

Energy Efficient Refrigerated Food Processing and Dispensing Machines for Quick Service Restaurants and Food Retail

Oak Ridge National Laboratory
Vishal Sharma, R&D Staff
865-576-5810 (sharmav@ornl.gov)



Project Summary

Objective and outcome

- Ensure successful transition of quick service restaurant industry from high GWP (>1400) refrigerants to **ultra low GWP** (<10) refrigerant
- At the end of this project, a leak mitigation strategy for propane based soft-serve ice-cream will be developed
- CO_{2,eq} savings potential – 416,000 MT

Team and Partners

Oak Ridge National Laboratory

Taylor Company (CRADA)

Stats

Start date: 10/01/2022

Planned end date: 9/30/2023

DOE budget: \$150K, Cost Share: \$75k

- Milestone 1: Complete experimental evaluation propane leakage in soft-serve machine (FY23 Q2)
- Milestone 2: Complete simulation of refrigerant leakage using computational fluid dynamic modeling of R290 based soft-serve ice-cream machine (FY23 Q3)



Problem

- **High GWP Refrigerant (>1400)**
- **416,000 metric tons of carbon emission**
 - Potential low GWP replacements
 - Natural (GWP < 3)
 - CO₂ (high pressure)
 - Propane (highly flammable)
 - Synthetic
 - R-454C (flammable, GWP:146)
- **No Safety Standards for alternative refrigerants**
- **OEMs need guidance for transitioning**
 - Significance for Taylor Company
 - Global Company with 500 employees
 - Industry leader in the US, 25% share in EU



Alignment and Impact

- 200,000 quick service restaurants in the US
- Current Refrigerant: R449A (GWP= 1400)
- Future Refrigerant: R290 (GWP = 3)
- Higher energy efficiency
- Direct CO_{2e} emission reduction = 99%
- Replacing refrigerant in all soft serve machines would reduce carbon equivalent by 416,000 metric tons
- Increases global footprint of US OEM



Approach

- **Previous Years work identified significant challenges in migrating towards low GWP solution**
 - Modeling Prototype Low GWP based Soft-Serve Ice-cream machine
 - Thermodynamic Analysis of CO₂ based machine
 - Evaporator and Condenser Modeling
 - Laboratory Evaluation
 - R454C based soft serve machine at different ambient temperatures showed insufficient capacity

Approach

- **CO₂ system analysis**
 - Thermodynamic Model development
 - Heat Pump Design Model
- **Issues**
 - High Operating Pressure
 - Inefficient
- **Flammable refrigerants**
 - R454C (Mildly Flammable): GWP-146
 - R290 (Highly Flammable): GWP-3

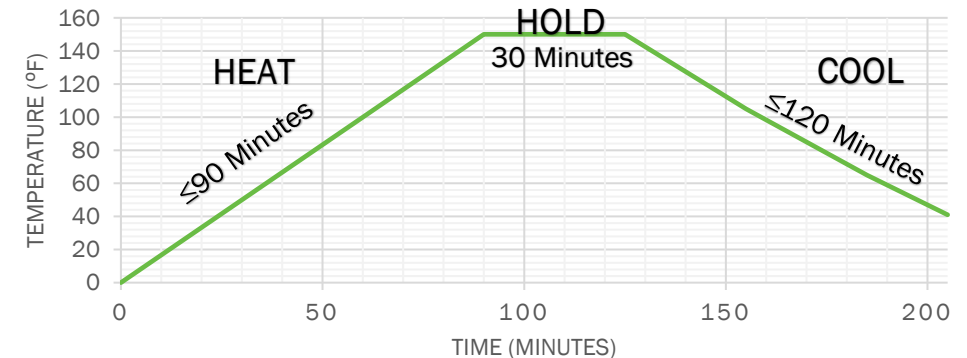
	System	Coefficient of Performance	Discharge Temperature (°F)	Condenser Pressure (psia)	Refrigerant Charge (lb/hr)	System Complexity	Store Retrofit
Single Stage System	CO ₂ Direct Expansion (DX) System	1.18	284	1350	196	Simple	NO
	CO ₂ DX system with SLHX	1.25	326	1310	170	Simple	NO
	CO ₂ DX with Gas Bypass	1.21	273	1345	198	Simple	NO
Two Stage System	CO ₂ DX system with SLHX (2 stage expansion)	1.24	283	1331	189	Moderate	NO
	CO ₂ DX system with 2 stage compression (intercooler)	1.49	188	1335	167	Moderate	NO
	CO ₂ system with 2 stage compression and 2 stage expansion	1.4	186	1335	189	Moderate	NO
	CO ₂ Booster System	1.42	232	1229	214	Moderate	NO

