



Unlocking Solar Thermochemical Potential: Leveraging CSP Experience for Solar Thermochemistry



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Solar Flux as a Thermal Energy Input



Motivation

- Decarbonizing industrial processes such as steel, ore refining, cement, fuel or chemical production, and food products
- Can provide both heat and electricity for processing
- Ability to achieve high temperatures

Key Considerations

- Intermittency
 - Integration into existing technology?
 - On-site production vs. transportation costs
 - Point of production does not always equal point of use
 - Location
 - Scale
 - Cost
- I will address some of these considerations in the context of solar thermal production of ammonia



Steel production



Solar fuels (Synhelion.com)

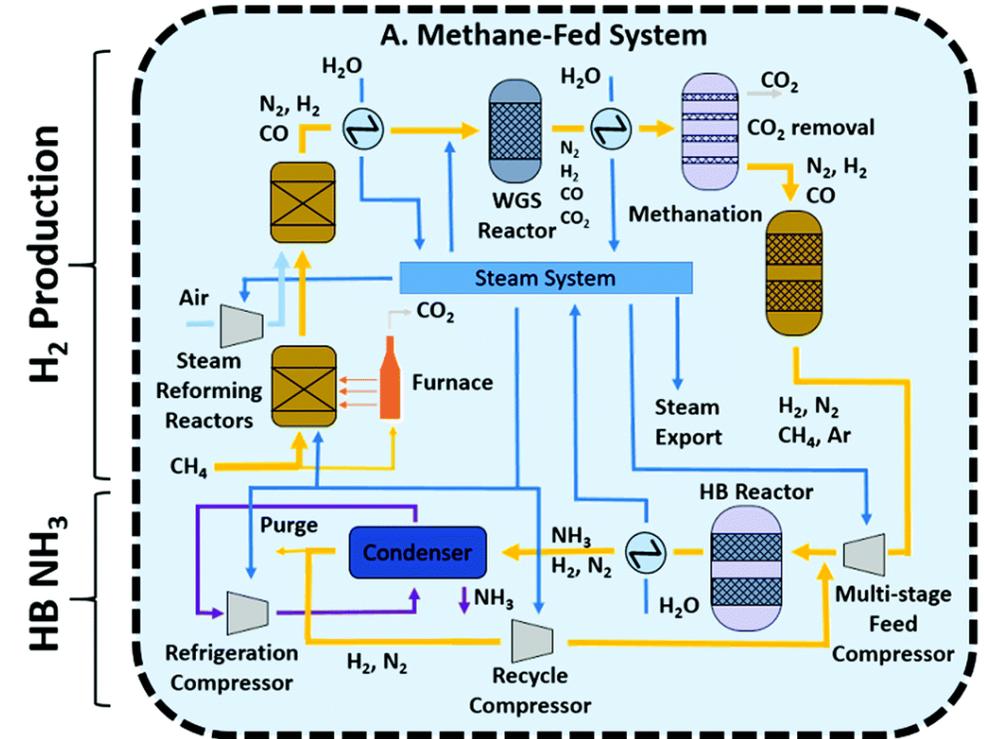


Sustainable pasta production; Mmmm, pasta. (DLR/Barilla)

Deep decarbonization

Example: Ammonia Production

- Ammonia (NH_3) is an energy-dense chemical and a vital component of fertilizer, hydrogen carrier, and energy supplier
- NH_3 synthesized via the Haber-Bosch process
 - Requires high pressures (15-25 MPa) and temperatures (400-500 °C)
 - Consumes > 1% of global energy use
 - Heat, power, and hydrogen are all sourced from hydrocarbons
- Process including H_2 production generates about 2.3 t of fossil-derived CO_2 per t of NH_3 , and is responsible for ~1.4% of global CO_2 emissions
- Steam reforming of natural gas for H_2 generation accounts for 84% of req'd energy



