



Solar thermochemical reactor design space overview

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Unlocking Solar Thermochemical Potential: Receivers,
Reactors, and Heat Exchangers Workshop

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Solar thermochemical reactors



concentrated
solar
irradiation

absorbed
heat

solar
thermochemical
reactor

reactants

products

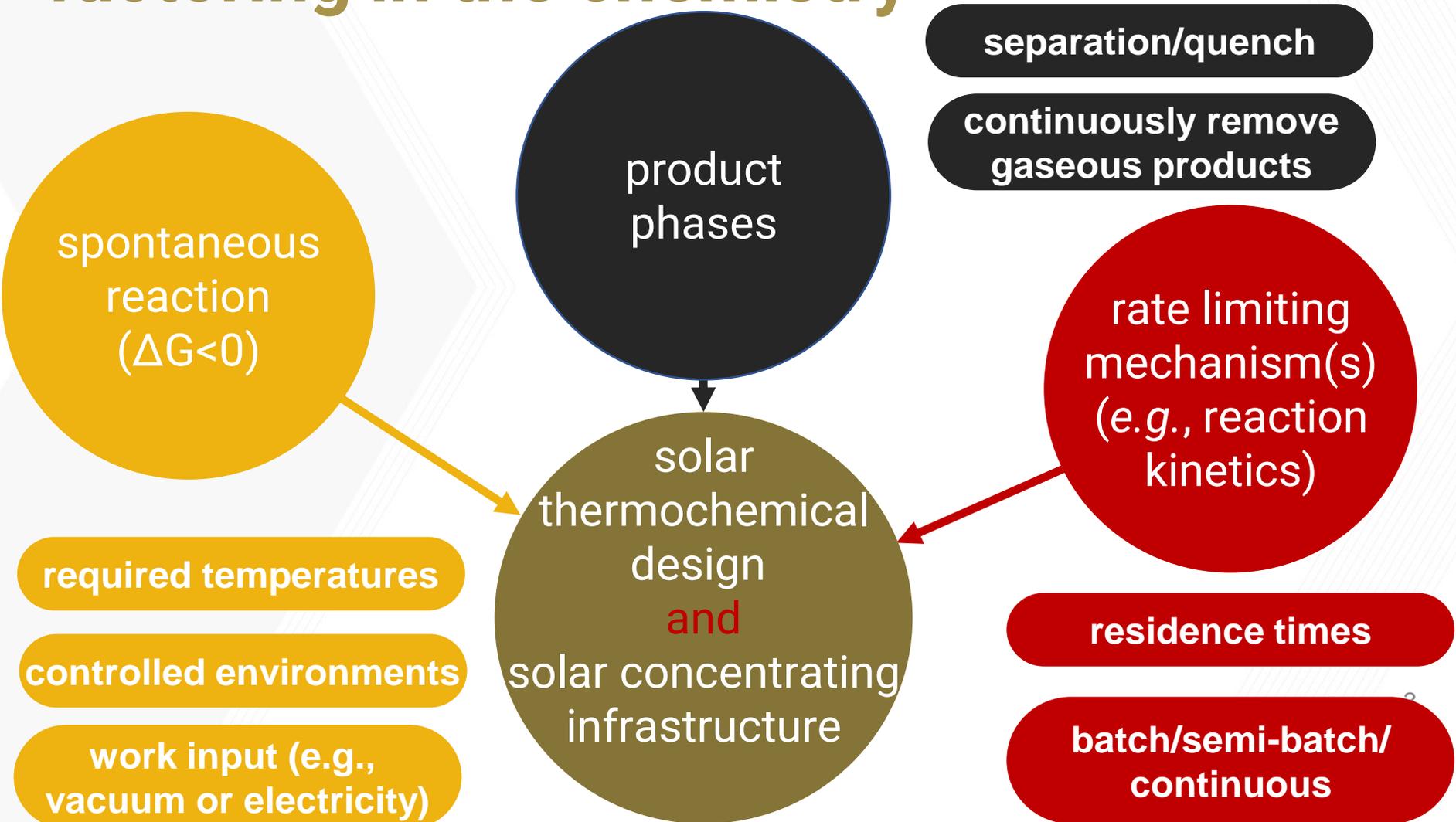
fuels (e.g., H₂, CO)

