



# DOE Bioenergy Technologies Office (BETO) 2021 Project Peer Review

## Integrated Reactive Catalytic Fast Pyrolysis System for Advanced Hydrocarbon Biofuels WBS 3.5.1.204

March 25, 2021

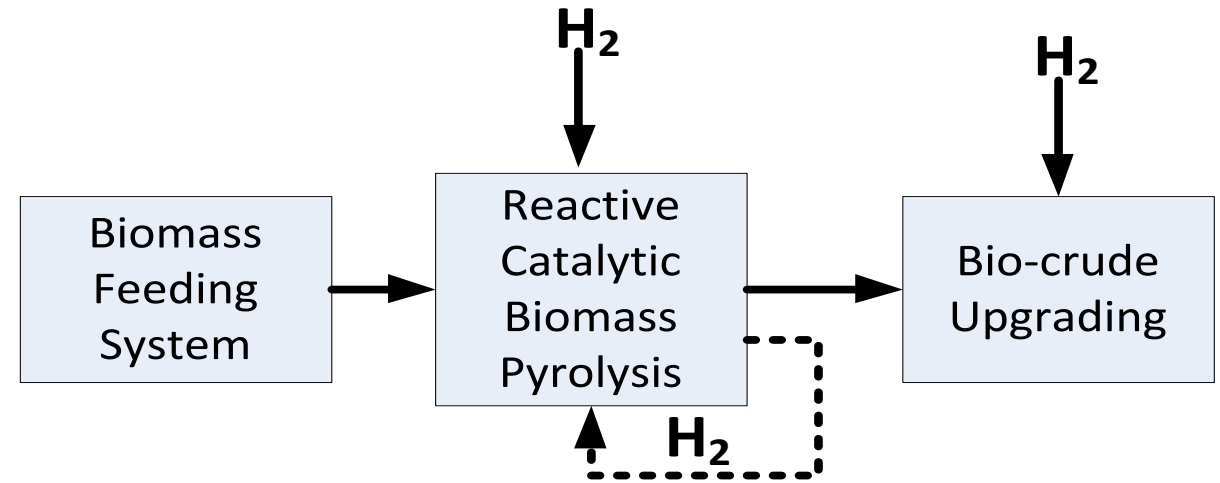
System Development and Integration  
Principal Investigator: David C. Dayton  
RTI International

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# Project Overview

## Project Goal

Design, fabricate, and operate an engineering-scale reactor system that can continuously maintain steady-state HDO activity to produce enough low oxygen content RCFP biocrude to support extensive upgrading studies and produce 100 gallons of drop-in renewable diesel



## Summary:

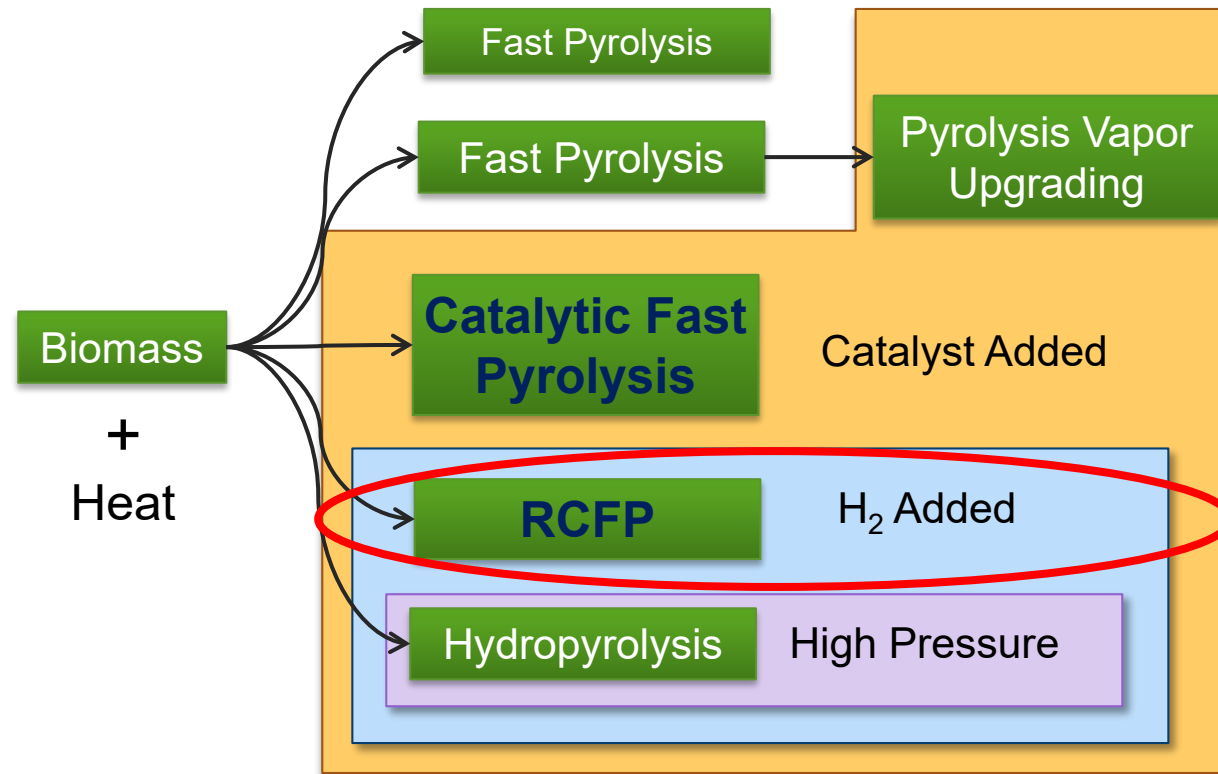
- 1) Design, fabricate, and install an engineering-scale (1-5 kg/hr) reactive catalytic fast pyrolysis (RCFP) reactor system
- 2) Scale up a fluidizable RCFP catalyst based on the formulation of commercially available extrudates
- 3) Optimize the process and maintain steady-state hydrodeoxygenation (HDO) catalyst activity to maximize biocrude yield and quality
- 4) Extensive upgrading studies to enhance the technical understanding of biocrude hydrotreating

