

The Challenge of Mass Transport Resistance in Catalyst Layers and Its Impact to Performance at High Current Density

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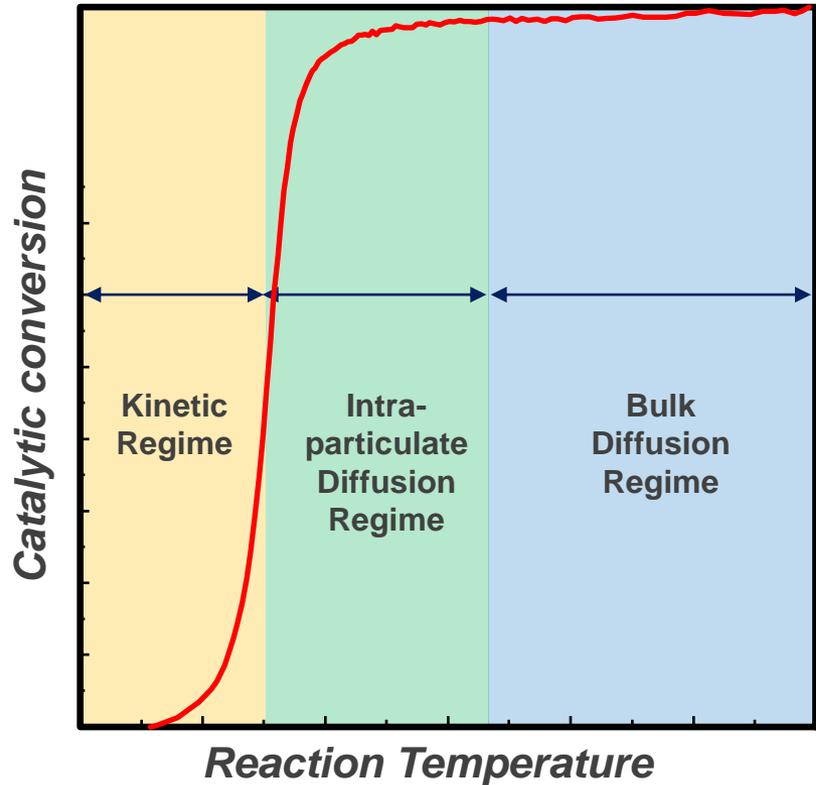
Presented at DOE CATALYSIS WORKING GROUP MEETING

Wednesday, July 27, 2016

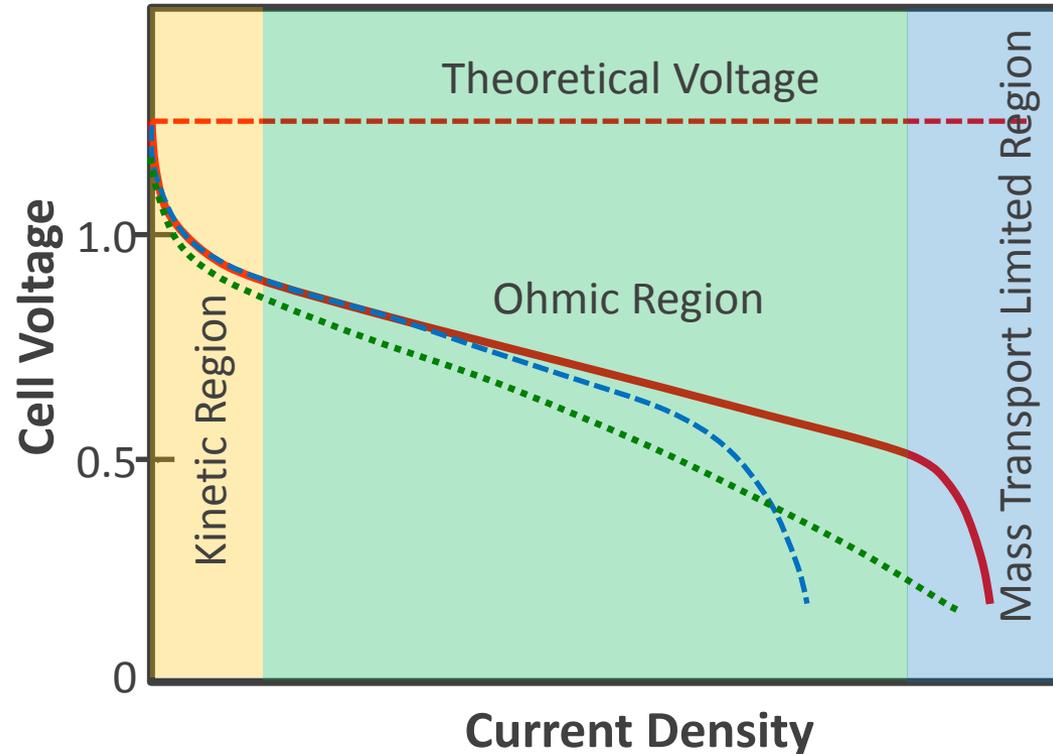
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Mass Transport Limited Region in Fuel Cells