metals/metalloids

thermochemical heat

purified gases

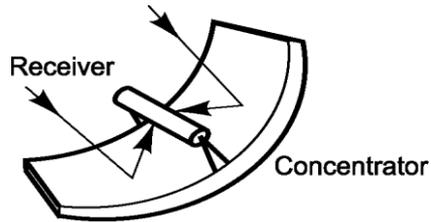
Considerations to inform thermochemical reactor design factoring in the chemistry



Concentrating solar irradiation infrastructure

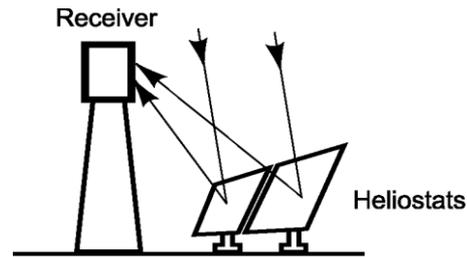
Trough

Solar concentrations of < 100 suns



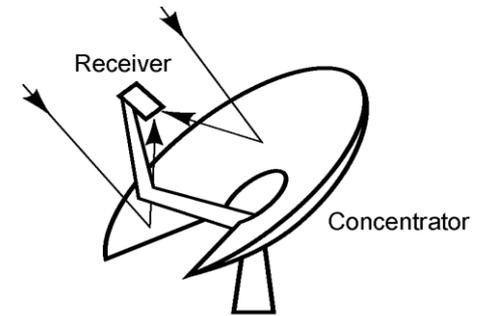
Tower

Solar concentrations of 500 – 2500 suns with secondary



Dish

Solar concentrations of 5000 – 10,000 suns



Maximum work potential extraction

$$\eta_{\text{overall,ideal}} = \eta_{\text{absorption}} \eta_{\text{Exergy}} = \underbrace{\left(1 - \frac{\sigma T^4}{I_{\text{DN}} C}\right)}_{\frac{\dot{Q}_{\text{solar}} - \dot{Q}_{\text{re-radiation}}}{Q_{\text{solar}}}} \cdot \underbrace{\left(1 - \frac{T_{\text{ambient}}}{T}\right)}_{\text{theoretical work potential from heat (exergy)}}$$

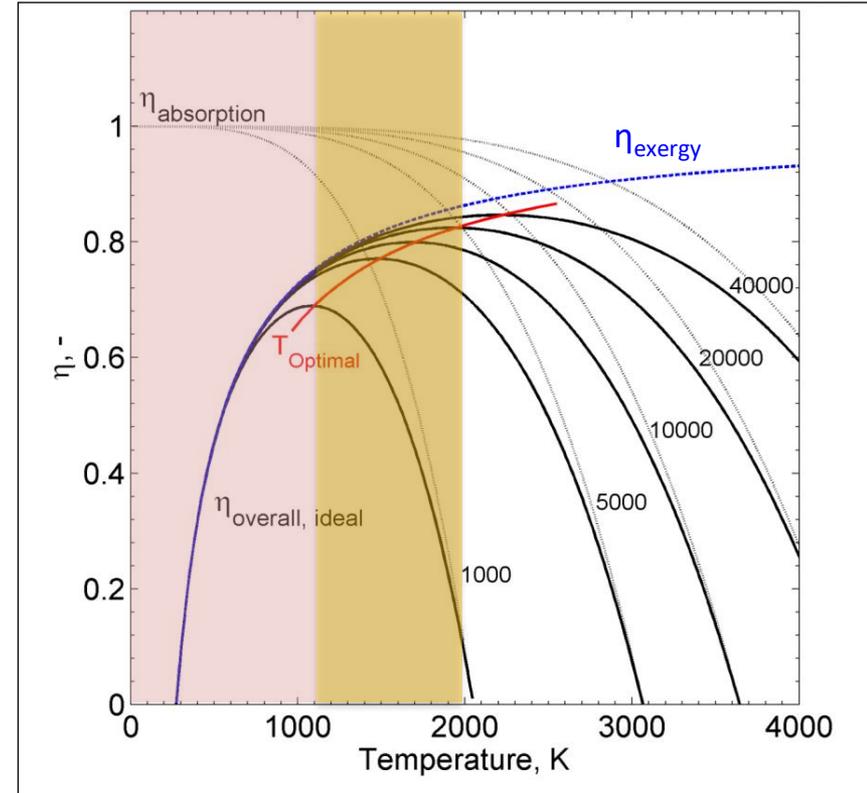
$$\eta_{\text{overall,ideal}} = 0 \rightarrow T_{\text{stagnation}} = \left(\frac{I_{\text{DN}} C}{\sigma}\right)^{0.25}$$