## Targets

- Verify 50 mole %C yield in RCFP biocrude at engineering scale.
- Demonstrate that the renewable diesel pathway has 50% less GHG emissions compared to fossil-derived diesel.

# Overview - Pyrolysis Pathways for Advanced Biofuels

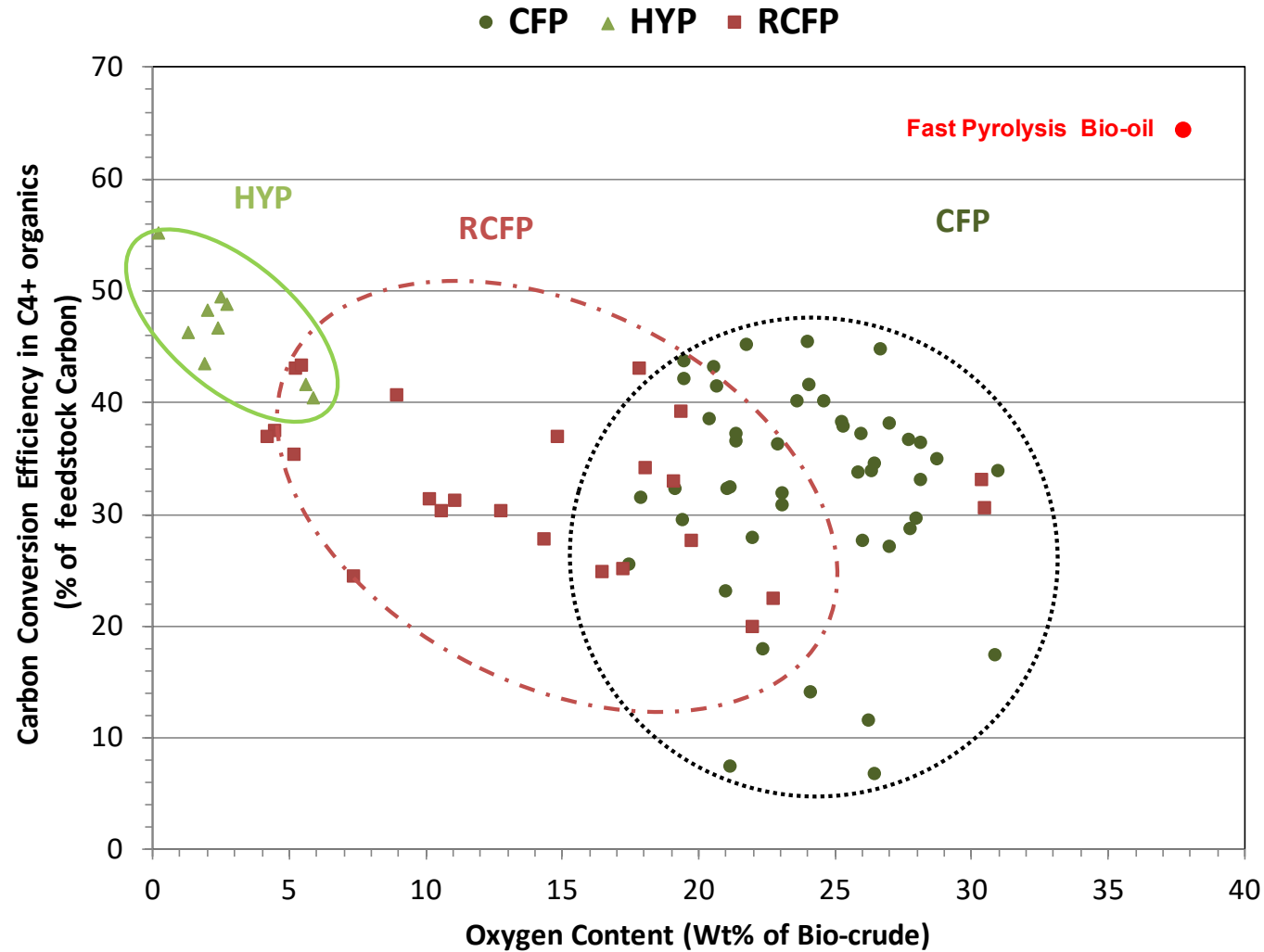
Application of catalysts to maximize yields and improve biocrude **quality** (oxygen content, chemical composition, thermal stability)



1. Mante, O. D., Dayton, D. C., Carpenter, J. R., Wang, K., & Peters, J. E. (2018), Pilot-scale catalytic fast pyrolysis of loblolly pine over  $\gamma\text{-Al}_2\text{O}_3$  catalyst. *Fuel*, 214, 569–579.
2. Cross, P.; Wang, K. G.; Weiner, J.; Reid, E.; Peters, J.; Mante, O.; Dayton, D. C., Reactive Catalytic Fast Pyrolysis of Biomass Over Molybdenum Oxide Catalysts: A Parametric Study. *Energy & Fuels* 2020, 34 (4), 4678-4684.

