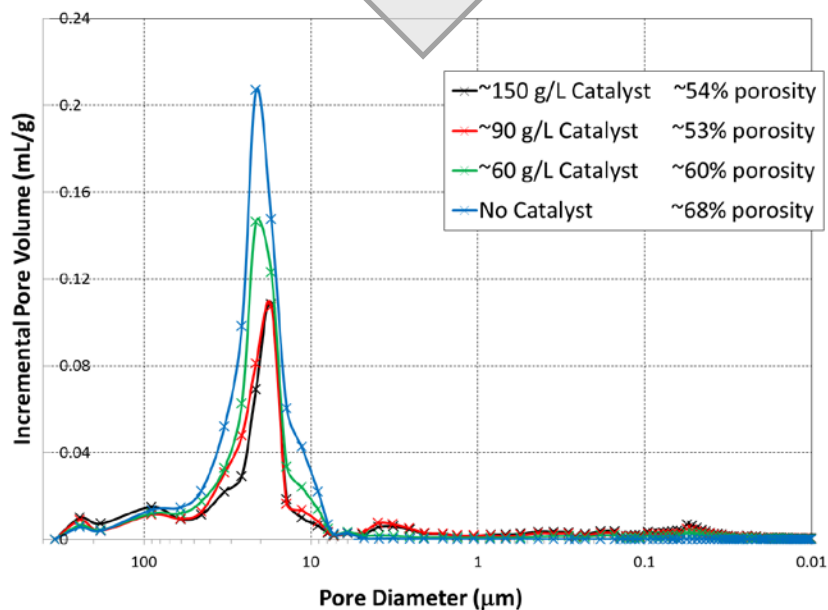
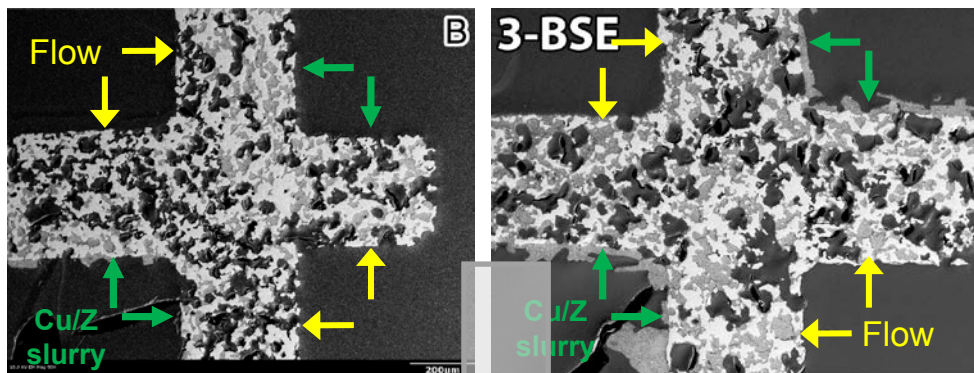
OPTIMIZING SCRF WASHCOAT

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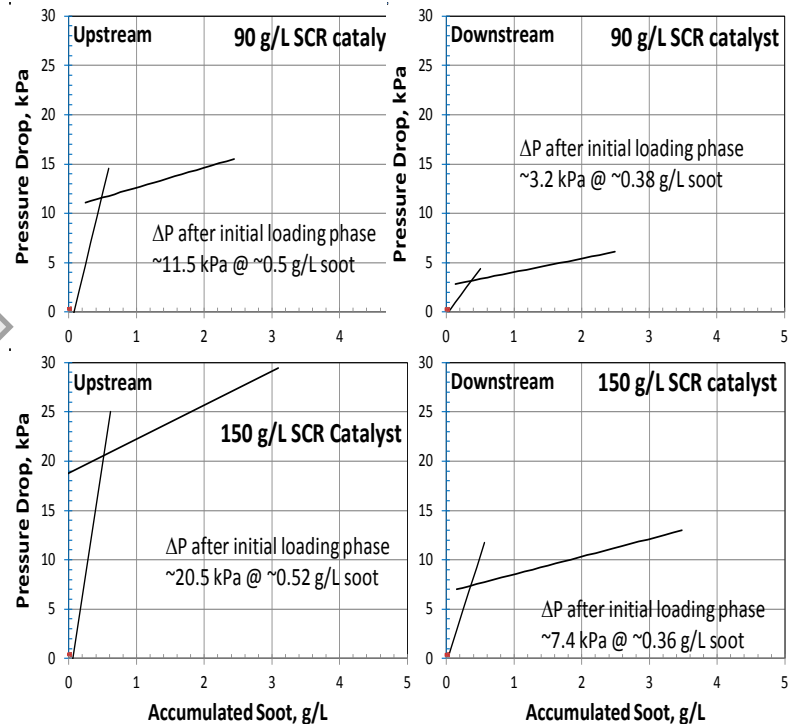
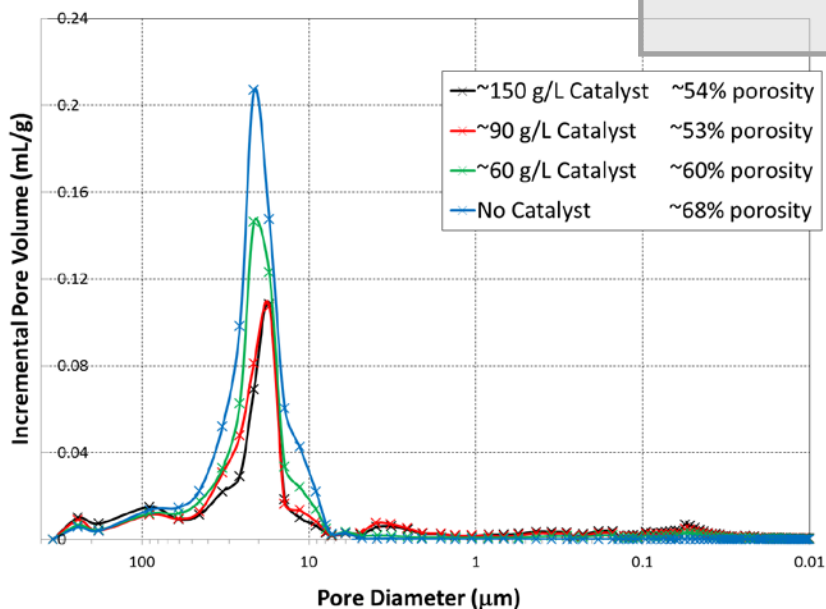
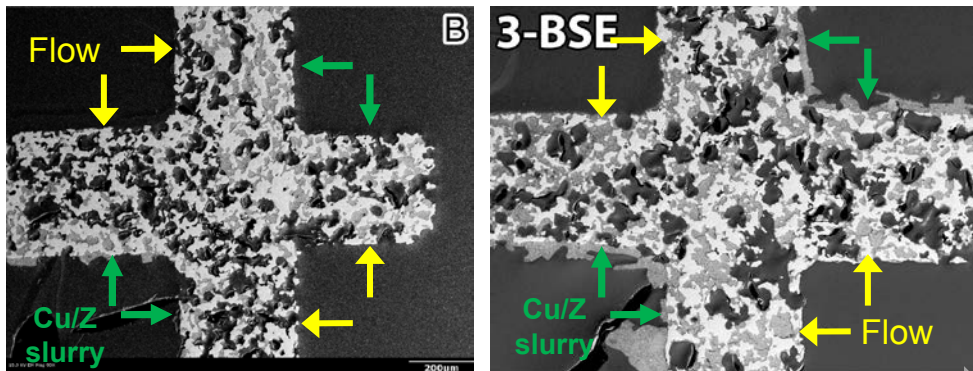
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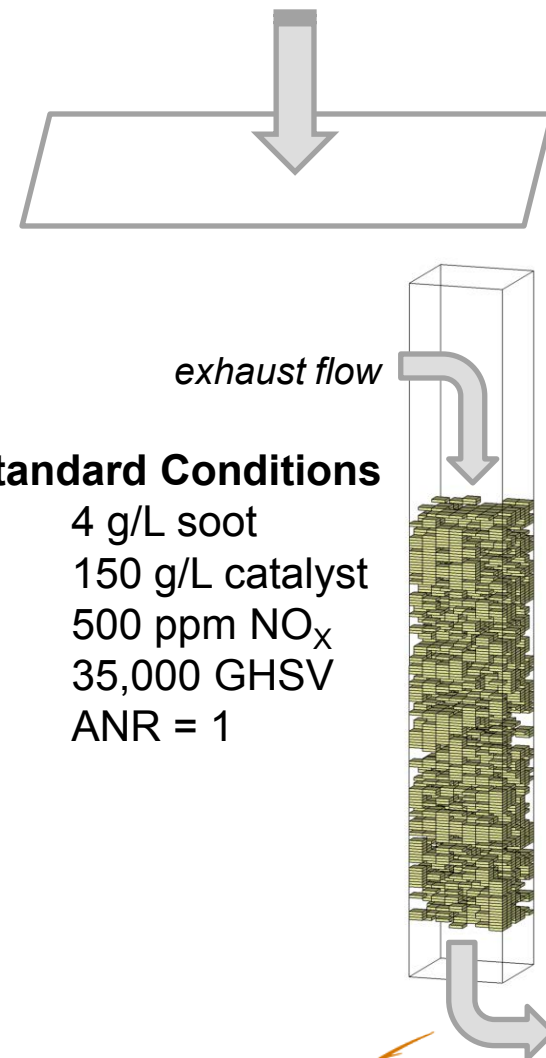
- ▶ Reaction competition
 - Passive soot oxidation vs. Selective catalytic reduction (SCR)