$$\frac{\partial \eta_{\text{overall,ideal}}}{\partial T_{\text{optimal}}} = 0$$

$$0 \rightarrow (T_{\text{optimal}})^5 - 3/4 T_{\text{ambient}} (T_{\text{optimal}})^4 - \left(\frac{T_{\text{ambient}} I_{\text{DN}} C}{4\sigma}\right) = 0$$

C	1000 suns	5000 suns	10000 suns
$T_{\text{stagnation}}$	2049 K	3064 K	3644 K
T_{optimum}	1106 K	1507 K	1724 K

nuclear range
ideal thermochemical cycles

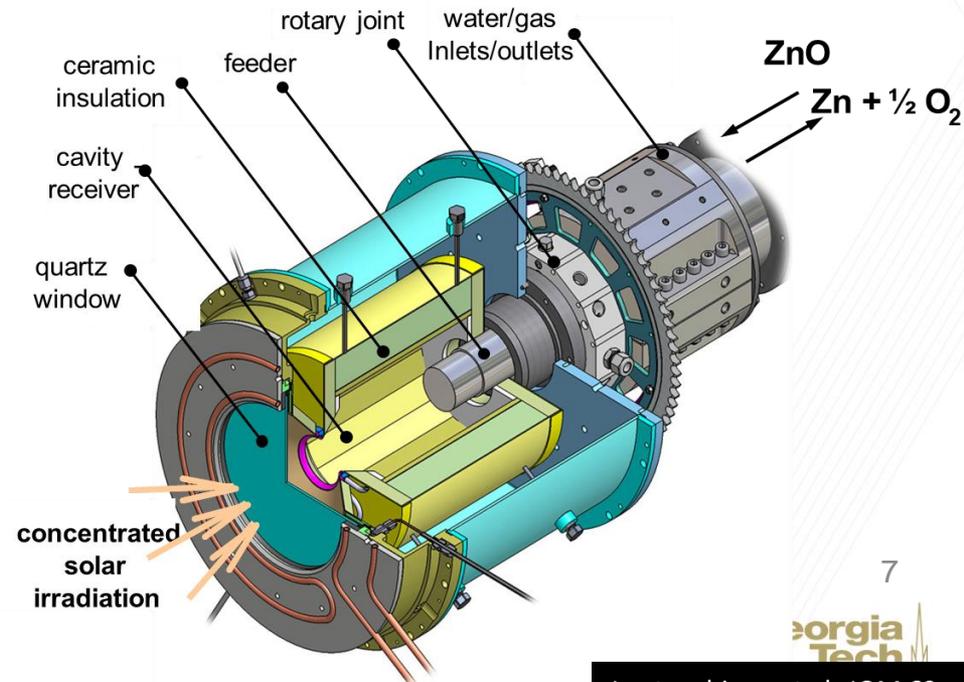
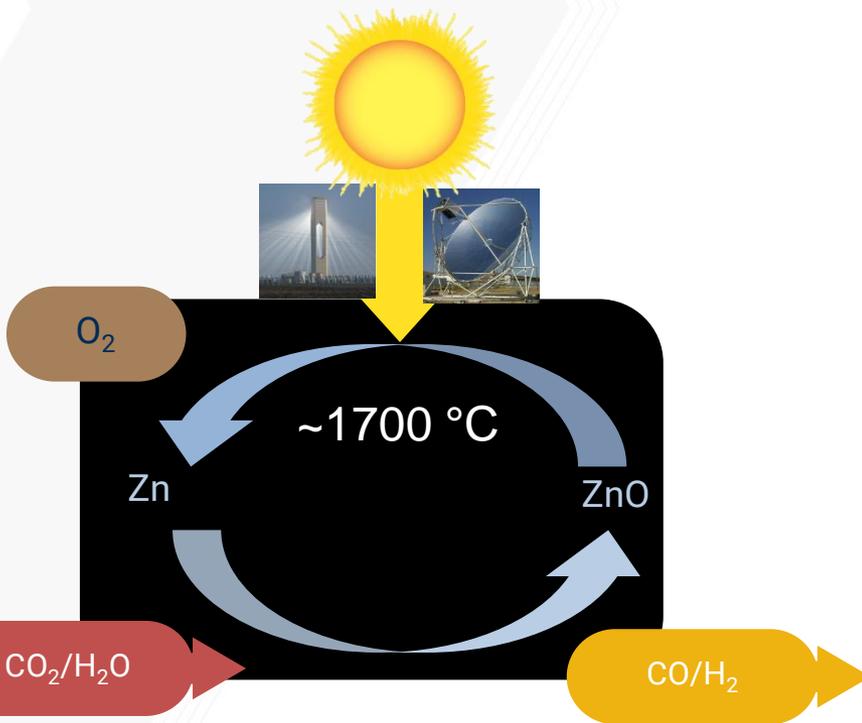


