

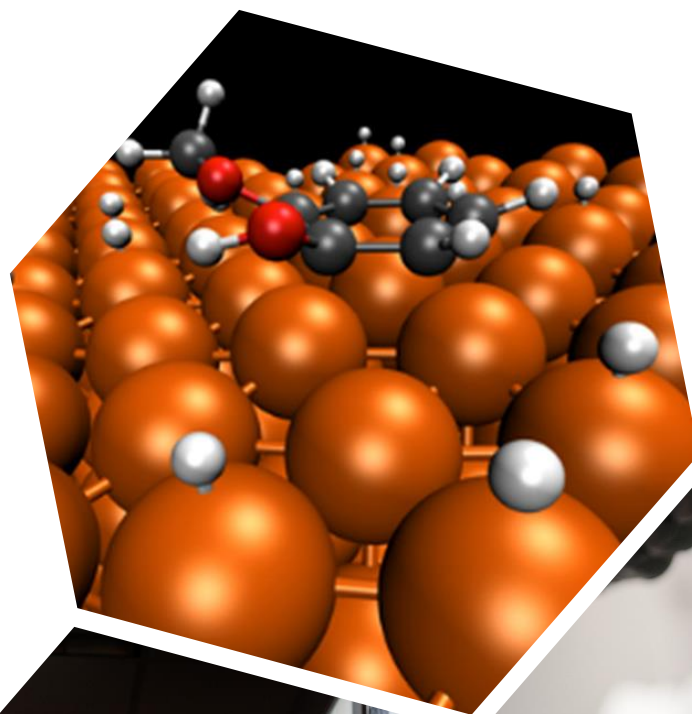


ChemCatBio
Chemical Catalysis for Bioenergy

DOE BETO 2019 Project
Peer Review: CO₂
*CO₂ Utilization: Thermo-
and Electro-catalytic
Routes to Fuels and
Chemicals*

Jack Ferrell, NREL

March 7th, 2019



U.S. DEPARTMENT OF
ENERGY

Office of ENERGY EFFICIENCY
& RENEWABLE ENERGY

BIOENERGY TECHNOLOGIES OFFICE

ChemCatBio Foundation

Integrated and collaborative portfolio of catalytic technologies and enabling capabilities

Catalytic Technologies

Catalytic Upgrading of Biochemical Intermediates

(NREL, PNNL, ORNL, LANL, NREL*)

Catalytic Upgrading of Indirect Liquefaction Intermediates

(NREL, PNNL, ORNL)

Catalytic Fast Pyrolysis

(NREL, PNNL)

Electrocatalytic and Thermocatalytic CO₂ Utilization

(NREL, ORNL*)

Enabling Capabilities

Advanced Catalyst Synthesis and Characterization

(NREL, ANL, ORNL, SNL)

Catalyst Cost Model Development

(NREL, PNNL)

Consortium for Computational Physics and Chemistry

(ORNL, NREL, PNNL, ANL, NETL)

Catalyst Deactivation Mitigation for Biomass Conversion

(PNNL)

Industry Partnerships (Directed Funding)

Gevo (NREL)

ALD Nano/JM (NREL)

Vertimass (ORNL)

Opus12(NREL)

Visolis (PNNL)

Lanzatech (PNNL) - Fuel

Gevo (LANL)

Lanzatech (PNNL) - TPA

Sironix (LANL)

Cross-Cutting Support

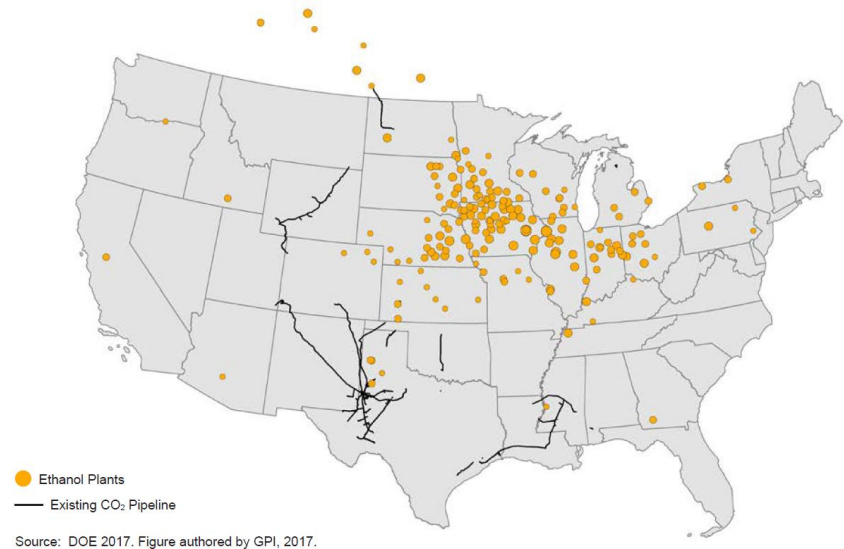
ChemCatBio Lead Team Support (NREL)

ChemCatBio DataHUB (NREL)

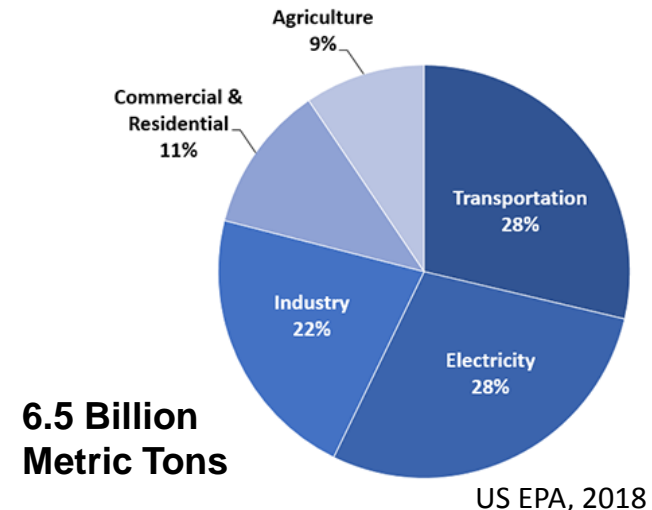
*FY19 Seed Project

Problem Statement

- Ethanol biorefineries largest supplier of CO₂ to US merchant gas markets¹
 - 200M gal/year ethanol plant releases 72 tons CO₂/hr
- Inexpensive, intermittent electricity available & increasing
- ***Opportunity to increase economic viability of biorefineries***
 - Drive down cost (MFSP) of primary product (ethanol)
 - Improve biorefinery carbon utilization
- First CO₂ Utilization technologies will use pure CO₂ waste streams
- Opportunity to develop technologies that will ultimately reach a *much larger market*



Total U.S. Greenhouse Gas Emissions by Economic Sector in 2016



Goal Statement

Goal: Advance the state-of-the-art (SOA) for both electrochemical and thermochemical conversion of CO₂ via catalyst and electrolyzer development. Provide an assessment of the potential of each route to enhance biorefinery profitability.