- ▶ Passive soot oxidation – NO₂ driven
 - The presence of SCR reaction(s) in a wall-flow filter **WILL** have a detrimental effect on passive soot oxidation
 - SCRF integration will NOT have oxidation component on filter, thus no NO₂ ‘recycle’ component present
 - Reaction competition: passive soot oxidation vs. SCR

- ▶ GOAL: maximize the passive soot oxidation feasibility of an SCRF
 - Minimize adverse effect of SCR on passive soot oxidation process
 - No additional downstream SCR
 - cannot sacrifice acceptable de-NO_x performance

▶ **MODELING WALL-SCALE SCRF**

- ▶ Single flat wall; exhaust flow in the normal direction
- ▶ Channel scale transport effects, axial variations are ignored
- ▶ Simplified SCR reaction network developed at PNNL
- ▶ Simplified porous media with similar porosity and tortuosity of the SCRF used in experiments
- ▶ 90 g/L of catalyst distributed evenly throughout the porous wall + 60 g/L placed on down-stream wall surface
- ▶ Lattice-Boltzmann model used to solve gas flow field
- ▶ Soot oxidation kinetic model by Messerer et al, 2006
- ▶ Soot present as cake layer on top of wall; assumed 50% oxidized soot
- ▶ *Conclusions dependent upon validity of assumptions and kinetics used*



▶ Simplified SCR kinetics model

Developed under CLEERS in cooperation with ORNL using bench-scale experiments with a current commercial cu-CHA catalyst

- **NH₃ oxidation** $2\text{NH}_3 + 3/2\text{O}_2 \rightarrow \text{N}_2 + 3\text{H}_2\text{O}$
- **Standard SCR** $4\text{NH}_3 + 4\text{NO} + \text{O}_2 \rightarrow 4\text{N}_2 + 6\text{H}_2\text{O}$
- **Fast SCR** $4\text{NH}_3 + 2\text{NO} + 2\text{NO}_2 \rightarrow 4\text{N}_2 + 6\text{H}_2\text{O}$

▶ Parametric matrix

- 250°C, 300°C, 350°C, 400°C, 450°C
- $\text{NO}_2/\text{NO}_x = 0.33, 0.50, 0.67$; $\text{NH}_3/\text{NO}_x = 1.0, 0.85$
- DPF versus SCRF

▶ Diffusivity adjusted for temperature (Massman, 1998)

► Example species fields – 350°C

NH₃ dosing ON

NH₃ dosing OFF

NO₂ [ppm]

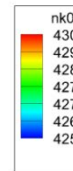
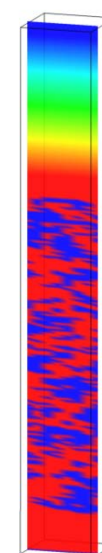
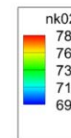
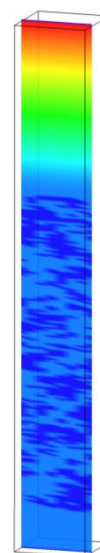
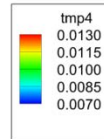
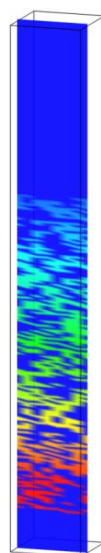
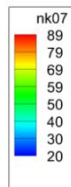
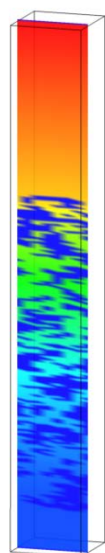
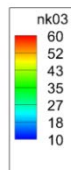
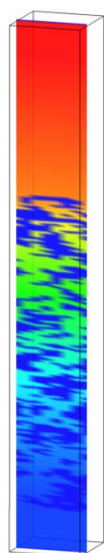
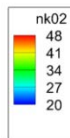
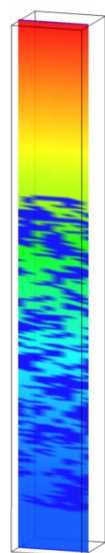
NO [ppm]

NH₃ [ppm]

NH₃ surface coverage

NO₂ [ppm]

NO [ppm]

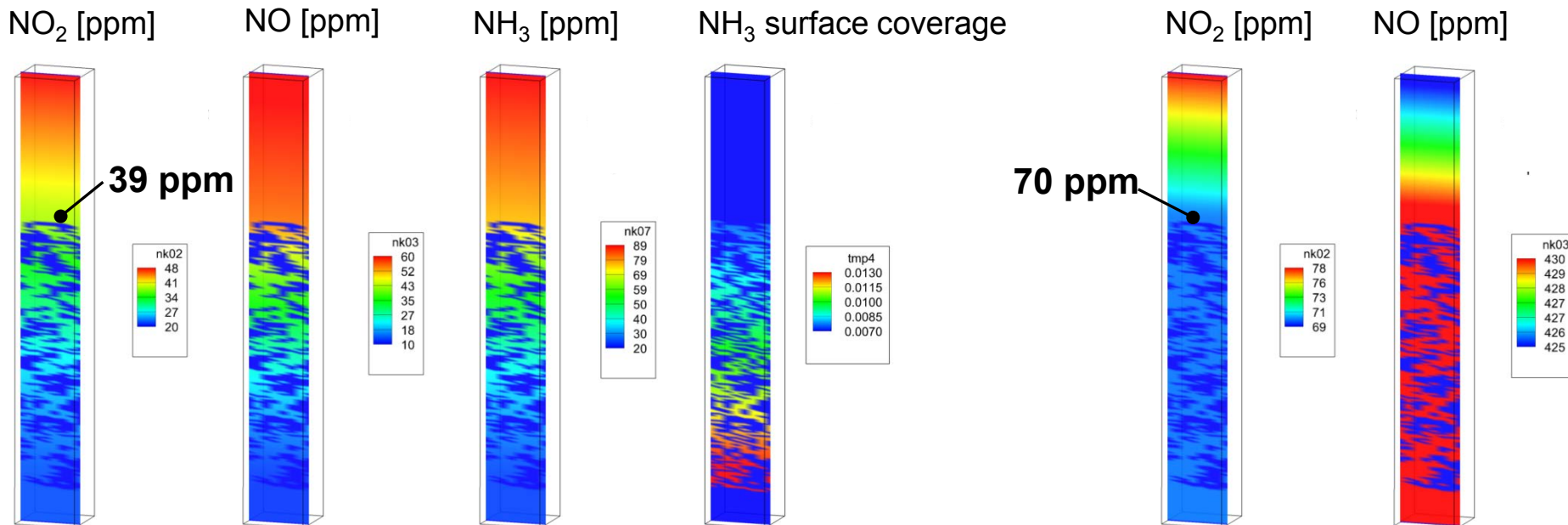


► In all SCRF cases: SCR catalyst creates gradients in active species concentrations and NH₃ surface coverage across the wall thickness

▶ Example species fields – 350°C

NH₃ dosing ON

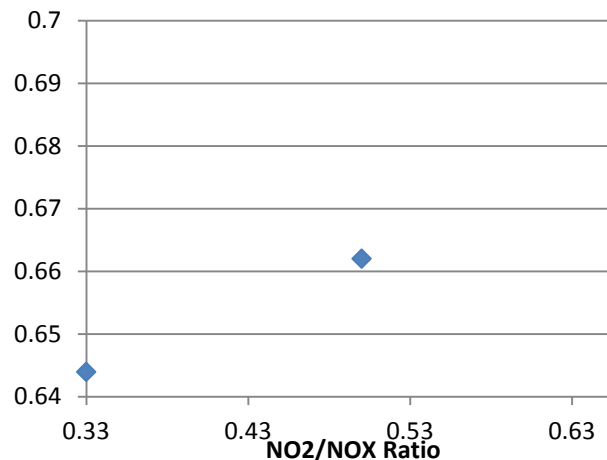
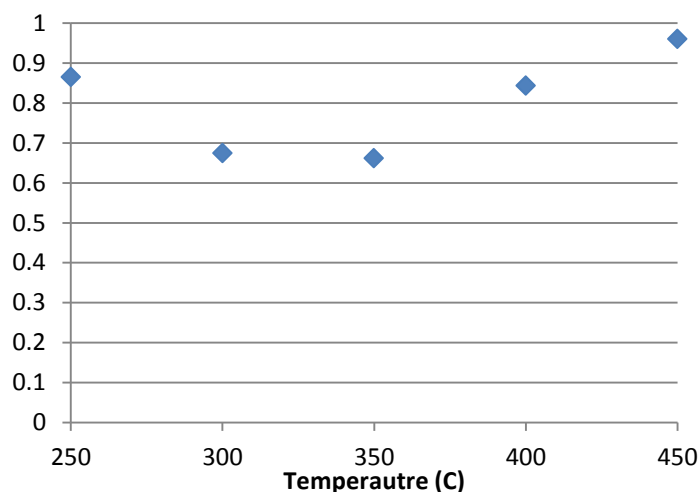
NH₃ dosing OFF



