

# Challenges and Development of sCO<sub>2</sub> heat exchangers

Heatric

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DOE sCO<sub>2</sub> Workshop October 2019



# Organisation structure

New customer-focused organisation aligned to end markets



## Airframe Systems

- Braking Systems
- Fire & Safety
- Power & Motion
- Avionics & Airframe Sensing
- Polymer Seals
- Fuel Systems & Composites



## Engine Systems

- Flow Control
- Thermal Systems
- Engine Composites
- Engine Sensors



## Energy & Equipment

- Defense Systems
- Training Systems
- Heatric
- Energy Sensors & Controls



## Services & Support

- Americas
- UK & Europe
- Asia Pacific

Effective January 1, 2019, Meggitt has adopted a **new organisation structure**, designed to accelerate growth by increasing alignment with our customers whilst simplifying our business.

# Heatric Timeline

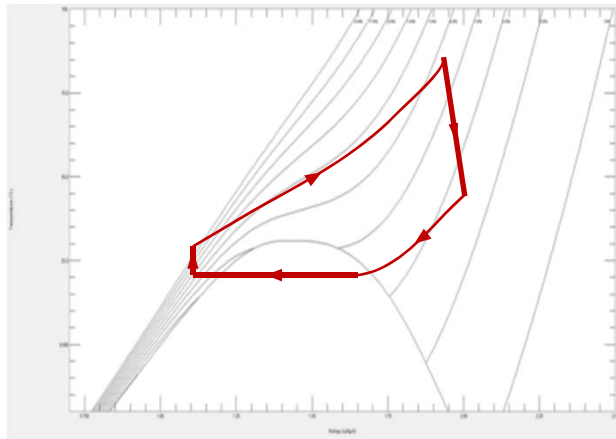
1985 - Present

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# Main sCO<sub>2</sub> cycles

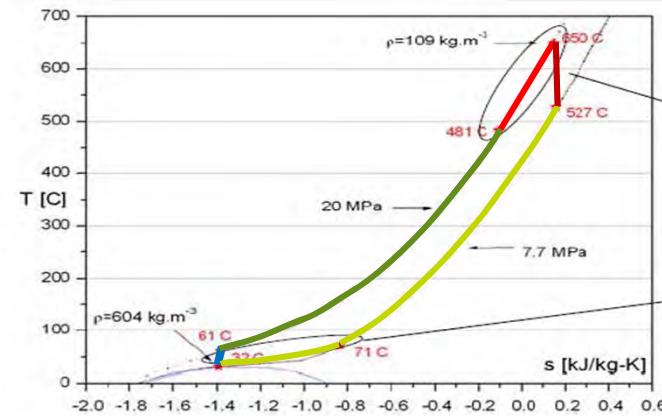
## Rankine sCO<sub>2</sub> Cycle



## Bottoming cycles

Mostly used as waste heat recovery applications for gas turbines, industrial heat and high temperature geothermal in the 10s MWe range

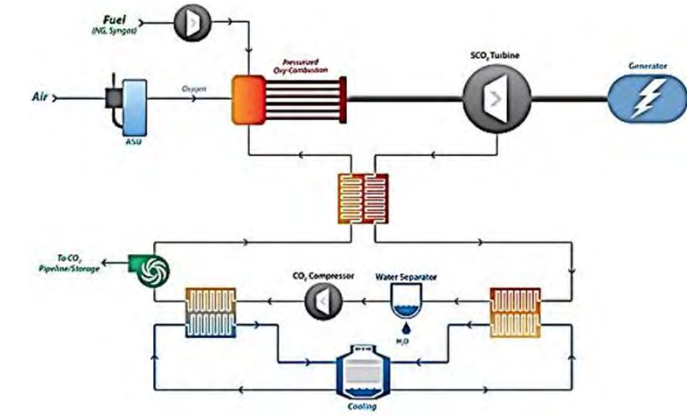
## Brayton sCO<sub>2</sub> Cycle



## Baseload cycles

Developed to displace steam for Fossil, Nuclear and CSP applications for 100s MWe range

## Oxy-fuel sCO<sub>2</sub> Allam Cycle



## Baseload with Carbon capture

Developed to provide electricity at high efficiency with 100% carbon capture and displace fossil plants with CCS in the 100s MWe range



