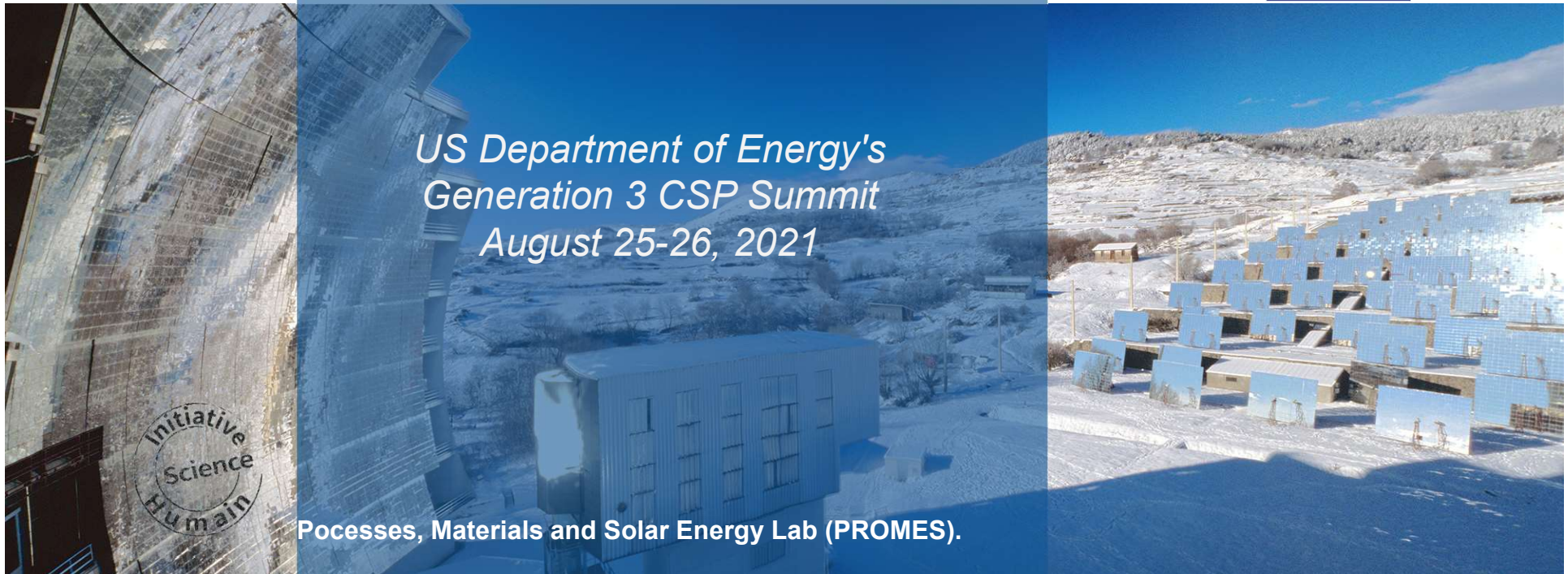




Fluidized bed-in-tube solar receiver and the « Next-CSP » solar loop.

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Generation 3 CSP Summit
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Processes, Materials and Solar Energy Lab (PROMES).

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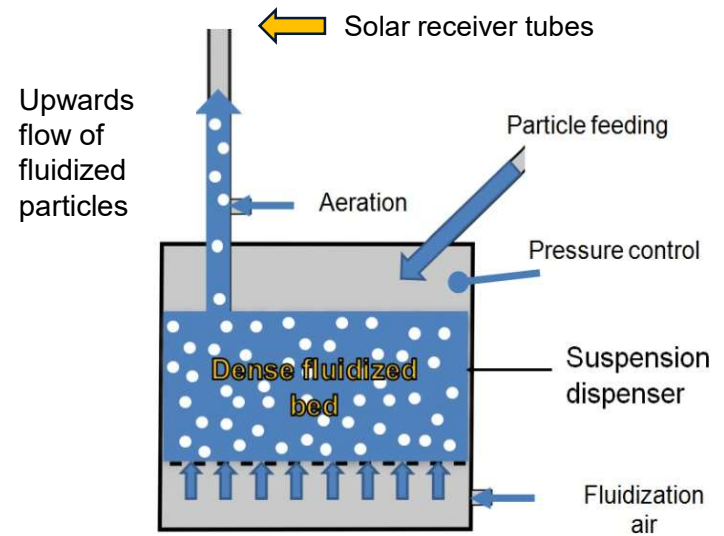
Concept

An upwards flow of fluidized particles is created inside the solar receiver tubes by increasing the pressure in the dispenser. A secondary aeration stabilizes the particle flow

Small size particles (<math><100 \mu\text{m}</math>) are used.

