

Fuel Cell vs. Low Temperature Electrolysis Materials

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QC Workshop
May 6th, 2021

Outline

- Approach of Sensitivity Assessment and Tolerance Determination
- Example: Effect of Processing on MEA Integrity
- Fuel Cell vs. Electrolysis Cell - Comparison of Material
- Future Electrolysis Systems
- Discussion: How can we port existing QC work over to LTE?
 - What is similar, what is new?

Approach of Sensitivity Assessment and Tolerance Determination

Approach

An “Inhomogeneity” can be classified as a “Defect” when one of the three following criteria applies:

1. An initial detrimental performance effect is observed.
2. The lifetime is reduced.
3. The performance over time suffers.

NREL conducts sensitivity studies varying size and/or other defining criteria of inhomogeneity:

Performance experiments

- With single cell & segm. cell

Accelerated stress tests

- With custom IR hardware

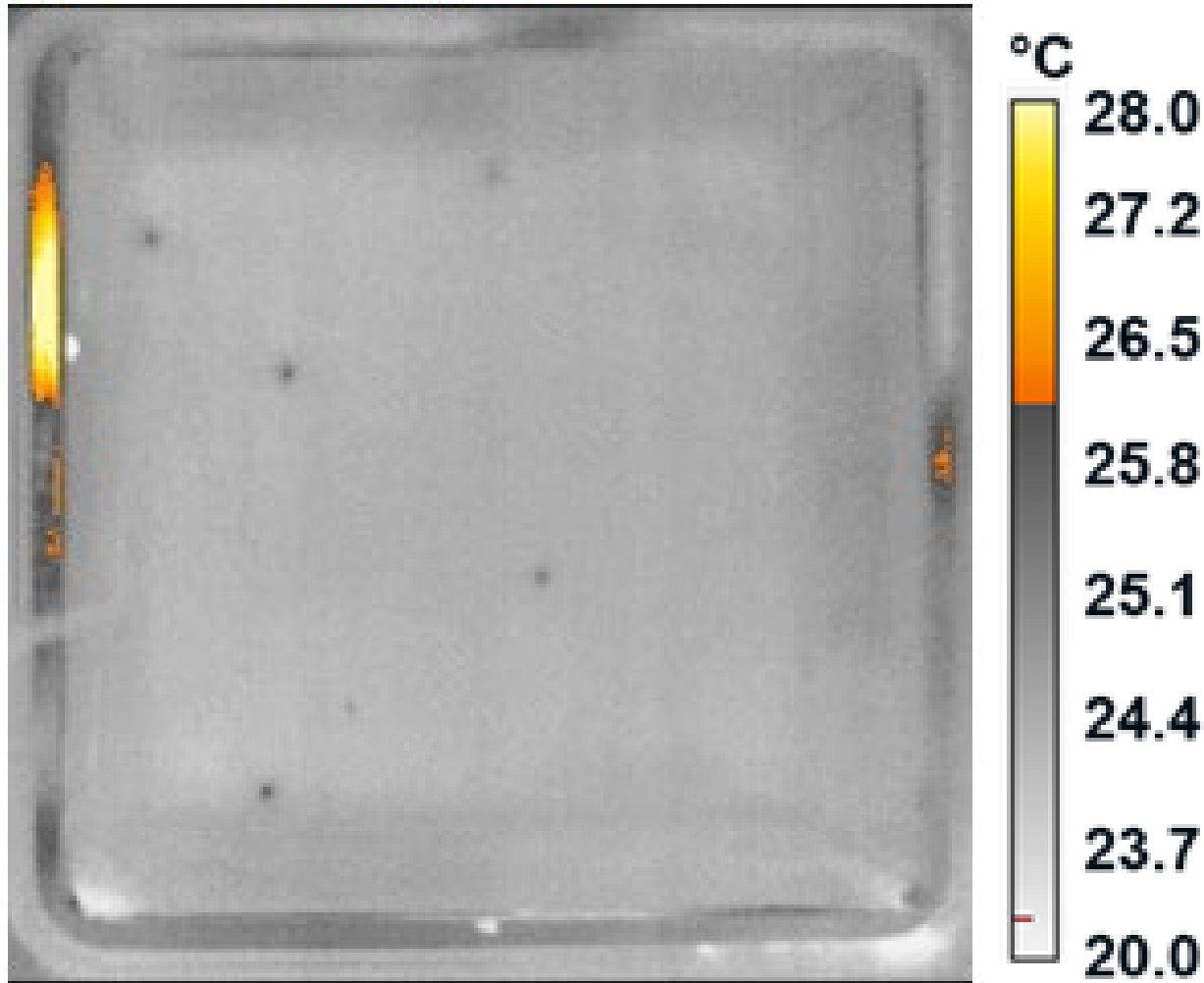
Drive cycle operation

Any **QC equipment** needs to be able to identify variations at or below the “Inhomogeneity” to “Defect” **threshold**.