# Overview - Biocrude Yield vs. Quality

## Product Quality (wt% O) vs. Yield



Dayton, D.C., Wang, K., Peters, J.E. and Mante, O.D. Chapter 5 - Catalytic Biomass Pyrolysis with Reactive Gases, in *Fast Pyrolysis of Biomass: Advances in Science and Technology*. 2017, The Royal Society of Chemistry. p. 78-95.

# Management Approach - Overview

Project will be executed in three budget periods (BPs) with 12 tasks that will span the 39-month period of performance.

- BP1 - Initial Verification (3 months)
- BP2 - Design a continuous RCFP reactor system (9 months)
- BP3 - Fabricate the engineering-scale (1-5 kg/hr) RCFP reactor system for RCFP biocrude production and upgrading (27 months)

## Go/NoGo Decision Criteria

- GN1: Go/No-Go Decision Point (Month 3): Block Flow Data have been reviewed and verified, experiments to replicate baseline data witnessed and verified, goals and performance metrics established to track technical progress for the remainder of the proposed project, and project goals and objectives are in alignment with BETO's programmatic goals.
- GN2: Go/No-Go Decision Point (Month 12):
  - Approved Engineering-scale Design for Fabrication
  - Fluidizable Catalyst: Demonstrated > 45 mole% C efficiency in C<sub>4</sub><sup>+</sup> products with less than 15 wt% oxygen in RCFP biocrude.

Final Project Goal: Biocrude upgrading to produce 100 gallons of a diesel blendstock to produce a 50/50 blend that meets ASTM D975 specifications. \$3.00 MFSP from TEA and 50% GHG reduction from LCA

# Management Approach– Task Structure

## **BP1 (Months 1–3)**

**Task 1—Initial Verification (Months 1–3)**

## **GN1**

## **BP2 (Months 4–12)**

**Task 2—Preliminary Design of Engineering Scale RCFP Unit (M4–M6)**

**Subtask 2.1—Process Flow Diagram**

**Subtask 2.2—Process Design Basis**

**Subtask 2.3 – Preliminary Technoeconomic Analysis**

**Task 3—Detailed Engineering Design (M6–M12)**

**Subtask 3.1—Design Review and Process Hazard Analysis**

**Task 4—RCFP Catalyst Scaleup (M4–M12)**

**Subtask 4.1—Fluidizable RCFP Catalyst Development**

**Subtask 4.2—Lab-scale Catalyst Evaluations**

**Task 5—BP2 Project Management (M4–M12)**

**Subtask 5.1—Interim Verification**

## **GN2**

## **BP3 (Months 13–39)**

**Task 6—RCFP Unit Fabrication (M13–M18)**

**Subtask 6.1—Factory Acceptance Test**

**Task 7—RCFP Unit Installation and Commissioning (M19–M21)**

**Task 8—RCFP Catalyst Production (M13–M21)**

**Subtask 8.1—Fluidizable RCFP Catalyst Production**

**Subtask 8.2—Fluidizable RCFP Catalyst Performance Testing**

**Task 9—RCFP Bio-crude Production (M22–M33)**

**Subtask 9.1—RCFP Unit Optimization**

**Task 10—RCFP Bio-crude Upgrading to Biofuel Blendstock (M22–M37)**

**Subtask 10.1—Biofuel Characterization**

**Subtask 10.2 – Catalyst Characterization**

**Task 11—Process Modeling (M32–M38)**

**Subtask 11.1—TEA**

**Subtask 11.2—LCA**

**Task 12—BP3 Project Management**

# Management Approach – Milestones

|                | Milestone   | Month |
|----------------|---|-------|
| <b>M2.1</b>    | Preliminary design package will form the basis of a request for proposals to find a vendor for detailed engineering in Task 3 and unit fabrication in Task 6. | 6     |
| <b>M3.1</b>    | Complete RCFP unit design package.  | 12    |
| <b>M3.1.1</b>  | Complete process hazard analysis and document recommended design changes.   | 11    |
| <b>M4.1</b>    | Develop method to scale up fluidizable RCFP catalyst.   | 12    |
| <b>M4.1.1</b>  | Finalize methods for catalyst scale-up.   | 9     |
| <b>M6.1</b>    | Complete fabrication of RCFP unit for delivery and installation at RTI.   | 16    |
| <b>M6.1.1</b>  | Verify that all major component specifications are met and basic functions of the system work.  | 17    |
| <b>M7.1</b>    | Install engineering-scale RCFP unit.  | 21    |
| <b>D8.1</b>    | Deliver fluidizable RCFP catalyst   | 15    |
| <b>M9.1</b>    | Complete continuous RCFP biocrude production.   | 30    |
| <b>M9.1.1</b>  | Determine operating conditions for maximum biocrude yields  | 25    |
| <b>M10.1</b>   | Complete at least 100 uninterrupted hours of RCFP biocrude upgrading.   | 33    |
| <b>M10.2</b>   | Complete at least 500 cumulative hours of RCFP biocrude upgrading.  | 36    |
| <b>M10.1.1</b> | Develop characterization protocols for biocrude and upgraded products.  | 22    |
| <b>M11.1</b>   | Techno-economic analysis (TEA) and life-cycle assessment (LCA) of a 2,000 TPD nth RCFP plant  | 36    |

# Initial Verification

## Verification Criteria :

Validate technical data, performance metrics, and targets for the proposed research.