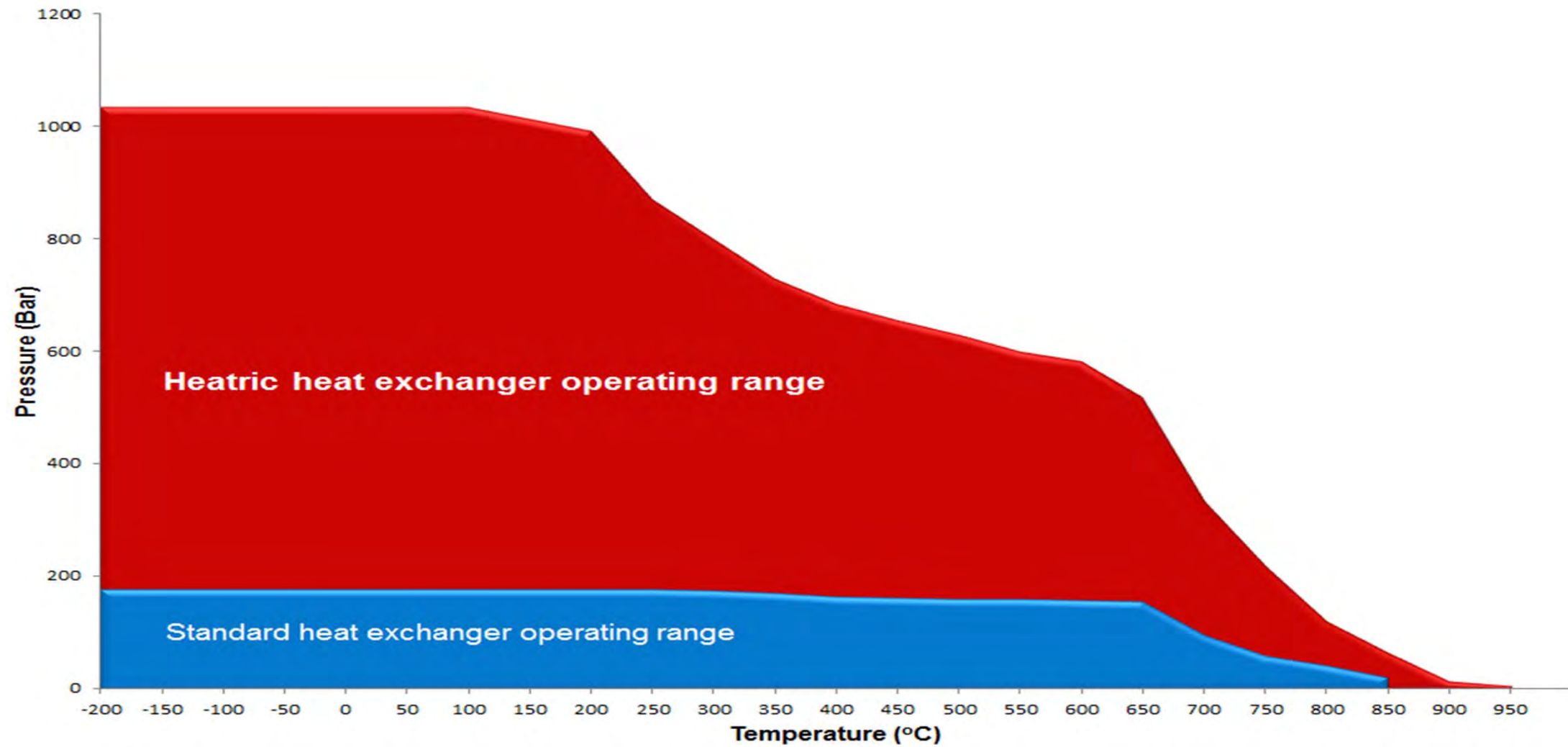
# sCO<sub>2</sub> Cycles

Application	Cycle type	Motivation	Size [MWe]	Temperature (°C)	Pressure [MPa]
Nuclear	Indirect sCO <sub>2</sub>	Efficiency, Size, Water Reduction	10 - 300	350 - 700	20 - 35
Fossil Fuel (PC, CFB, ...)	Indirect sCO <sub>2</sub>	Efficiency, Water Reduction	300 - 600	550 - 900	15 - 35
Concentrating Solar Power	Indirect sCO <sub>2</sub>	Efficiency, Size, Water Reduction	10 - 100	500 - 1000	35
Shipboard Propulsion	Indirect sCO <sub>2</sub>	Efficiency, Size	<10 - 10	200 - 300	15 - 25
Shipboard House Power	Indirect sCO <sub>2</sub>	Efficiency, Size	<1 - 10	230 - 650	15 - 35
Waste Heat Recovery	Indirect sCO <sub>2</sub>	Efficiency, Size, Simple Cycles	1 - 10	< 230 - 650	15 - 35
Geothermal	Indirect sCO <sub>2</sub>	Efficiency	1 - 50	100 - 300	15
Fossil Fuel (Syngas, nat gas)	Direct sCO <sub>2</sub>	Efficiency, Water Reduction, CO <sub>2</sub> Capture	300 - 600	1100 - 1500	35

Extract from DoE Quadrennial Technology Review 2015 - Chapter 4: Advancing Clean Electric Power Technologies

# PCHE pressure and temperature design range

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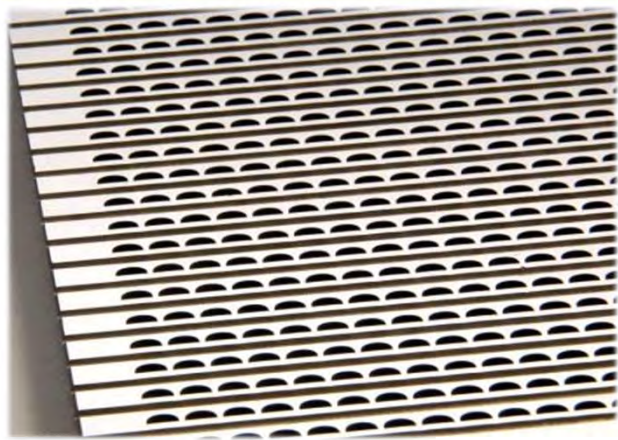