Objectives:

- Identify & rank most desired CO₂ conversion products
 - In collaboration with the Feasibility Study (Schaidle PI)
- Establish experimental baseline based on published results
- Develop catalysts & electrolyzer configurations that outperform baseline (**Target:** 20% reduction in overpotential for C₂₊ products)

Outcome

- Facilitate economic processing of large biorefinery waste stream

Quad Chart Overview

Timeline

- Start: 10/1/2017
- End: 9/30/2020
- 47% Complete

Budget

	Total Costs Pre FY17	FY 17 Costs	FY 18 Costs	Total Planned Funding (FY 19-Project End Date)
DOE Funded			354k	1500k

Collaboration within BETO

- *Feasibility Study of Utilizing Electricity to Produce Intermediates from CO₂ and Biomass. 2.1.0.304 (Josh Schaidle PI)*
- *CO₂ Valorization via Rewiring Metabolic Network. 2.3.2.106 (Pin-Ching Maness PI)*
- *Advanced Catalyst Synthesis and Characterization (ACSC). 2.5.4.304 (Susan Habas PI)*

BETO Barriers Addressed

- Ct-E: Improving Catalyst Lifetime
- Ct-F: Increasing the Yield from Catalytic Processes
- Ct-G: Decreasing the Time and Cost to Developing Novel Industrially-Relevant Catalysts

Objective:

- Develop catalysts & electrolyzer configurations that outperform established baseline

End of Project Goal:

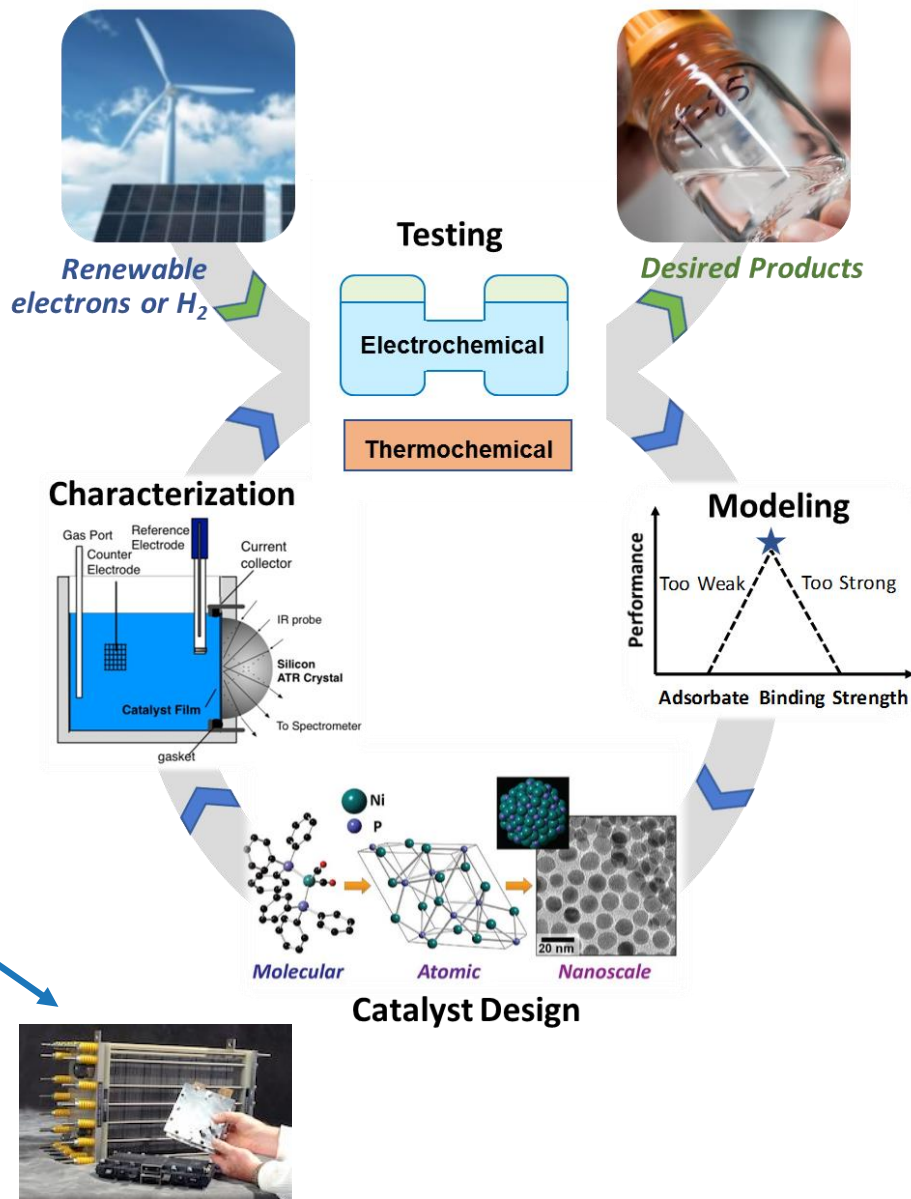
- Demonstrate Enhanced Biorefinery Profitability: For the most promising pathway studied, show how a biorefinery could increase profits from a CO₂ waste stream.