- RCFP C<sub>4</sub><sup>+</sup> yields > 45 mole%C with less than 15 wt% O in biocrude
- Review RCFP biocrude upgrading results

## Pre-read Documents:

1. Revised Block Flow Data
2. Revised Statement of Project Objectives
3. RTI Publications:

Cross, P.; Wang, K. G.; Weiner, J.; Reid, E.; Peters, J.; Mante, O.; Dayton, D. C., Reactive Catalytic Fast Pyrolysis of Biomass Over Molybdenum Oxide Catalysts: A Parametric Study. *Energy & Fuels* 2020, 34 (4), 4678-4684.

Dayton, D.C., et al., CHAPTER 5 Catalytic Biomass Pyrolysis with Reactive Gases, in *Fast Pyrolysis of Biomass: Advances in Science and Technology*. 2017, The Royal Society of Chemistry. p. 78-95.

Wang, K., Dayton, D., Peters, J. E. & Mante, O. D. Reactive catalytic fast pyrolysis of biomass to produce high-quality bio-crude. *Green Chemistry*, (2017) 19(14): p. 3243-3251.

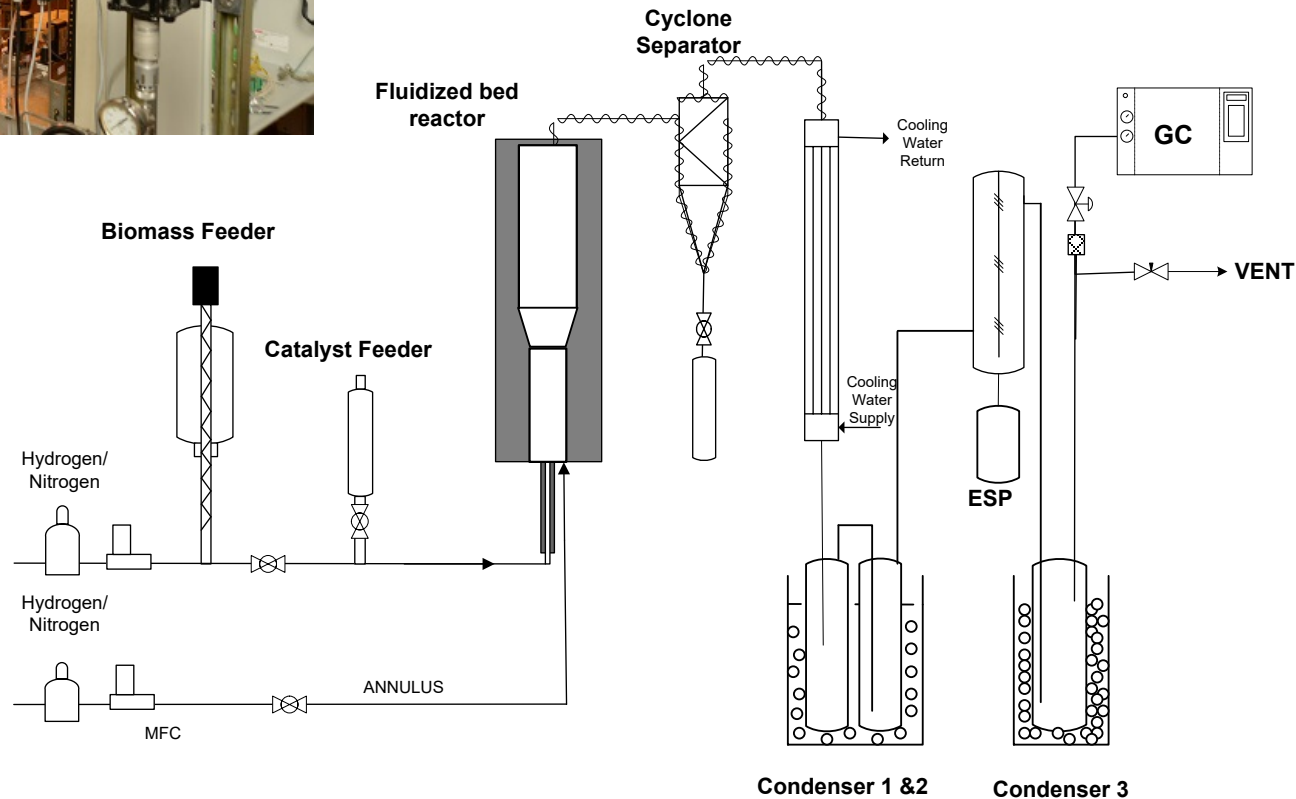
Mante, O. D.; Dayton, D. C.; Gabrielsen, J.; Ammitzboll, N. L.; Barbee, D.; Verdier, S.; Wang, K. G., Integration of catalytic fast pyrolysis and hydroprocessing: a pathway to refinery intermediates and "drop-in" fuels from biomass. *Green Chemistry* 2016, 18 (22), 6123-6135



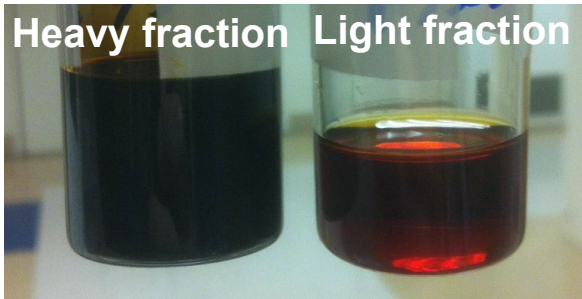
# Process Development and Biocrude Production



- 2.5" fluidized bed reactor with 4" disengagement zone
- Biomass feeding rate: 2-5 g/min
- Liquid collection: 3 condensers and 1 ESP
- Non-condensable gases analyzed by on-line microGC
- Liquid product analyzed by Karl Fischer titration, elemental analysis, GC/MS, etc.