# What is a **Heatric** PCHE?

## Printed Circuit Heat Exchangers

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### Superior Performance

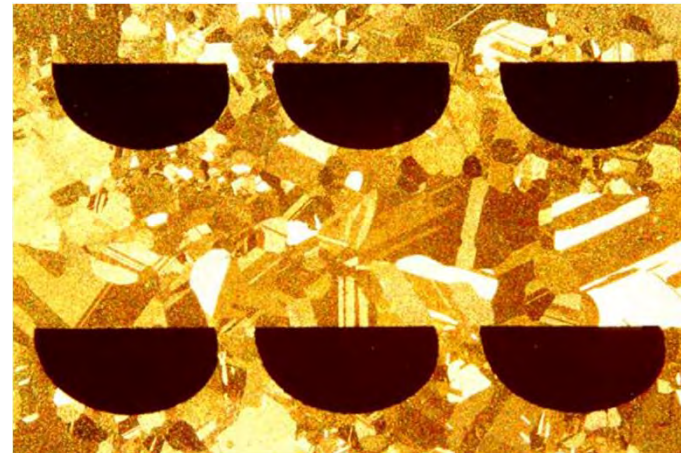


#### OPEX saving across wide range of processes

Heatric PCHEs are bespoke diffusion bonded compact heat exchangers providing:

- close temperature approaches ( $>2^{\circ}\text{C}$ )
- very high thermal performance (i.e.  $13.6\text{MWth/m}^3 \text{ sCO}_2$  recuperator)
- high pressure capability ( $>1,000 \text{ Bar}$ )
- widest range of temperatures ( $-196^{\circ}\text{C}$  to  $983^{\circ}\text{C}$ )

### Safe



#### Reduced operational risks

Using diffusion bonding with a fully welded construction, PCHEs:

- can operate at full differential pressure between streams
- are immune to flow induced vibrations and pressure fluctuations
- do not suffer from catastrophic failure mode
- have 30 years track record of safe operation and  $>3,000$  exchangers supplied

### Compact and Modular



#### Overall project CAPEX saving

Heatric PCHEs are up to 85% smaller than Shell and Tube exchangers, offering:

- modularisation for ease of transport, on-site installation
- reduced foundation structure
- reduced pipework and safety valves
- retrofit capability in lieu of S&T