Example:

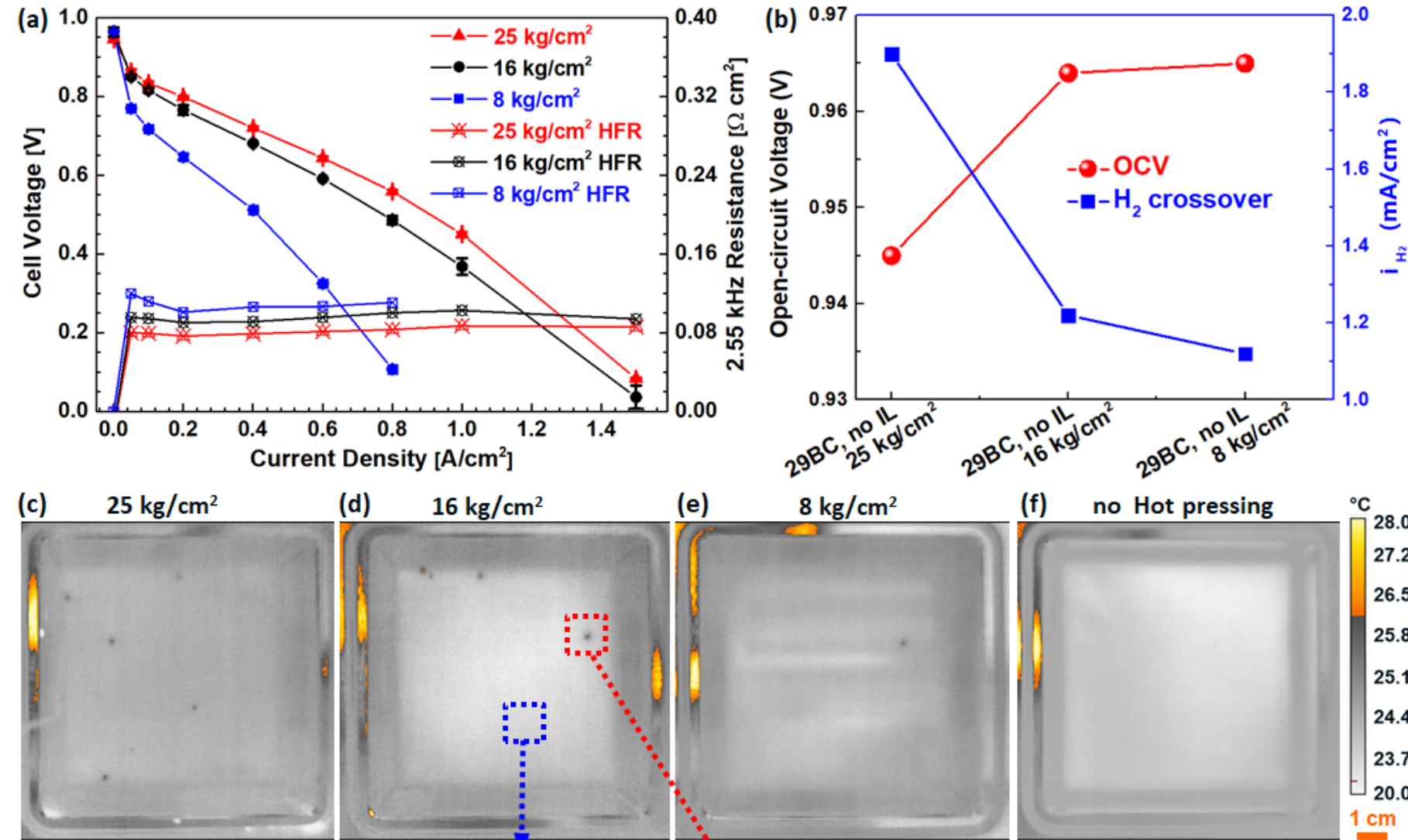
Effect of Processing on MEA Integrity

Process Induced Morphology Changes



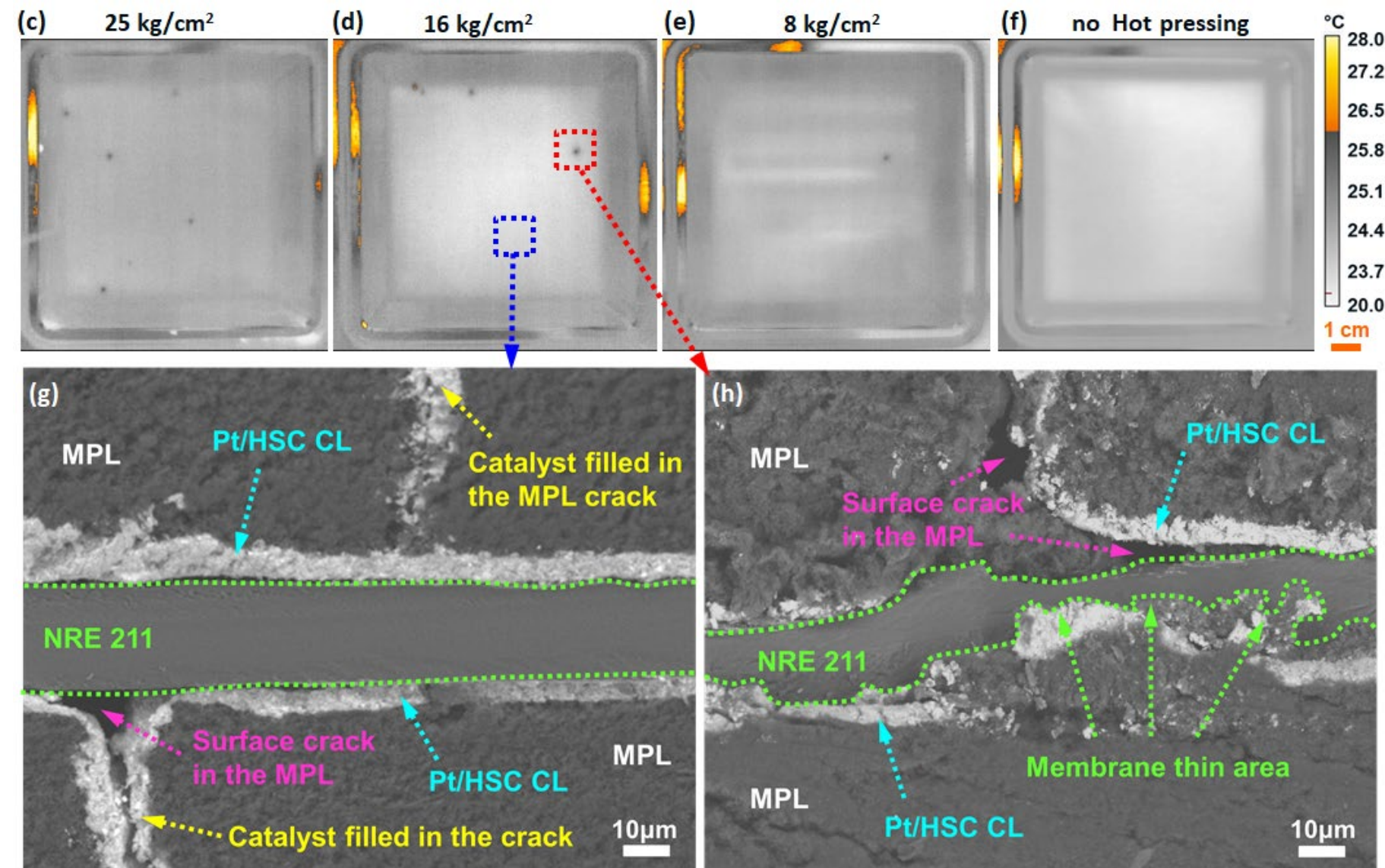
- **Beginning of Life (BOL) high resolution hydrogen crossover (H2Xover) measurement using IR camera**
- **Dark spots indicate localized areas of increased H2Xover**
- **Such areas were repeatedly detected with two different gas diffusion electrodes**