Heavy fraction Light fraction



# Biocrude Upgrading - Hydrotreating



## Biocrude Upgrading Goals:

- Steady-state deoxygenation activity, hydrogen demand, and process severity as a function of biocrude quality (wt%O)
- Long-term operation to determine catalyst stability and lifetime (500-1000 hrs)

## Biocrude upgrading Options:

- Process whole biocrude in one or multiple steps
- Refinery integration and co-processing strategies
- Fractionate biocrude and process each fraction separately

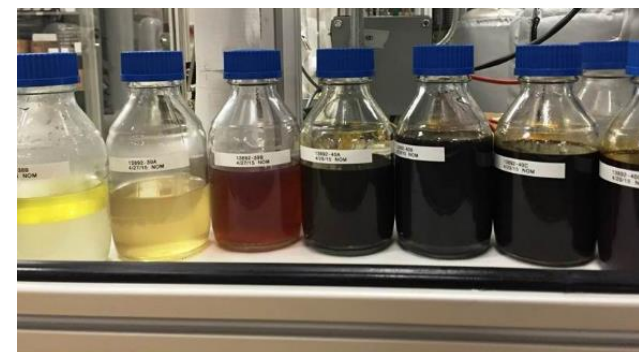
## Challenges:

- Reactor plugging
- Process severity correlated to biocrude composition

### UNIT OPERATIONS

- Oil feed system including pumps and flow control
- Gas feed system
- Reactor system
- Separator system
- Gas and liquid sampling system

Reactor volume - 350 mL  
Catalyst volume - 20 to 250 mL  
Design temperature: 450C  
Max. operating temperature: 430C  
Max. operating pressure: 170 bar (2500 psig)



Demonstrate a direct biomass liquefaction advanced biofuels pathway that produces a low-oxygen content, thermally stable biocrude intermediate that can be upgraded to hydrocarbon biofuels in a standalone biorefinery or co-processed in an existing petroleum refinery.

## Technology Highlights:

- Hydrogen in the pyrolysis reactor improves bio-crude yield and quality while reducing char and coke formation
- Low pressure process avoids potential operational issues feeding biomass across a pressure boundary
- RCFP biocrude intermediate does not foul or plug the hydrotreating reactor during upgrading.

The integrated RCFP/Upgrading process has the potential to reduce biofuels production cost with a novel, low-severity in situ CFP process to convert lignocellulosic biomass to hydrocarbon fuels. This directly supports the DOE/BETO goal to validate an nth plant modeled MFSP of \$3/GGE (2014\$) for a pathway to hydrocarbon biofuel with GHG emissions reduction of 50% or more compared to petroleum-derived fuel.

# RCFP Biocrude Production and Upgrading

12-L RCFP biocrude produced in 2" FBR over 10 months

Average Hydrogen Consumption: 2.3 wt% Biomass

## Reaction Conditions

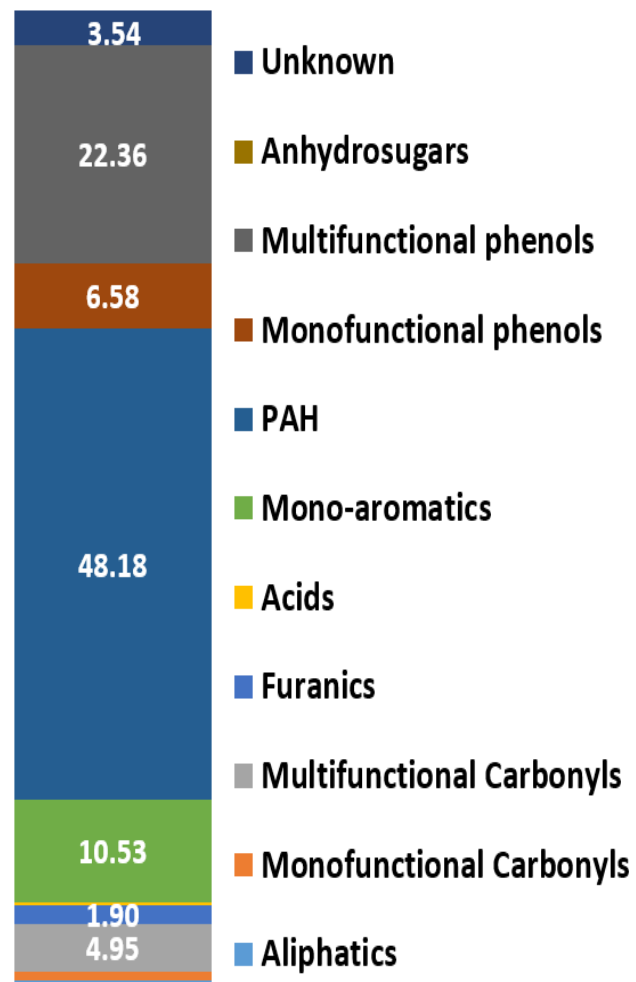
Catalyst: Mo/Al<sub>2</sub>O<sub>3</sub>