# Heatric sCO<sub>2</sub> Key Delivered Project Timeline

Since 1994

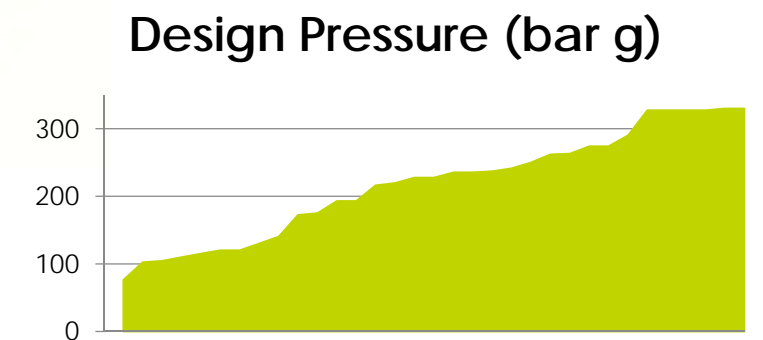
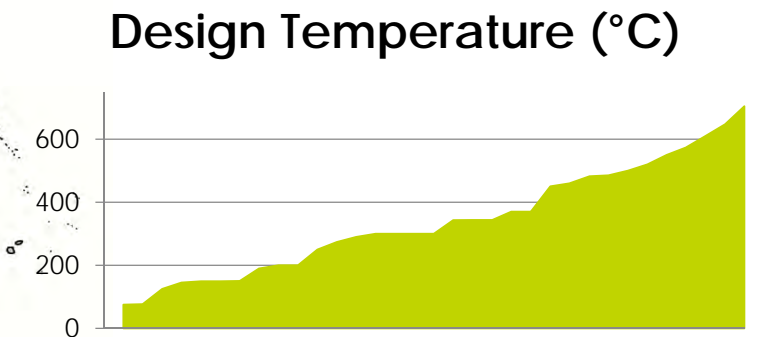
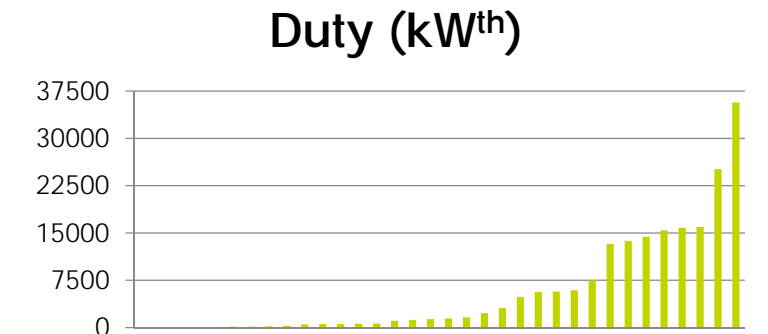
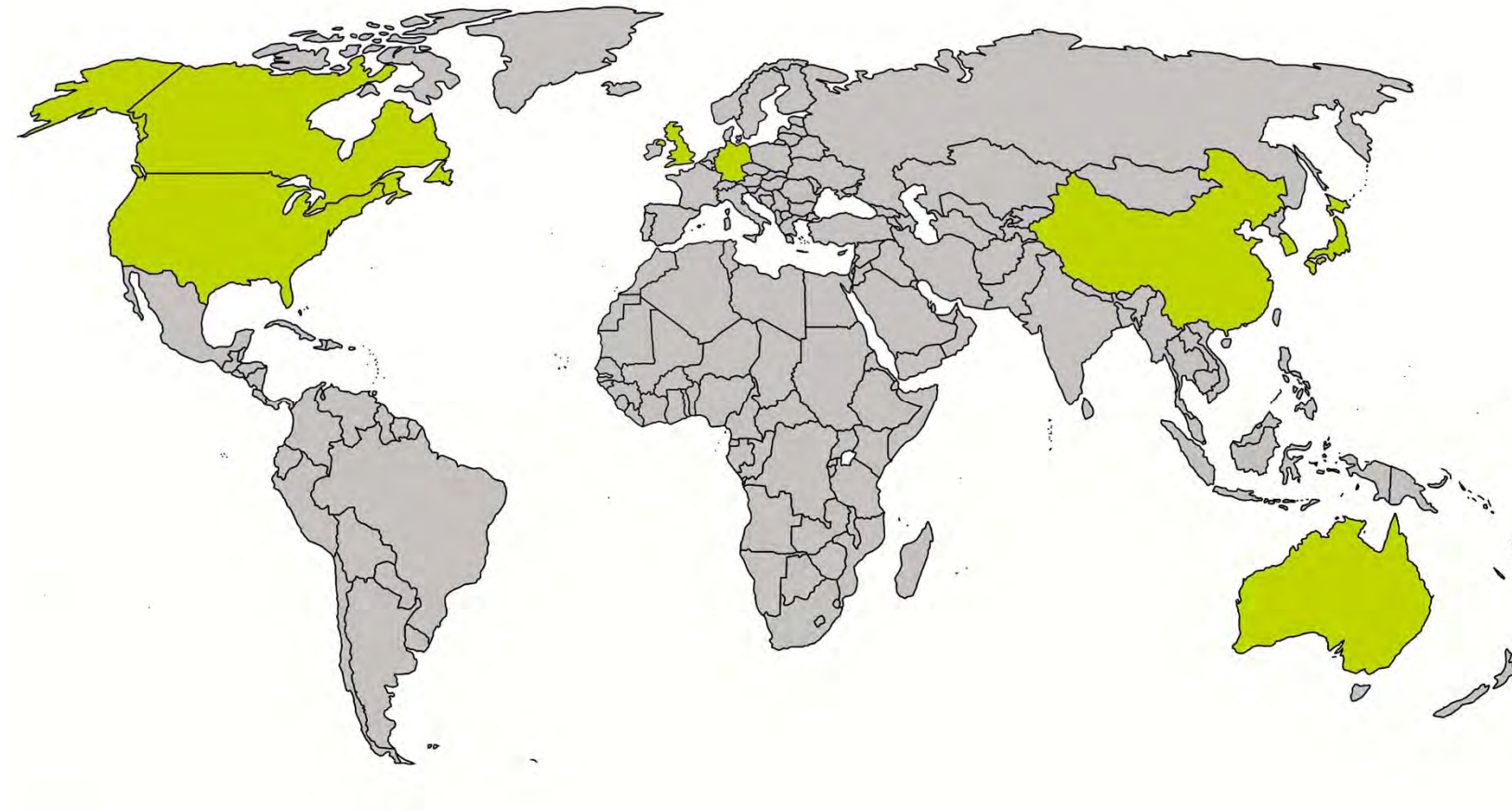
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# Heatric sCO<sub>2</sub> Exchangers – 18 Major Projects to date\*