Process Induced Morphology Changes



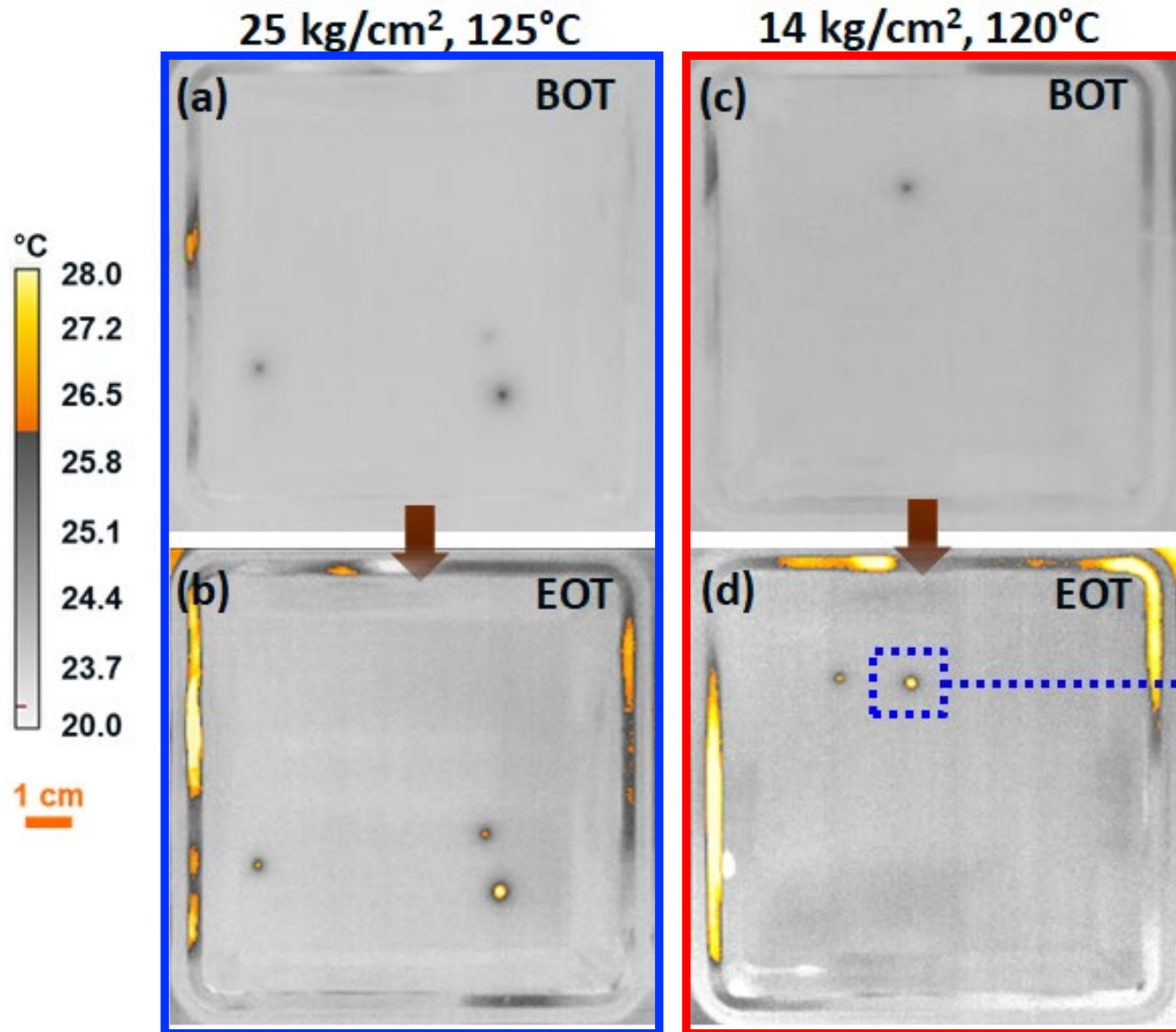
- Phenomena was dependent on fabrication conditions, i.e. applied hot pressing force & temperature
- Fabrication conditions impact performance

Process Induced Membrane Irregularities (PIMs)



- Closer investigation found that morphology of membrane was impacted by combination of local GDE features and process parameters