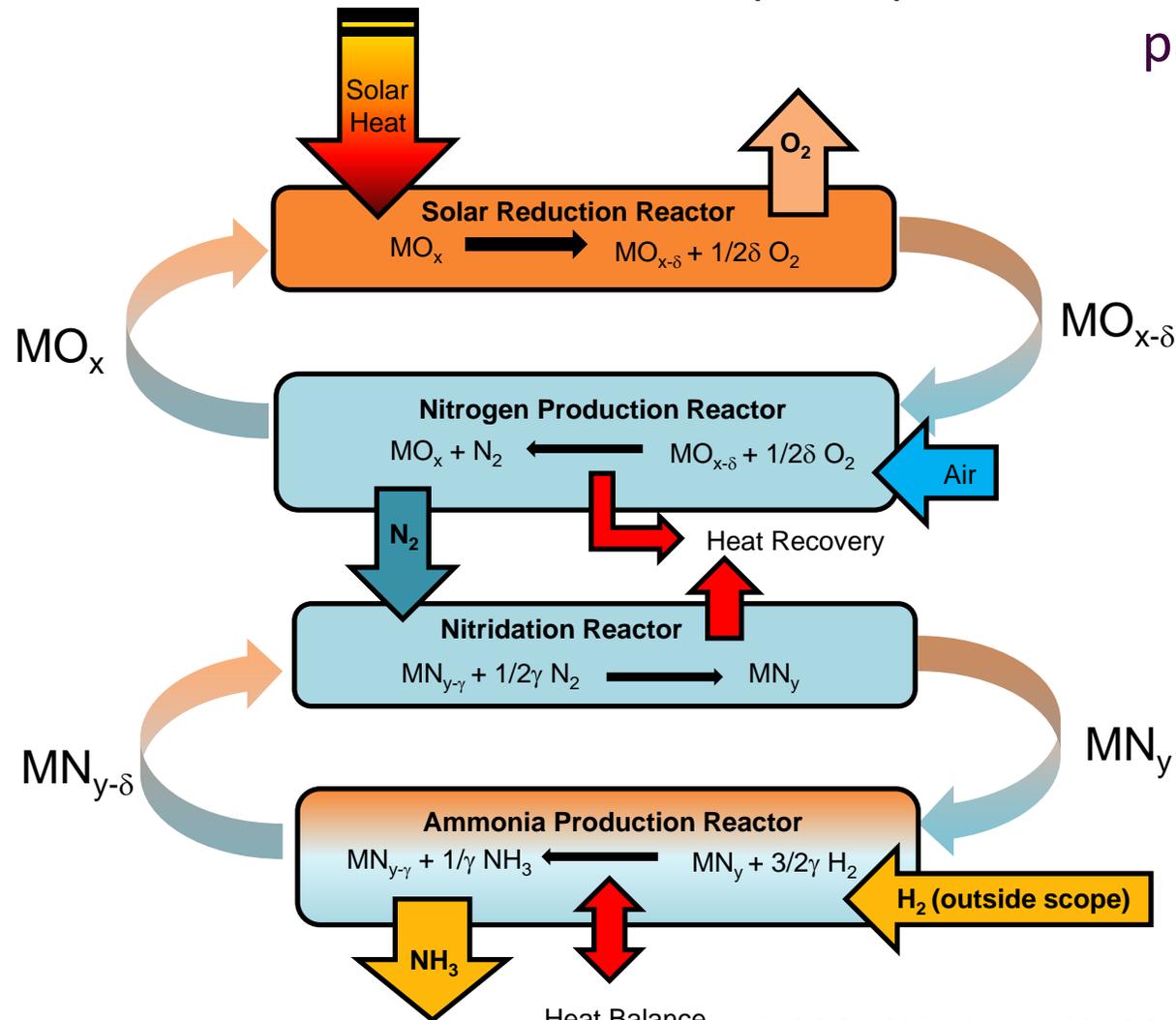
Schematic diagram of a typical conventional methane-fed Haber Bosch process (*Energy Environ. Sci.*, 2020,13, 331-344.)