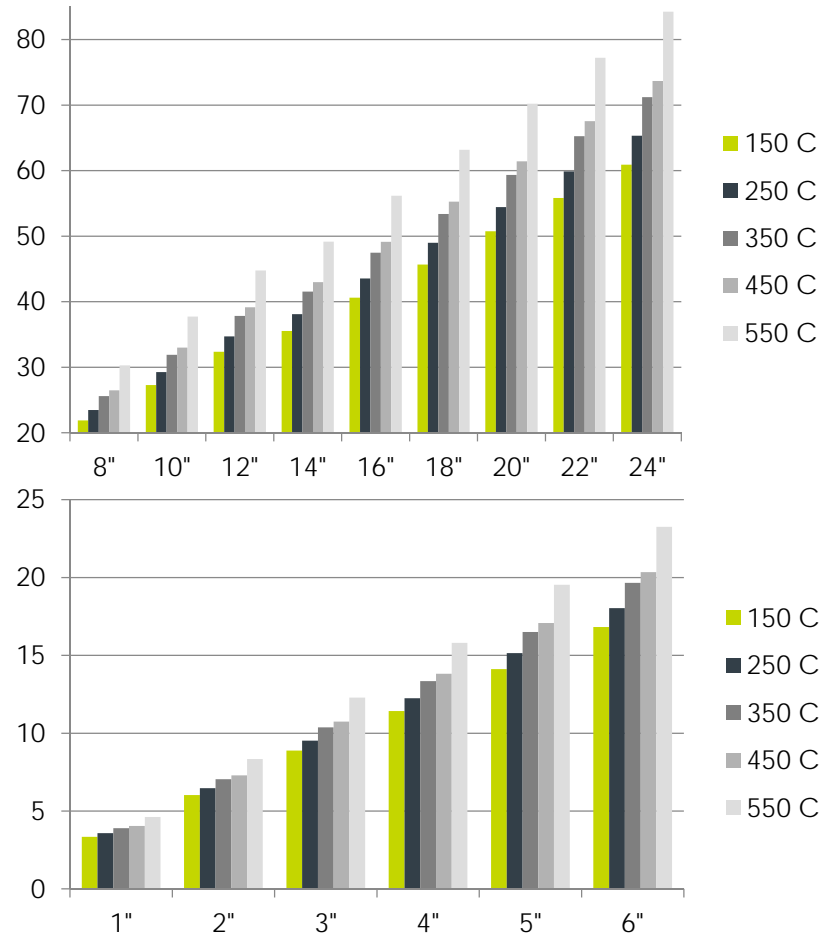
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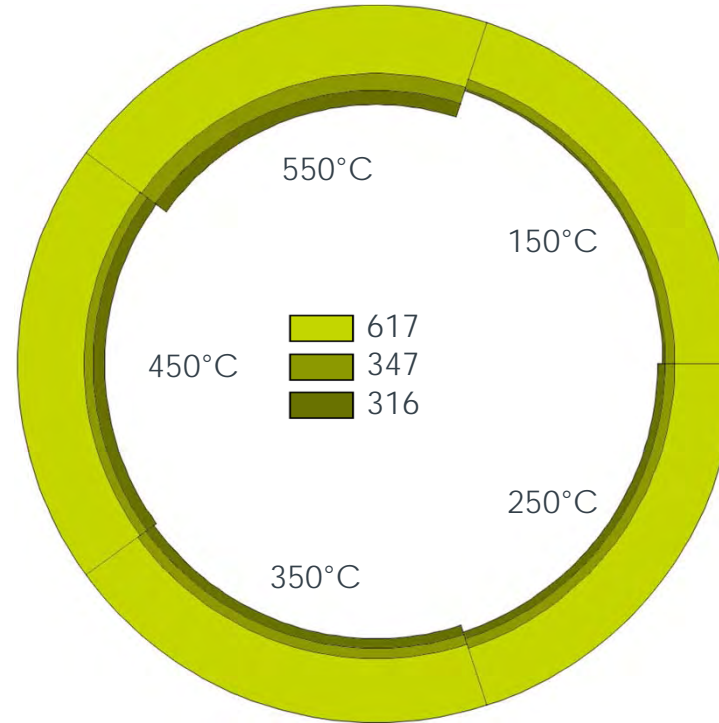
	USA	Australia	U.K.	Germany	Canada	China	Japan	Korea
N° Project	10	1	2	1	1	1	1	1
N° Units	21	3	2	2	2	2	1	1

\* 40 sCO<sub>2</sub> exchangers delivered, 270 sCO<sub>2</sub> projects quoted, >1,000 exchangers bespoke designs

# Component cost – 316, 347, 617 Pipe (ASME B31.3)

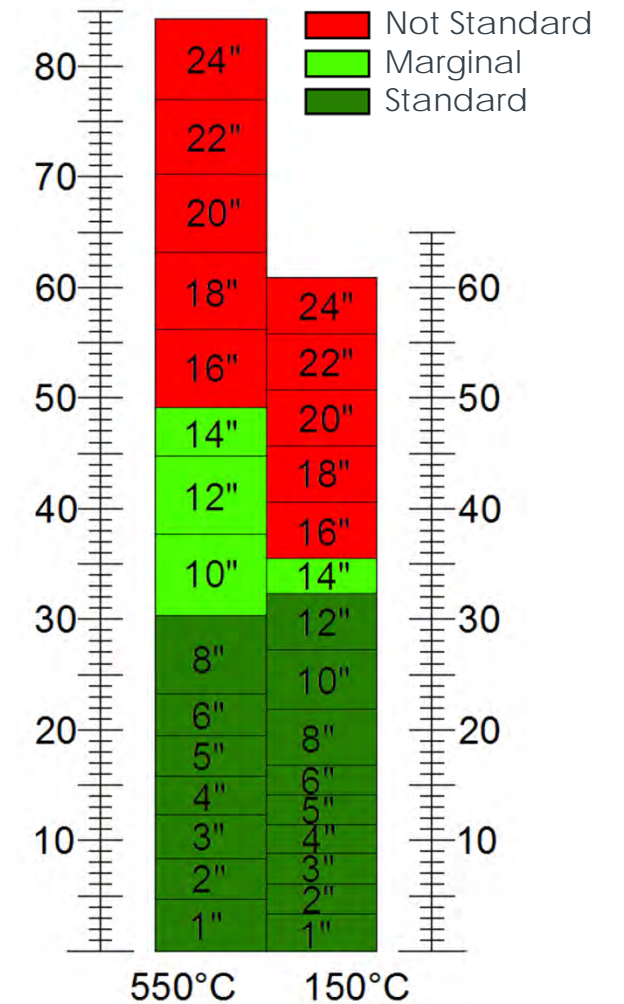


316 Pipe thicknesses vs. design temperature (250 Bar design pressure)



	150°C	250°C	350°C	450°C	550°C
316 vs 347	3%	9%	12%	13%	14%
316 vs 617	17%	22%	24%	23%	31%