Failed Pressure Test



Approach

- **R454C Machine Evaluation**
 - Continuous Run Test
 - Product Quality
 - Product Draw Rate
 - Capacity and Hopper Cooling Test
 - Refrigeration Capacity
 - Recovery time
 - Heat Treatment Test
 - NSF/ANSI 6- Dispensing Freezers
 - Product temperature > 150°F for 30minutes

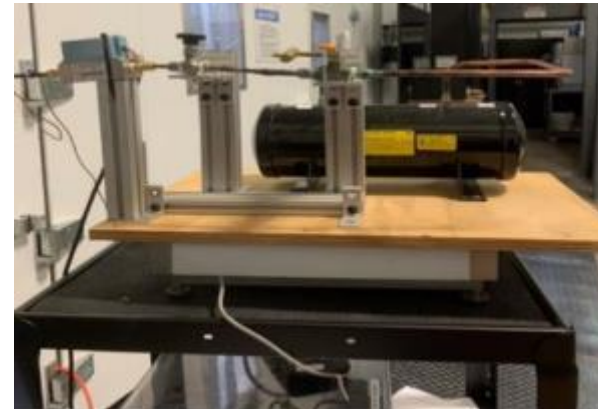


Approach

- R290 is only remaining ultra low GWP option
- Flammable
- Taylor C602 machine has over 65 components not rated for hazardous environment
- No Safety Standards for flammable refrigerant usage in soft serve machines
- Compartmentalize system charge to minimize potential leak under 150 gms



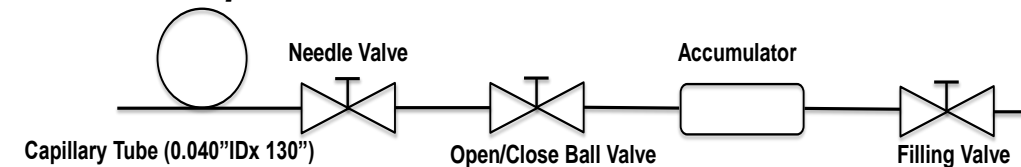
Infrared sensor



Propane Leak Setup



Instrumented Prototype machine



Propane Leak Setup Schematic

Progress

– Adopted IEC 60335-2-89

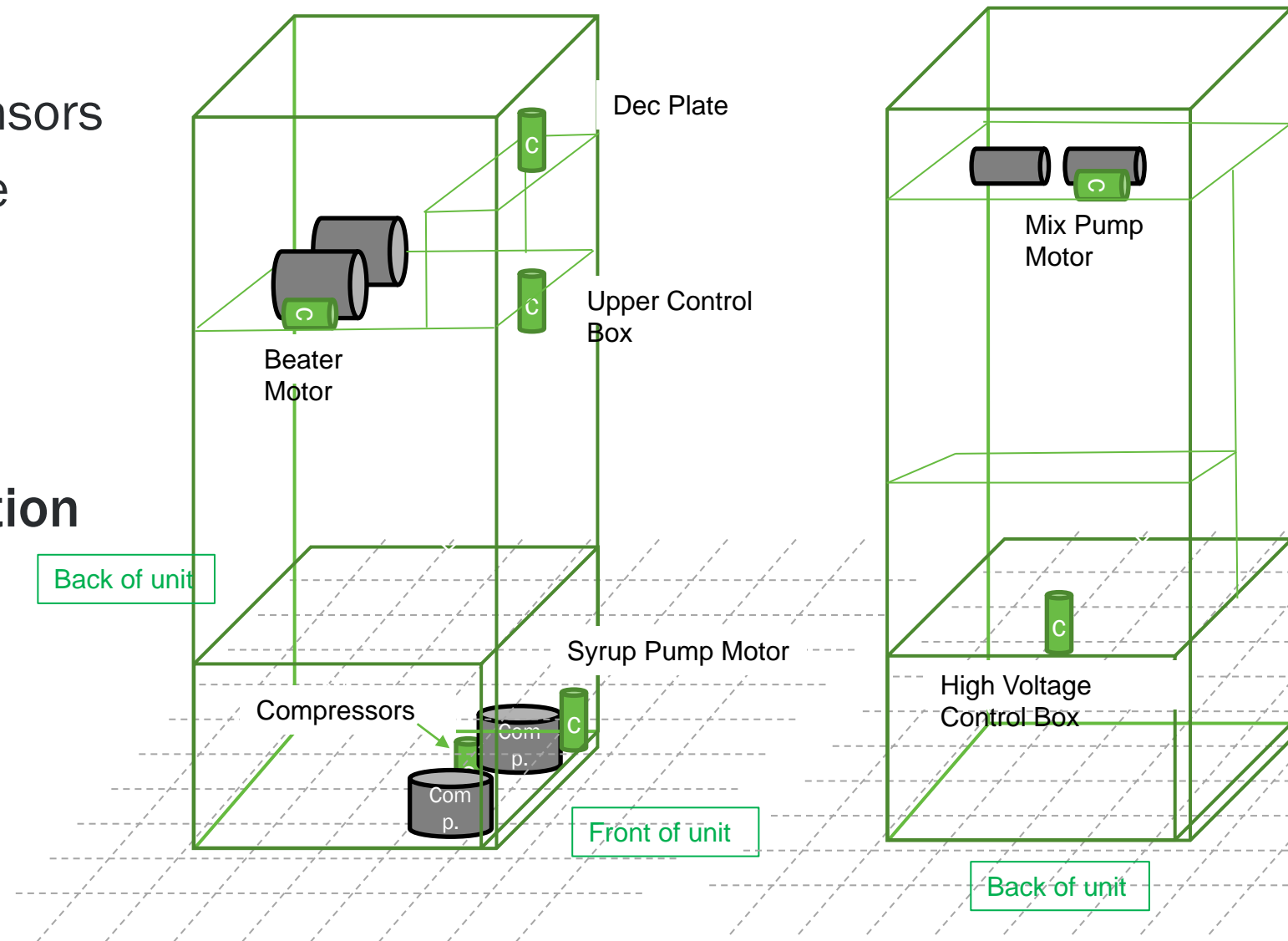
» Safety standard for commercial refrigeration appliances and ice-makers