- ▶ Gradients in active species concentrations facilitate diffusion effects that are significant and effect concentrations upstream
- ▶ Of particular interest: NO₂

▶ Passive soot oxidation (ANR = 1)

Ratio of soot oxidation rates [w/NH₃ dosing / w/o NH₃ dosing]



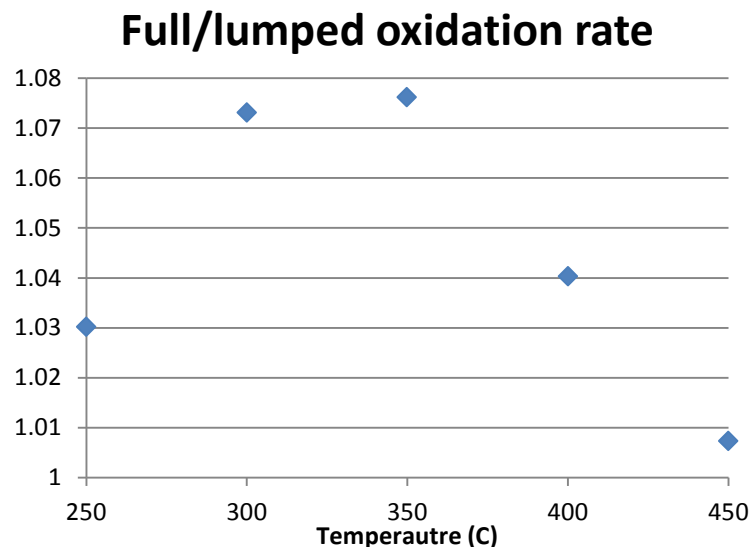
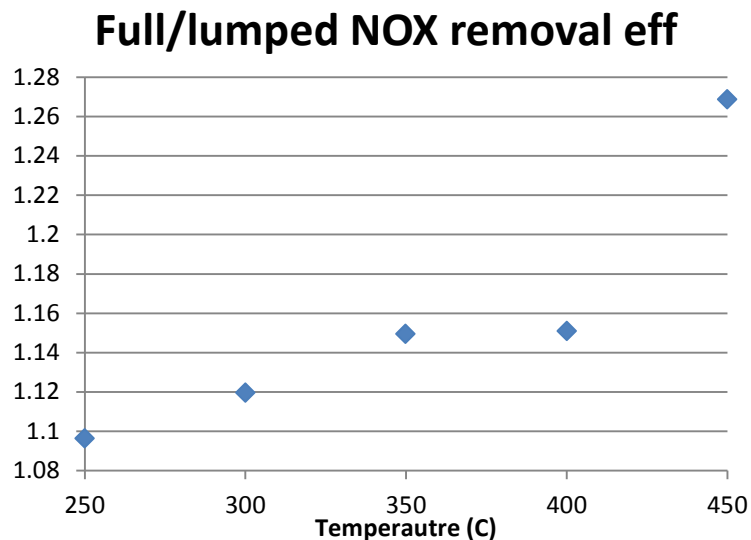
- ▶ Impact of SCR on soot oxidation is temperature dependent
 - SCR reactions decrease oxidation rate by about 35% at intermediate temperatures, but only 4% at higher temperatures
- ▶ Increased NO₂ fraction decreases inhibiting effect of SCR

- ▶ Full simulation (as described in initial model description)
 - Simplified porous media with similar porosity and tortuosity of the SCRF used in experiments
 - 90 g/L of catalyst distributed evenly throughout the porous wall + 60 g/L placed on down-stream wall surface
 - Soot present as cake layer on inlet channel surface of porous media

- ▶ Lumped simulation
 - Soot & SCR catalyst co-located
 - No porous media
 - Provides initial guesses for SS concentrations and NH_3 coverage

- ▶ Comparison provides a means of evaluating effect of spatial separation within wall-flow filter
 - Soot oxidation and SCR reaction components the same
 - Bulk-flow (i.e. convective) component the same
 - Allows evaluation of effect of concentration gradient(s) and resulting conductive transport (i.e. diffusive) effects

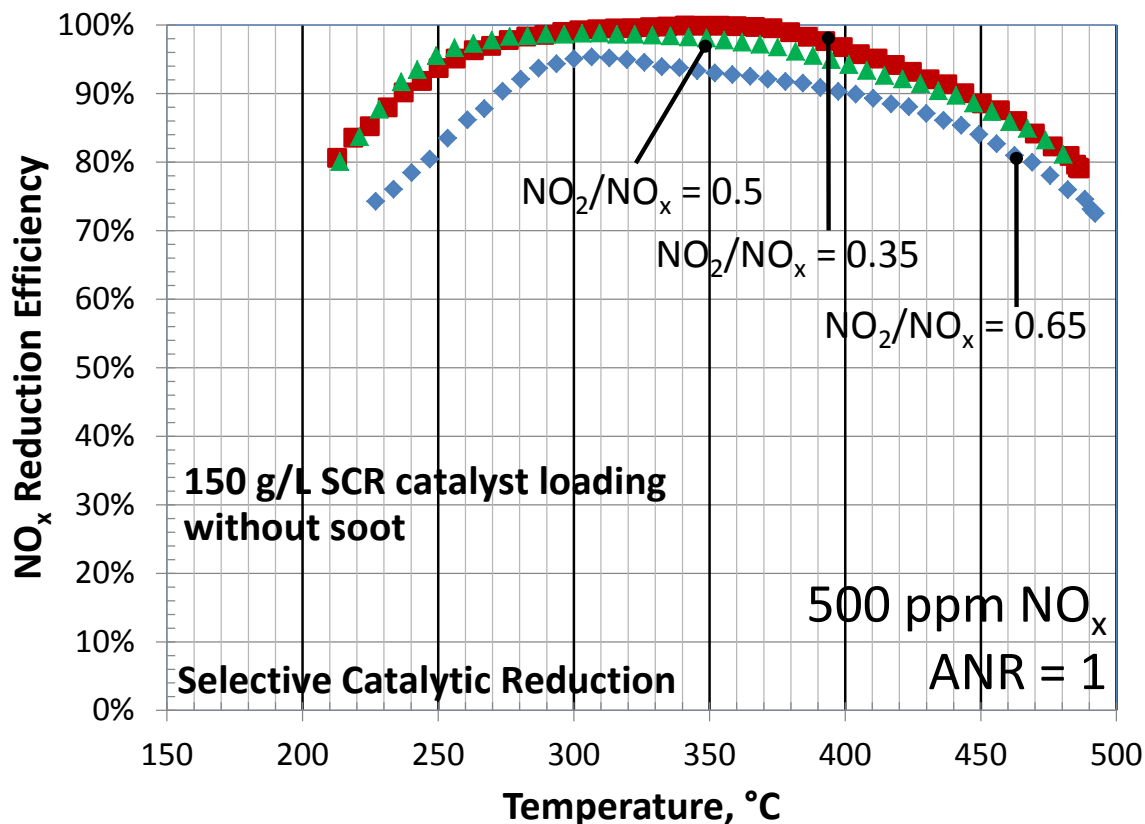
► Spatial separation within wall-flow filter



- Spacial separation (of SCR from soot) results in a small benefit for soot oxidation and NRE
 - Benefit for soot oxidation smaller
- Effect is small: kinetics of competing reactions and resulting conductive transport effects dominant for all cases