Process Induced Morphology Changes

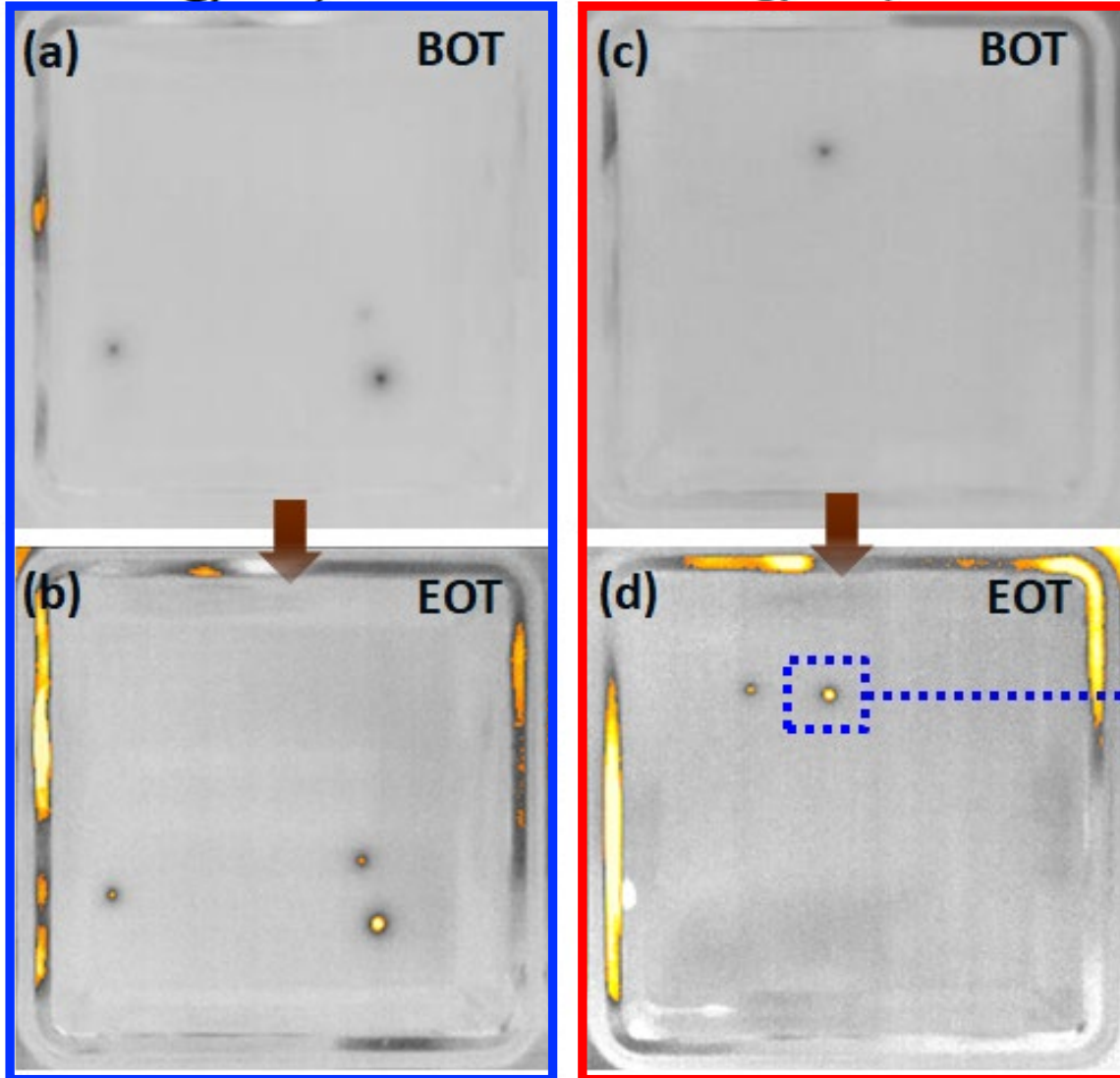


- No significant initial performance impact, but...
- ...the PIMs developed into failure locations and reduced MEA lifetime

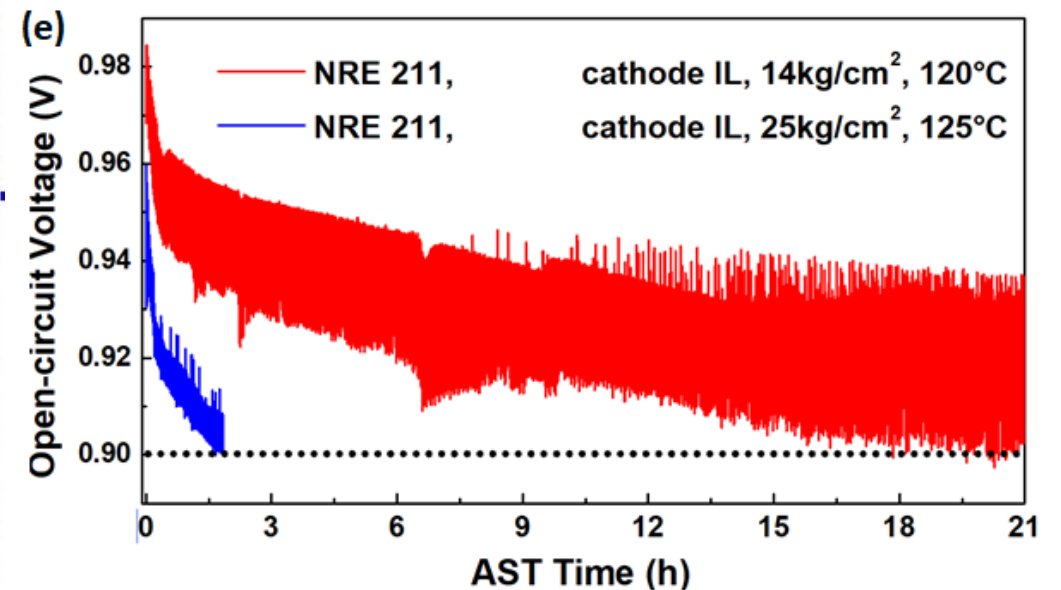
Process Induced Morphology Changes

25 kg/cm², 125°C

14 kg/cm², 120°C



- No significant initial performance impact, but...
- ...but the PIMs developed into failure locations and reduced MEA lifetime
- Processing conditions were able to mitigate PIM development