The tubes are made of refractory alloy.

Only 1 m-long (irradiated part) tubes have been tested before the Next-CSP EU project



Positioning of the fluidized bed technology



- Particles are well mixed in fluidized beds (small thermal gradient)
- Wall-to-bed heat transfer is efficient. FB heat exchanger can be applied
- Dust emission can be controlled because the particle loop is closed
- The concept is scalable



- The maximum solar flux on the tube walls is limited to $\sim 500 \text{ kW/m}^2$ due to wall material issue





Main objectives and challenges of the Next-CSP EU project

Main objectives

To design, construct, implement and test a complete prototype-scale ($>1 \text{ MW}_{\text{th}}$) particle CSP loop including a solar receiver, a storage, a heat exchanger and a hybrid gas turbine.

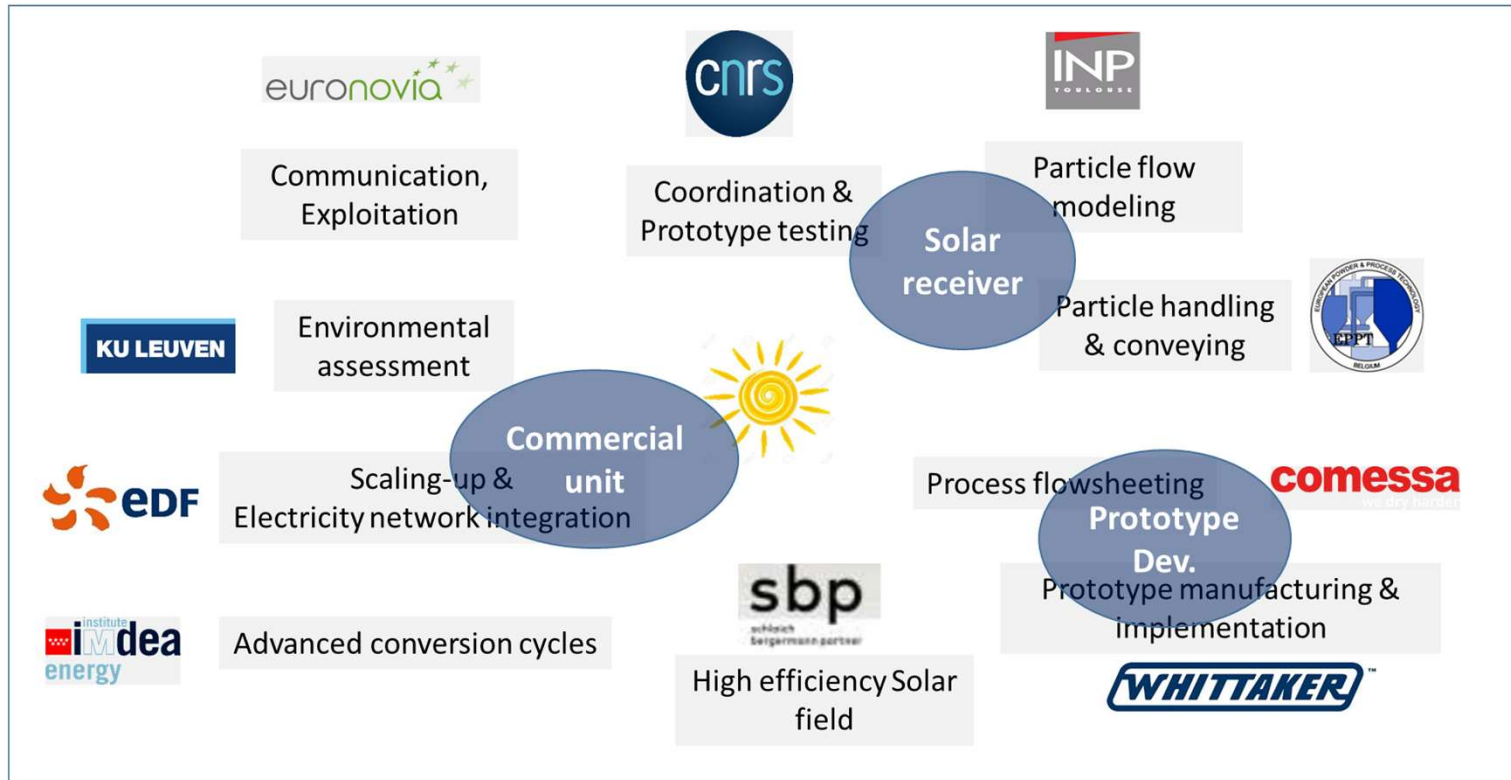
To identify the barriers to large scale development.

