

**DOE Bioenergy Technologies Office (BETO)
2022 Project Peer Review**

**Novel Method for Biomass Conversion to
Renewable Jet Fuel Blend**

April 3 2023

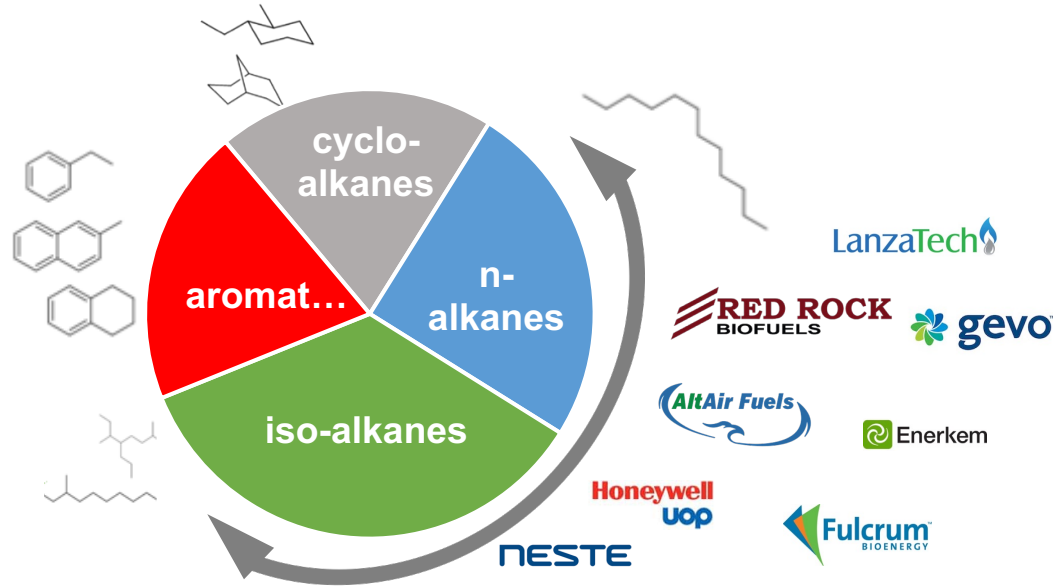
System Development and Integration

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Technology Holding

Project Overview

- *Higher Energy Density drop-in renewable jet fuel blendstock*
- *Project goal: Develop the process to produce renewable superior jet fuel blend*
- **Project Description**
 - *Commercialize renewable jet fuel*
 - *Current Alternatives: Petroleum derived jet and Hydrotreated renewable (F-T fuels) or hydrotreated esters and fatty acids (HEFA)*
 - *Important to demonstrate superior jet fuel from biomass*
 - *Risks: First of a kind plant capital, competition with petroleum jet*

The Problem: SAF Technical Attributes



	HEFA	FT-SPK	ATJ
Energy Density (MJ/L)			
Biogenic Carbon Yield (%)			
% of Blend SAF			
Aromatics Needed?	Yes	Yes	Yes
Current Players			

Key Issues in Aviation:

- Aviation is the hardest sector to decarbonize and represents ~1 gigaton⁽¹⁾ of annual CO₂ emissions (12% of total transport CO₂ emissions)
- Current aviation fuel demand is ~360BN liters, and demand is projected to be ~800BN liters by 2050






Key Issues with Current SAF Processes:

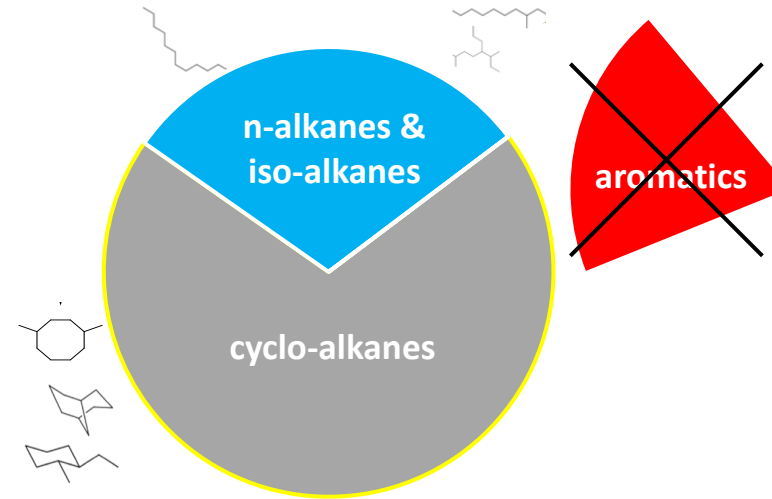
Current SAF processes are based on modifications of established procedures, like FT-SPK and ATJ, and produce n-alkanes and iso-alkanes that have:

- Lower energy density than permitted standards
- O-ring swelling considerations
- Substandard and limited economical viability
- Need for petroleum-based additives
- Requires use of aromatics, which have issues with contrails

(1) 2019 figure sourced from June 2020 IEA report
Source: EIA, Statista

Fundamental Redesign of Superior SAF

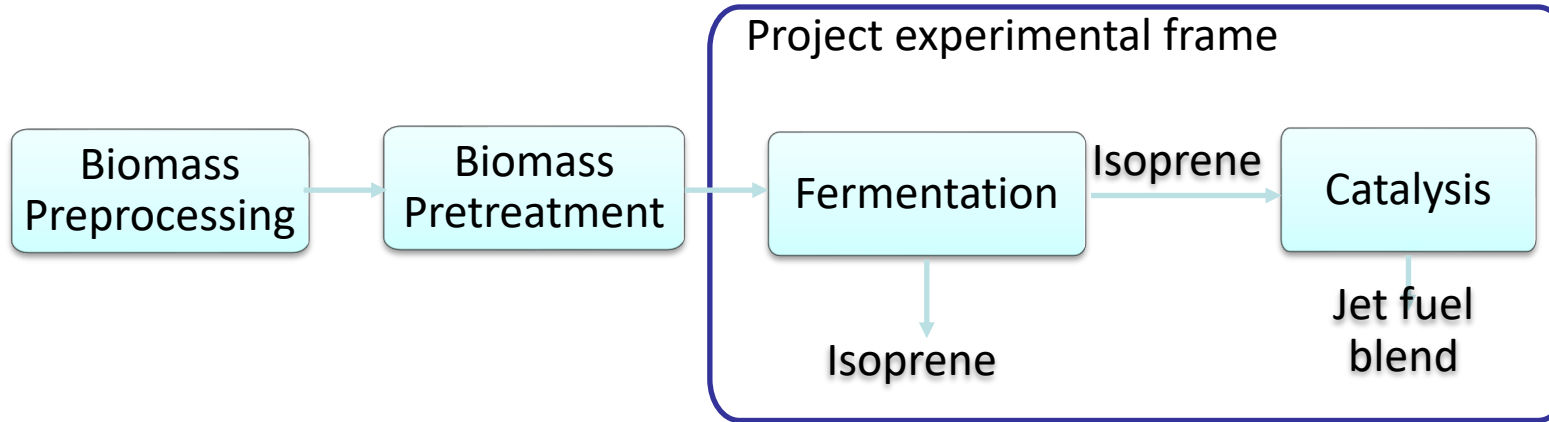
Process	CJ CycloSAF	CleanJoule SAF...
Product	SAF	 <i>More Sustainable</i>
Key Takeaways	Superior energy density; no aromatics; petroleum-free 100% "drop-in"	 <i>Longer Range</i>
Energy Density (MJ/L)	●	 <i>High Quality</i>
Biogenic Carbon Yield (%)	●	 <i>More Efficient</i>
% of Blend SAF	●	 <i>No Blend Needed</i>
Aromatics Needed?	No aromatics needed	