Can NH_3 be synthesized via a renewable, carbon-neutral technology powered by concentrating solar ?

Solar Thermal Ammonia Production (STAP)



An advanced solar thermochemical looping technology to produce and store nitrogen (N_2) from air for the subsequent production of ammonia (NH_3) via an advanced two-stage process

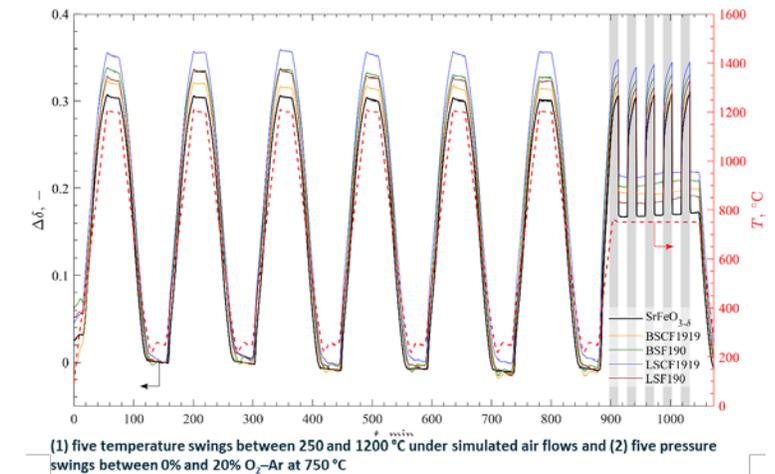
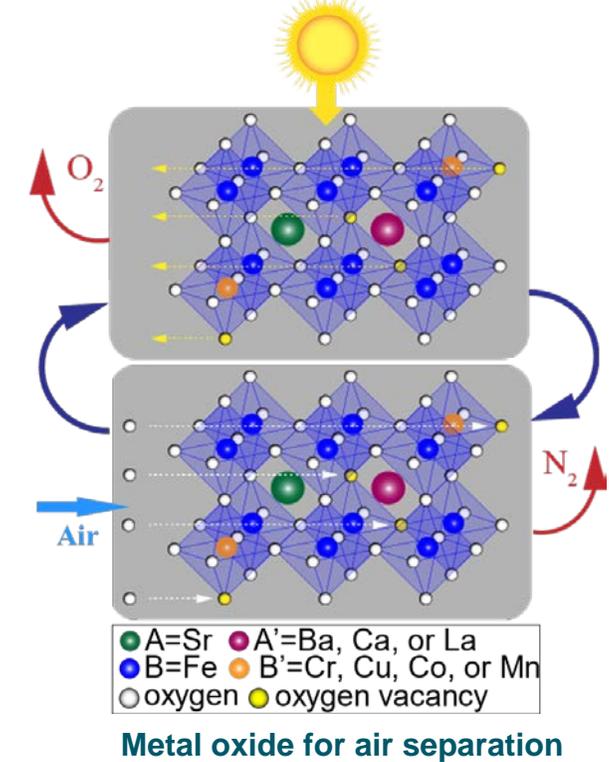


- Inputs are sunlight, air, and hydrogen; the output is ammonia
- Significantly lower pressures than Haber-Bosch
- Greatly decreases or eliminates carbon footprint
- The process consumes neither the oxide nor the nitride particles, which actively participate cyclically
- The project consists of four thrusts:
 - N_2 production via air separation
 - NH_3 production via a cyclic nitride reaction
 - Reactor modeling and design
 - Systems analysis
- Low TRL