Heterogeneous Catalytic Conversion



Fuel Cell Polarization Curves



Availability → Accessibility → Activity



Key Factors Hampering Fuel Cell Performance at High (or low) Current Domain

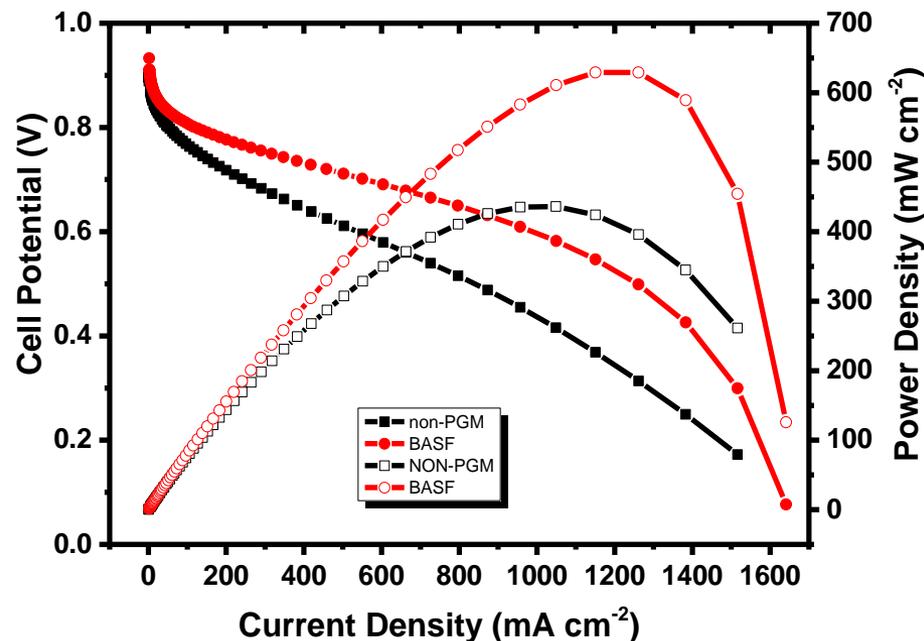
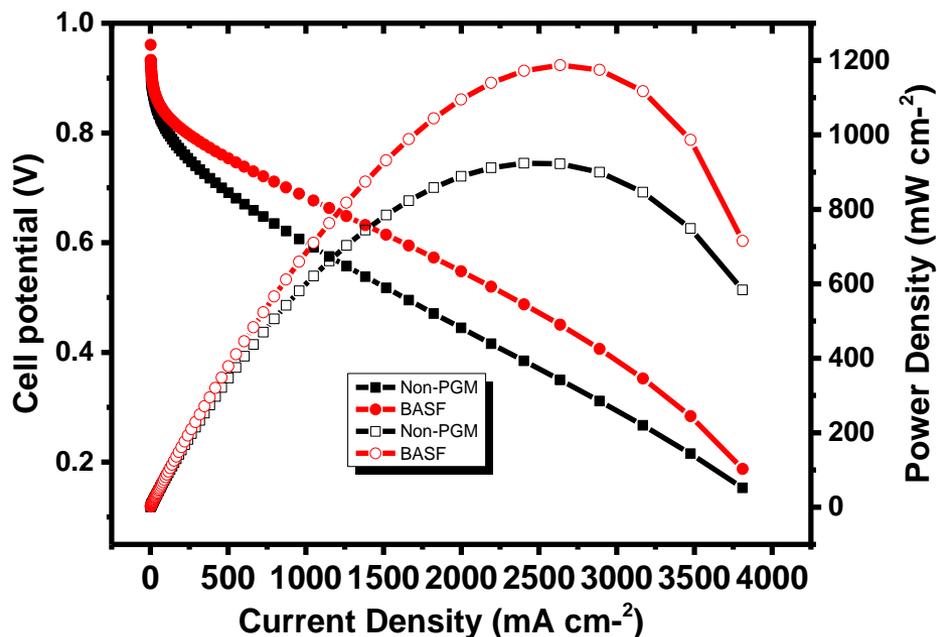
- Lack of Activity – low turn-over-frequency (TOF)
- Lack of Accessibility – active site not near triple-phase boundary
- Lack of Accessibility – mass transport resistance
- Lack of Availability – insufficient active site density
- Lack of Reactant – mass transfer rate $<$ conversion rate