Main Challenges

- ✓ Particle flow regimes in dense phase inside the solar receiver tubes and associated heat transfer
- ✓ Manufacturing of the compartmented fluidized particle heat exchanger
- ✓ Integration of the components at the Themis solar tower focal area
- ✓ Control of the particle circulation in closed loop and particle conveying
- ✓ Choice of the most promising conversion cycle accounting for the technology particularities
- ✓ Solar receiver and system upscaling



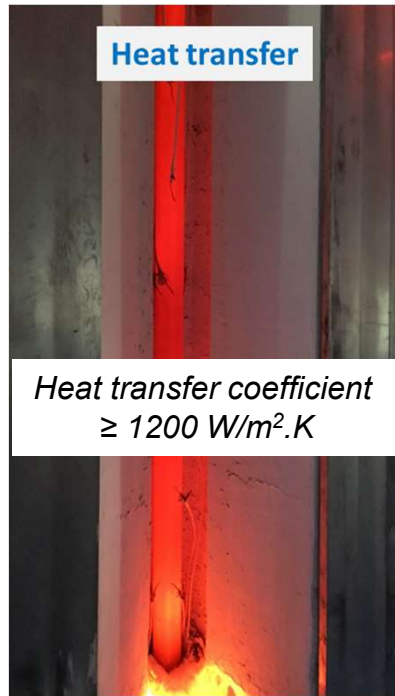
Contribution of the Next-CSP Consortium members