- Unprotected Cooling System: 22.112 – Not Energized
 - Through an orifice for 1 hour
 - 80% of nominal charge within 10 mins
 - Maximum conc. should not exceed 75% LEL
 - Maximum conc. should not exceed 50% LEL for more than 5 mins
- Outside the Food Storage Compartment: 22.113 – Not energized
 - Constant rate through an orifice for 1 hour
 - 50% of nominal charge within 1 hour
 - Maximum conc should not exceed 75% LEL
 - Maximum conc. should not exceed 50% LEL for more than 5 mins



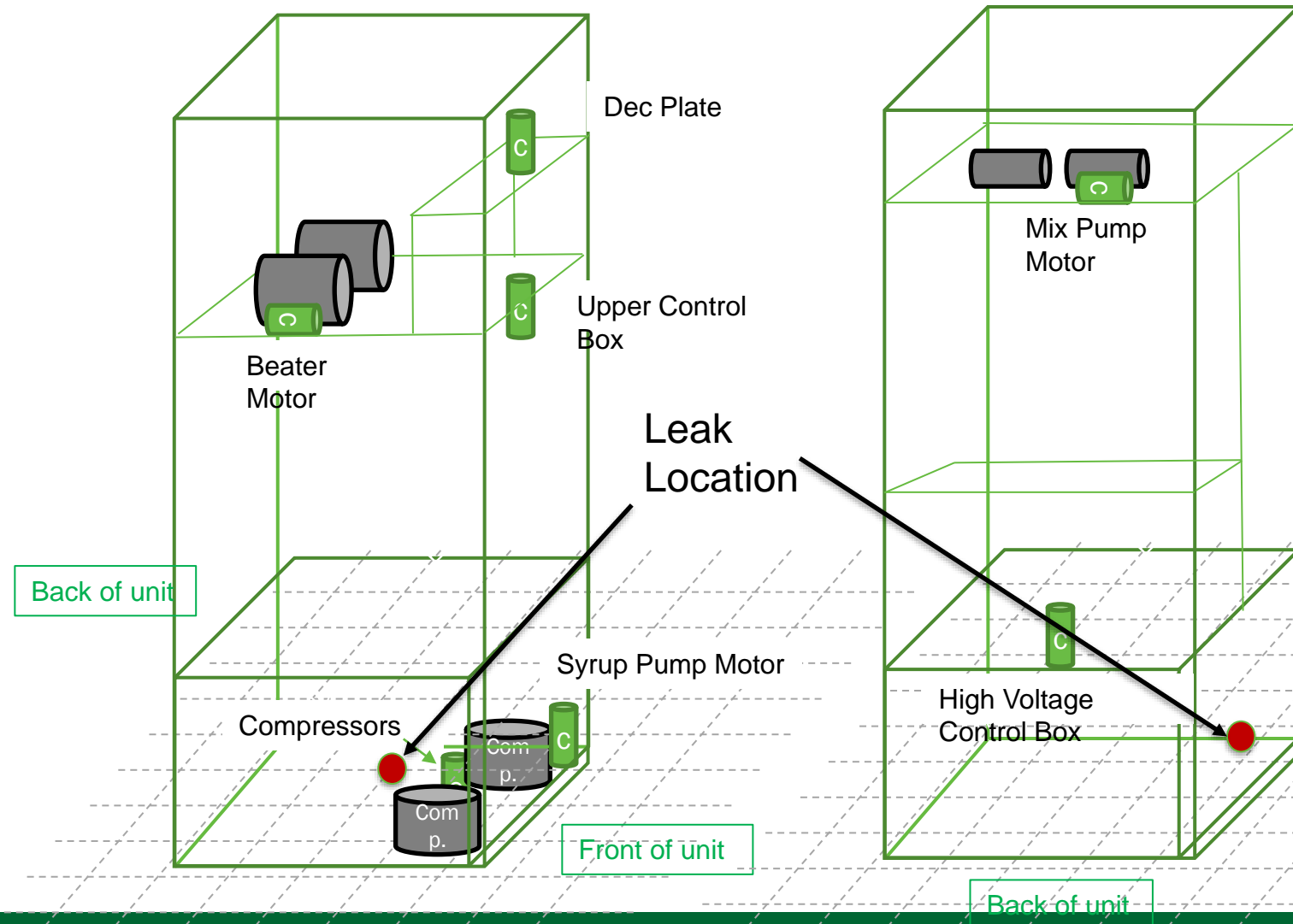
Progress

- **Sensors**
 - 11 IR propane sensors
 - 7 inside, 4 outside
- **Leakage Study**
 - 150g leak
 - 300g leak
- **No Leakage Mitigation**



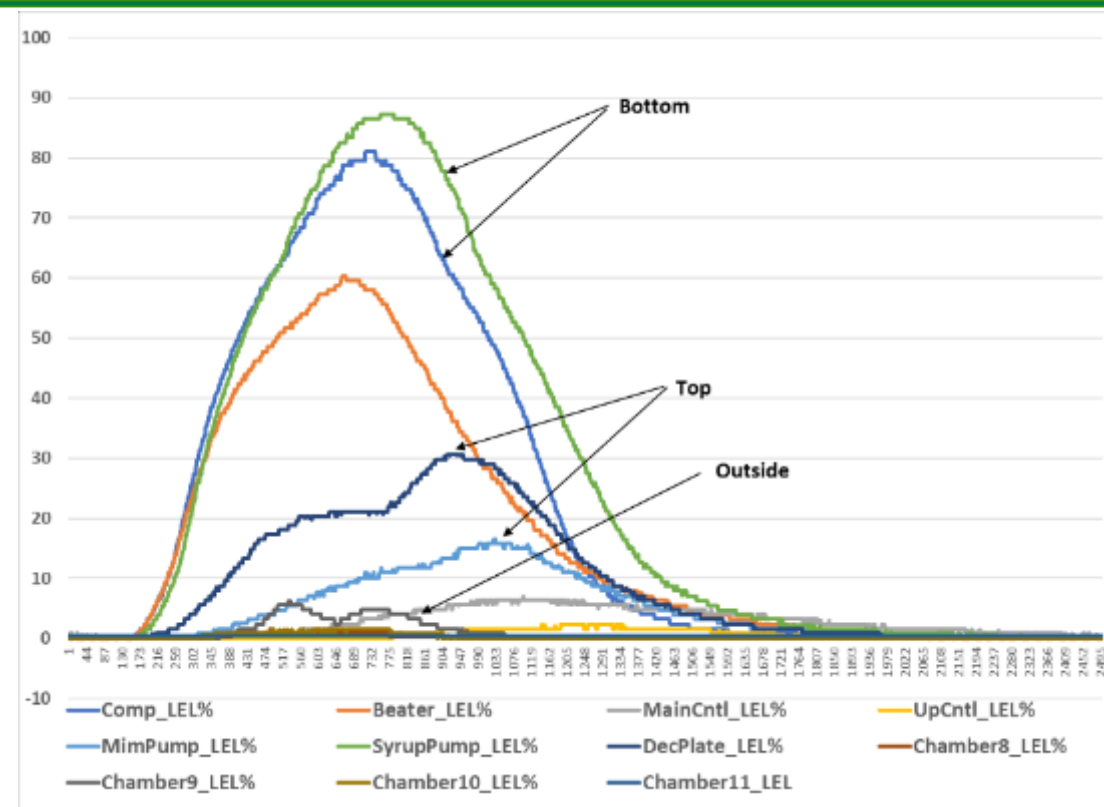
Progress

- Bottom Leak using 300gms (Standard 60335.2.89: 22.113)