Design considerations

- Scale required for the applications
 - Solar thermochemical storage for electricity productions needs to be scaled for integration with power block
 - Fuels production and materials processing varies between modular units and/or large scale production but necessitates storage
- Temperatures required for different applications
 - Windowed reactors allow for direct exposure to solar concentrated irradiation with losses due transmission and limited scales
 - Indirect reactors heat an absorber plate composed of resilient, highly conductive materials that conducts heat to reactants mitigate depositions with irreversibilities (temperature drops due to heat transfer)
 - Resilient reactor materials required for high temperatures
- Optimizing absorption of concentrated solar irradiation
 - Spectral selectivity for low temperatures
 - Cavity reactors for high temperatures
 - Optimized reactant geometries to ensure deep penetration of solar irradiation (e.g., reticulate porous structures, etc.)

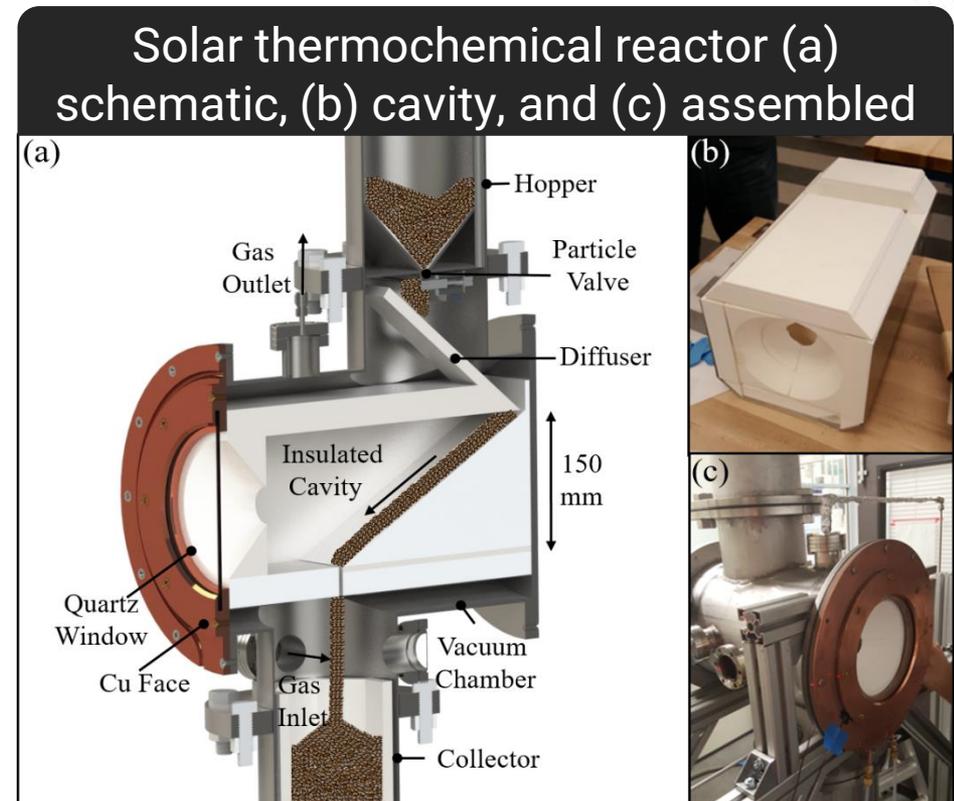
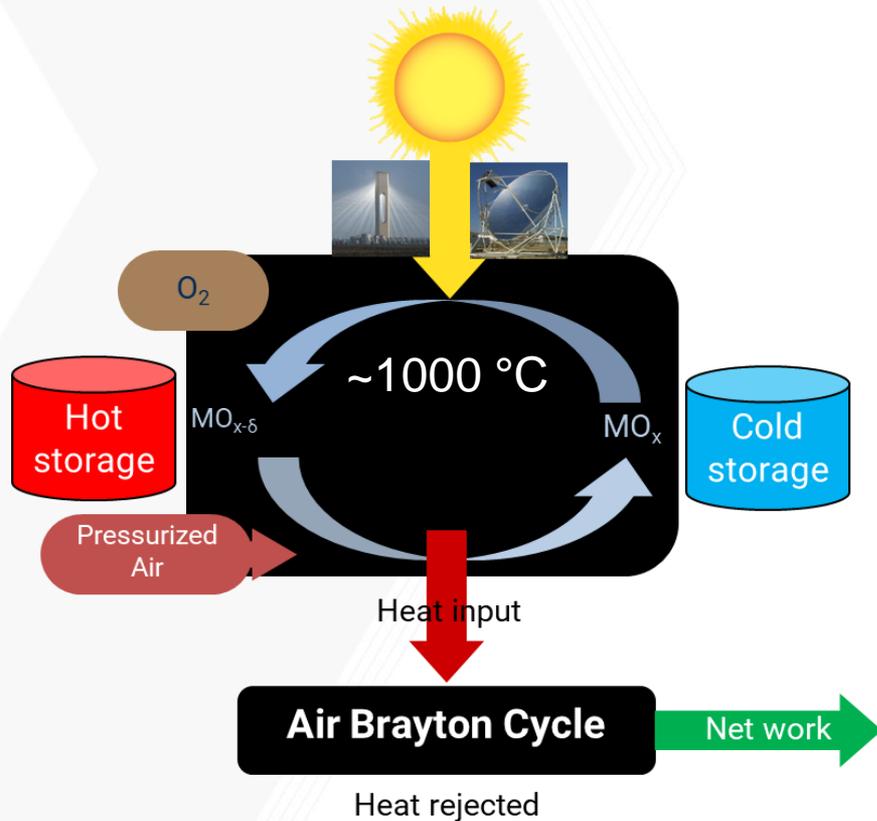
CO₂/H₂O splitting based on ZnO/Zn redox reactions

- Ultra high-temperatures necessitated a window and inert environment
- Zn(g) produced requires a quench process
- Goal to maximize Zn production for subsequent H₂ and/or CO production