Other Inhomogeneities

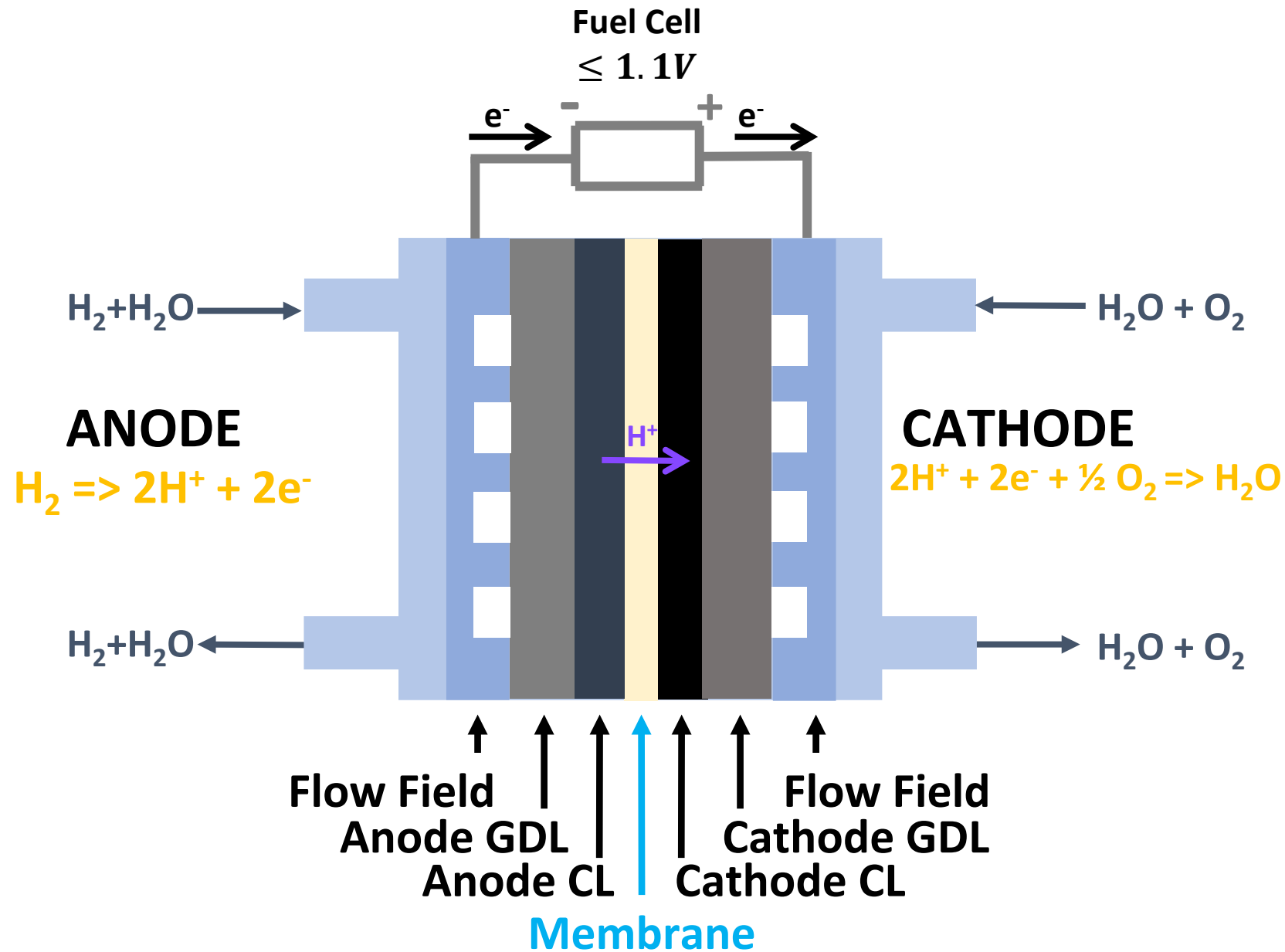
Similar work was conducted at NREL on:

- **Coating drops/blobs**
- **Catalyst layer**
 - **Voids**
 - **Thin spots**
 - **Thick spots**
- **Pinholes**
- **Trapped bubbles in membranes**