Examples of Performance Differences at High Current Region between PGM and PGM-free Catalyst Electrodes

One-bar Oxygen

One-bar Air

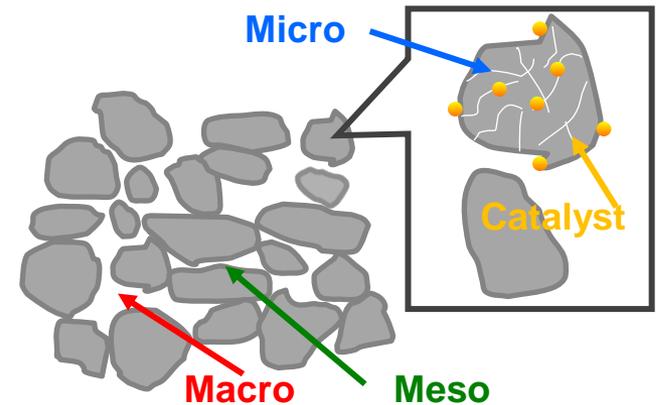


Condition: P_{air} or $P_{\text{O}_2} = P_{\text{H}_2} = 1$ bar (back pressure = 7.3 psig) fully humidified; $T = 80$ °C; N-211 membrane; 5 cm² MEA; PGM-free cathode catalyst = 3.5 mg/cm², anode catalyst = 0.3 mg_{Pt}/cm².
Commercial BASF MEA, cathode catalyst = 0.35 mg_{Pt}/cm², Anode catalyst = 0.2 mg_{Pt}/cm²



Challenges in Catalytic Structure using Conventional Carbon Support

- **Micro→meso→macro tiered structure held by vdW force**
- **Mass transfer through propagation of different porosities (Knudsen vs. molecular diffusions)**
- **Charge/heat transfer through particle contact percolation**