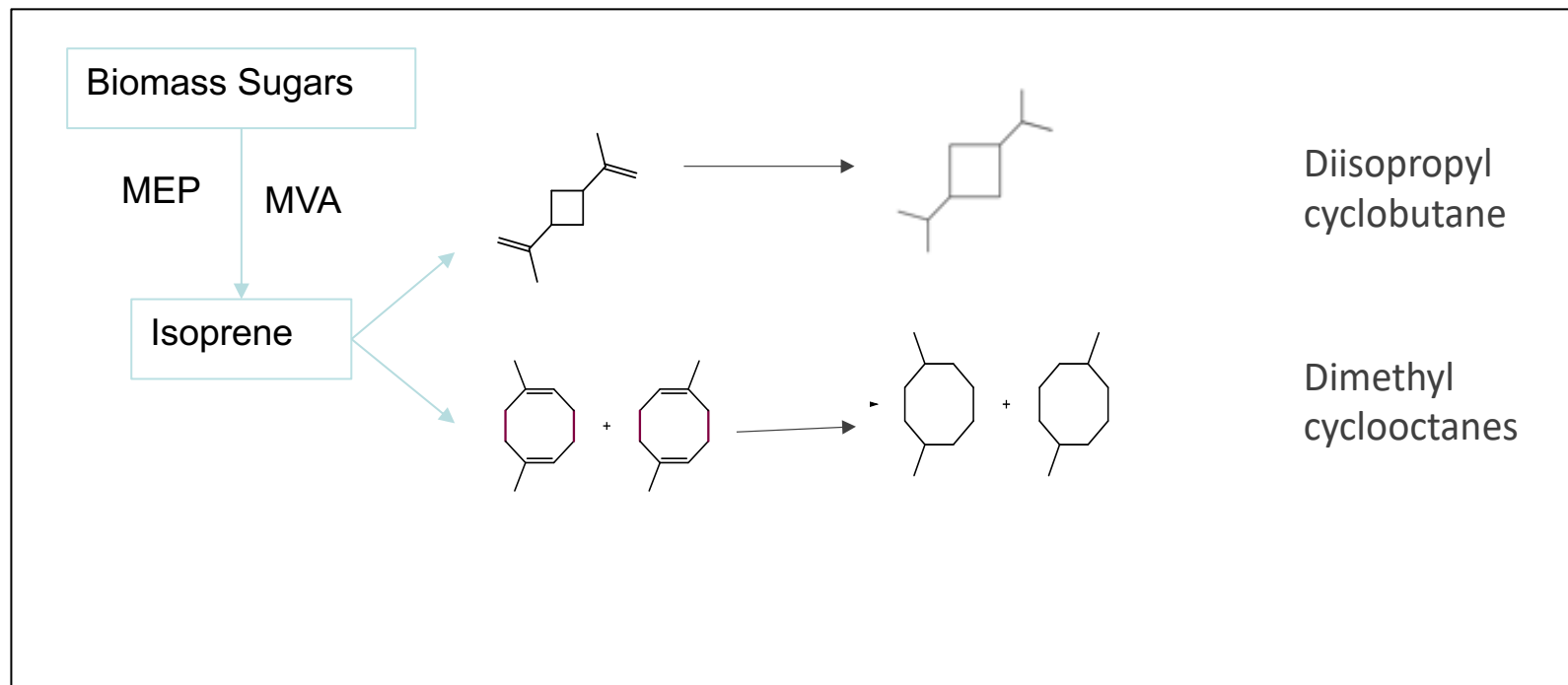
Market size for CycloSAF: 70 Billion Gallons

- ✓ Has Higher Energy Density
- ✓ Has Higher Biogenic Carbon Yield
- ✓ Produces SAF at Low Temp and Low Pressure
- ✓ Is Aromatics Free
- ✓ Fits in Existing Infrastructure
- ✓ Makes Full SAF Tank (100% Drop-in SAF)
- ✓ Highly sustainable (Carbon neutral to negative)

1 – Approach



- *Optimize and scale-up isoprene production using biomass hydrolysate*
- *Optimize the catalytic conversion of isoprene to drop-in jet fuel blend to produce higher specific energy jet fuel*
- *Process integration*
- *Deliver 100 gallons of fuel blend for characterization*
- *Develop overall process system, LCA and TEA models*



2 – Progress and Outcomes

- ✓ BP1 (verification) Go/No-Go (task 1)
- ✓ Successful chromosomal integration (2.1)
- ✓ Performed directed evolution using biomass hydrolysate (Milestone 2.2)
- ✓ Master cell banking (Milestone 2.3)
- ✓ Bioreactor parametric optimization (3.1) - 2X improvement in titer of isoprene compared to verification period (in progress)
- ✓ Catalyst optimization for DIPCB (4.1)
- ✓ Catalyst/Activator Optimization for Hydrogenation Protocols (4.2)
- ✓ Integrated cyclodimerization and hydrogenation (4.3)
- ✓ Produced 4 Liter DMCO for detailed characterization as a blend with HEFA and jet A (6.1)
- ✓ Pilot plant design in progress (Task 7)

3 – Impact

ASTM D7566 Table 1

Property	DMCO / HEFA Blend	ASTM D7566 / ASTM D1655
Density (g/mL)	0.780	> 0.775
$\eta(-20\text{ }^\circ\text{C})$ [mm^2s^{-1}]	5.03	< 8.0
$\eta(-40\text{ }^\circ\text{C})$ [mm^2s^{-1}]	10.54	< 12
NHOC (MJ kg^{-1})	43.76	> 42.8
Flash Point ($^\circ\text{C}$)	51	> 38
Corrosion (No.)	1A	1
Smoke Point (mm)	49.4	> 25
Conductivity (pS/m)	STADIS	STADIS 50-600 (Jet-A)
Simulated Dist. (T50-T10)	28.5	> 15
Simulated Dist. (T90-T10)	104	> 40
Exist. Gum (mg/100 mL)	4	< 7
Lubricity (mm)	0.734	< 0.85
Thermal Stability	Code: 1; pressure drop (0 mmHg); deposits (7.050 nm)	Code (<3); pressure drop (<25 mmHg); deposits (<85 nm)
Acidity (mg KOH/g)	0.001	< 0.10
Derived Cetane No.	44.1	> 30