316, 347, 617 Pipe thickness reduction vs. temperature (250 Bar pressure)



316 Pipe thickness vs. Std Pipe schedule (250 Bar pressure)

## Lesson learned

### sCO<sub>2</sub> heat exchangers are expensive?

Yes they can be depending on the process design:

Increasing design temperature:

- May shift equipment built from conventional material to high grade alloys (10x – 20x more expensive)

Increasing design Pressure:

- Will require thicker walls with much more expensive non standard product forms for some components (i.e. hubs, special forgings, pipes)

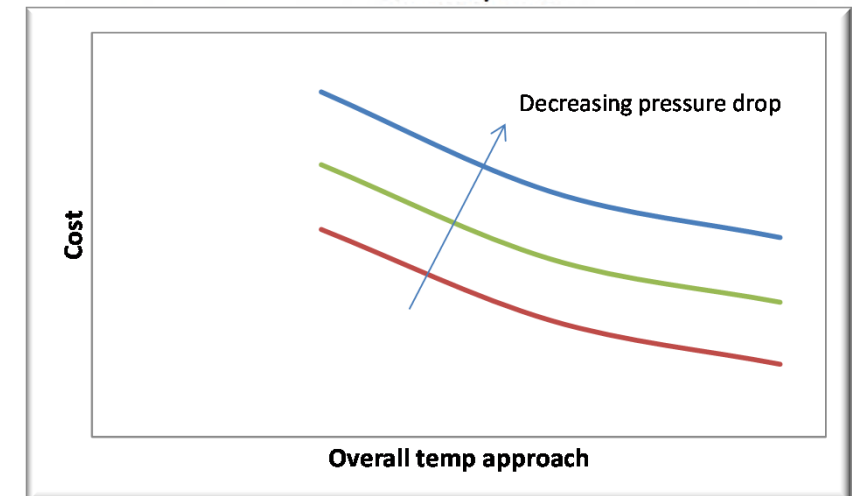
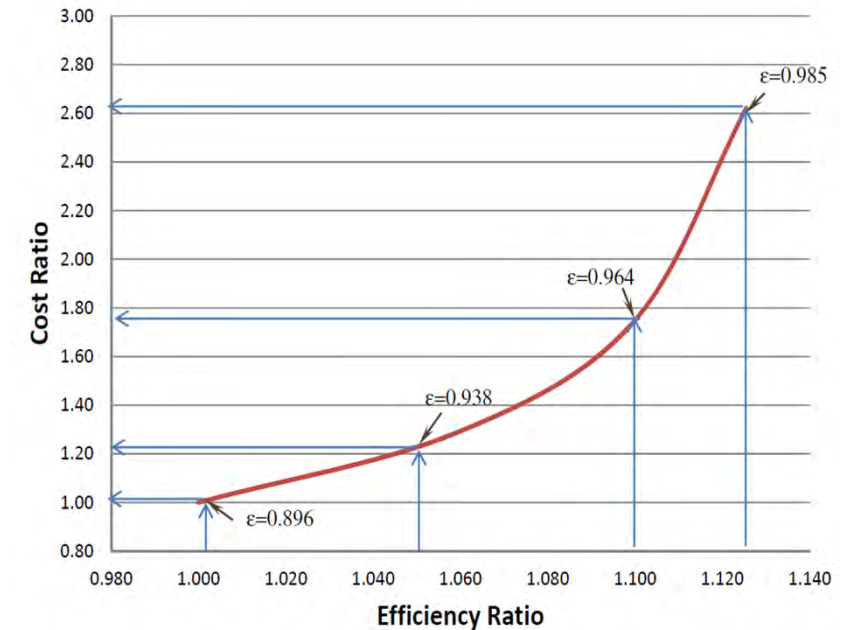
Temperature approaches:

- Will lead to diminish efficiency returns versus exchanger potentially doubling in size for minimum gains ( $Q=U.A.LMTD$ )

Allowable pressure drop:

- Will lead to very high free flow area requirements increasing the size of the exchanger potentially beyond compressor / pump cost savings

**sCO<sub>2</sub> process design must be balanced between equipment cost and efficiency gain**



# Path to commercialisation

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## Supply Chain

Cost reduction  
Product availability

Even in stainless steel, material price and product form availability can be a challenge; Supply chain must be engaged with to providing competitive materials in suitable product forms.

## Standardisation

Process | Products  
Performance

Standardisation of the various sCO<sub>2</sub> processes will lead to standard products, potential for off-the shelf with mass production and guaranteed performance based on previous supplies results operational records.

## Modularisation

Flexibility | Footprint  
Plant integration | Deployment

Modularisation brings benefits in flexible designs with minimum changes, defined footprints facilitating plant integration and facilitation deployment even in remote area (i.e. containerized).

## Collaboration

Faster R&D | No duplication  
Better use of funds

Improve international coordination / communication to ensure most R&D activities going forward are not replicating existing research in other territories / regions.