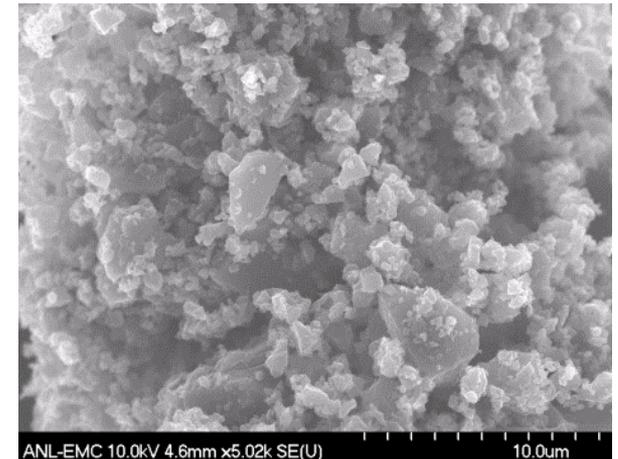


Gas diffusion inside electrode

$$D_{\text{eff}} = \varepsilon D / \tau; \varepsilon = \text{porosity}$$

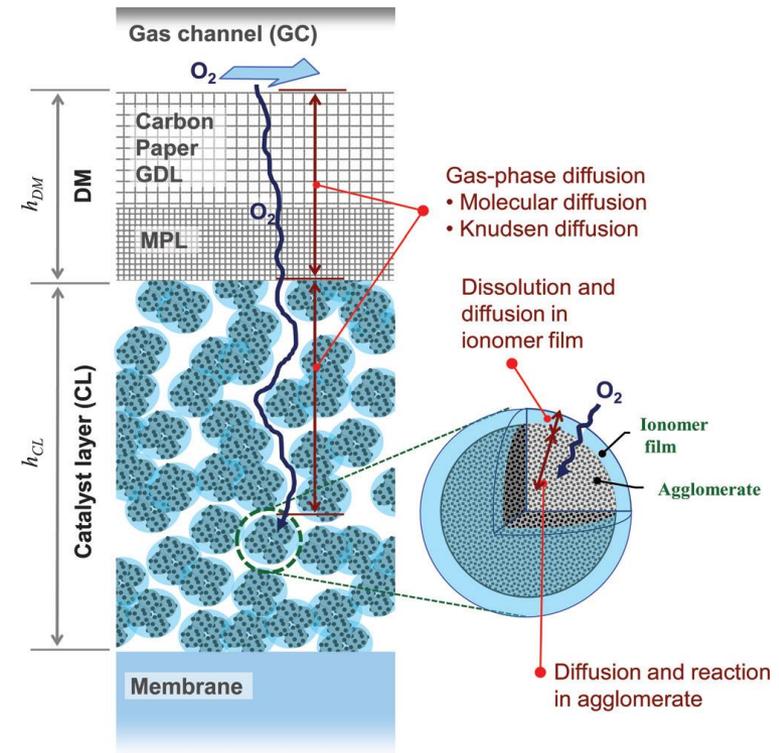
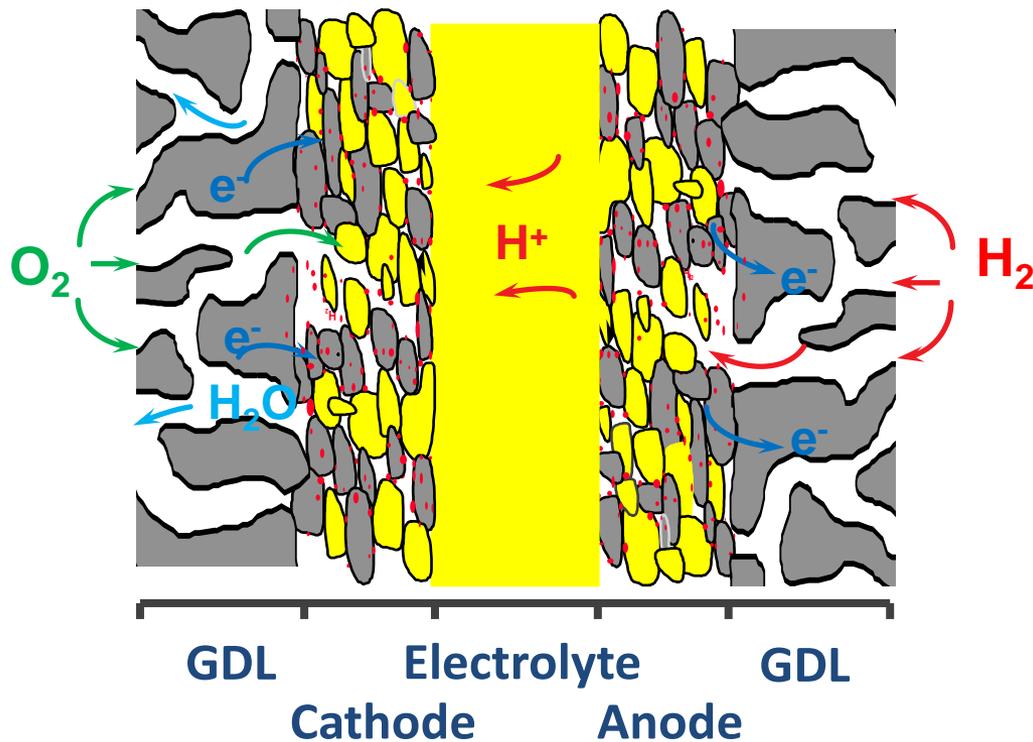
$$\tau = (\text{path } l / \text{straight } l)^2$$

$$1/D_{\text{eff}} = 1/D_{\text{micro}} + 1/D_{\text{meso}} + 1/D_{\text{macro}}$$