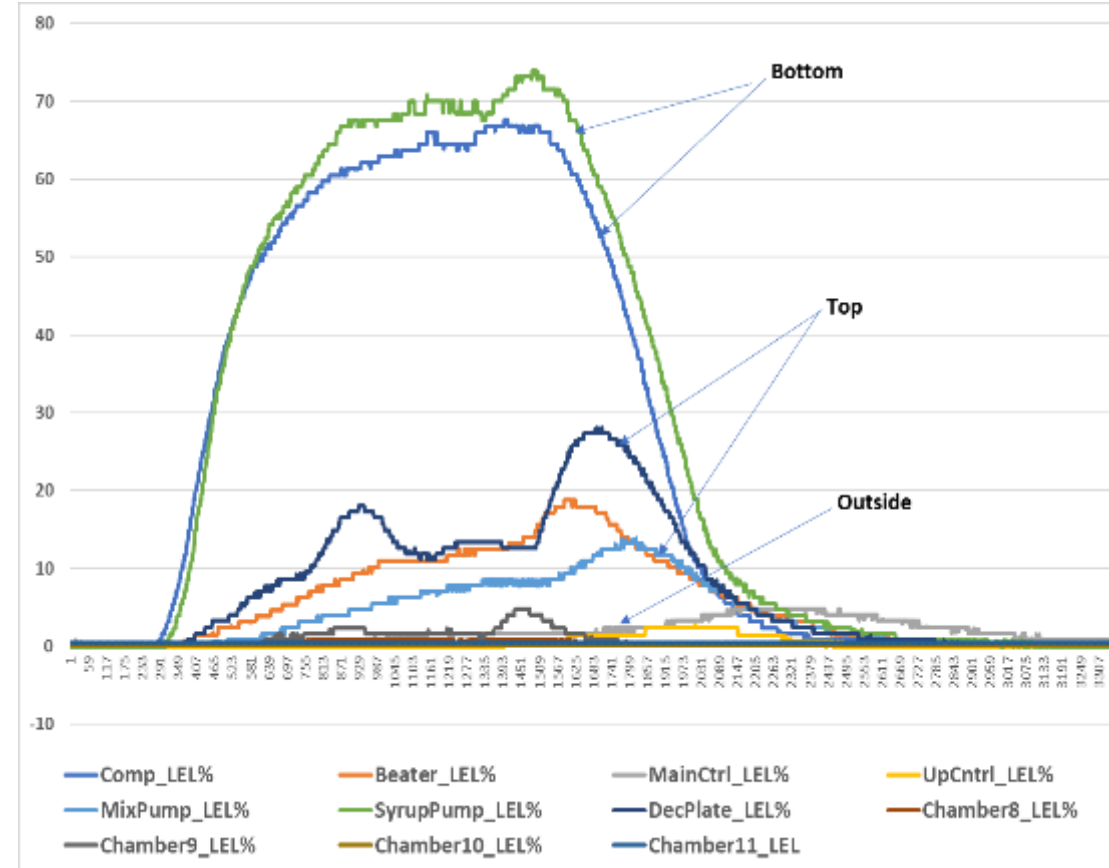
Progress

- **Bottom Leak using 300gms (22.113)**
 - Representing Compressor Leak
 - Propane concentration levels inside machine
 - 50% LEL within 2 mins of leak initiation
 - **Test Failed:** 75% LEL within 4 mins of leak initiation
 - Gas conc continued to increase in top after shutdown
 - Peak conc reached 88%
 - Minimal leakage to surrounding
 - Peak concentration never exceed beyond 6% LEL