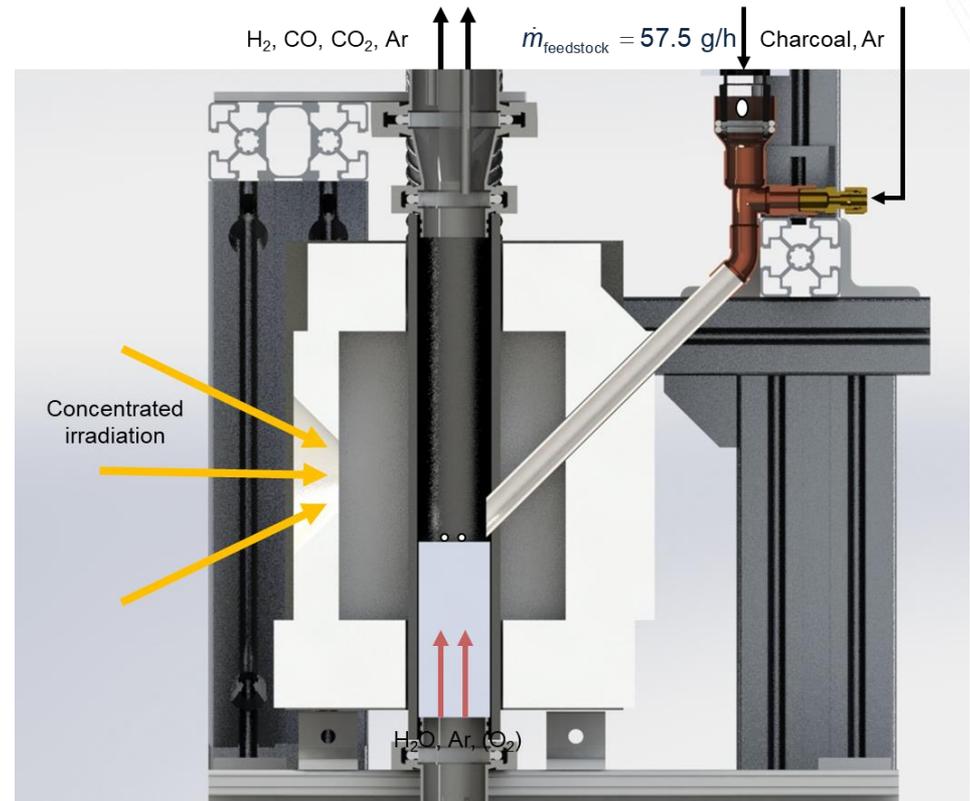
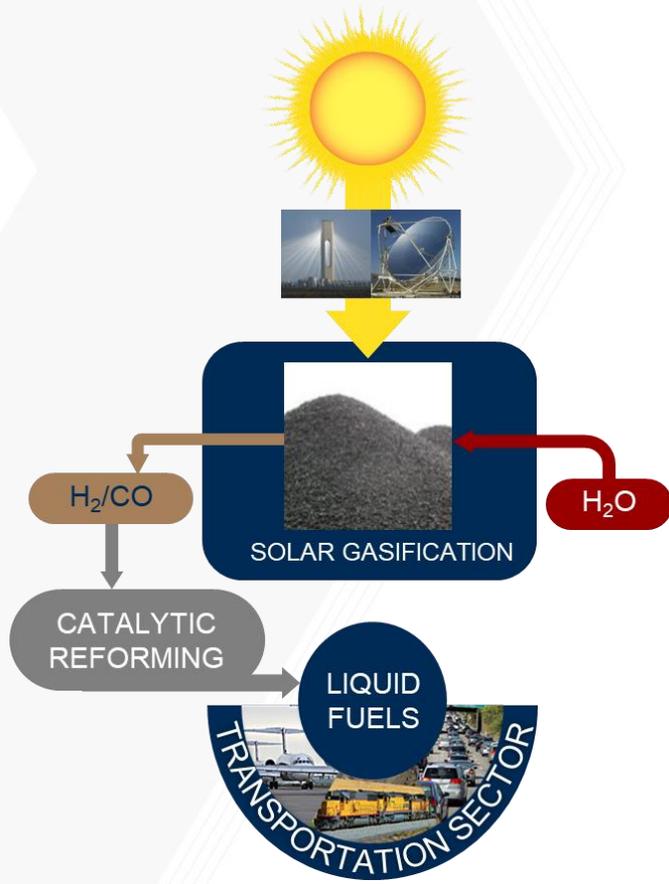
Solar thermochemical storage based on $\text{CaAl}_{0.2}\text{Mn}_{0.8}\text{O}_{3-\delta}$ redox reactions