Challenges in Electrode Architecture using Conventional Carbon Support

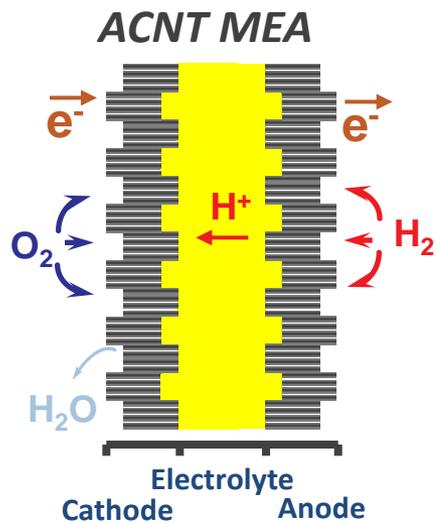
Conventional Membrane Electrode Assembly



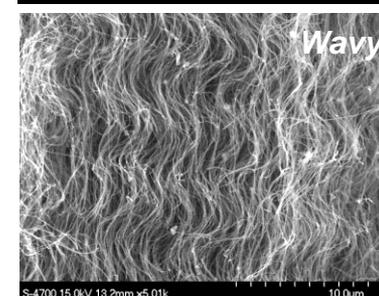
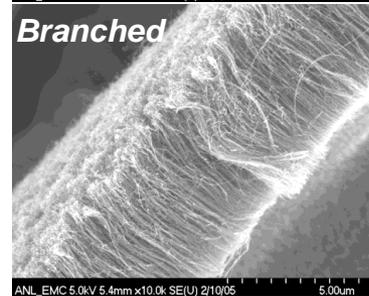
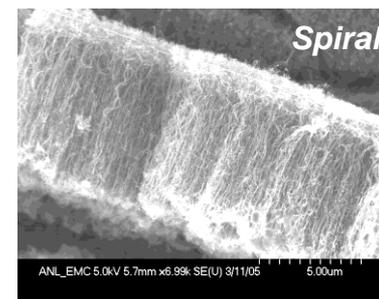
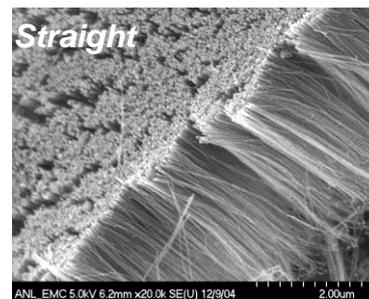
Nonoyama, et. al. *JES* 158 (4) B416, (2011)

Aligned Carbon Nanotube (ACNT) as Catalytic Support for PEMFC

Advantages of ACNT based MEA

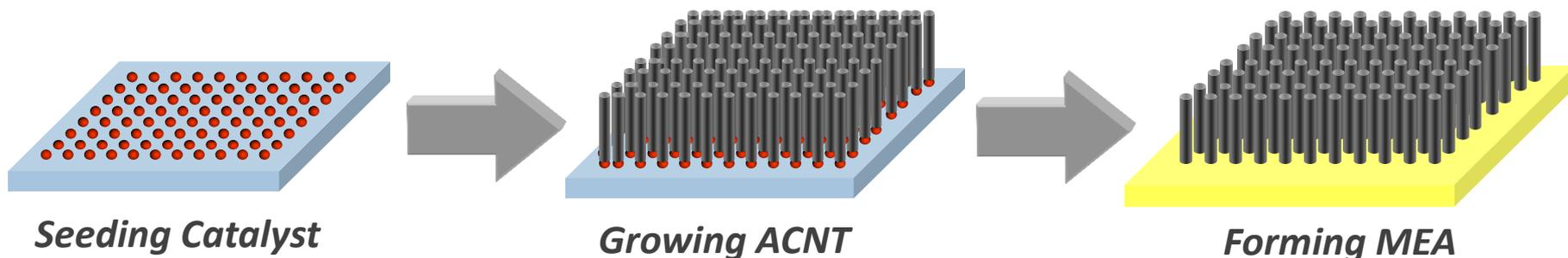


- Better catalyst utilization
- Better support stability
- Better electrical & thermal conductivity
- Better water management
- Better mass transport
- Functionalized ACNT as PGM-free catalyst