▶ BENCH-SCALE REACTION STUDIES

► Effect of NO₂ fraction on NRE

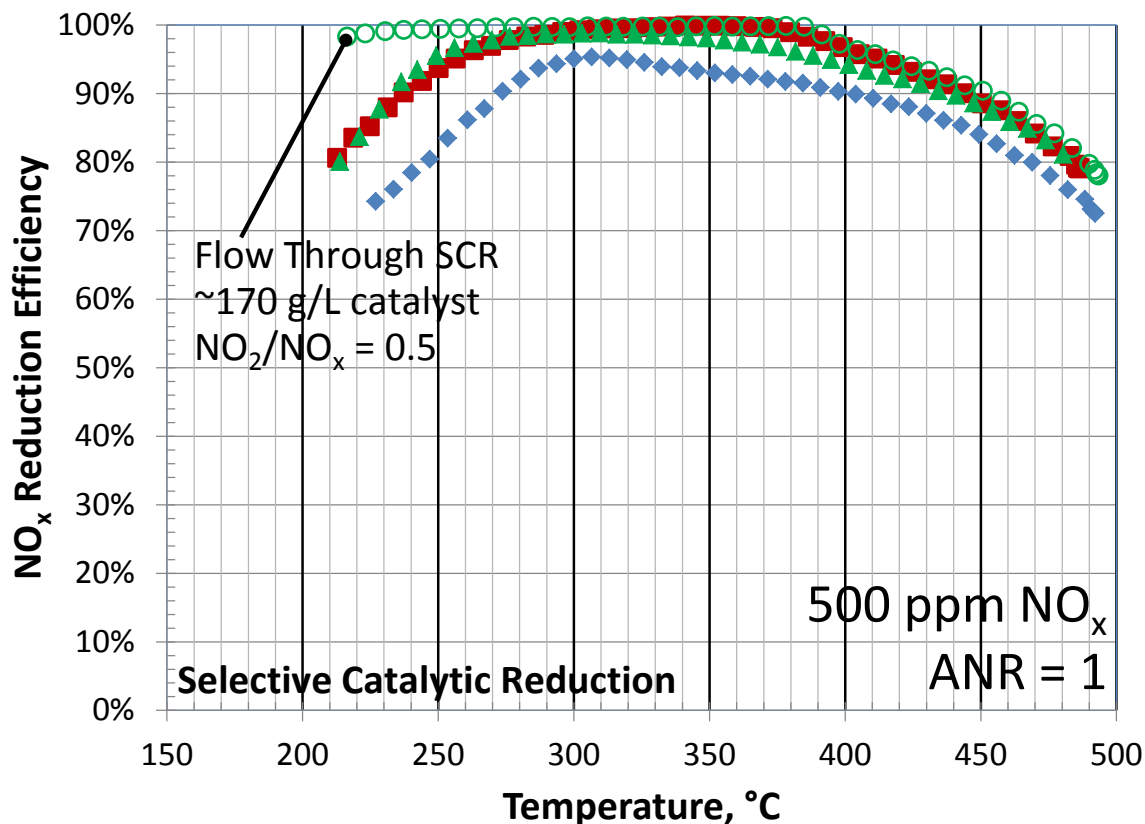


SCR performance:

Minimally affected
at NO₂ /NO_x < 0.5

Detrimental effect
at NO₂ /NO_x > 0.5

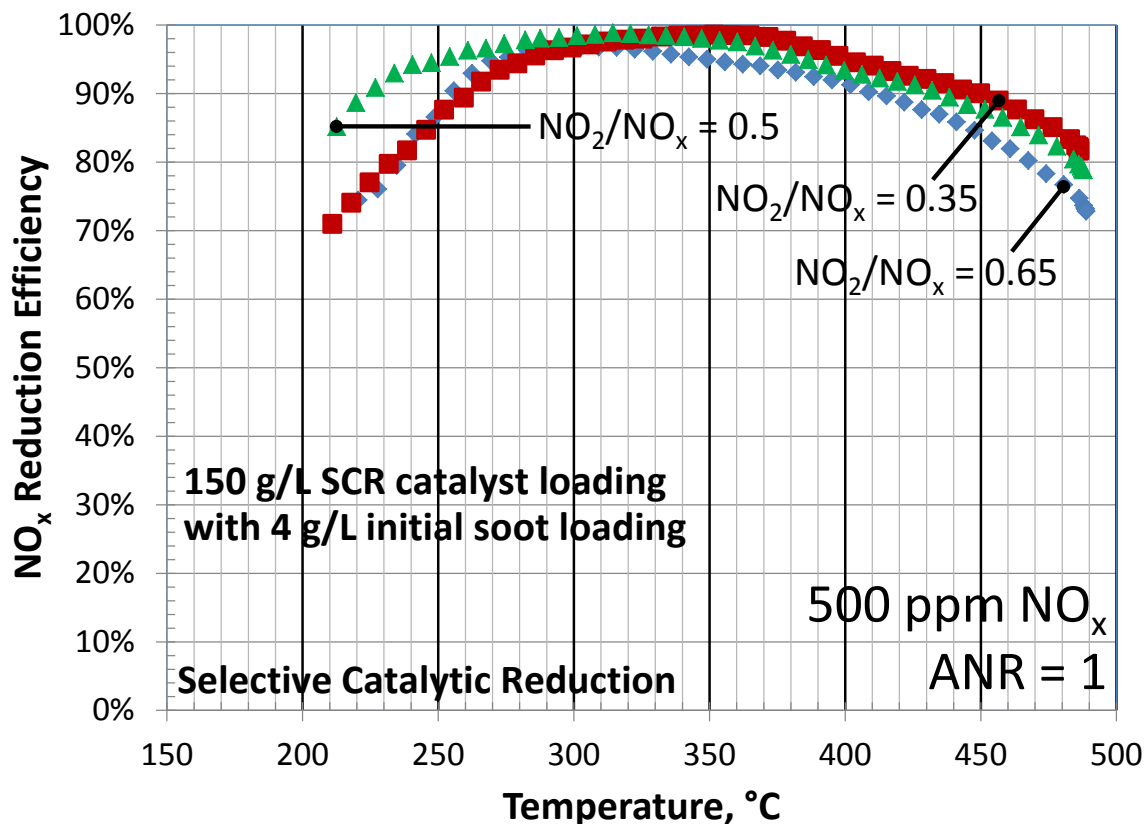
► Effect of NO₂ fraction on NRE



Detrimental effect of wall flow versus flow through

Especially at temp < ~275°C

► Effect of NO₂ fraction on NRE



SCR performance not significantly affected by soot

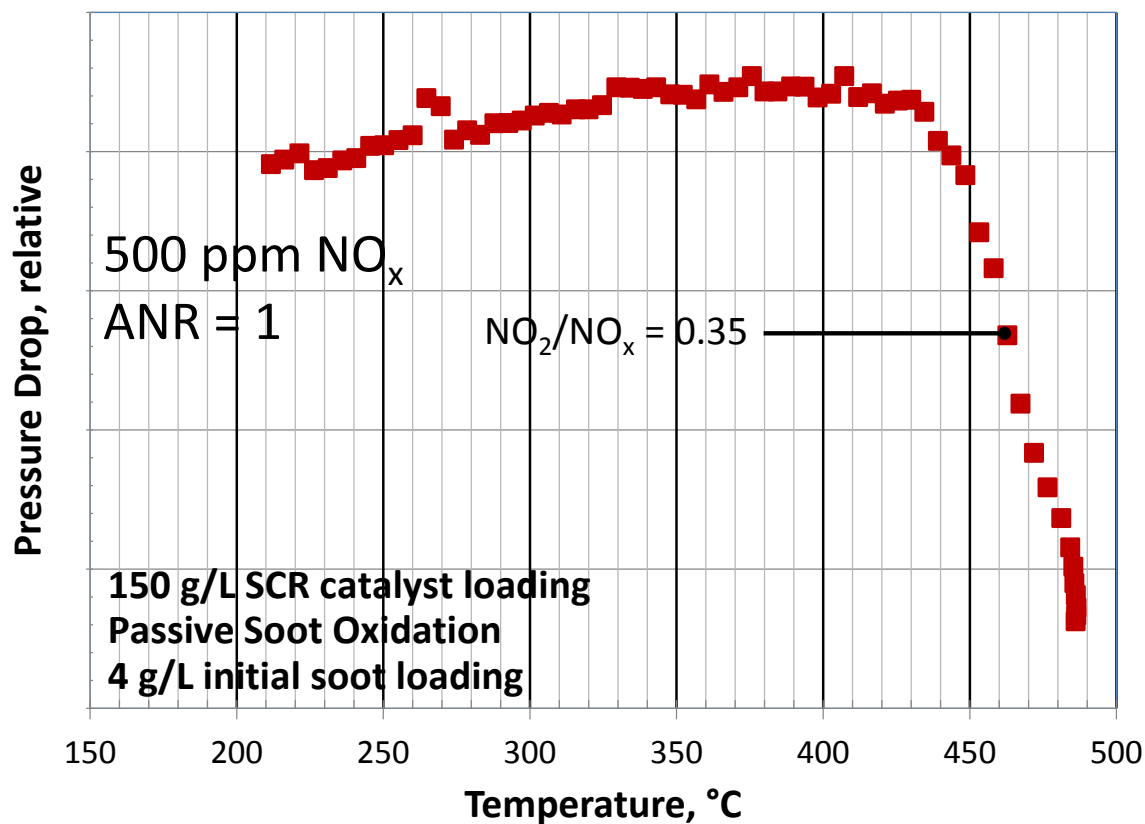
NO₂ /NO_x > 0.5 improved

Contribution of passive soot oxidation

PASSIVE SOOT OXIDATION

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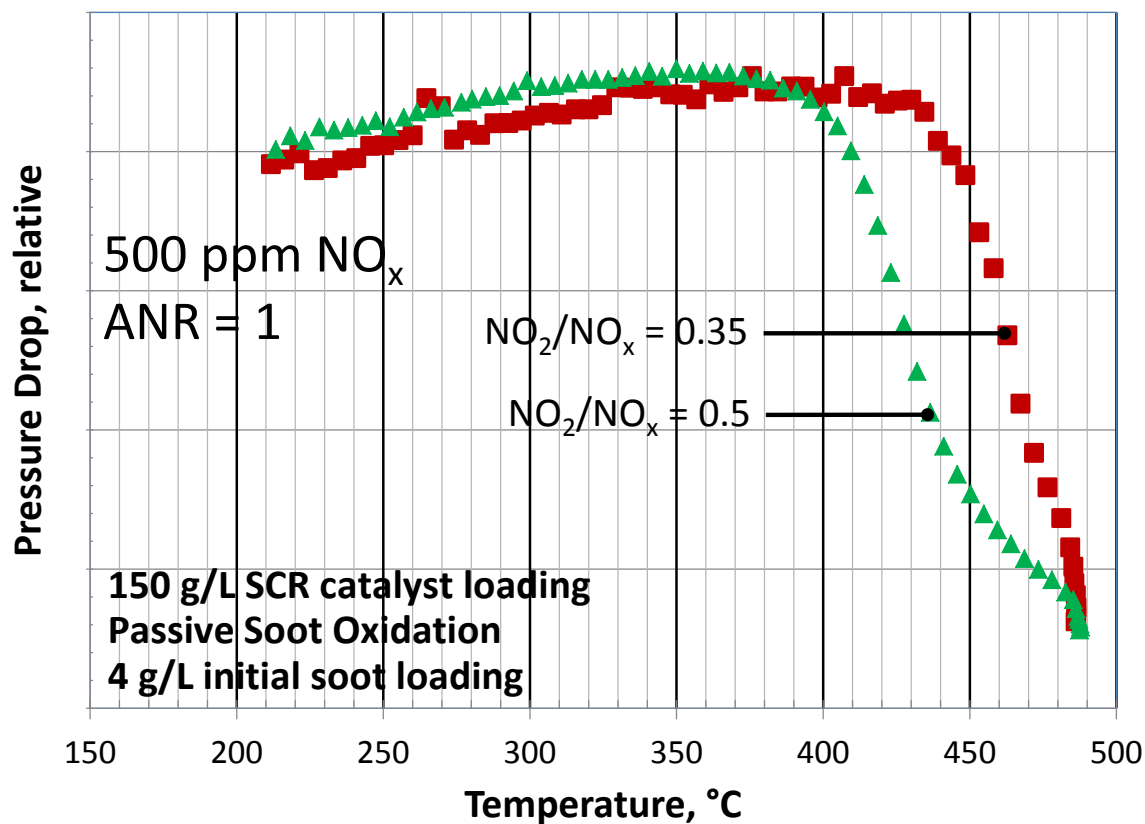
- ▶ Effect of NO_2 fraction on soot oxidation rate



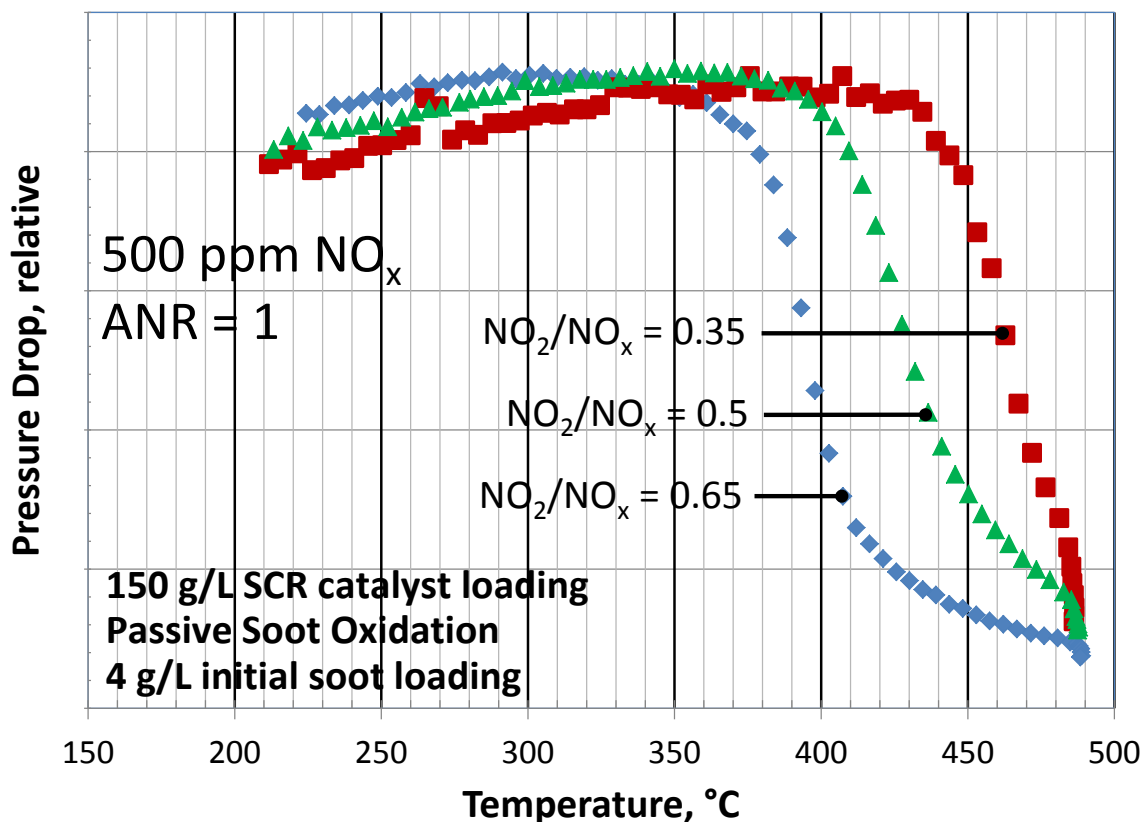
PASSIVE SOOT OXIDATION

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- ▶ Effect of NO_2 fraction on soot oxidation rate



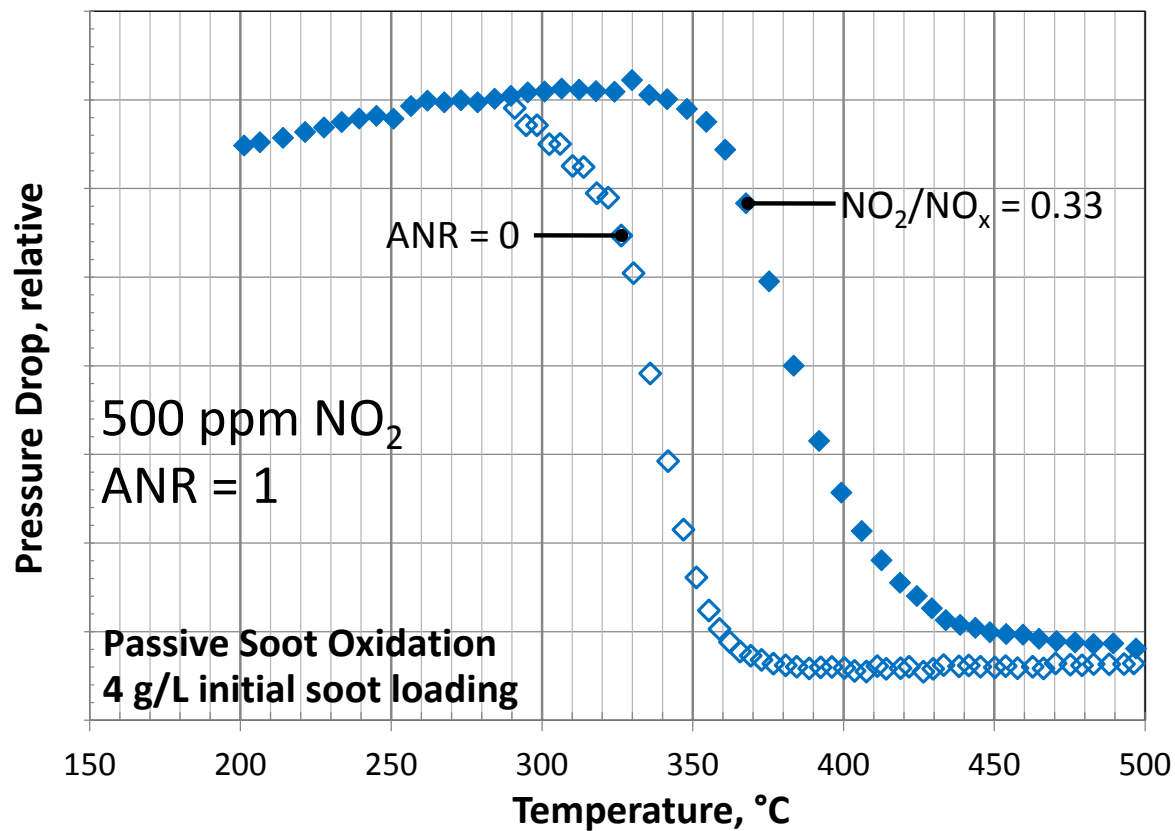
- ▶ Constant NO_x : effect of NO_2 fraction on soot oxidation rate