Materials

Materials choice influences every aspect of system design

- Materials must be carefully and comprehensively characterized
 - Reactivity
 - Durability: is structural integrity maintained
 - Thermodynamics: enthalpy, reactivity, reaction temperature
 - Kinetics: does the reaction proceed quickly (determines time on-sun)
 - Cyclability: can they be cycled repeatedly with no loss of performance
 - Particle size: affects kinetics, heat and mass transfer
 - Chemical stability: no undesired phase changes, deactivation
- Economic considerations
 - Synthesis: can they be easily synthesized and scaled up?
 - Cost/Availability: avoid critical elements

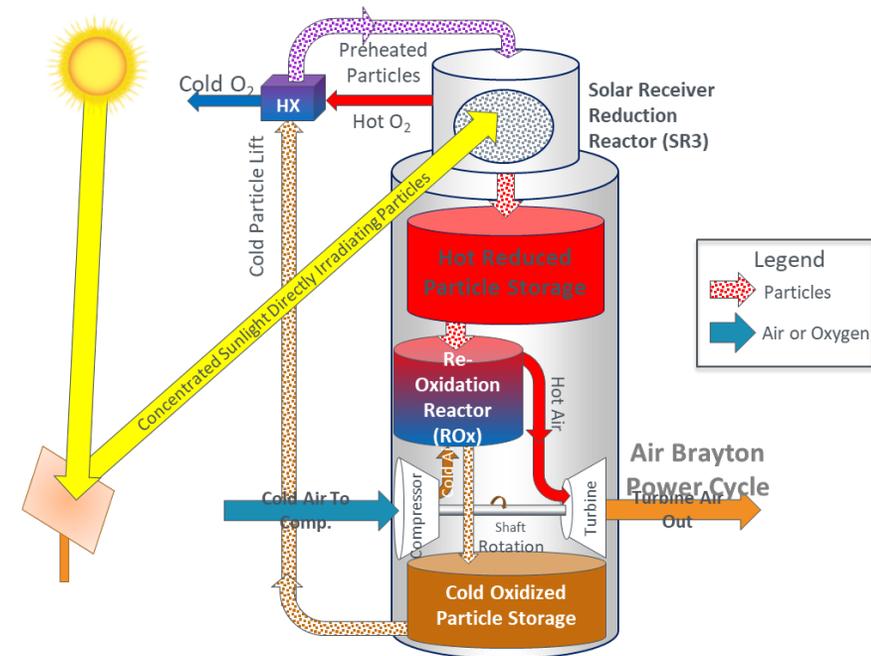


TGA showing redox capacity and cyclability

Intermittency

To maximize productivity, a plant must be able to operate 24/7

- A feature of CSP is the ability to store heat for off-sun operation or electricity generation
 - Storage can be sensible (molten salt, particles), latent (phase change), or thermochemical (sensible + reaction enthalpy)
 - Solids are generally easier to store— they are dense, do not require compression, noncorrosive, stable at $T > 1100\text{ }^{\circ}\text{C}$, and are amenable to multiple scales
 - Thermochemical materials have added benefit of storing energy in the form of chemical bonds, irrespective of storage temperature
- H_2 generated on-site via solar thermochemical water splitting can also act as a chemical storage material, in addition to as a feedstock for chemical processes, e.g., ammonia production