Fuel Cell vs. Electrolysis Cell Comparison of Material

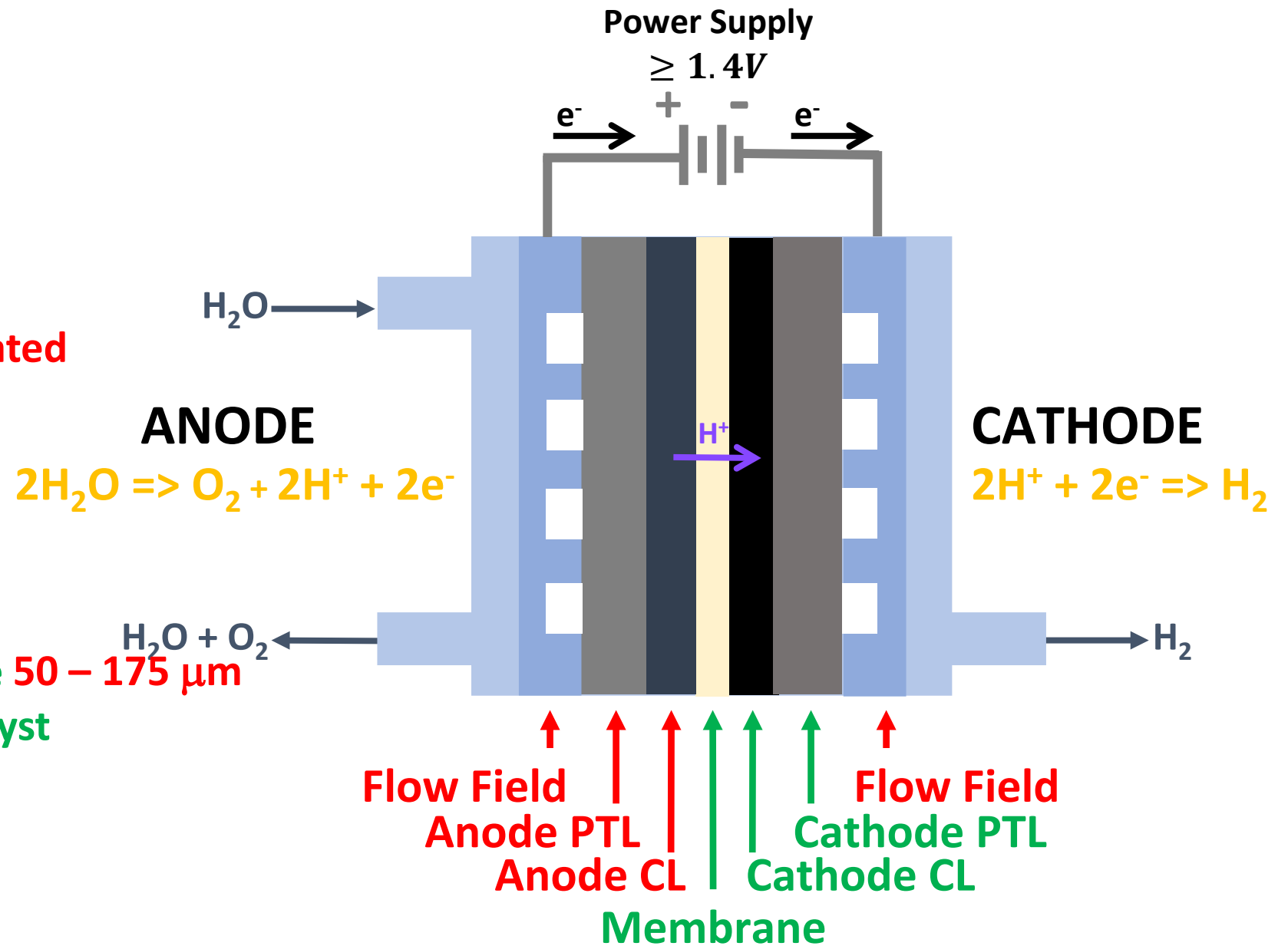
Fuel Cell

- Gas to electrical power generating $\leq 1.1\text{ V}$
- Graphite or coated metal flow-fields
- Carbon based porous gas diffusion media with microporous layers
- Carbon supported Pt catalyst layers
- Thin proton conductive membrane $\leq 25\ \mu\text{m}$



Electrolysis Cell

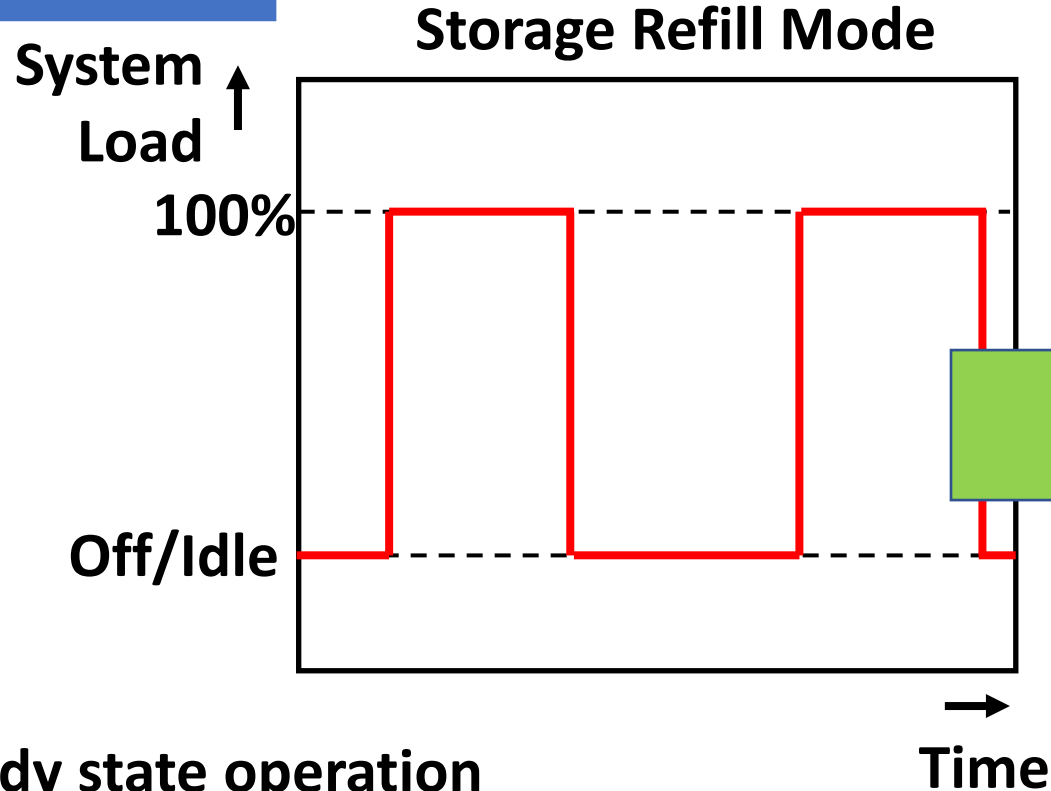
- Electric Power to Gas at Potentials $\geq 1.4\text{ V}$
- Titanium anode flow-field coated with PGM
- Sintered porous titanium material coated with PGM
- Unsupported IrO_2 anode catalyst layer
- Proton conductive membrane $50 - 175\ \mu\text{m}$
- Supported Pt/C cathode catalyst layer
- Untreated carbon paper
- Titanium or other bipolar cathode flow-field (based on anode material)