Cross Office Collaboration

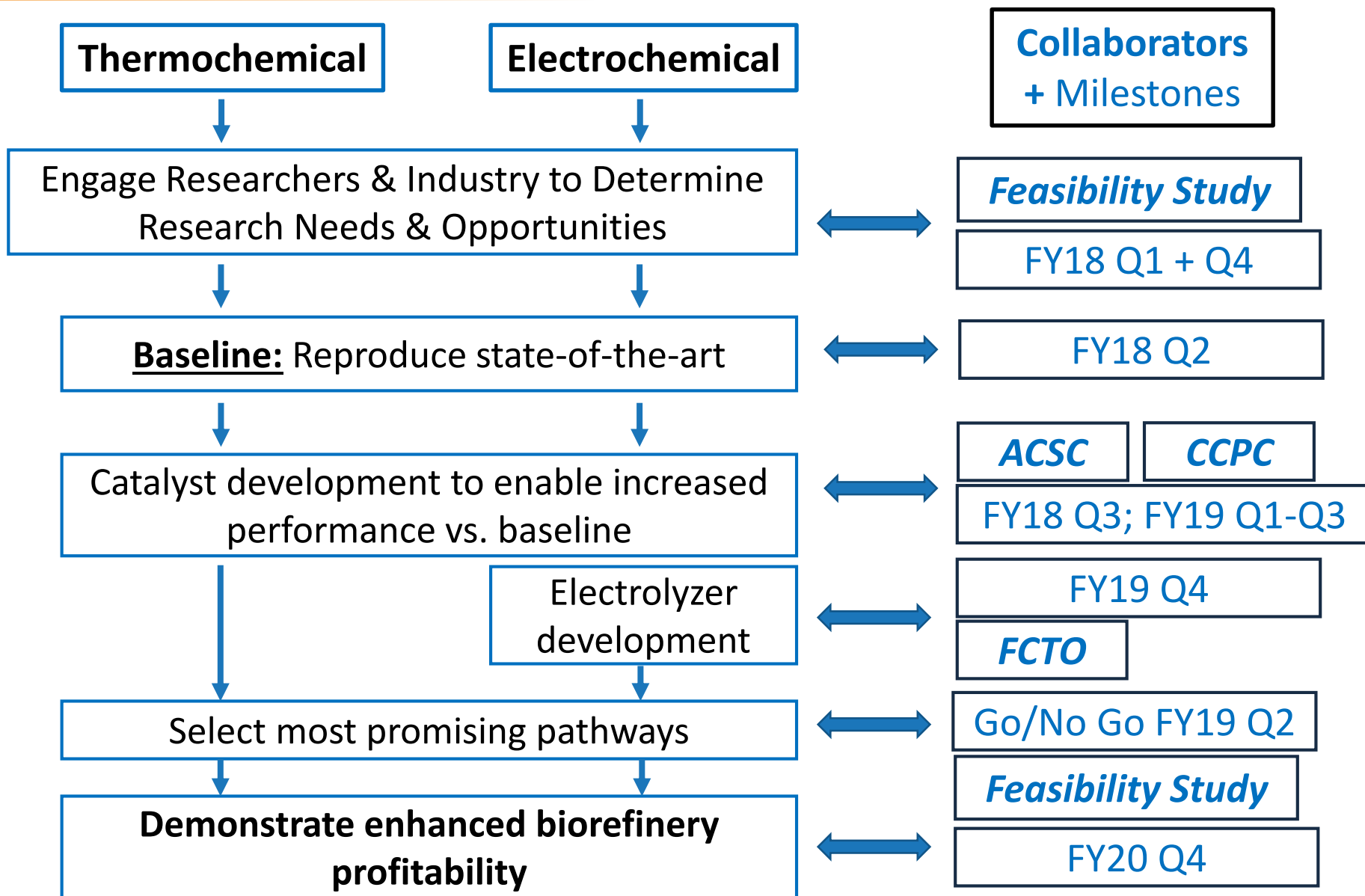
- *Industrially scalable waste CO₂ reduction to useful chemicals and fuels. FCTO (Todd Deutsch PI)*

Project Overview

- Catalyst development for two routes
 - Thermochemical
 - Water electrolysis to produce renewable hydrogen
 - Electrochemical (low-temp)
 - Direct use of renewable electricity to drive CO₂ conversion
- Leverage advanced capabilities within ChemCatBio
 - **Identify, synthesize, characterize, and test new catalysts for CO₂ conversion to desired C₂₊ products**
- Electrolyzer development – existing options insufficient
 - Order of magnitude difference in performance between aqueous cell and electrolyzer with gas-phase CO₂
- Creation of *standard methods for electrocatalyst evaluation* in relevant environment



Management Approach



Technical Approach: Tunable Materials

Top Technical Barriers Identified by Feasibility Study

Electrochemical

- High overpotential, low energy efficiency
- Poor selectivity to individual C₂₊ products
- Low single-pass CO₂ conversion

Thermochemical

- Process Intensification & Scale-down
- Developing multi-functional water and CO₂ tolerant catalysts

Hypothesis: Tune key reaction into

Stronger CO Binding

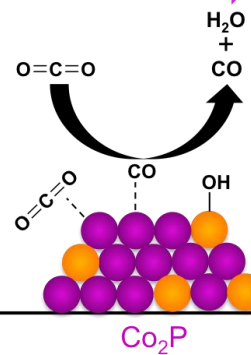
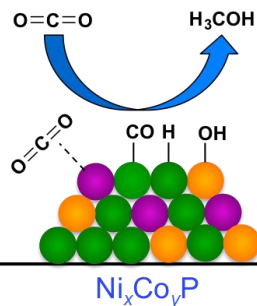
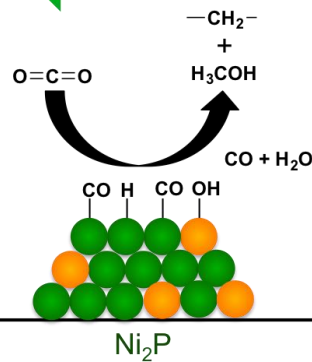
Targeted Reactivity

Weaker CO Binding

or stabilization of
ance catalysts

- Identify pr
& Chemisti

- Synthesize

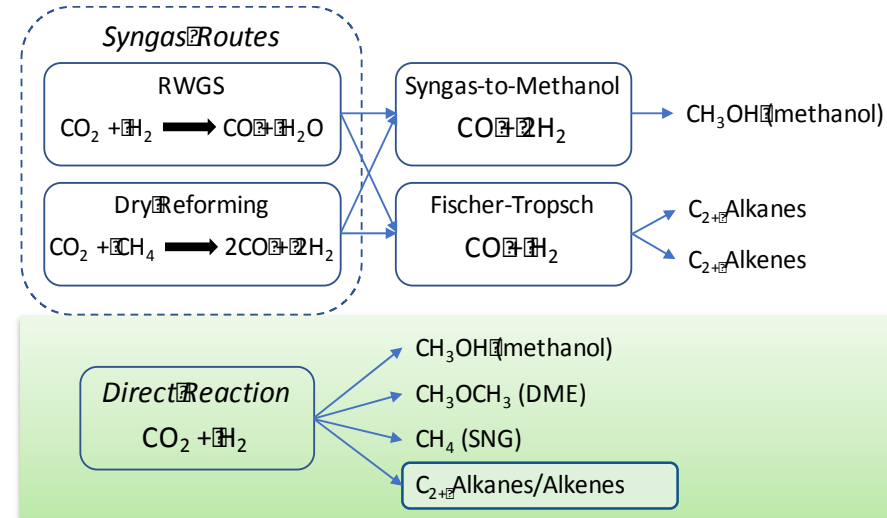
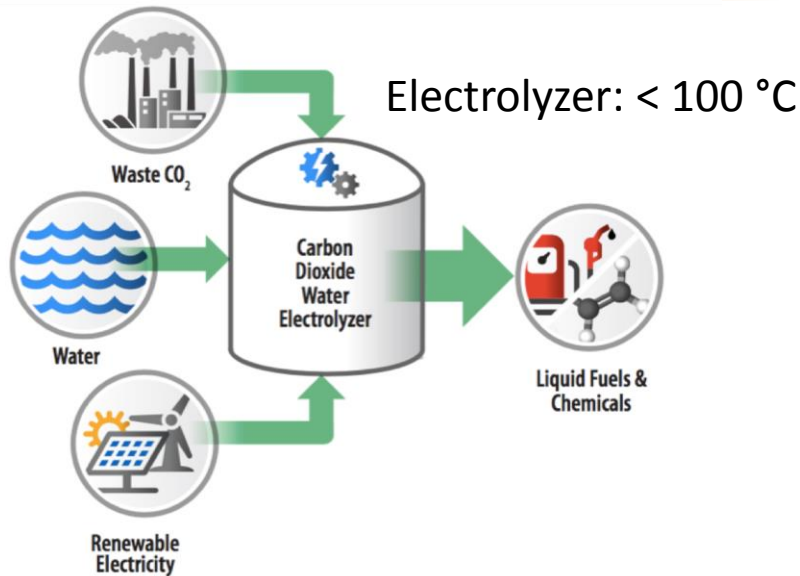