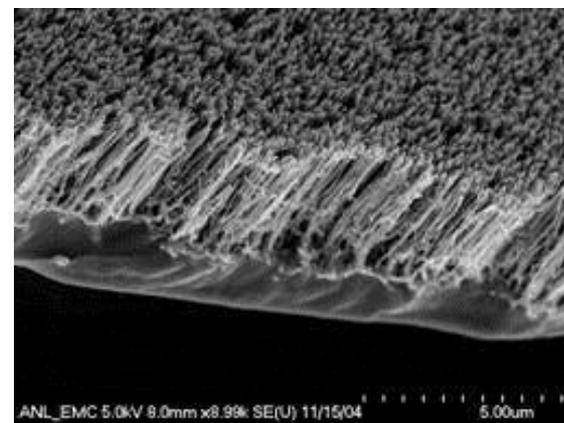
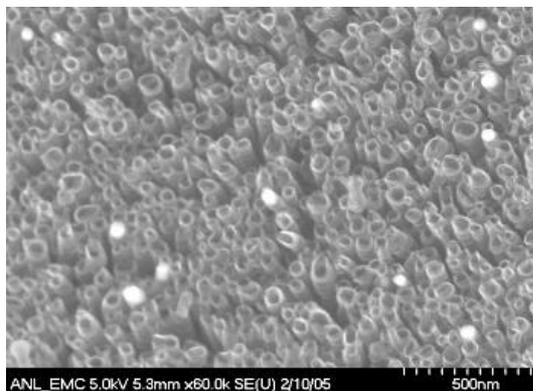
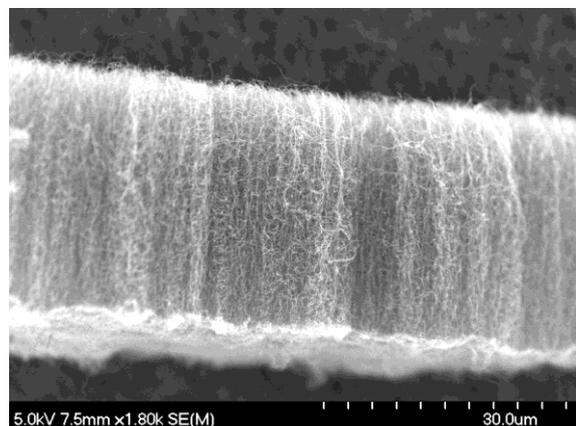


- J. Yang, G. Goenaga, A. Call and D.-J. Liu*, *Electrochem. Solid-State Lett.*, (2010) 13 (6) B55-B57,
J. Yang, D.-J. Liu*, N. Kariuki and L. X. Chen, *Chem. Comm.* 3 (2008) 329 – 331
D.-J. Liu*, J. Yang, N. Kariuki, G. Goenaga, A. Call, and D. Myers, (2008), *ECS Trans.*, 16 (2) 1123-1129
J. Yang and D.-J. Liu*, *Carbon* 45 (2007) 2843–2854.
D.-J. Liu, J. Yang and D. Gosztola, *ECS Transc.* (2007) 5(1) 147-154

Process of Fabricating ACNT as Catalyst Support of MEA



Fabricating ACNT as catalyst support in MEA



“Method of fabricating electrode catalyst layers with directionally oriented carbon support for proton exchange membrane fuel cell”, Liu & Yang, **US Patent 8,137,858**