Hydrogen: 80 vol%

Temperature: 460°C

|  | Carbon Balance* | Mass Balance |
|--|-----------------|--------------|
| Aqueous                                | 2.5             | 27.4         |
| Organic (C <sub>4</sub> <sup>+</sup> ) | 43.0            | 19.6         |
| <i>Liquid Bio-crude</i>                | 26.4            | 15.9         |
| <i>C4-C6</i>                           | 16.6            | 3.7          |
| Gas                                    | 26.8            | 13.1         |
| Char+Coke                              | 30.1            | 35.9         |
| Total                                  | 102.4           | 96.0         |

## RCFP Biocrude Composition (GC-MS Area%)

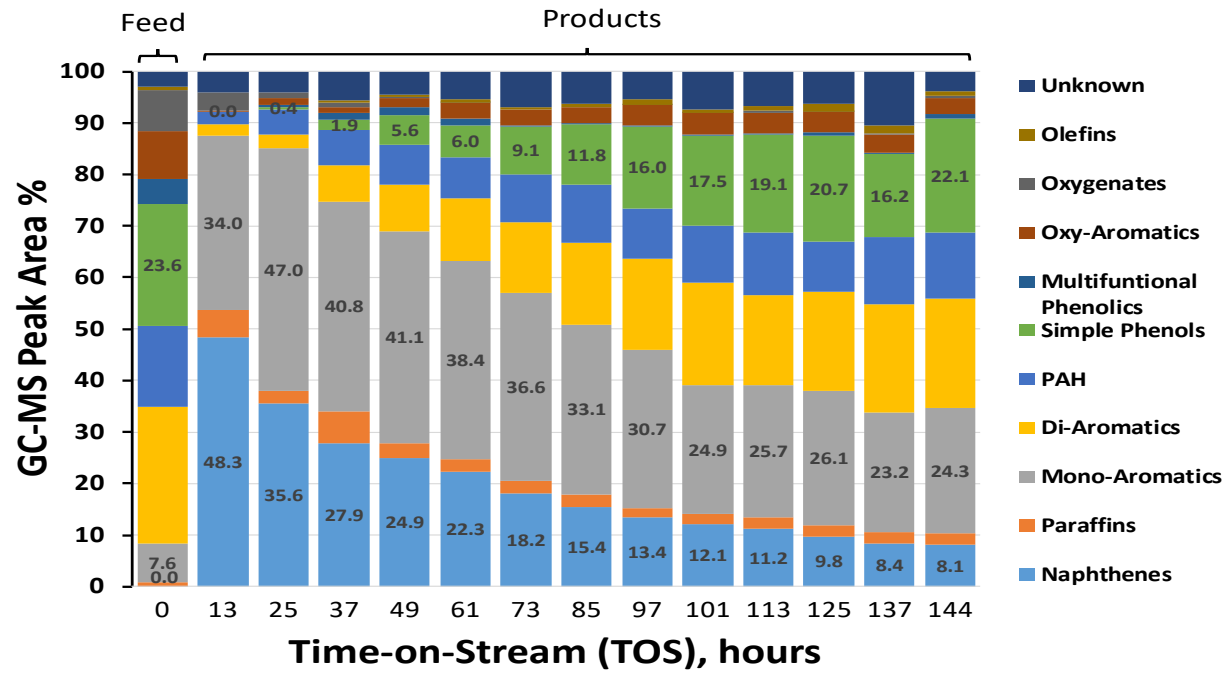
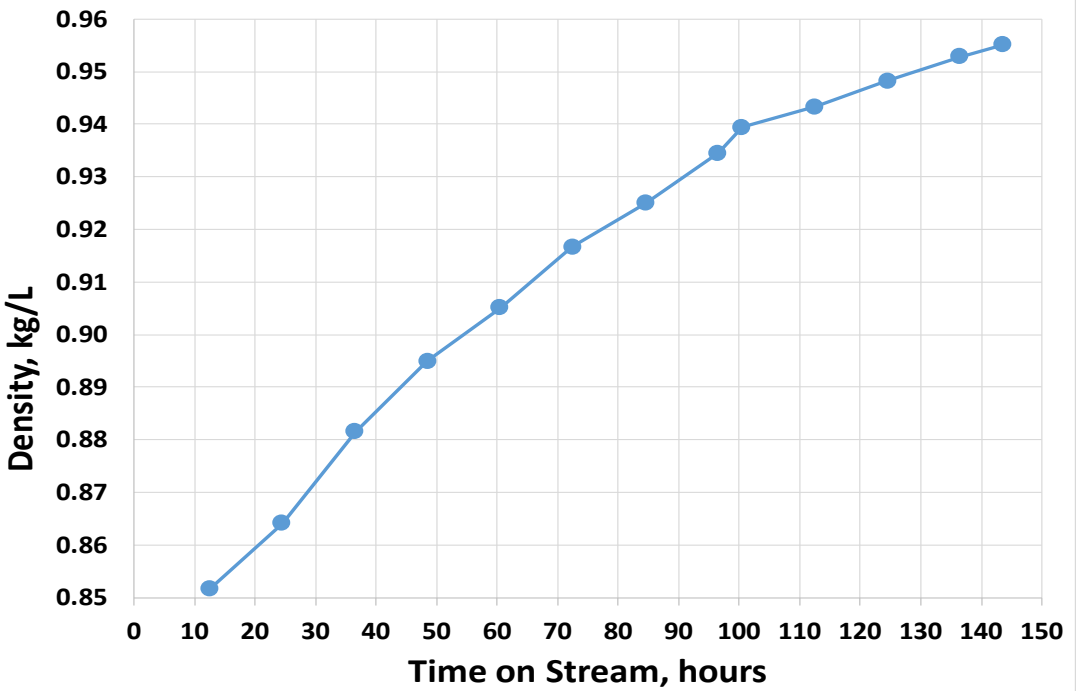
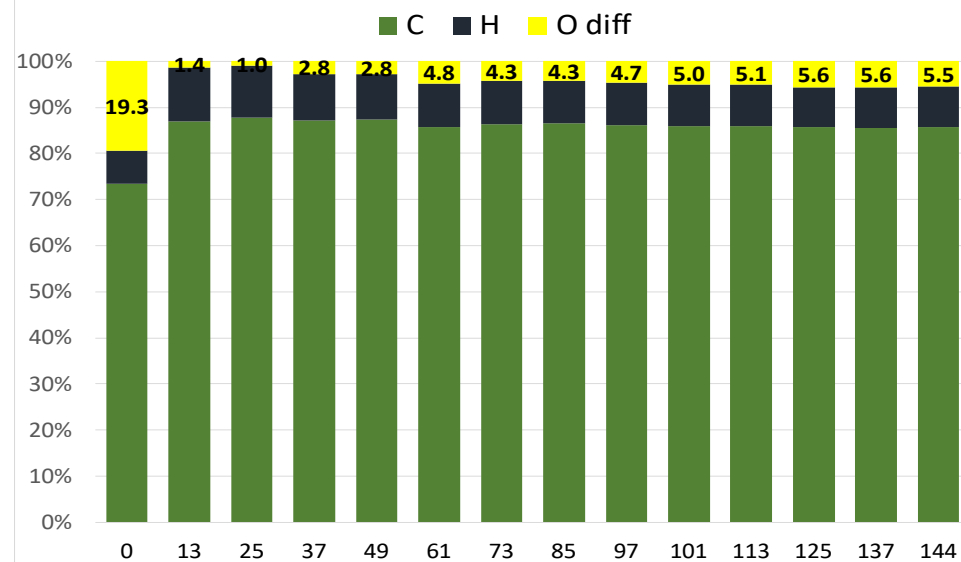