Increased NO_2 facilitates increased soot oxidation

Combined effect of more NO_2 and increased NO_2 fraction

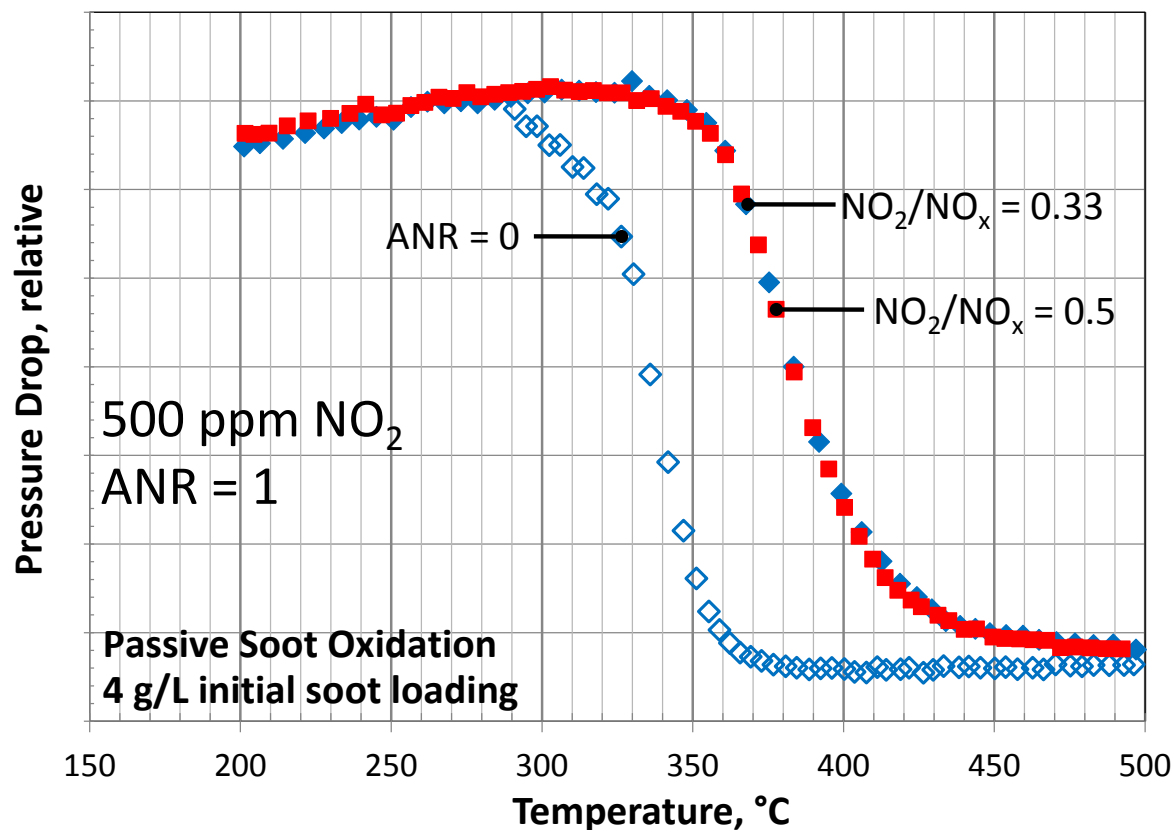
► Separating NO₂ fraction



PASSIVE SOOT OXIDATION

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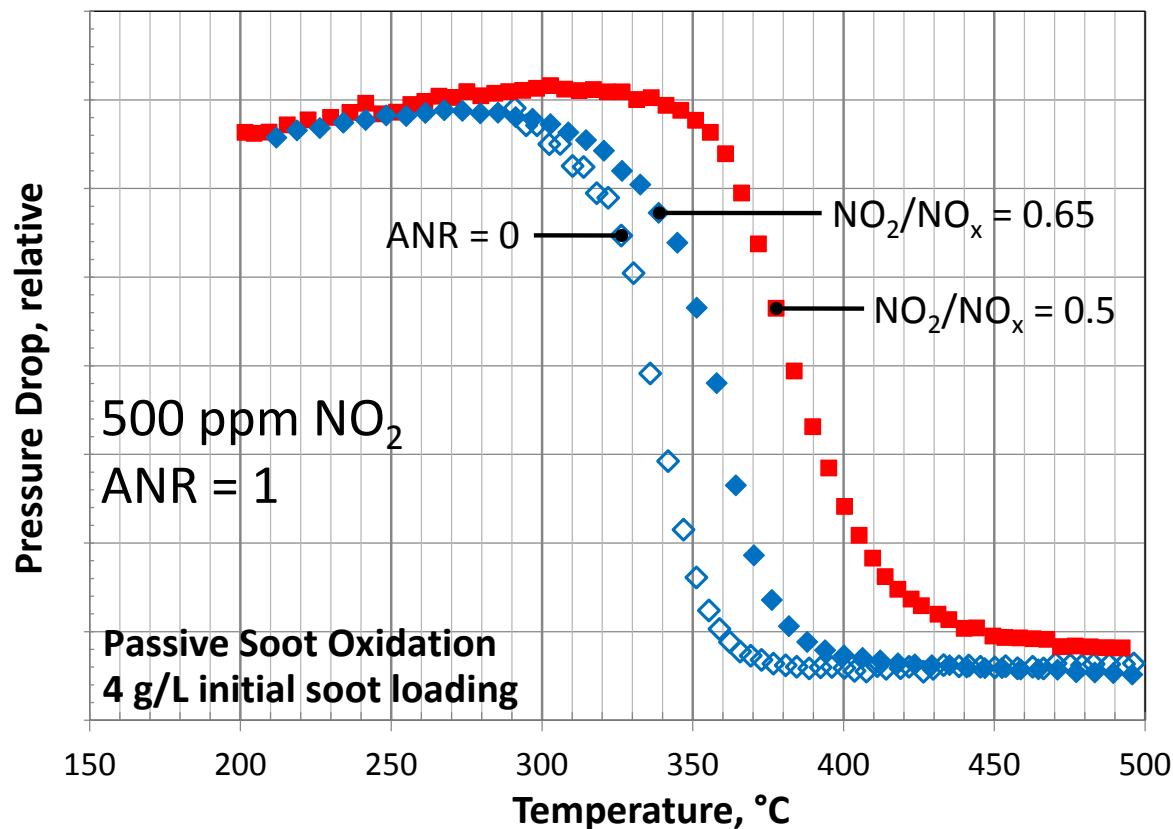
- ▶ Separating NO_2 fraction
 - NO_2 constant, varying total NO_x