onal Physics

d Synthesis

Success Factor: Develop catalysts that advance state-of-the-art by addressing identified technical barriers

Technical Approach



Electrochemical

- Targeting formation of C_{2+} products with high efficiency & selectivity

Thermochemical

- Targeting direct formation of C_{2+} products via multi-functional catalysts

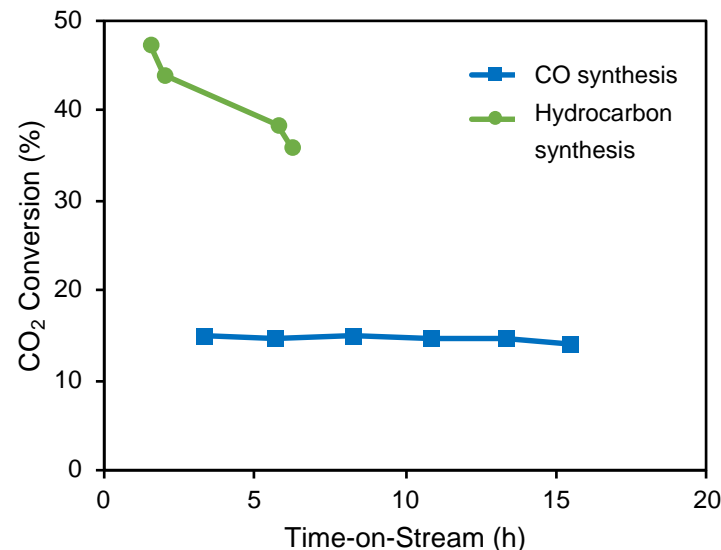
Success Factors

- **Electrochemical**: Develop catalysts & electrolyzers that enable long-term and efficient operation at high currents
- **Thermochemical**: Develop catalysts that enable process intensification & scale-down

Progress: Thermochemical

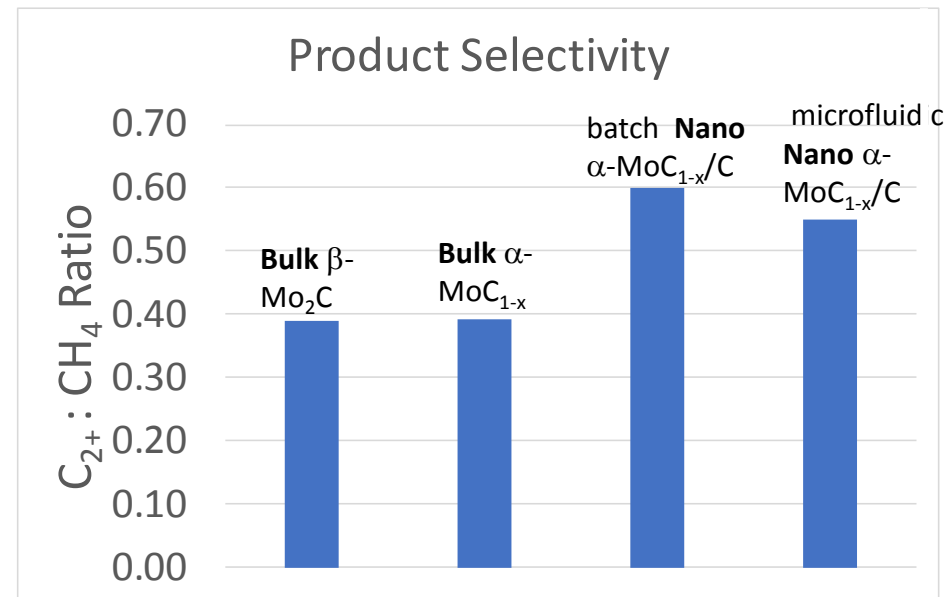
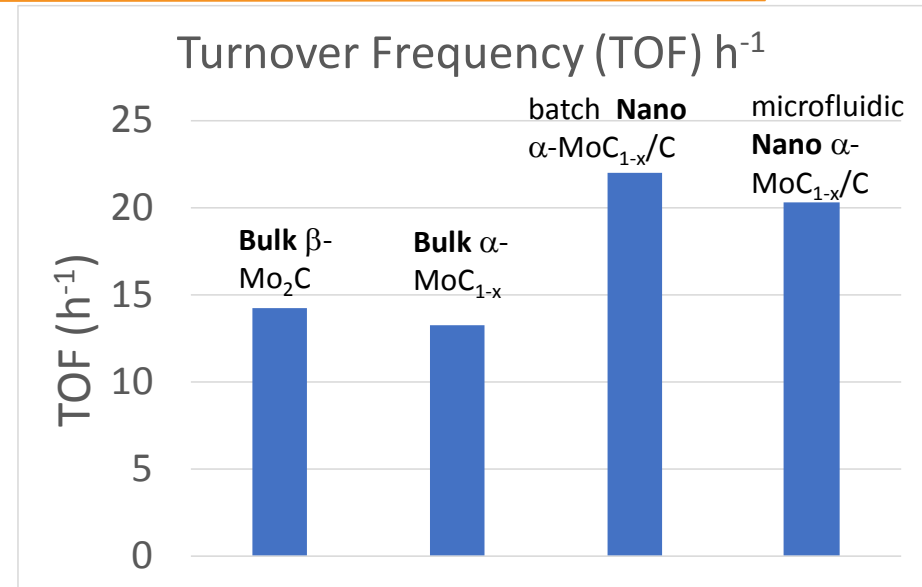
- Bulk MoC is state-of-the-art for thermochemical CO₂ conversion
- **Reproduced literature values** with NREL catalysts @ two conditions
 - Cokes during C-C coupling
- Despite good RWGS activity, *MoC binds CO₂ too strongly*
 - Undesirable terminal product
- CH₄ main hydrocarbon product
 - Undesirable terminal product