Future Electrolysis Systems

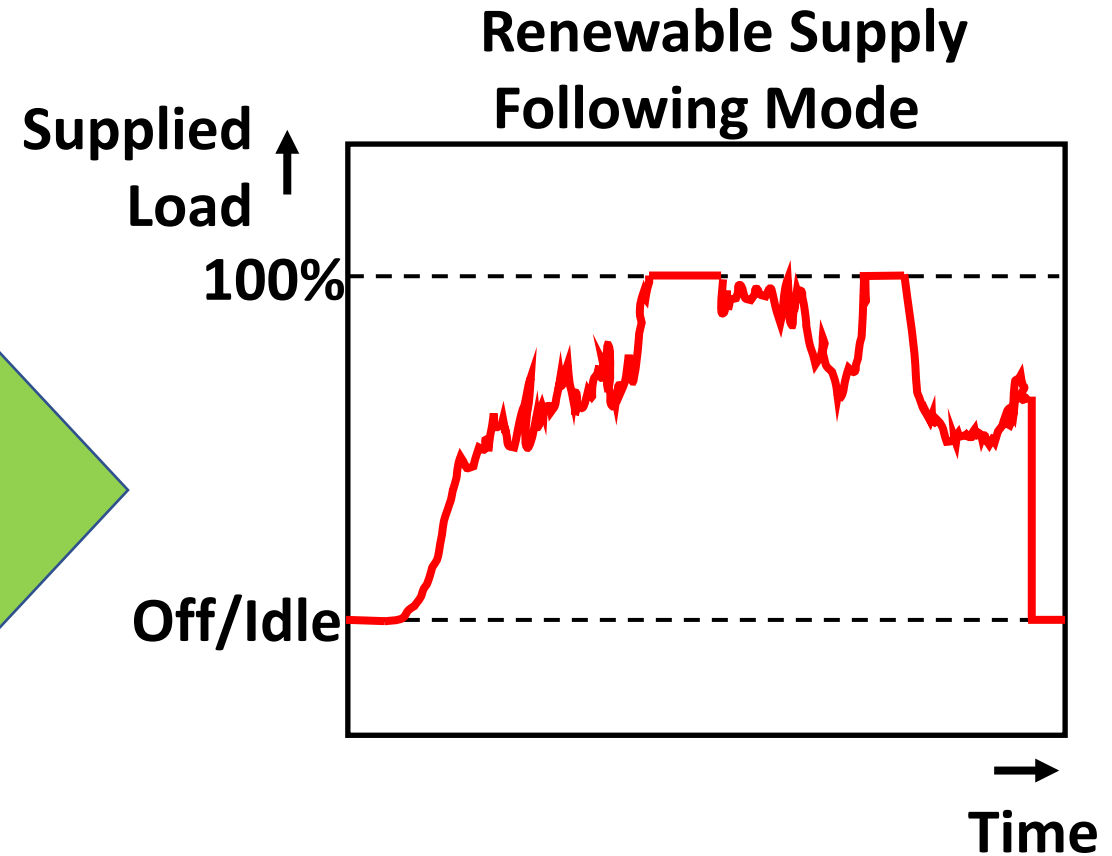
Operating Strategies

Existing Systems



- Steady state operation
- Turn system on at certain vessel pressure
- Refill system at 100% system power
- Switch system to off or idle

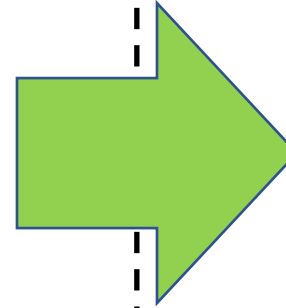
Future Systems



- Follow renewable energy supply
- Maybe cap high and low performance to minimize degradation

Existing Systems

- **2V @ 2A/cm²**
- **2-3 mg/cm² PGM catalyst loading on anode & cathode**
- **60k – 80k hours in commercial units**
- **Niche applications**
 - Life support
 - Industrial H₂
 - Power plants for cooling
- **\$3.7/kg H₂ production***



Future Systems

- **2V @ \geq 2A/cm²**
- **Thinner membranes**
- **Lower loadings**
- **\geq 80k hours**
- **Supply following Renewable & Net integrated applications**
 - Wind
 - Solar
 - Nuclear
- **\$2/kg H₂ production***

*High volume projection of hydrogen production for electrolysis:

<https://www.energy.gov/sites/prod/files/2017/10/f37/fcto-progress-fact-sheet-august-2017.pdf>