NO_2/NO_x 0.33 \rightarrow 0.5

No improvement in passive oxidation

- ▶ Separating NO_2 fraction
 - NO_2 constant, varying total NO_x

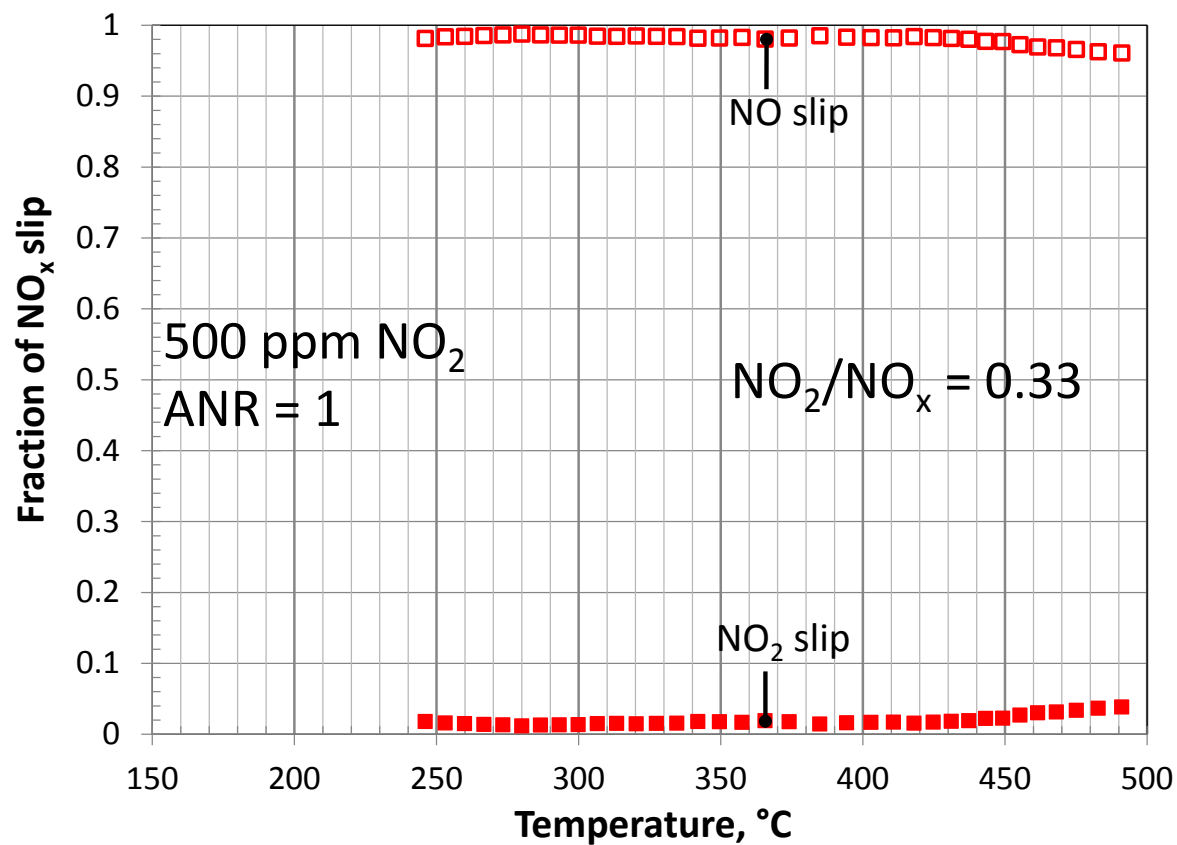


Fast SCR dominating

KEY:
Availability of NO_2
past equimolar
 $\text{NO}:\text{NO}_2$ reaction

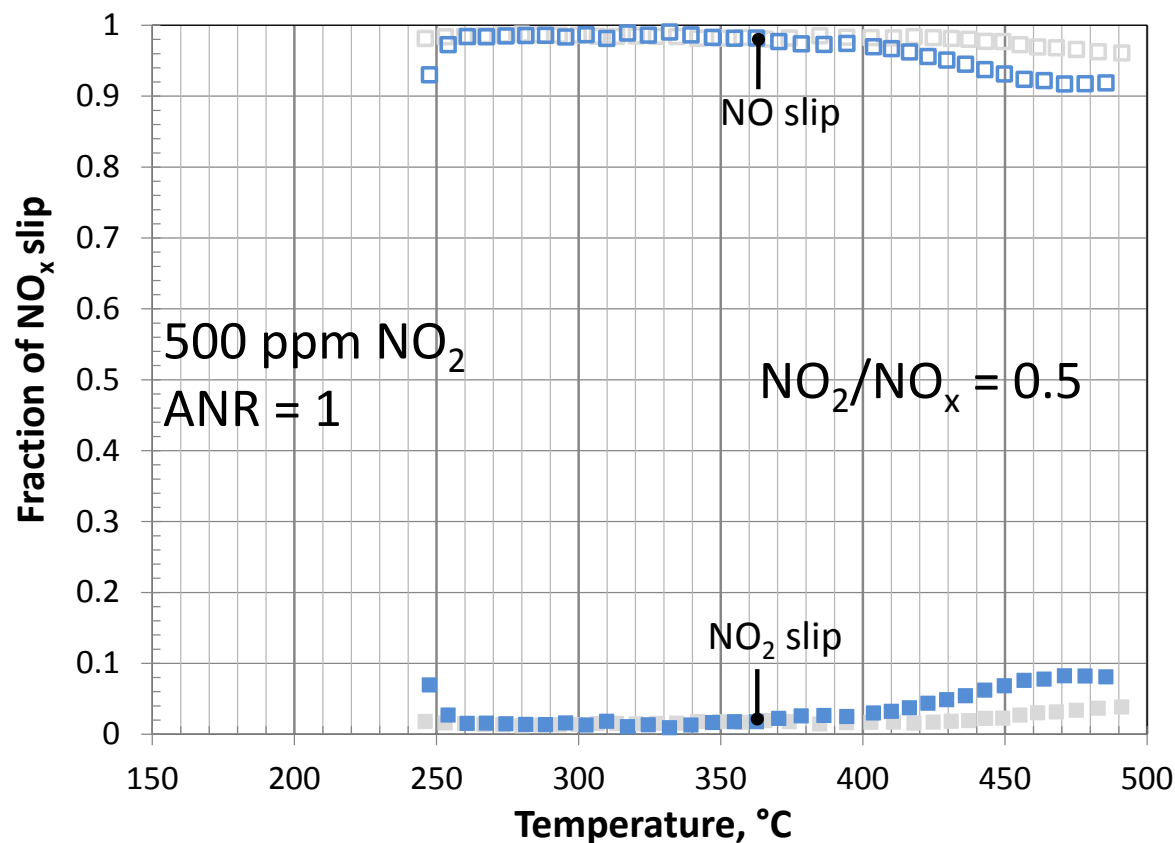
► Separating NO₂ fraction

- NO₂ constant, varying total NO_x



► Separating NO₂ fraction

- NO₂ constant, varying total NO_x

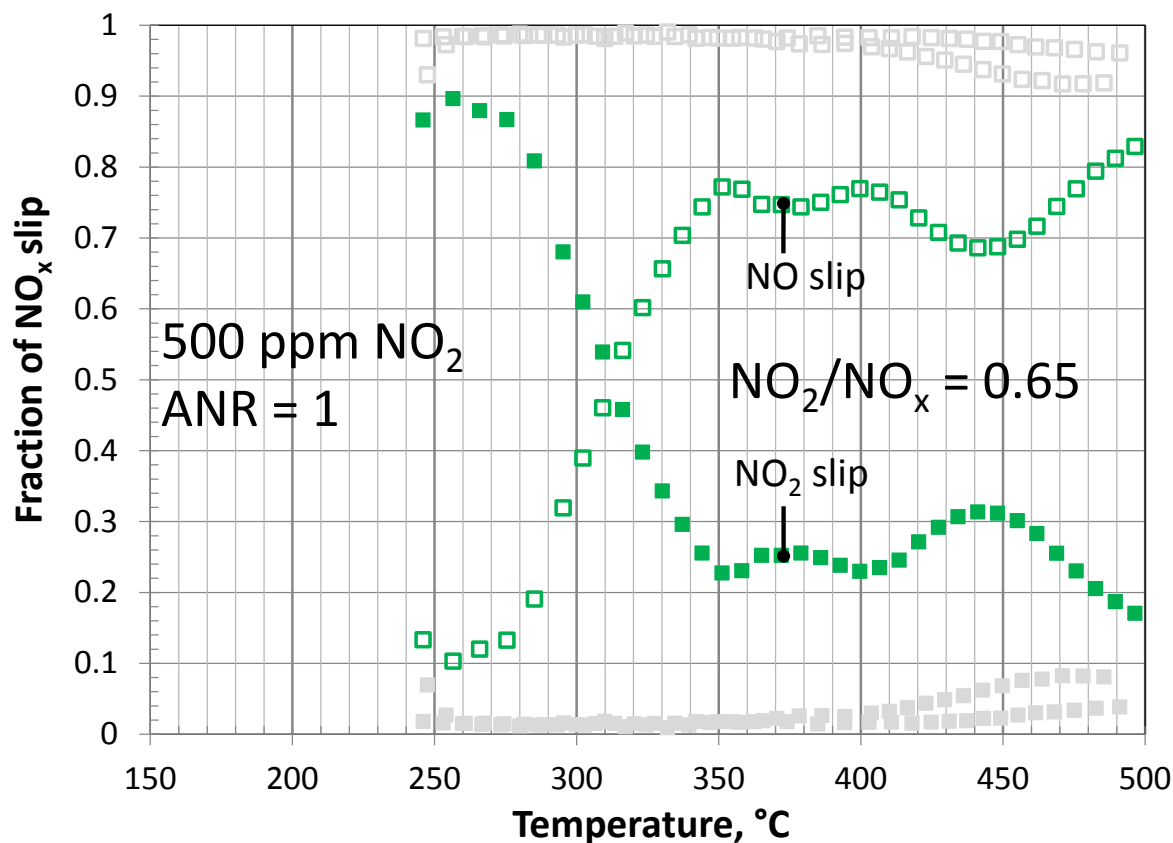


NO₂/NO_x 0.33 → 0.5
Extremely similar
NO & NO₂ fraction of
NO_x slip

Thus similar
oxidation behavior

► Separating NO₂ fraction

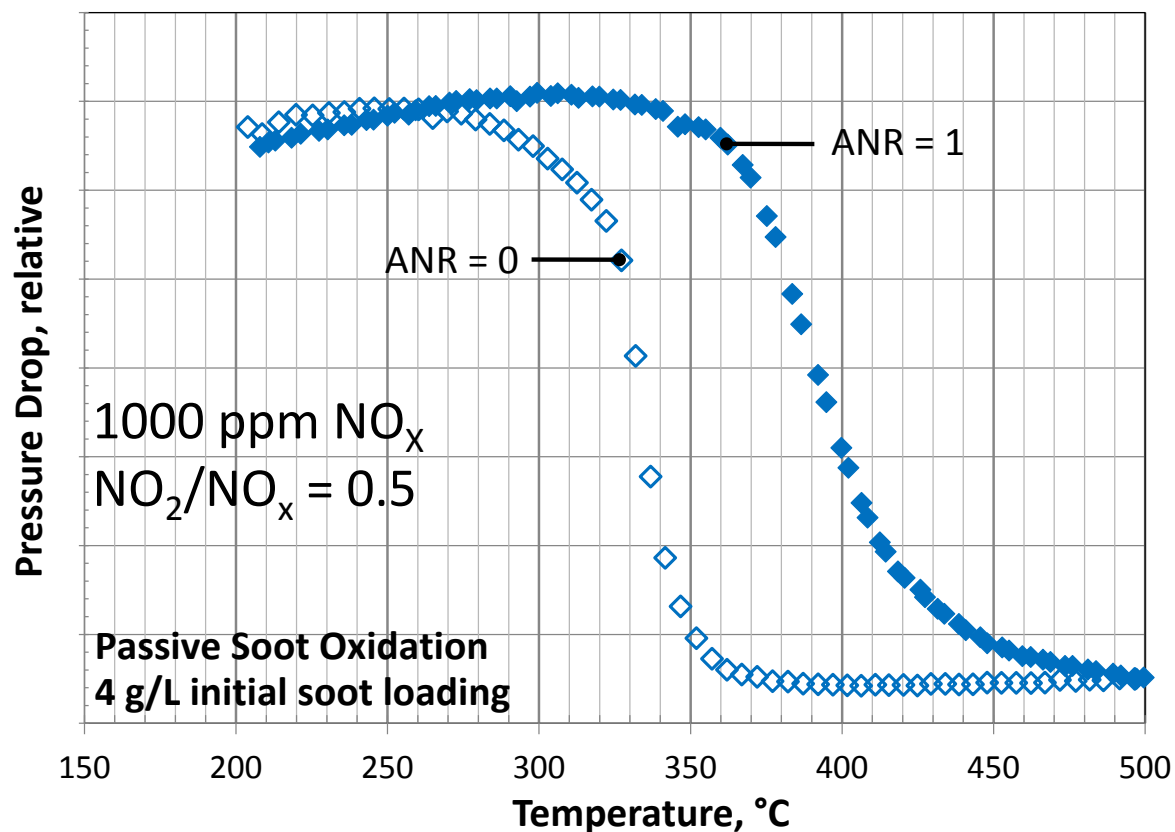
- NO₂ constant, varying total NO_x



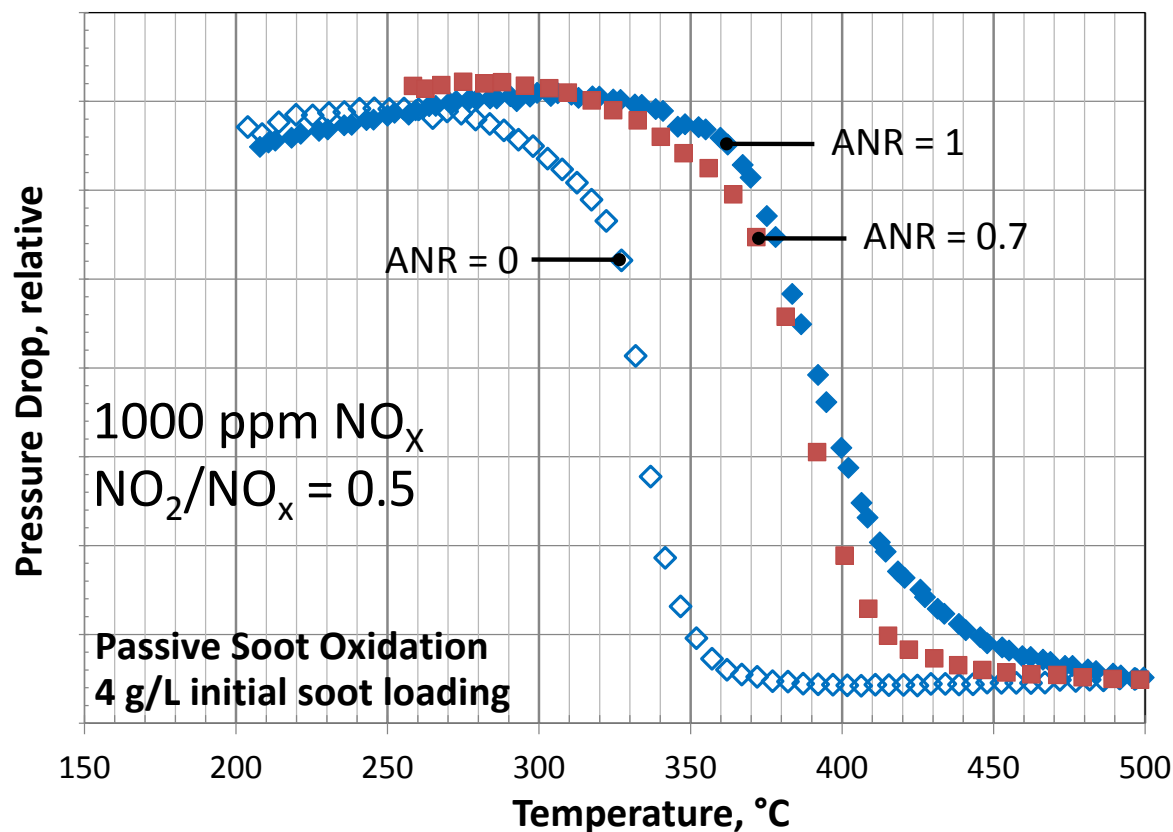
NO₂/NO_x 0.5 → 0.65
Increased NO₂
fraction of NO_x slip

Demonstrates NO₂
availability and
subsequent key role
in passive oxidation

- ▶ Effect of decreased NH₃/NO_x ratio at NO₂/NO_x = 0.5



- ▶ Effect of decreased NH₃/NO_x ratio at NO₂/NO_x = 0.5