Temp. (°C)	Press. (MPa)	WHSV (h ⁻¹)	H ₂ :CO ₂ ratio	Conv. (%)	Selectivity (mol%)				Ref.
					CO	CH ₄	C ₂ H ₆	C ₃ H ₈	
<i>CO synthesis</i>									
300	0.1	23.6	2	14.8	93.3	4.8	1.5	0.3	
300	0.1	23.6	2	8.7	93.5	6.5	–	–	1
<i>Hydrocarbon synthesis</i>									
300	2	3.9	5	36.0	6.4	68.9	17.5	5.1	
300	2	3.9	5	24	28	45	13	9	2



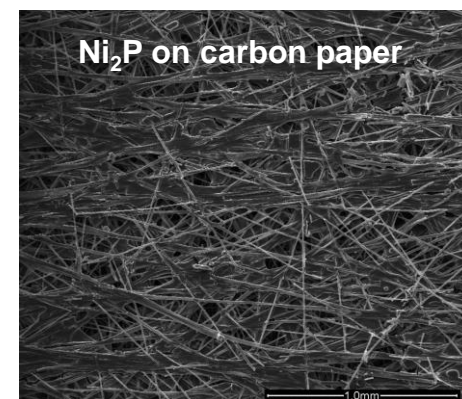
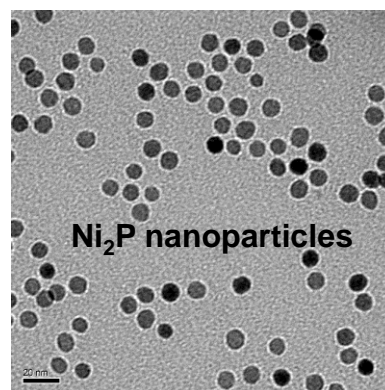
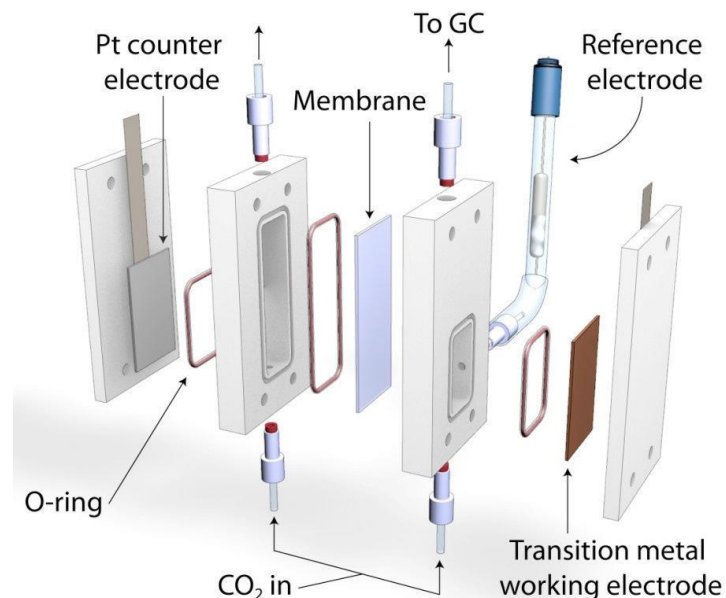
Progress: Thermochemical - Nanoscale Carbides

- **Nanoscale carbides promising: more active, more selective**
- Bulk carbides show slight deactivation
- Nanoscale MoC shows increase in conversion with TOS
- *Nanoscale MoC more active per Mo site*
- Bulk β - Mo_2C favors complete hydrogenation to CH_4
- *Nanoscale catalysts enhance selectivity to C_{2+} products relative to CH_4*



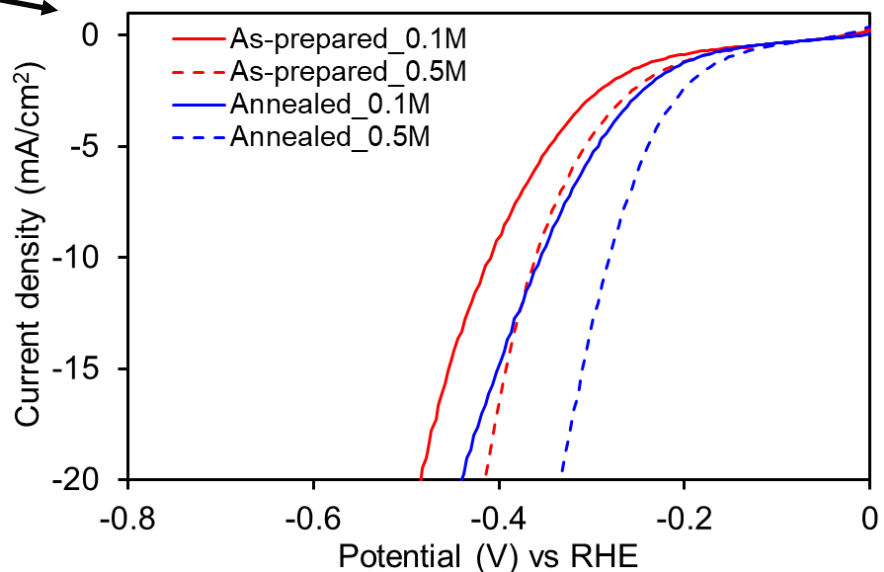
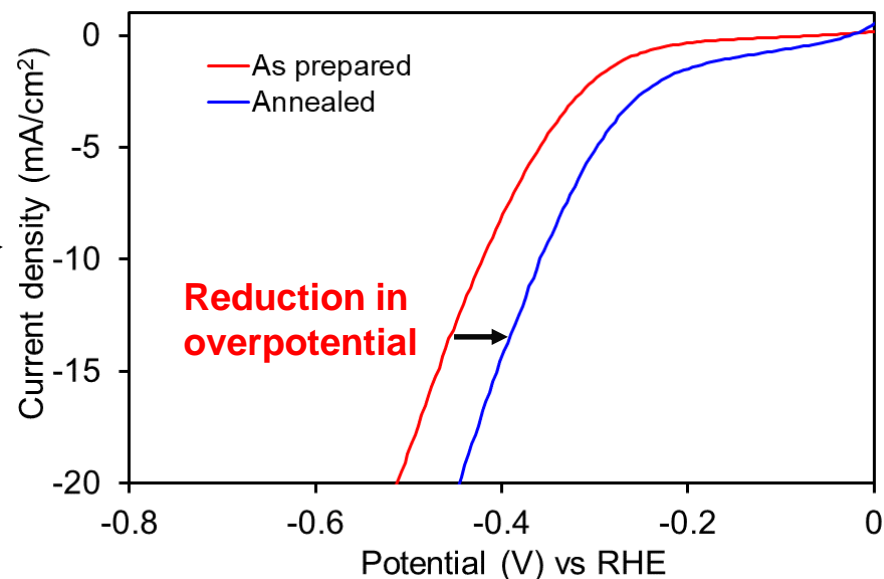
Progress: Electrochemical - Metal Phosphides