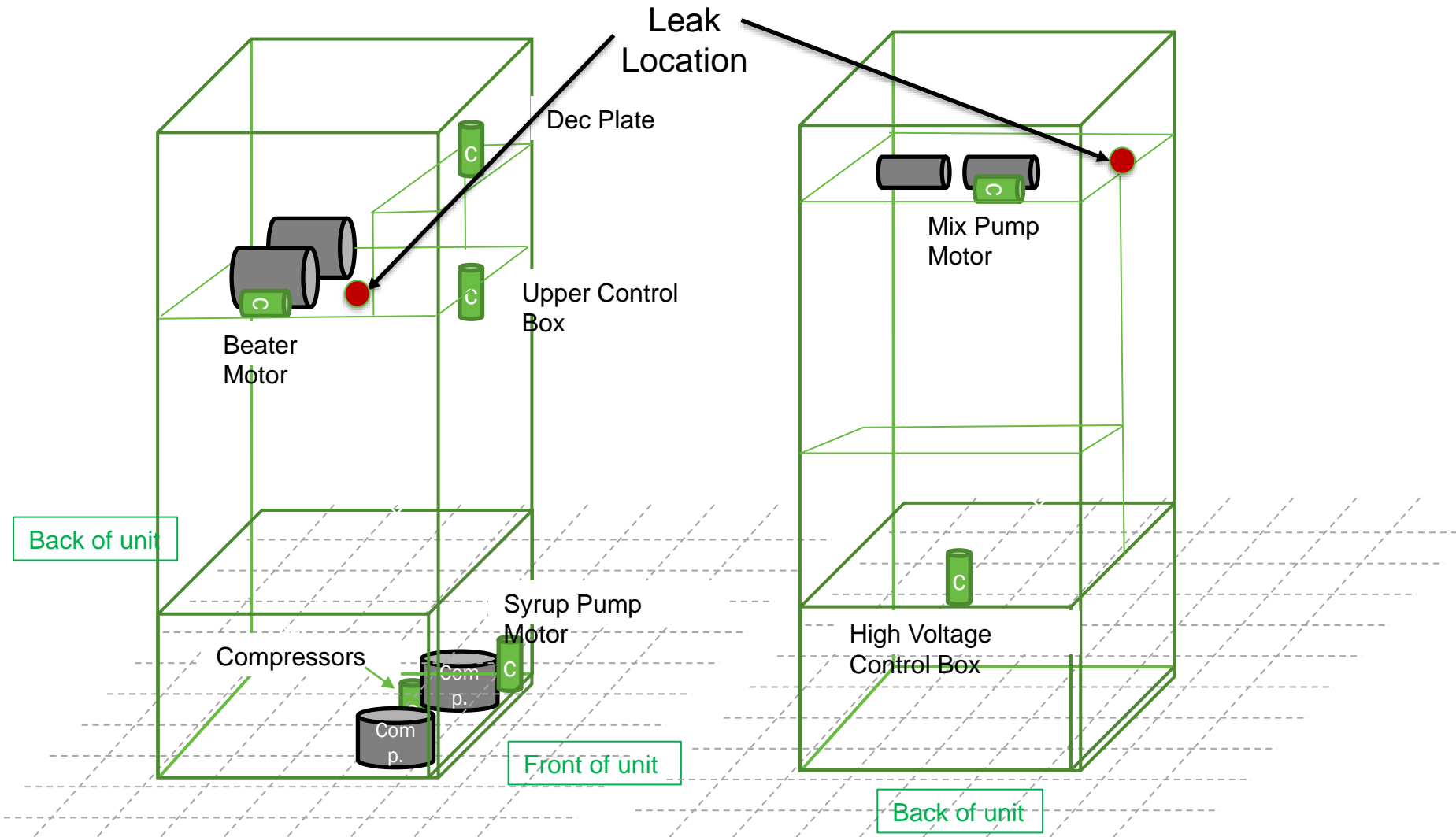
Progress

- **Bottom Leak using 150gms (22.113)**
 - Representing Compressor Leak
 - Propane concentration levels inside machine
 - 50% LEL within 4 mins of leak initiation
 - **Test Failed:** Conc. level exceed 50% for more than 5 mins
 - Peak conc reached never exceed 74 LEL%
 - Minimal leakage to surrounding
 - Peak concentration never exceed beyond 5 LEL% LEL using 150 gms (22.113)