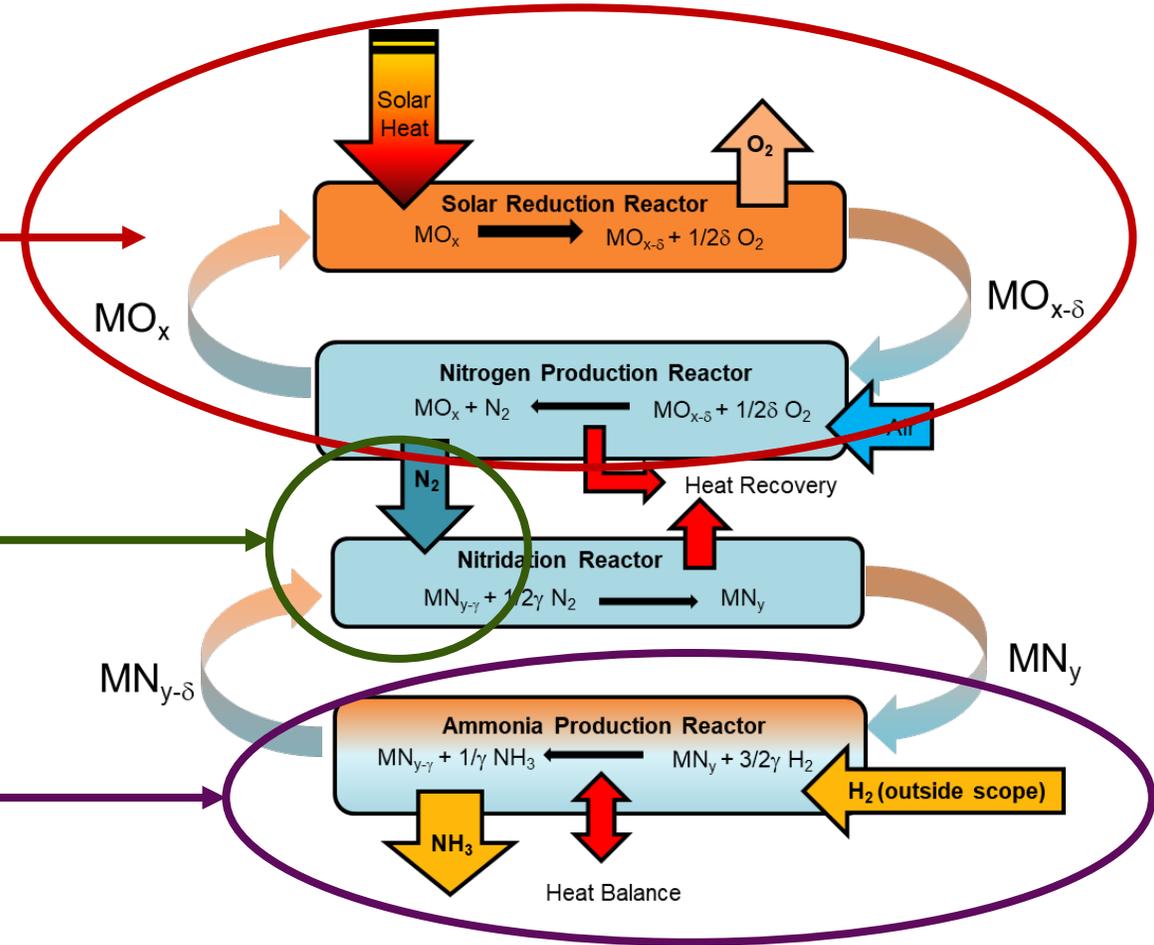
PROMOTES: High Performance Reduction/Oxidation Metal Oxides for Thermochemical Energy Storage

7 Intermittency (cont'd)



To maximize productivity, a plant must be able to operate 24/7

- Process can be decoupled:
 - High temperature cycle, e.g., air separation, can be performed on-sun
 - Resulting N_2 can be stored as compressed gas or chemically, as the nitride (MN_y)
 - Ammonolysis can be run off-sun or evening utilizing recuperated or stored heat
- Similar decoupling can apply to other chemical processes



New vs. Existing Plants



- Co-locate CSP plant with existing Haber-Bosch infrastructure
 - Hybrid model: CSP replaces methane reforming to synthesize H₂ for H-B process via thermochemical water splitting
 - Retains H-B infrastructure; no need to build new plant or transportation lines
 - Not completely green
 - Can be a bridge to fully green process
 - Also an option (or necessity) for processes such as steel production, ore refining, food processing