**Making  
sCO<sub>2</sub>  
Viable?**



# Technology development

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## PCHE

PCHEs typical channels are 1 mm deep (2 mm semi circular)

They are well suited for sCO<sub>2</sub> but not for exhaust side due to pressure drop constrains

PCHEs are already used as Recuperators in sCO<sub>2</sub> systems

Heatric has developed deep etch technology currently able to achieve 2.5 mm deep channel (5 mm semi circular)

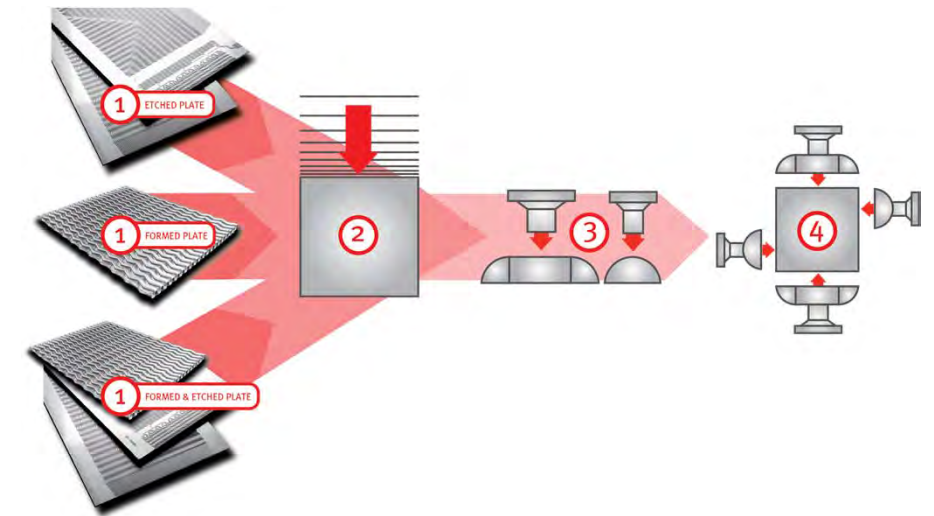
## HYBRID

H<sup>2</sup>Xs aim to combine 2 or more different product forms in a single product

To date H<sup>2</sup>X has been considering combining Fins to PCHE channels

Work is in progress to validate H<sup>2</sup>X as part of the Cranfield test loop