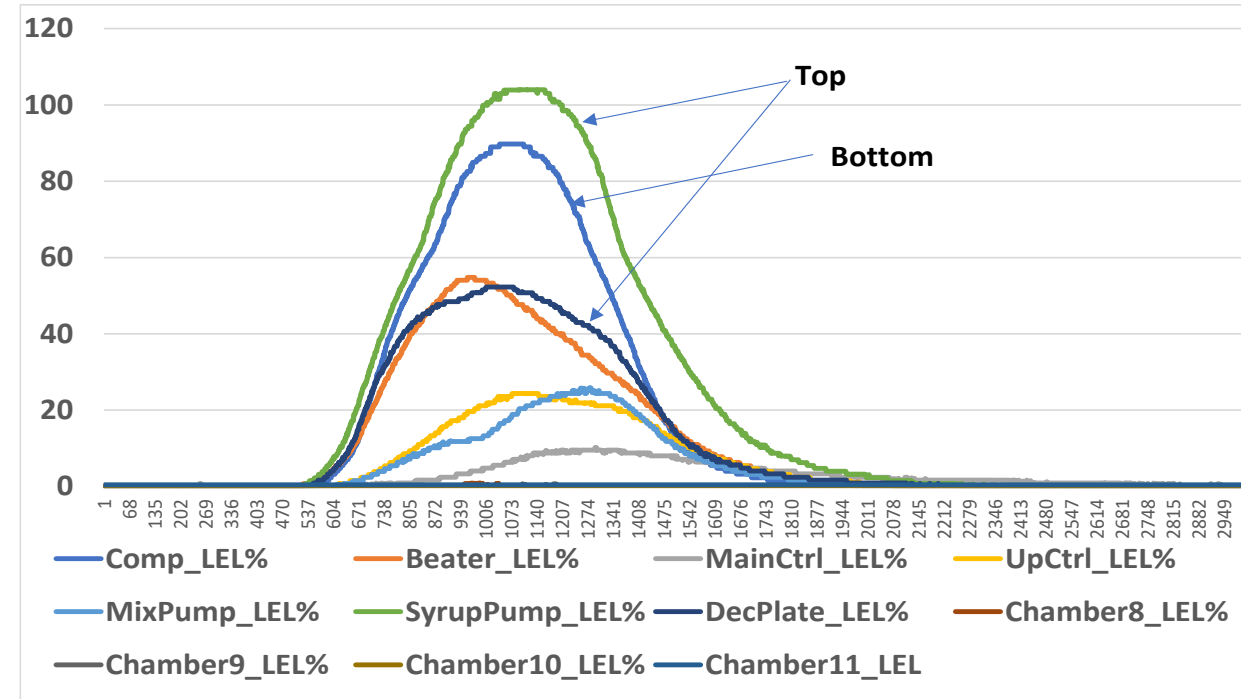
Progress

- Top Leak using 300gms (Standard 60335.2.89: 22.113)



Progress

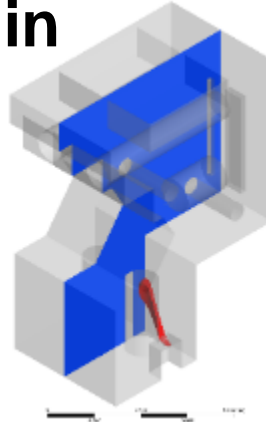
- **Top Leak using 300 gms (22.113)**
 - Representing Evaporator Leak
 - Propane concentration levels
 - 50% LEL within 2 mins of leak initiation
 - 75% LEL within 3 mins of leak initiation
 - Peak conc reached above LEL
 - Minimal leakage to surrounding
 - Peak concentration never exceed beyond 3% LEL using 300 gms



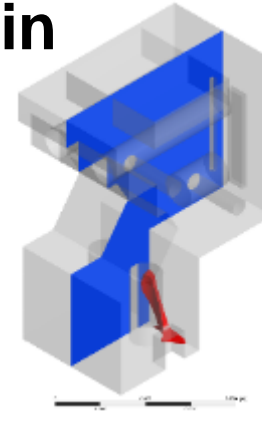
Leak Diffusion

- Leak diffusion in a static environment
- Leak source and the CAD model
- Concentration profiles
- Flammable zone is shown in red color (3D)
- Model agrees with experimental results
- Leak rate – 1.05 g/min

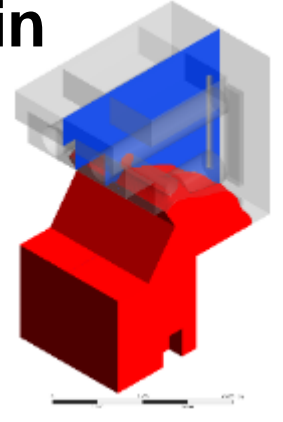
1 min



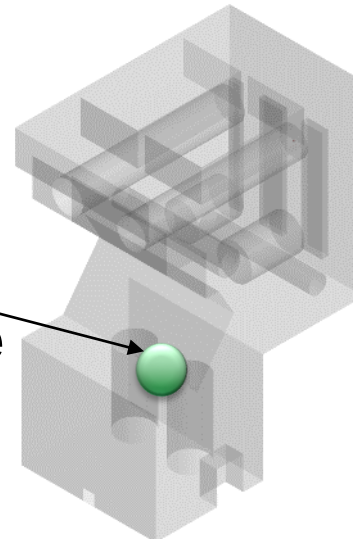
3 min



10 min



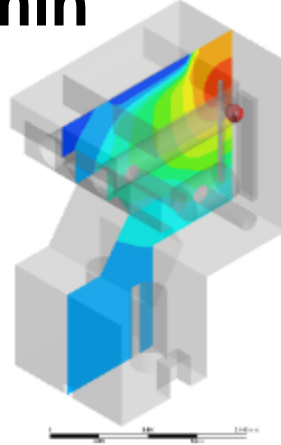
Leak
source



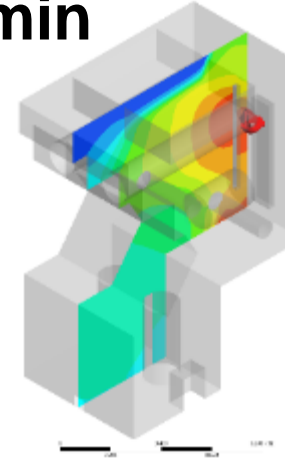
Leak Diffusion (contd.)