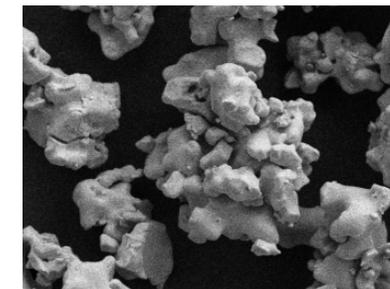
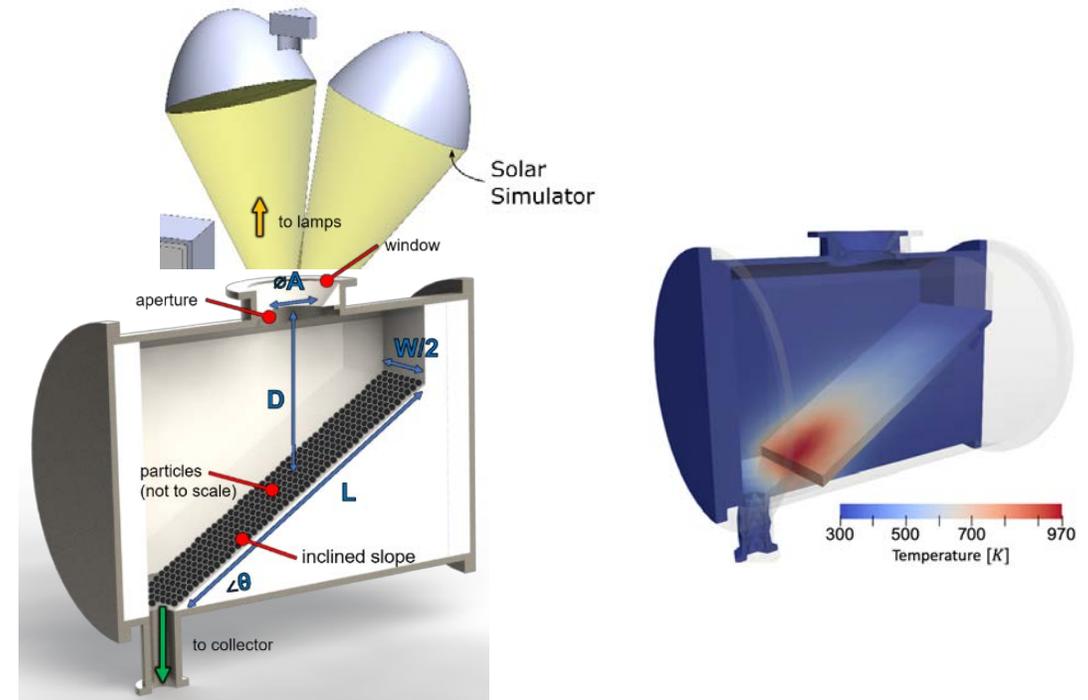
- Construct new plant for renewable NH₃ synthesis utilizing alternative process, e.g. STAP
 - Large up-front CapEx
 - Complete decarbonization of process – both environmentally sound and fiscally beneficial in case of carbon tax
 - Potential savings in long run due to less expensive, cyclable materials, lower temperatures and pressures
 - Consider smaller, distributed plants