- **Successfully reproduced SOA results with Cu¹**
 - 10 mA/cm² total current @ 1.1 V (vs. RHE)
 - *Low current typical of aqueous systems*
 - Built electrochemical cell to match SOA
 - Small electrolyte volume, large electrodes – aid in product detection
- Recent results with phosphides promising – C₃-C₄ products²
- **Ni₂P** electrochemical testing
 - Supported on carbon paper
 - KHCO₃ electrolyte
 - 0.1 M and 0.5 M

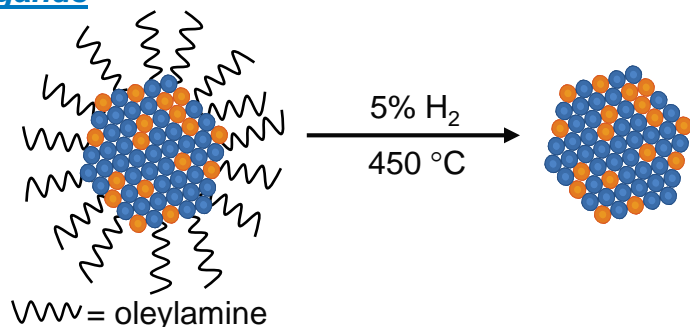


Progress: Electrochemical - Nickel Phosphide

- Ni₂P supported on carbon paper is electrochemically active
- **Annealing** (removal of ligands) has positive effects on electrochemical activity
 - Reduction in overpotential
 - Increase in electrochemically-active surface area
 - Reduction in charge transfer resistance
- Effect of KHCO₃ concentration
 - Reduction in overpotential for both Ni₂P catalysts in more concentrated electrolyte



Ni₂P annealed to remove insulating organic surface ligands



Progress: Electrolyzer Development

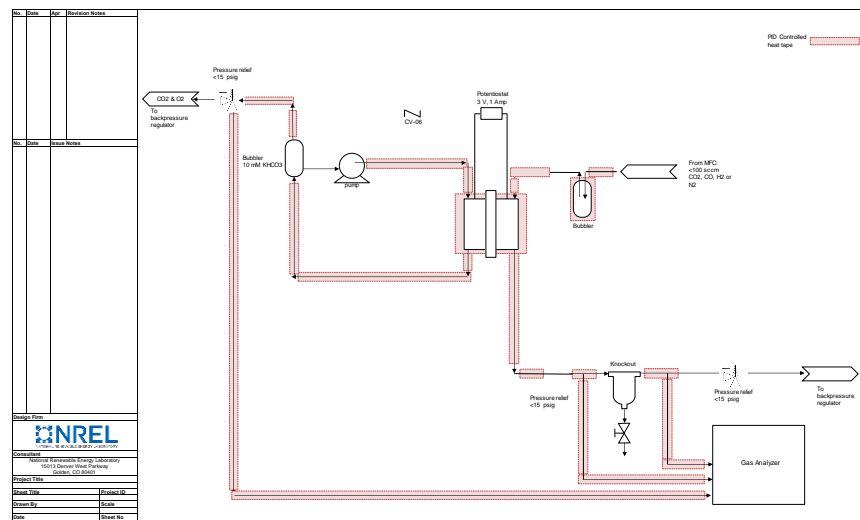
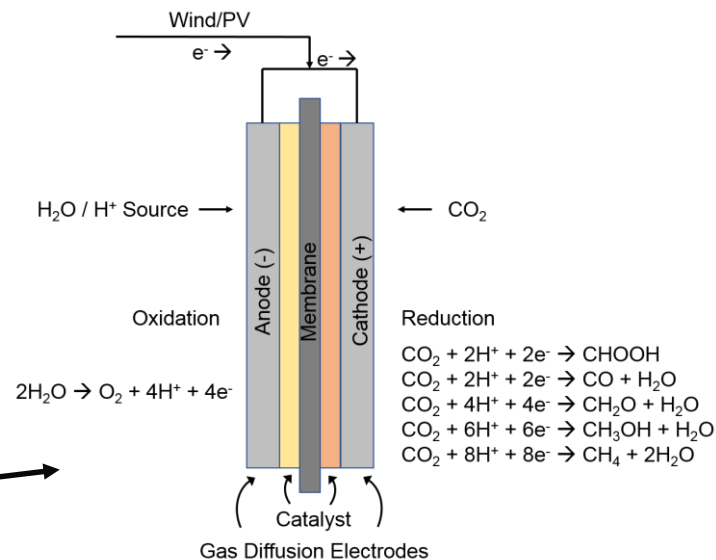
- Widely-accepted that any scalable electrolyzer *must operate on gas-phase CO₂*
 - Aqueous systems mass transfer limited (~20 mA/cm²)
 - Aqueous results may not translate to electrolyzer*

- Focusing on membrane-electrode-assemblies (MEAs)**

- Polymer membrane + catalysts
- Stacked together for scaleup

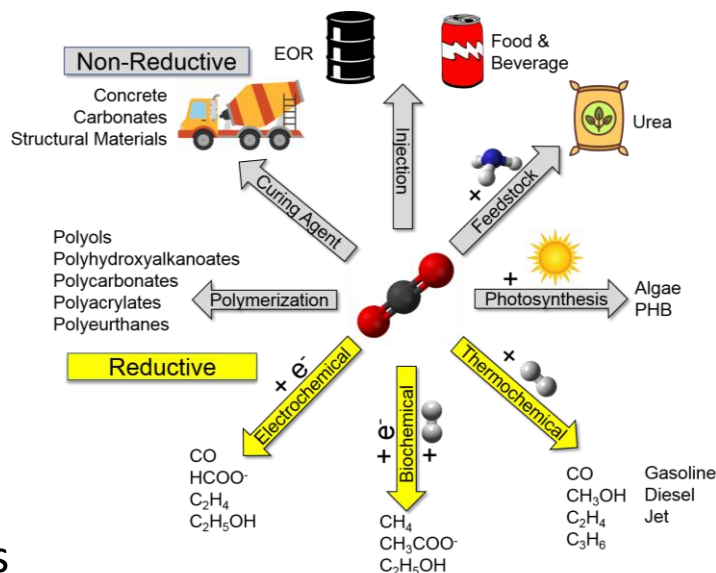
- Design/Retrofit/Build electrolyzer**

- Experiment in ventilated enclosure
- Interface analytical
- Liquid circulation



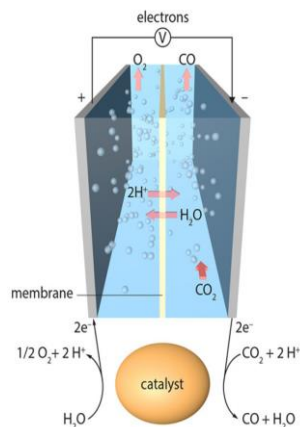
Relevance

- **Expanding BETO feedstock slate**
 - BETO actively investigating strategies for adding value to waste streams such as CO₂
- **Addressing top technical barriers** identified by Feasibility Study for C₂₊ products
 - Electrochemical: New catalysts to reduce overpotential & increase selectivity, new electrolyzer architectures
 - Thermochemical: New catalysts to enable process intensification & scale-down
- Will assess impact of new catalysts on MFSP
- **Tunable multi-functional materials** to advance state-of-the-art
 - Thermochemical: carbides to enable process intensification
 - Electrochemical: phosphides + electrolyzer development