### Elemental Properties

| Properties    |      |
|---------------|------|
| Moisture, wt% | 8.5  |
| C wt%, dry    | 73.2 |
| H wt%, dry    | 7.3  |
| N wt%, dry    | 0.2  |
| O (by diff)   | 19.3 |

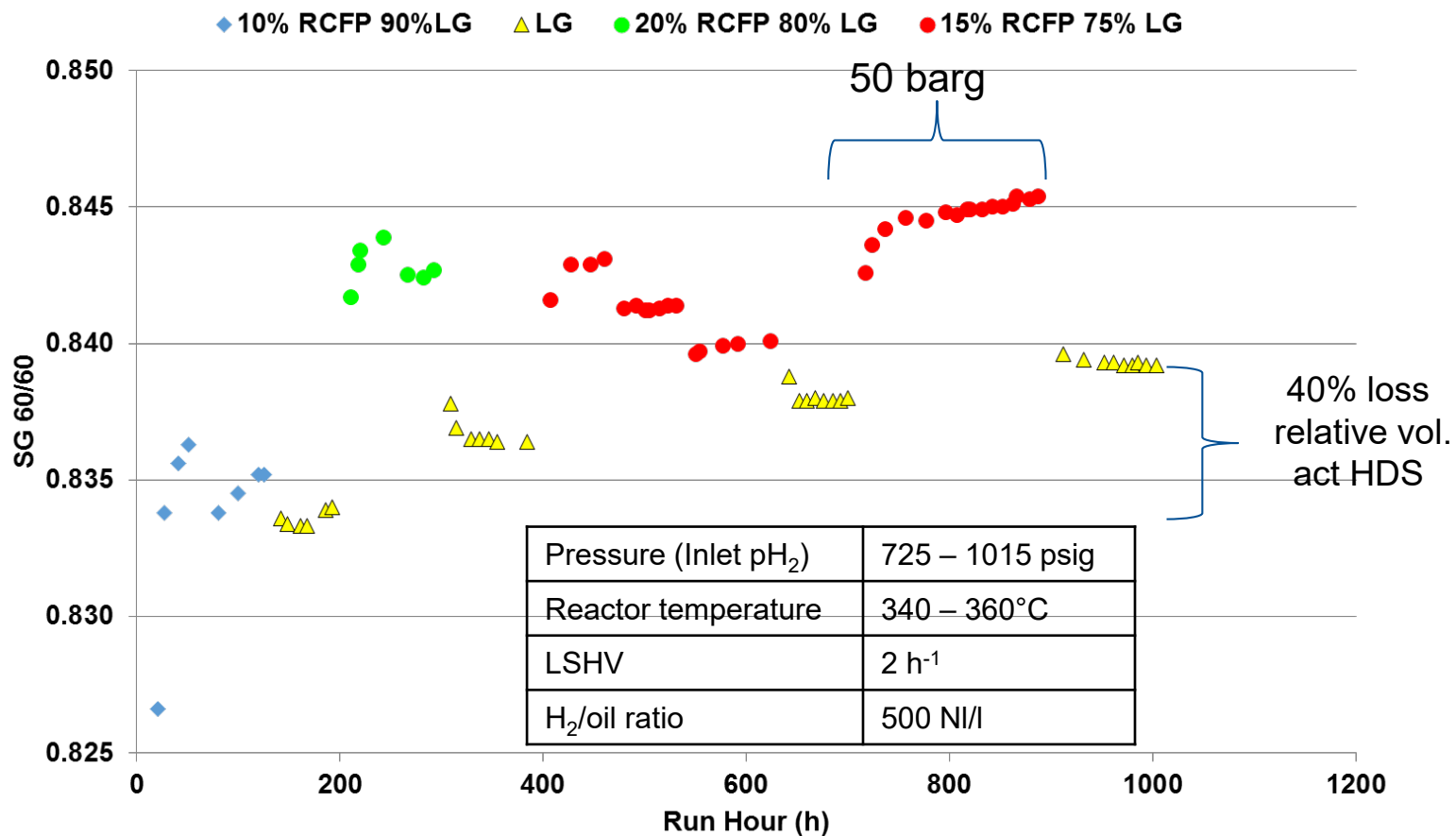
# RFCP Biocrude Upgrading: Physico-chemical Properties