9 Receiver/Reactors

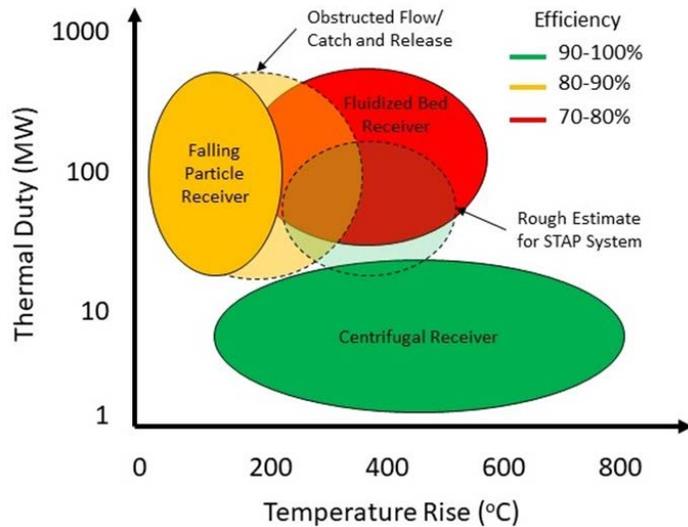


Design and scale of receiver/reactor must be assessed early in the process

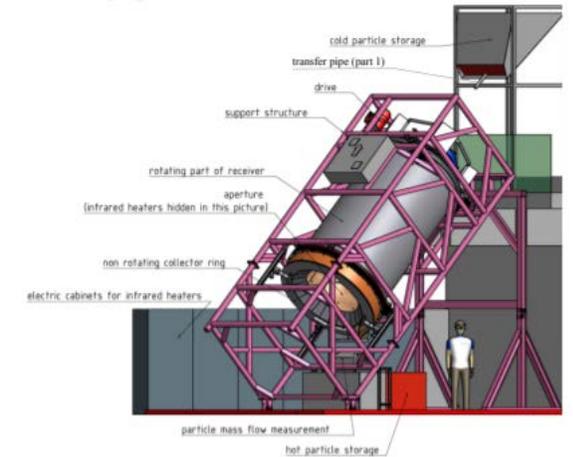
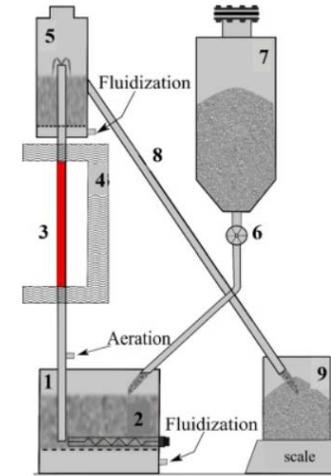
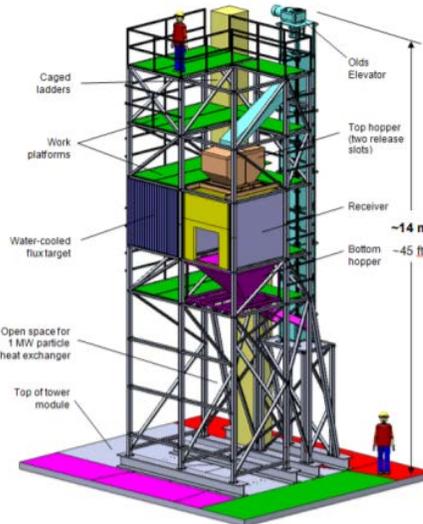
- Many considerations:
 - Direct or indirect irradiation?
 - Temperature requirements?
 - Size?
 - Window or windowless receiver?
 - Particle or monolith working material?
 - Batch or moving particle reactor?
 - Sweep gas or pumping?
- Requires combination of experiment and modeling
 - Decisions will be informed by properties of reactive material
 - In the case of STAP, oxide and nitride particles
 - Heat and mass transfer modeling, supported by experimental data, will inform scale and design



Receiver Designs



From material implications and system modeling, best estimate for receiver conditions is a temperature rise of 200-500 °C and scale <100 MW