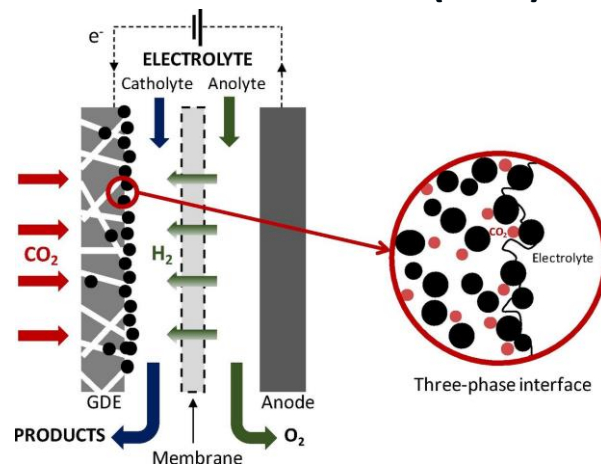


Relevance

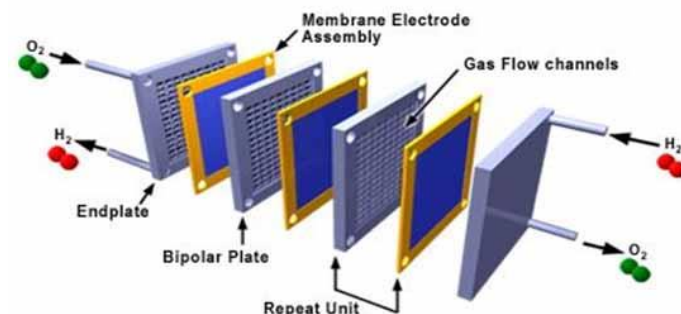
Aqueous



Gas Diffusion Electrode (GDE)



Membrane Electrode Assembly (MEA)



Experimental Accessibility

Commercial Applicability

- $[CO_2] \sim 35\text{mM}$ in aqueous solution
- Currents to $\sim 1\text{-}20\text{ mA/cm}^2$
- *Bulk of catalyst development performed in aqueous systems*

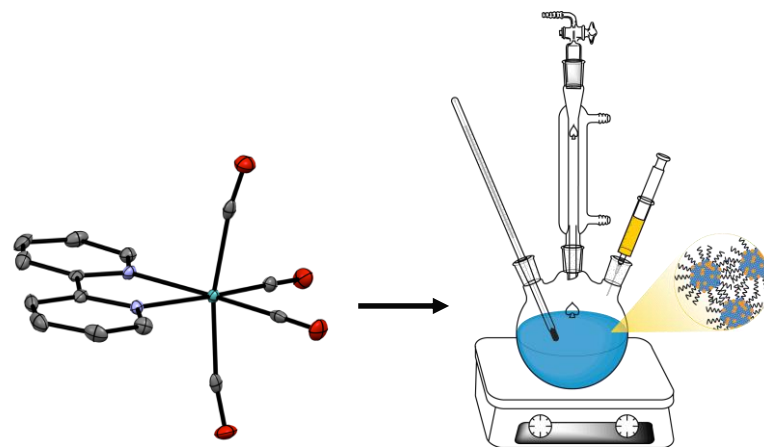
- GDE with flowing liquid electrolytes
- Currents to 100's mA/cm^2
- *Scalable with flowing electrolytes? Long-term operation?*

- Gas-phase operation
- Currents to 100's mA/cm^2
- Easily scalable into a stack configuration
- **No consensus on CO_2 MEA**
 - Alkaline, proton exchange, or bipolar membrane
 - Buffer layers to control pH

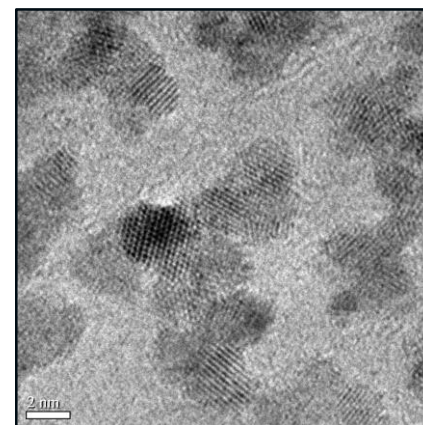
Future Work: Thermochemical

- ***Inform next-generation of catalysts for CO₂ conversion***
- Catalyst development for direct C₂₊ hydrocarbons & olefins
 - Tunable nanoscale carbides
 - Control size, shape, composition
 - Tunable hydrogenation & acidic sites
 - Alloying & Metal modification
 - High surface area supports (C, SiO₂, TiO₂, Al₂O₃)
- Investigate catalyst under working conditions
 - *In-situ* or post-reaction characterization to monitor catalyst changes during CO₂ conversion
 - Correlate catalyst features with performance
 - *FY19 Q3 Milestone*

Leverage ACSC Capabilities

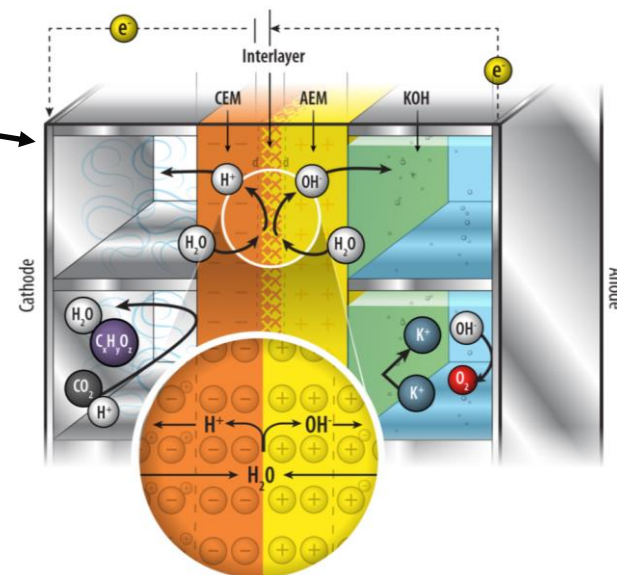
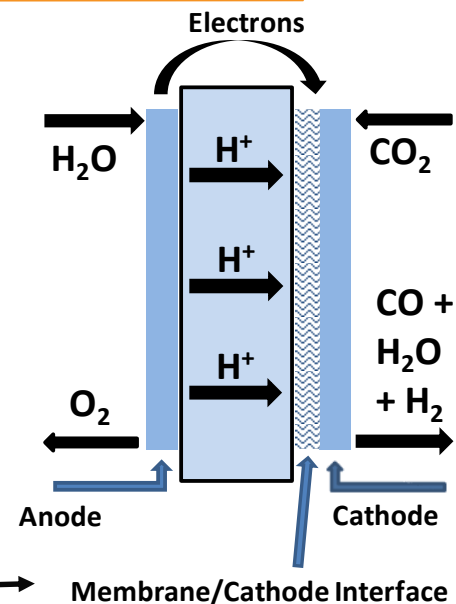