- Leak diffusion in a static environment
- Leak source and the CAD model
- Concentration profiles
- Flammable zone is shown in red color (3D)
- Model agrees with experimental results
- Leak rate – 1.05 g/min

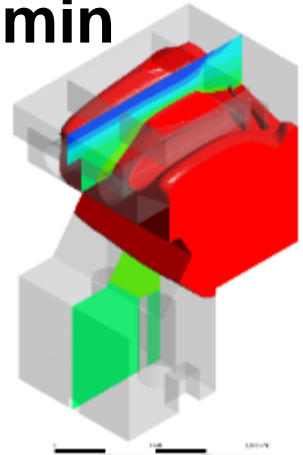
1 min



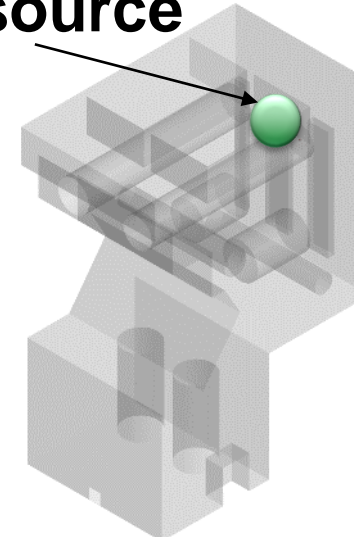
3 min



10 min



Leak source



Lessons Learned

- Evaporator leak mitigation is critical
- Trends of propane concentration in energized machine are expected to match unenergized machine trends
- Shut-off valves and charge compartmentalization is needed to reduce propane conc levels
- Redesigning of condenser location needed

Future Work

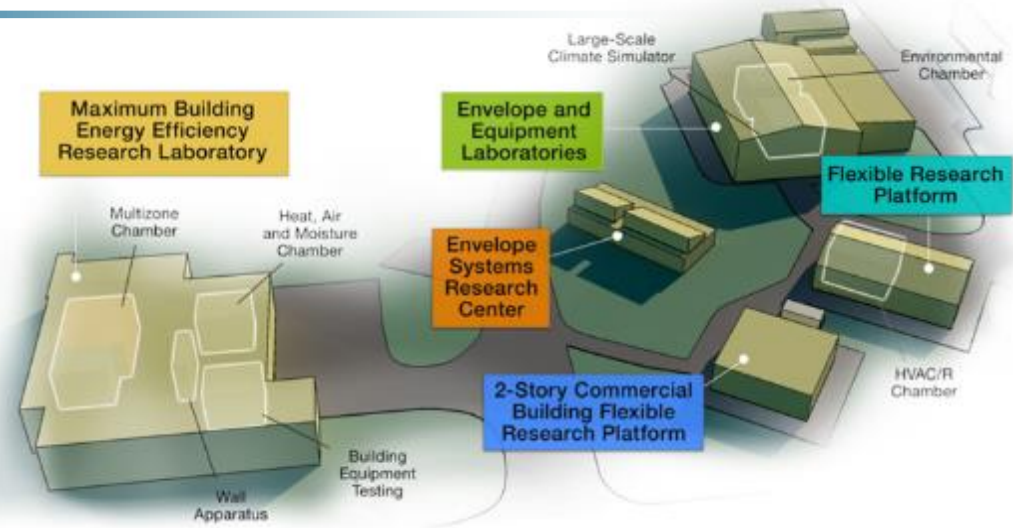
- **Propose leak mitigation methods**
 - Identify strategic placement of sensor(s) within the systems
 - System controls integrated mitigation
- **Condenser Fan Design Modification**
 - Vertical Coil vs. A-Coil Design

Thank you

Oak Ridge National Laboratory

Vishal Sharma

865-574-5810 (sharmav@ornl.gov)



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238 publications in FY20
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REFERENCE SLIDES

Project Execution

Required to complete, but does not count towards total slide count and doesn't need to be focused on during presentation

	FY2023				FY20YY				FY20ZZ			
Planned budget												
Spent budget												
	Q1	Q2	Q3	Q4	Q1	Q2	Q3	Q4	Q1	Q2	Q3	Q4
Past Work												
Complete final testing and data analysis												
Complete Final Report												
Current/Future Work												
Insert more Milestones as needed												

- Go/no-go decision points
- Explanation for slipped milestones and slips in schedule

Team

- **Oak Ridge National Laboratory Research Team**

- Vishaldeep Sharma
- Bo Shen
- Praveen Cheekatamarla
- Tugba Turnaoglu
- Mingkan Zhan

- **Service & Safety Team**

- Tony Gehl, Tim Dyer, Jeff Taylor and Gerald Barth

- **Taylor Company**

- Stephen Wadle (Senior Project Engineer)
- Jim Minard (COO)