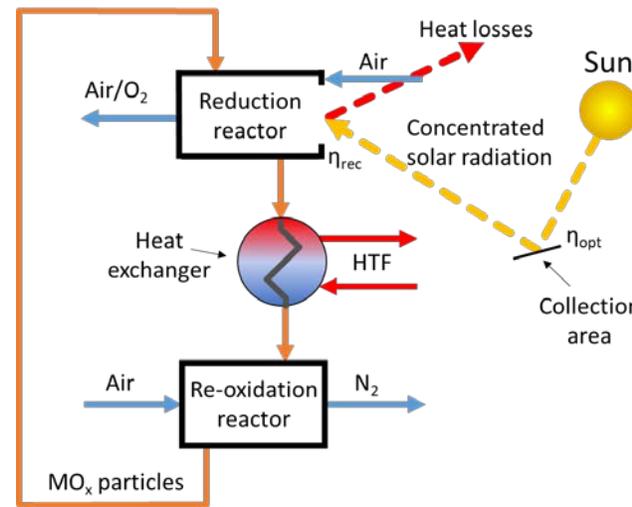
	Falling Particle Receiver (SNL)	Fluidized Bed Receiver (PROMES-CNRS)	Centrifugal Receiver (DLR)
Advantages	<ul style="list-style-type: none"> Direct irradiance can lead to high efficiency No high-cost nickel materials Demonstrated at 1MW scale with significant operational experience 	<ul style="list-style-type: none"> Direct control over residence time and temperature rise Possible to control oxygen partial pressure with enclosed tubed Particle loss can be controlled 	<ul style="list-style-type: none"> Direct irradiance leads to high efficiency Direct control over residence time and temperature rise Particle loss can be controlled Low particle velocity and nod angle minimizes advective loss
Disadvantages	<ul style="list-style-type: none"> Advective loss is sensitivity to particle and wind velocity Particle loss is an economic concern Requires face-down configuration at 100 MW scale (taller tower) Difficult to achieve curtain opacity with high temperature rise 	<ul style="list-style-type: none"> Tube bundles have flux limitations, which reduces efficiency Fluidization gas is an energy parasitic Limited experience with scaling or multi tube receivers 	<ul style="list-style-type: none"> Commercial scale size limits (~10 MW) Requires multiple apertures for surround field



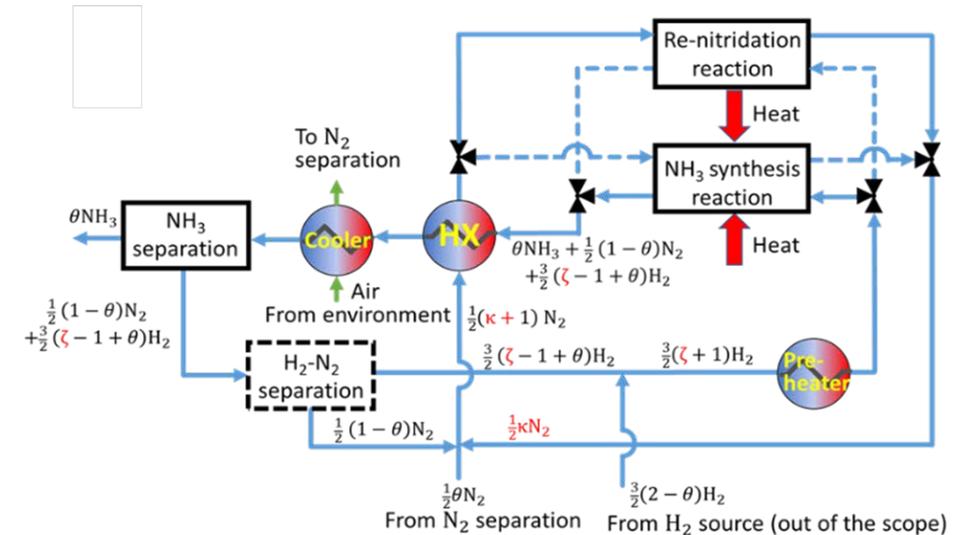
Techno-economics and Systems Analyses



- To attract industry and investment, it's essential to model systems and techno-economics from the beginning of a project
- Continuously refine model as data is collected
- Techno-economic considerations:
 - CAPEX (infrastructure, construction costs, raw materials, labor...)
 - Capacity
 - Energy inputs/outputs
 - O&M
 - Lifecycle
 - Return on investment
- Systems analysis:
 - Solar input
 - Balance of plant
 - Scale
 - Operating conditions
 - Efficiency
 - *Are there any show-stoppers?*



System description of air separation cycle



System description of ammonia synthesis cycle

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THANK YOU FOR YOUR ATTENTION