- Higher temperatures, continuous flows, and heat and mass transfer limitations required window
- A roughened incline slope controlled residence and distributed concentrated irradiation over a thin particle flow



Solar gasification

- Semi-batch mode with gaseous products exiting the top facilitated an solar gasifier and associated chemical kinetics
- Inert bed mixed with activated carbon and H₂O in a SiC tube for gasification at 900 °C for indirect heating

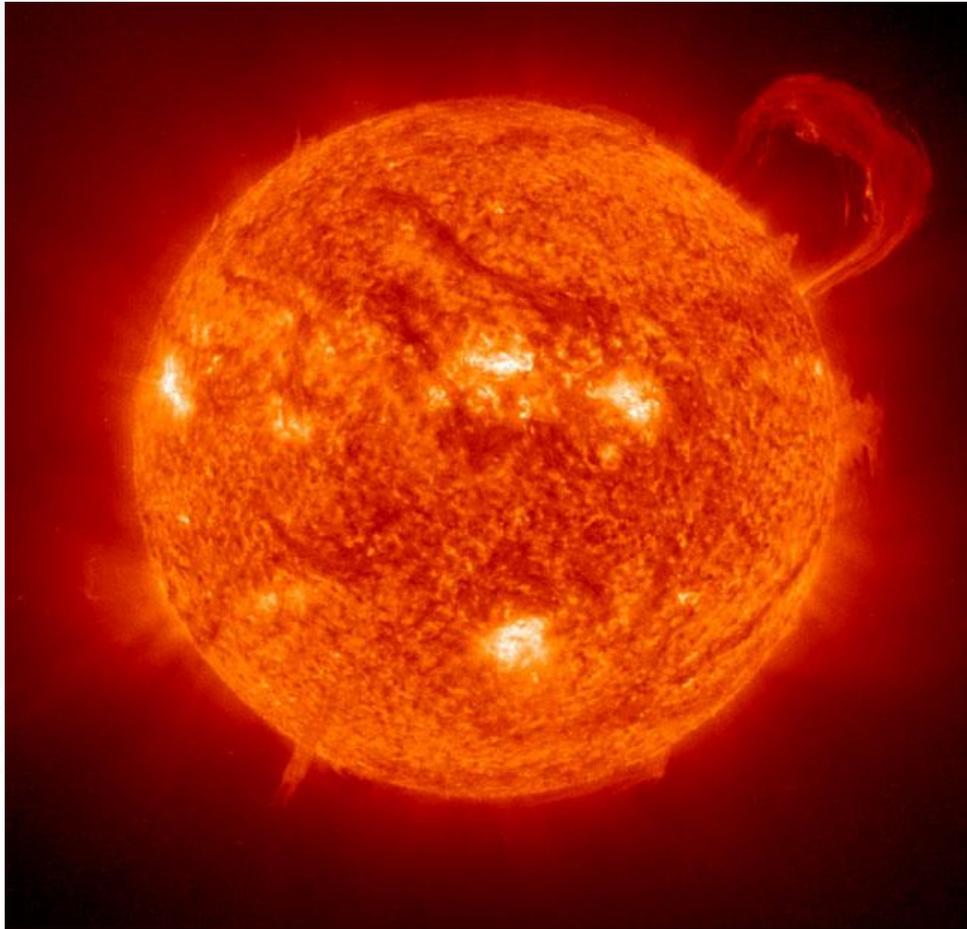


Summary and conclusions

- Solar thermochemical reactor design must be coupled to detailed knowledge of the reaction chemistry
- Different chemical reactions will inherently lead to different solar thermochemical reactor designs, including direct (with window) or indirect (absorber plates) with different scaling obstacles and losses

Outlook

How does the future look?



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