|                                  |        |
|----------------------------------|--------|
| Catalyst                         | TK-341 |
| H <sub>2</sub> Flow Rate (sccm)  | 3300   |
| Feed Rate (g/h)                  | 62     |
| Pressure (psig)                  | 2000   |
| Average Temperature (°C)         | 300    |
| LHSV (h <sup>-1</sup> )          | 0.31   |
| H <sub>2</sub> /oil ratio (NI/I) | 3300   |



# RCFP Biocrude Co-processing with Light GasOil

| Analysis      | Unit   | LG     | RCFP  | 10/90 RCFP/LG | 15/85 RCFP/LG | 20/80 RCFP/LG |
|---------------|--------|--------|-------|---------------|---------------|---------------|
| SG at 60/60°F |        | 0.8541 | 1.005 | 0.8667        | 0.8726        | 0.8782        |
| O             | wt %   | -      | 9.65  | -             | -             | 2.17          |
| S             | wt %   | 1.30   | 0.001 | 1.14          | 1.04          | 1.01          |
| N             | wt ppm | 148    | 425   | 165           | 180           | 201           |
| H             | wt %   | 13.09  | 8.28  | 12.59         | 12.43         | 12.18         |



# Summary

- Design, fabricate, and operate an engineering-scale reactor system (1-5 kg/hr) that can continuously maintain steady-state HDO activity
- Scale up a fluidizable RCFP catalyst based on the formulation of commercially available extrudates
- Optimize the RCFP process and maintain steady-state hydrodeoxygenation (HDO) catalyst activity to maximize biocrude yield and quality
- Produce enough low oxygen content RCFP bio-crude to support extensive upgrading studies.
- Produce 100 gallons of diesel blendstock that meets ASTM D975 specifications
- Support DOE/BETO Program Goal to validate an nth plant modeled MFSP of \$3/GGE (2014\$) for a pathway to hydrocarbon biofuel with GHG emissions reduction of 50% or more compared to petroleum-derived fuel.

# Integrated Reactive Catalytic Fast Pyrolysis System for Advanced Hydrocarbon Biofuels (DE-EE0008918)

|  |  |
|--|--|
| <p><b>Timeline</b></p> <ul style="list-style-type: none"> <li>• Award Date: 10/1/2019</li> <li>• Award Negotiations Concluded: 10/6/2020</li> <li>• Initial Verification Meeting – January 11-15, 2021</li> <li>• Proposed Budget Period 1 end date: 3/31/2021</li> <li>• Authorization to move into BP2: TBD</li> <li>• Budget Period 2: 4/1/2021 – 3/31/2022</li> <li>• Budget Period 3: 4/1/2022 – 9/30/2023</li> </ul> | <p><b>Project Goal</b></p> <p>Design, fabricate, and operate an engineering-scale (1-5 kg/hr) reactor system that can continuously maintain steady-state HDO activity to produce enough low oxygen content RCFP bio-crude to support extensive upgrading</p> <p><b>End of Project Milestone</b></p> <p>Advanced biofuels technology that integrates reactive catalytic biomass pyrolysis and hydrotreating to produce 100 gallons of renewable diesel blendstock that meets ASTM D975 specifications</p> |
|--|--|

**Partners**

RTI International: Project lead, RCFP process development and biocrude upgrading, project management

Haldor Topsoe, A/S: RCFP catalyst scaleup, biocrude upgrading support, and hydrotreating catalyst provider

| Budget       | Federal            | Cost Share       | Total Costs        | FY20Q1 Actuals  |                |
|--------------|--------------------|------------------|--------------------|-----------------|----------------|
|              |                    |                  |                    | Federal         | Cost Share     |
| BP1          | \$54,126           | \$13,532         | \$57,658           | \$14,405        | \$3,601        |
| BP2          | \$428,863          | \$107,216        | \$536,079          | ---             | ---            |
| BP3          | \$1,873,675        | \$468,419        | \$2,342,094        | ---             | ---            |
| <b>Total</b> | <b>\$2,356,665</b> | <b>\$589,166</b> | <b>\$2,945,831</b> | <b>\$14,405</b> | <b>\$3,601</b> |

**FY19 Bioenergy Technologies Office Multi-Topic Funding Opportunity Announcement**

**Area of Interest 4: Systems Research of Hydrocarbon Biofuel Technologies**

*Verify innovative technologies at engineering-scale to enable cost-competitive integrated biofuels technology pathways.*



## Additional Slides

# Responses to Previous Reviewers' Comments

- Not applicable

# Publications, Patents, Presentations, Awards, and Commercialization

- Publications: none
- Patents: none
- Presentations:
  - Virtual Verification Meeting, Integrated Reactive Catalytic Fast Pyrolysis System for Advanced Hydrocarbon Biofuels (DE-EE0008918), RTI International, RTP, NC. January 11, 2021