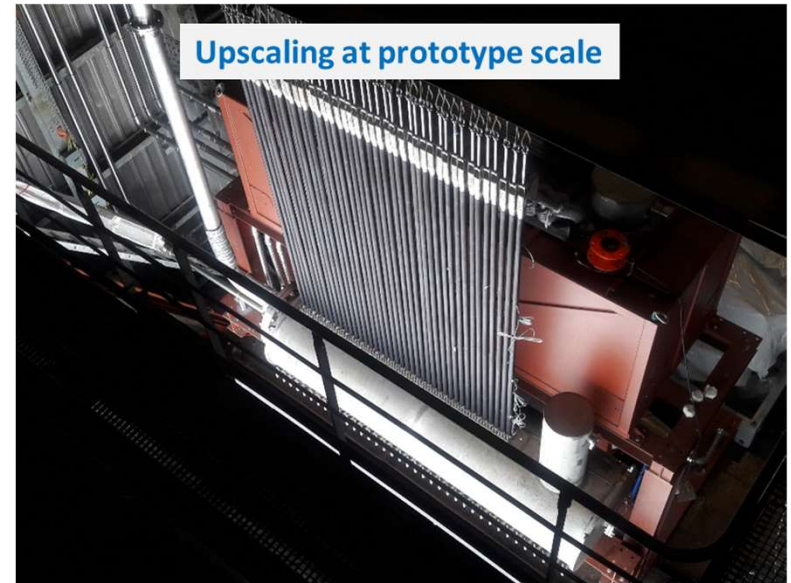
Critical components Solar receiver



Cold mockup
3-8m-long tubes



Hot mockup
1m-long tubes

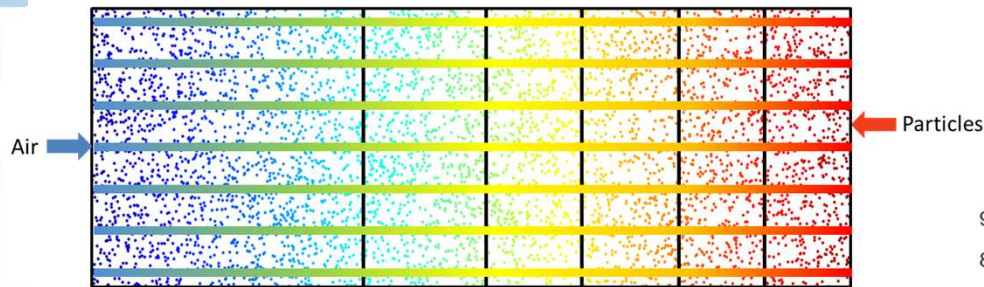


2.5 MW_{th} 3m-long solar receiver (40 tubes)



Critical components

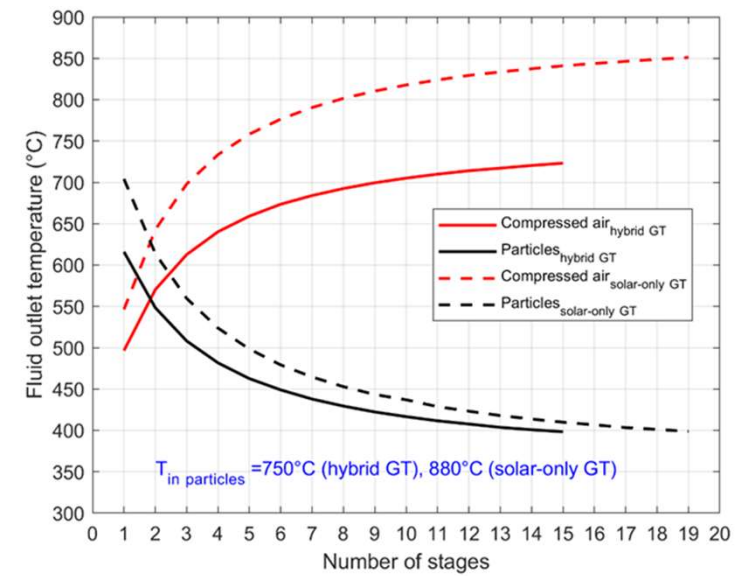
Heat exchanger



Multi-stage compartmented fluidized bed concept with compressed air in tubes

Approximately 15 stages for $30^{\circ}\text{C } \Delta T$
 ΔT = temperature difference between inlet particle and outlet air

Variation of air and particle temperature with the number of stages



Critical components

Particle conveying

Issue:

- The size of a single solar receiver is limited to approximately $50 \text{ MW}_{\text{th}}$ due to the limitation of the tube length (8 m).
- Cavity type is needed for thermal efficiency $\geq 80\%$

- **For a single tower**, only vertical elevation of the particles must be considered
- **For a multi-tower concept**, horizontal and vertical conveying are necessary



Critical components

Conversion cycle

Three options studied:



- Combined cycle
- Supercritical steam
- Supercritical CO₂

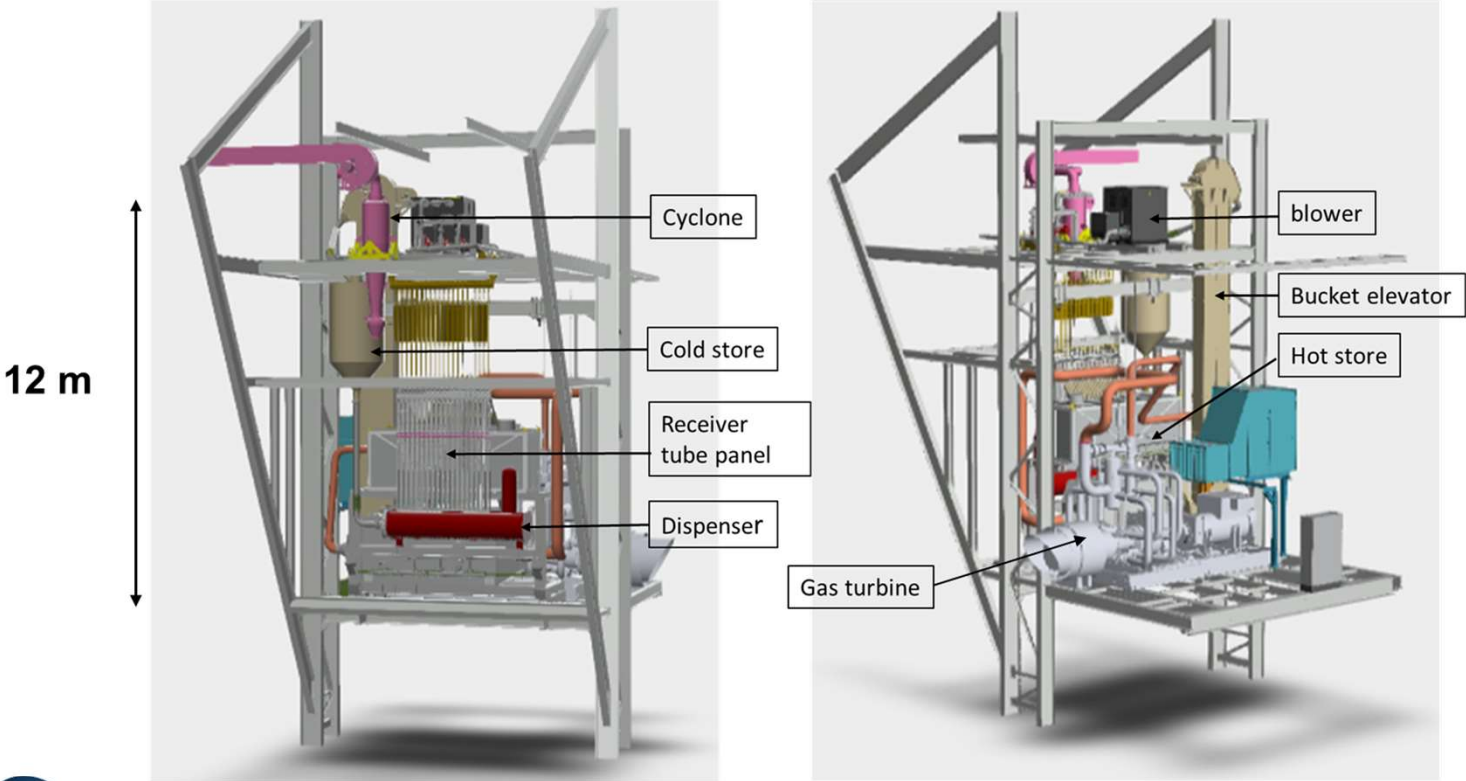
With cycle efficiency ~50%



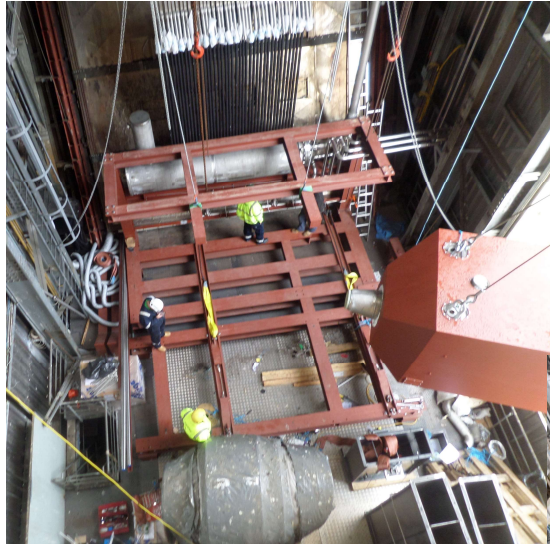


Prototype development

All the components are integrated atop the tower

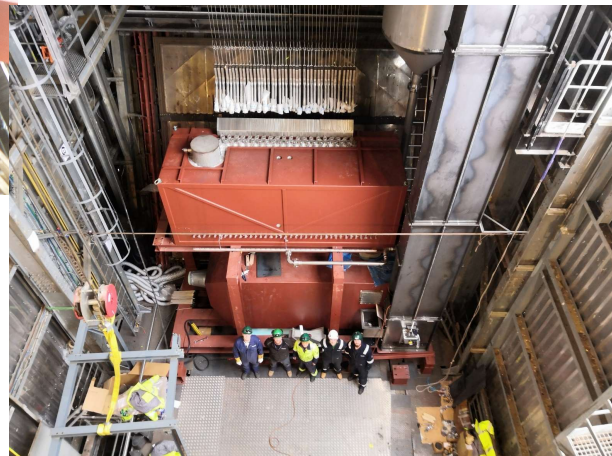


Prototype implementation



*Heat exchanger
lifted at the tower top*

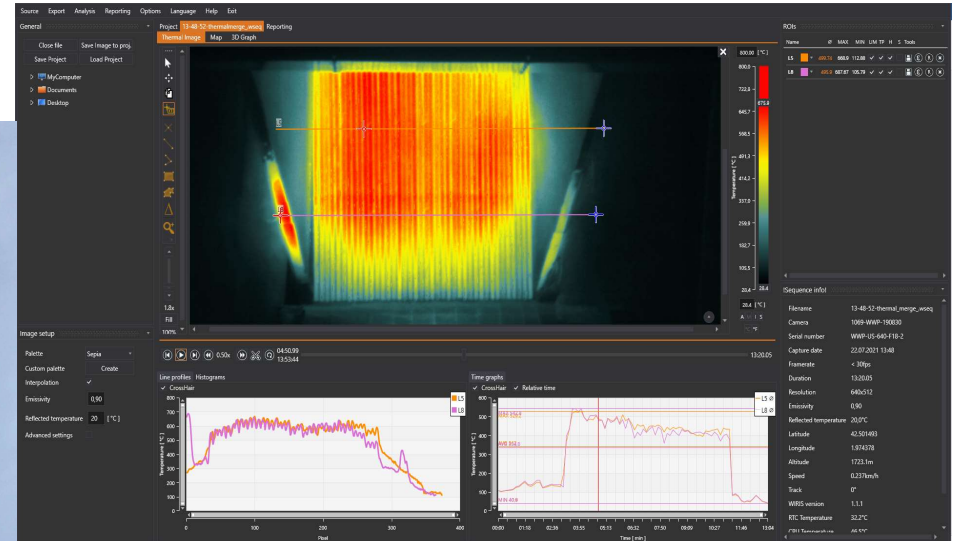
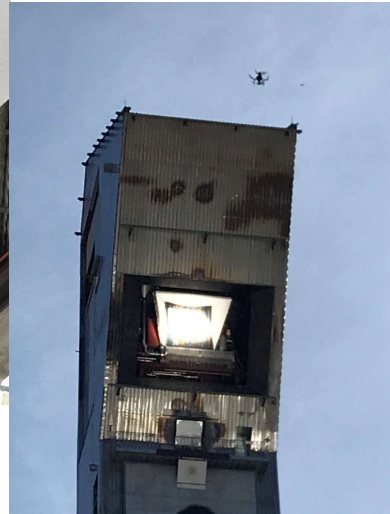
*The complete
particle loop*



*Pressurized air
connexion between
the heat exchanger
and the gas turbine*



Results of the first solar receiver test campaign

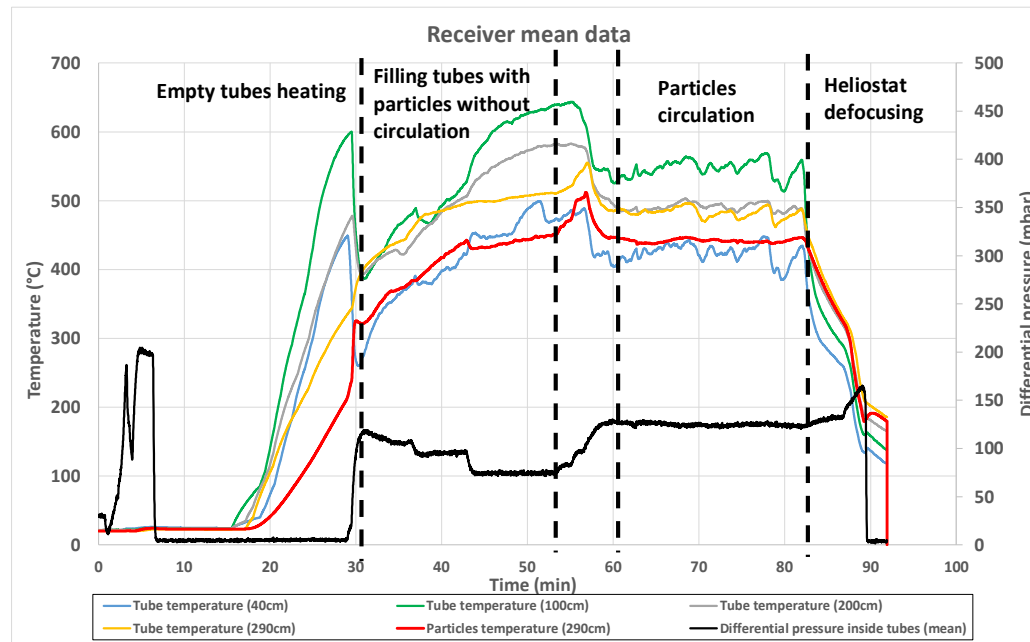


The solar receiver

*IR image of the tube temperature
(measured by a drone)*



Results of the first solar receiver test campaign



Particle mass flow rate:
0,6-3,5 kg/s

P_{solar} : **550-850 kW**

ΔT particle : **100-400°C**

Efficiency: **40-75%**



Lessons learned

- The instrumentation developed proved to be accurate and reliable
- Tuning aeration mass flow rate resulted in a precise control of particle mass flow rate
- Particle temperature increase as large as 400°C have been measured
- Solar receiver starting and shut down are very fast (10-15 minutes)
- Unexpected issue: large difference of solar flux distribution on tubes can result in particle circulation stop due to air velocity difference





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