Further work is on-going to expand channel size on the exhaust side to dH > 5 mm

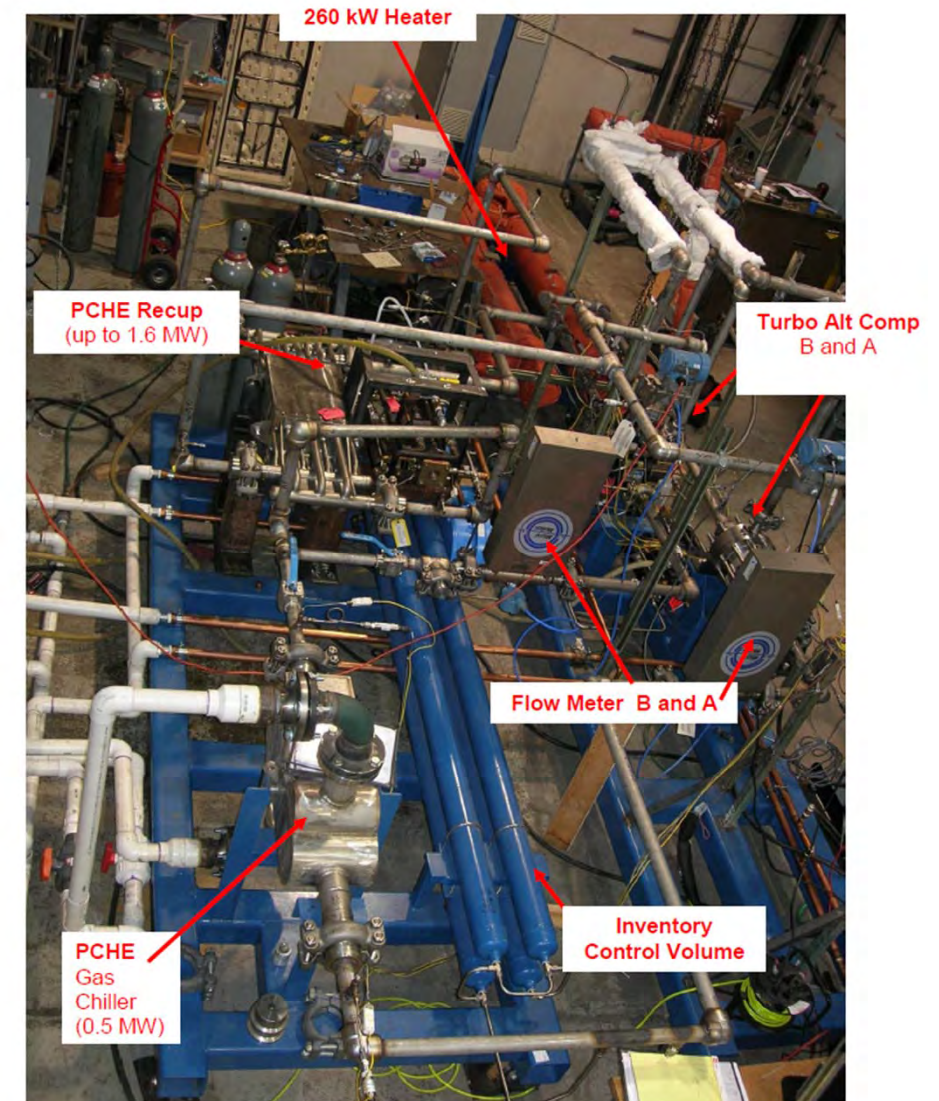


# Sandia National Laboratories – sCO<sub>2</sub> Brayton Cycle

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- HT Recuperator
  - 2.27 MW
  - 482°C (900°F)
  - 17.24 MPa (2500 psig)
- LT Recuperator
  - 1.6 MW
  - 454°C (849°F)
  - 17.24 MPa (2500 psig)
- Gas Chiller
  - 0.53 MW
  - 149°C (300°F)
  - 19.31 MPa (2800 psig)

3 sCO<sub>2</sub> exchangers delivered  
>2.2 tons combined





# Echogen EPS100 – sCO<sub>2</sub> Rankine Cycle

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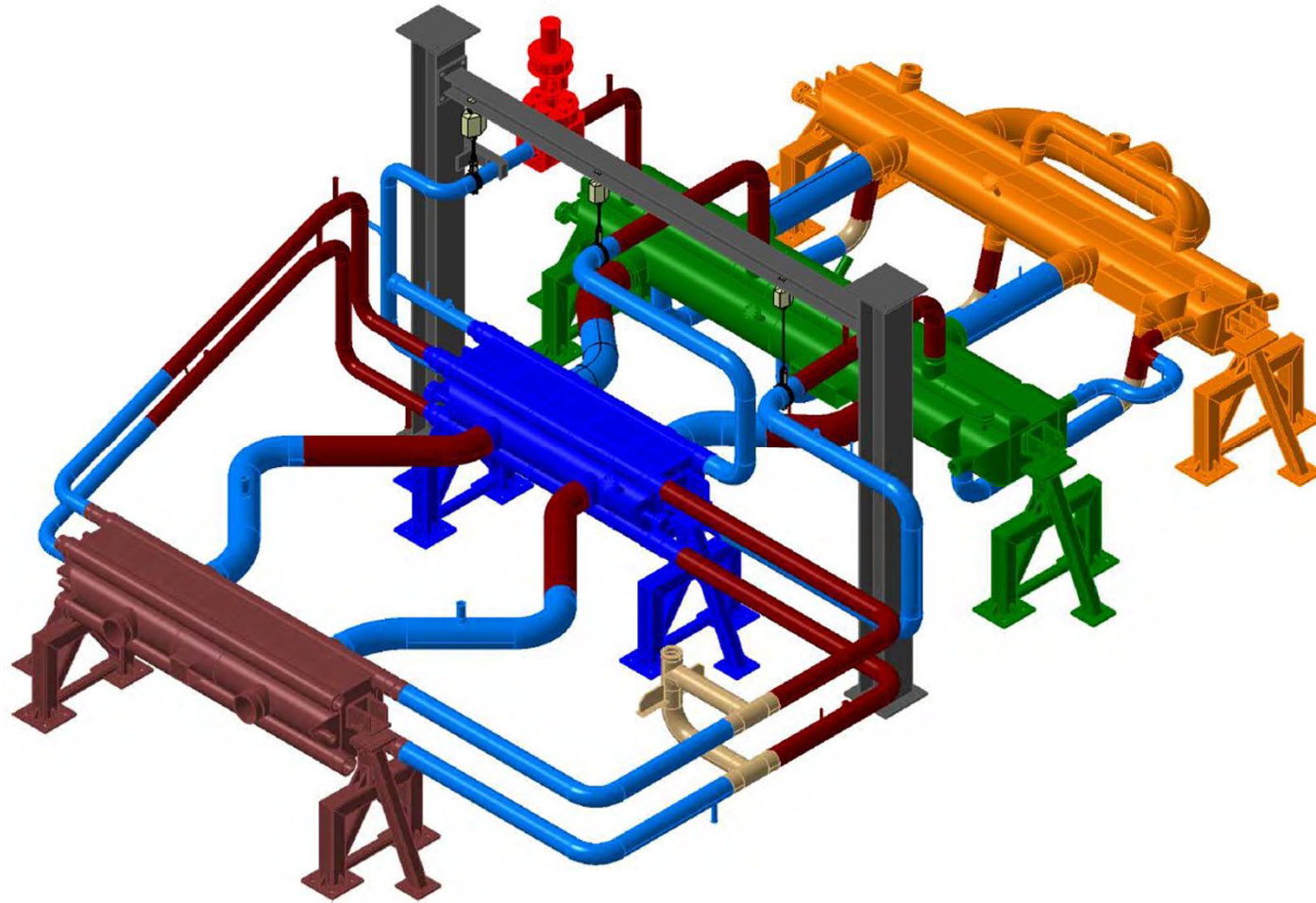


3 sCO<sub>2</sub> exchangers delivered  
>30 tons combined



# Net Power 25MWe – sCO<sub>2</sub> Oxy Fuel Allam Cycle

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4 sCO<sub>2</sub> exchangers delivered (including one 617 unit)  
60 tons combined





# Disclaimer

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