TSI of DMCO is 10.8 compared to jet fuel at 15-29

D7566 Requires:

DMCO: Dimethyl

cyclooctane

HEFA: Hydrogenated esters and fatty acids

Aromatic content of 8-25% (O-ring swelling properties of DMCO will be sufficient for operability)

Zero-aromatic SAF will reduce coking, emissions and potentially reduce maintenance requirements

Mercaptan mass percent of less than 0.003% (Not measured since feedstock contains no mercaptans)

Maximum sulfur content 0.3% (zero to trace sulfur in the SAF, lubricity requirements met)

Freezing point of <-40 °C (DMCO freezing point <-78 °C. HEFA – not measured, however a viscosity value at -40 °C suggests lower freezing point)

DMCO eliminates the need for blending with petroleum

3 - Impact

10:90 Blend Test Results

Property	10:90 DMCO:Jet-A	ASTM D7566
Density (g/mL)	0.808	> 0.775
$\eta(-20\text{ °C})$ [mm^2s^{-1}]	4.10	< 8.0
$\eta(-40\text{ °C})$ [mm^2s^{-1}]	8.03	< 12
NHOC (MJ kg^{-1})	pending	> 42.8
Flash Point	pending	> 38
Corrosion (No.)	1A	1
Smoke Point (mm)	pending	> 25
Conductivity (pS/m)	255	50-600 (Jet-A)
Simulated Dist. (T50-T10)	34.3	> 15
Simulated Dist. (T90-T10)	102.6	> 40
Exist. Gum (mg/100 mL)	pending	< 7
Lubricity (mm)	0.590	< 0.85
Thermal Stability	Code: 1; pressure drop (13 mmHg); deposits (10.8 nm)	Code (<3); pressure drop (<25 mmHg); deposits (<85 nm)
Acidity (mg KOH/g)	0.013	< 0.10
Derived Cetane No.	43	> 30

***D7566 Table 1
properties met with
10:90 DMCO and Jet A
blend***

3 – Impact

- *Feasible to replace aromatics (ring swelling issue addressed)*
- *In-service Engine maintenance addressed*
- *Co-product (intermediate) isoprene as a feedstock to chemical industry*
- *In discussions with one Aircraft manufacturer and two Oil and Gas Companies*
- *Interest from Air Force Research Laboratory for defense applications*
- *Interest from various segments of the US Navy*

Path to ASTM Certification

Phase I
(Initial
screening)

Tier 1
(Specification
Properties)

Tier 2 (Fit for
purpose
properties)

Phase II
(Follow-on
Testing)

Tier 3
(Component
Rig Testing)

Tier 4
(Engine /
APU Testing)

Balloting
and
Approval

FAA Review

ASTM
balloting

ASTM
Specifications

Tier 1 Spec Tests: upto 10 Gallons

Tier 2 FFP: 10 – 100 gallon

Tier 3:

Component and Rig Tests: 250 -10,000 gallons

Engine Tests: upto 225,000 gallons

Summary

- Meets ASTM D7566 Table 1 requirement as a blend with jet A as well as HEFA
- Higher energy content (2.4% higher gravimetric and 4.5% volumetric)
- Promising renewable jet fuel blend
- Valuable intermediate / co-product
- High level of industrial and DOD interest
- Highly favorable full spectrum characterization for blending
- Potential to replace aromatics
- Potentially reduced engine maintenance

Quad Chart Overview

Timeline

- 10/01/2018
- 03/31/2023

	FY22 Costed	Total Award
DOE Funding	\$607668.69	\$2,499,999
Project Cost Share	\$147,870.69	\$625,001

TRL at Project Start: 3

TRL at Project End: 4

Project Goal

Demonstrate techno-economic feasibility of producing high energy density renewable jet fuel blend

End of Project Milestone

1. Production of 10 gallon finished fuel blend
2. complete a non-location specific basic engineering package (BEP) for the renewable jet fuel engineering scale (1 dry metric tonne per day biomass feedstock) process
3. Detailed fuel characterization profile

Funding Mechanism

FOA: DE-FOA-0001926

Topic Area 1: Drop-in renewable jet fuel blendstocks, FOA year: 2018

Project Partners

- Princeton University
- Naval Airfare Warfare Center, Weapons Division