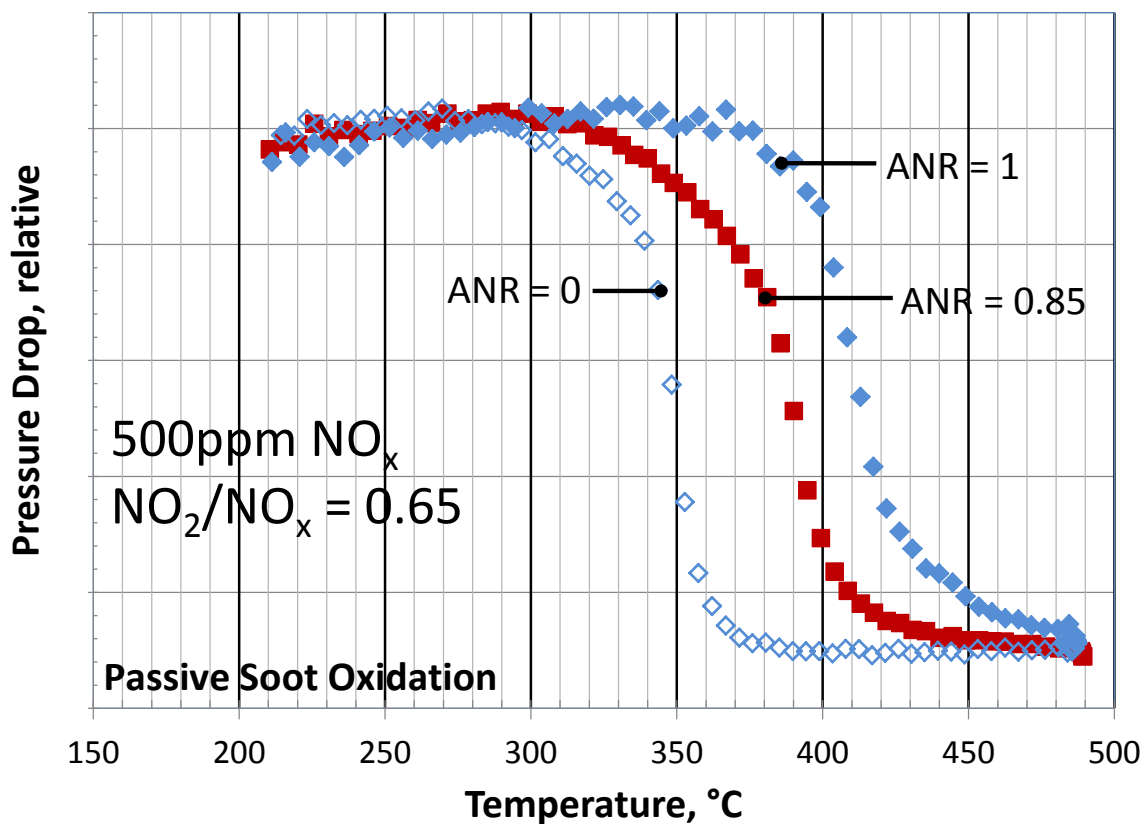


At NO₂/NO_x = 0.5

Soot oxidation
affected little by
decreased ANR

(supported by
modeling and NO₂
concentration profile)

- ▶ Effect of decreased NH₃/NO_x ratio at NO₂/NO_x = 0.65



At NO₂/NO_x > 0.5

Decreased ANR facilitates greater soot oxidation

KEY:
NO₂ availability

- ▶ Facilitating passive soot oxidation
 - **Reaction competition:** passive soot oxidation vs. SCR
 - KEY: NO₂ balance in the system, with the primary driver being the fast SCR reaction (equimolar NO & NO₂ consumption)

- ▶ Modeling can help guide us to develop an understanding of proper reactive and thermal management of SCRF

- ▶ Implementation & control – Truck & engine OEMs
 - Thermal management
 - DOC specification
 - etc.

- ▶ Work funded through DOE's Vehicle Technologies Program
- ▶ BASF – Heavy Duty Systems Development Group
- ▶ Corning
- ▶ Dr. Maruthi Devarakonda (formerly PNNL)
 - SCR kinetic model development