Nanoscale α -MoC_{1-x}



Future Work: Electrochemical

- Electrocatalyst development
 - Metal phosphides & mixed metal phosphides (*FY19 Q2 Milestone*)
 - Incorporation of promising catalysts into MEAs
- Electrolyzer development
 - Test alkaline and proton exchange membrane MEAs (*FY19 Q4 Milestone*)
 - Effect of different buffer layers
 - Compare with bipolar membrane MEAs
 - In collaboration with FCTO (Deutsch PI)
 - Explore economic tradeoffs in collaboration with the Feasibility Study (2.1.0.304, Schaidle PI)
 - *Testbed: reproducible system for catalyst evaluation in realistic environment*
 - *Standard methods for electrocatalyst testing*



Summary

Approach: CO₂ Utilization has potential to increase biorefinery profitability

- Both ***electrochemical*** and ***thermochemical*** routes under investigation
 - Catalyst development required to advance both
 - Leveraging capabilities within ChemCatBio & NREL

Progress: Reproduced state-of-the-art results

- Thermochemical: nanoscale carbides have advanced state-of-the-art
- Electrochemical: actively researching novel phosphides & new electrolyzer architectures

Relevance: Engaged CO₂ community to determine research needs

- Executing research to address needs and ***advance state-of-the-art***
- *Opportunity for biorefineries to be first players in growing field*

Future Work: Continue catalyst & reactor development

- Economic projections (with Feasibility Study) to remain relevant

Acknowledgements

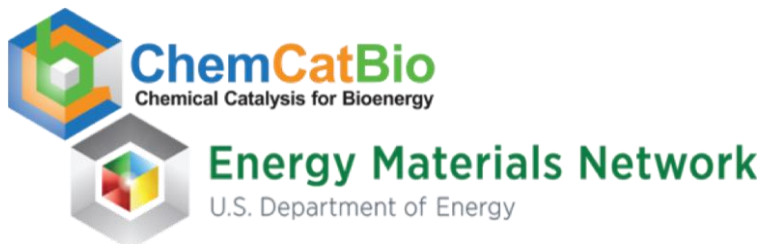
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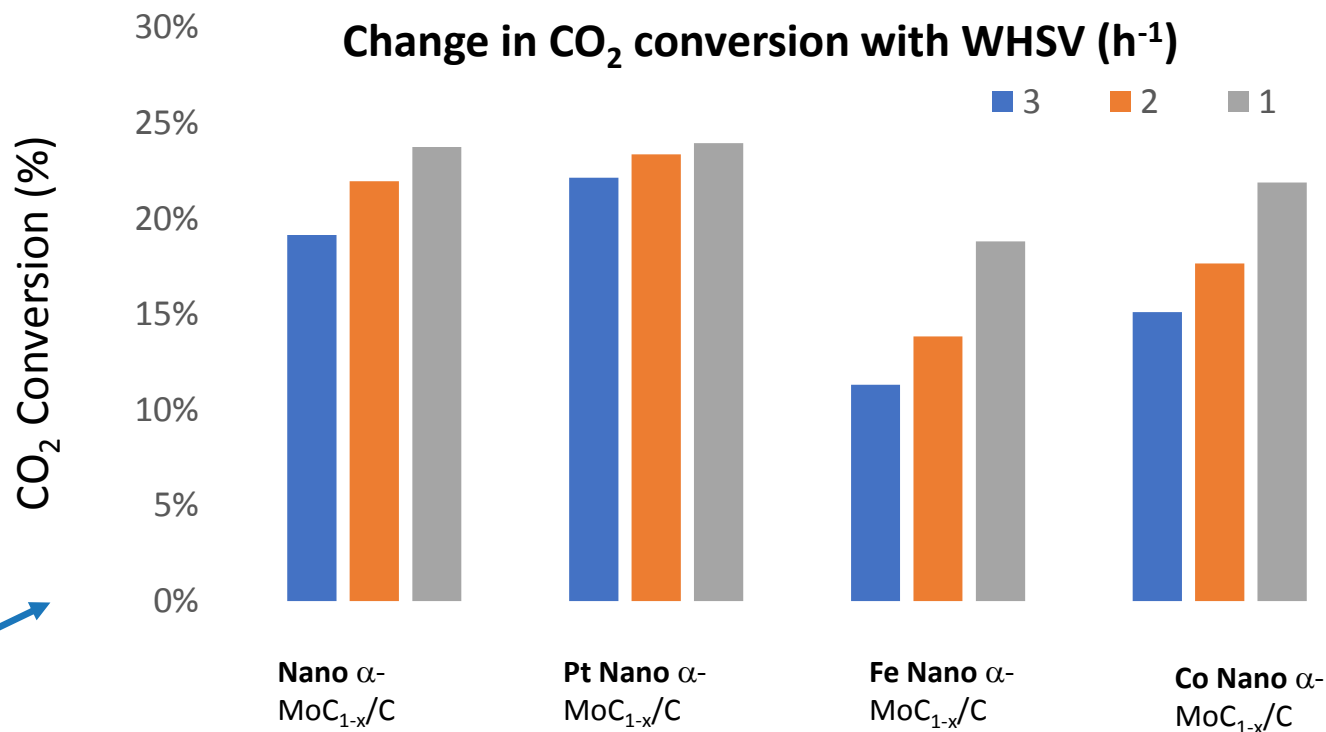


Questions?



Progress: Thermochemical - Metal-Modified Nanoscale Carbides

- **Pt, Fe & Co** metal-modifiers
- Metal-modified catalysts *reach stable performance more quickly*



- Activity: Pt/MoC > MoC > Co/MoC > Fe/MoC
- Pt/MoC & MoC operate near RWGS equilibrium (~23% conversion)
- Consistent selectivity change with CO₂ conversion – *sequential reaction path*
 - CO₂ → CO → Hydrocarbons