** K.Ayers, AMR Presentation PD094, 06/2014

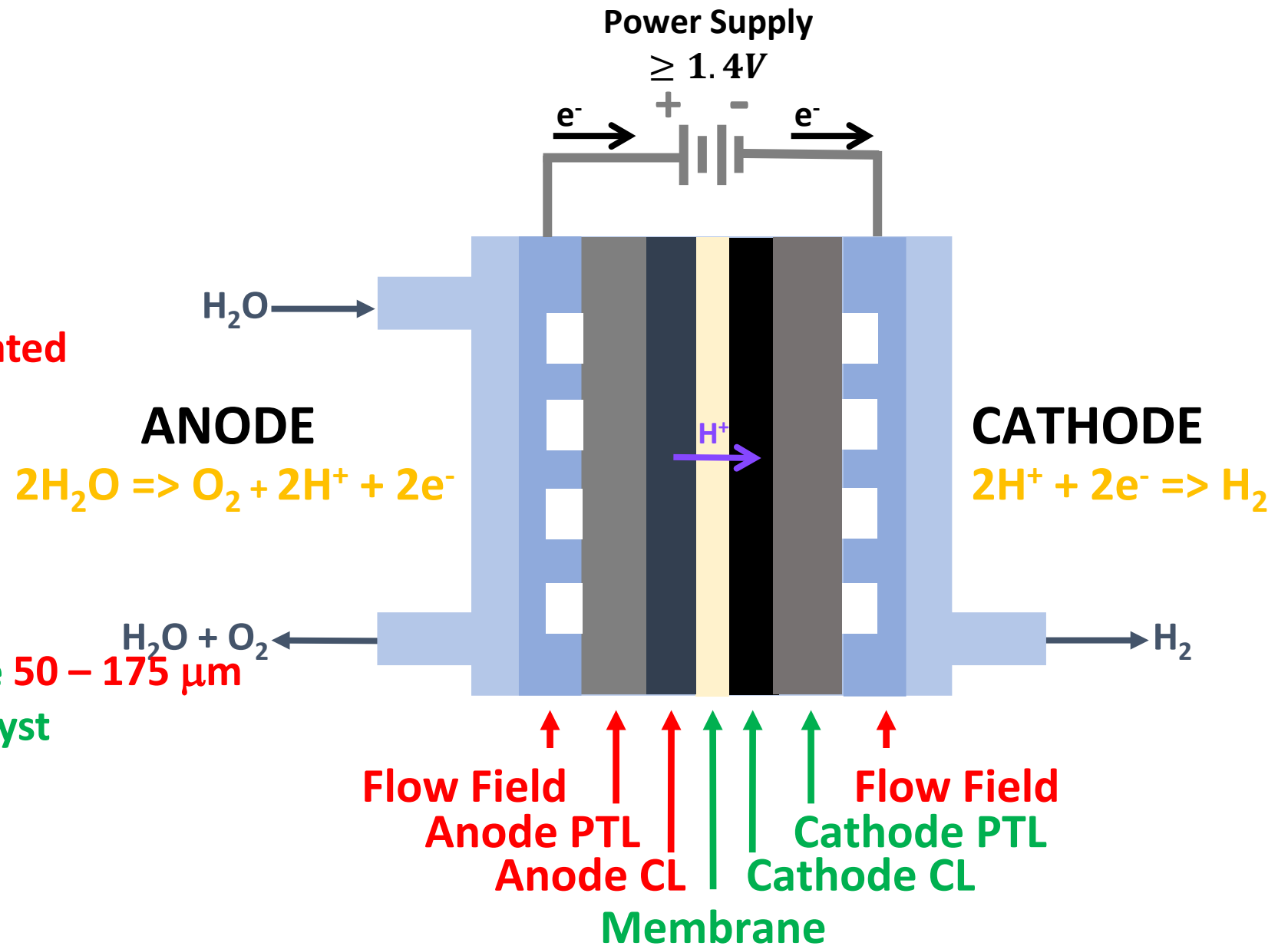
Discussion:

How can we port existing QC work over to LTE?

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Electrolysis Cell

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High potential requires materials with high corrosion resistance

- Titanium => TiOx passivation
 - ⇒ Thickness of oxide layer prior to coating or to install
 - ⇒ Contact resistance measurement?
- Titanium requires coatings
 - ⇒ Improve interface
 - ⇒ Protect functionality by preventing TiOx growth
 - ⇒ Loading of coating
 - ⇒ Coating continuity
 - ⇒ Thickness
 - ⇒ Voids
 - ⇒ Lamination

Electrolysis Cell

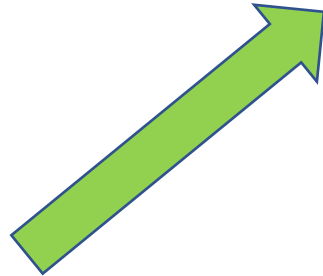
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High potential requires materials with high corrosion resistance

- Very different catalyst material
 - ⇒ Metal to oxide ratio
 - ⇒ not very reproducible standard material
 - ⇒ Catalyst Utilization
 - ⇒ no reliable ECSA measurement
 - ⇒ Catalyst Loading
 - ⇒ XRF
 - ⇒ In-plane resistance of electrode layer
 - ⇒ depends on fabrication method & ink formulation
- Catalyst layer thickness or voids can impact PTL coating durability
 - Exposure of PTL coating to very low pH
 - ⇒ Pt dissolution
 - ⇒ Loss of PTL functionality
 - ⇒ Local catalyst loading
 - ⇒ XRF mapping, optical 2D mapping methods

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- **Thicker membranes**
- **Operation may include high differential pressures**
 - $\Delta 30$ bar or higher
 - ⇒ **Creep through assembly or compression**
 - ⇒ **Hydrogen crossover**
 - ⇒ **Membrane reinforcement**
 - ⇒ **Membranes may include Gas Recombination Layers (GRC)**
 - ⇒ **Loading & Distribution**
 - ⇒ **XRF mapping**

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Electrolysis Cell

Stack Assembly Considerations

- **PTL**
 - Total thickness
 - Thickness variation within sheet
 - Sharp edges
- **Gasket thickness variations**
- **Membrane / Gasket creep due to high compression**
- **Particles / Debris inclusion**
- **Membrane swelling resulting in deformation / shearing**

Questions?

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