“Catalytic Membranes for Fuel Cells”, Liu & Yang, **US Patent 7,927,748**

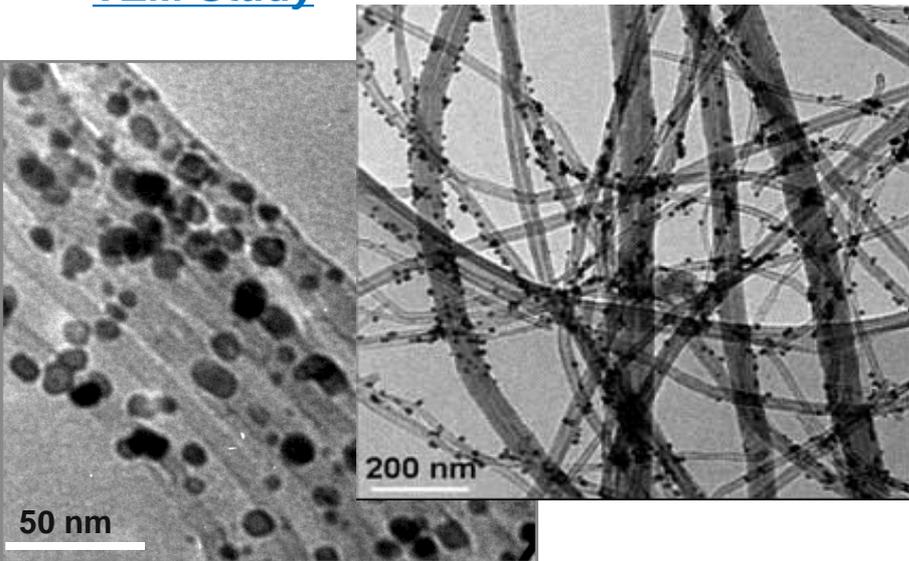
“Aligned carbon nanotube with electro-catalytic activity for oxygen reduction reaction”. Liu, Yang & Wang, **US Patent 7767616**

“Method of fabricating electrode catalyst layers with directionally oriented carbon support for proton exchange membrane fuel cells”, Liu, Yang & Wang, **US Patent 7,758,921**

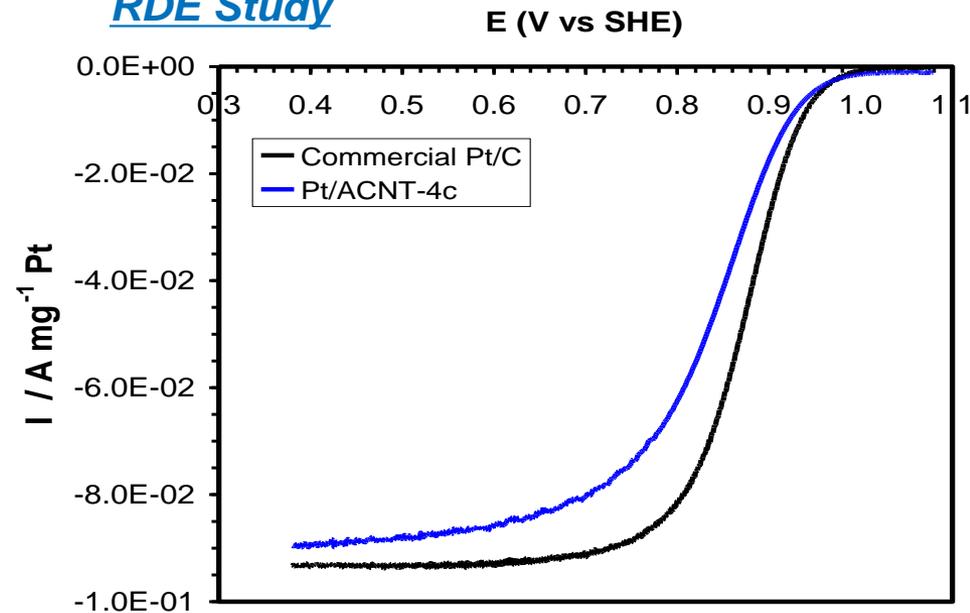
Catalyzing ACNT with Pt via Dry and Wet Chemistries

- Bifunctional solvents needed to avoid nanotube bundling
- CVD processes enable >20 wt% Pt incorporated in ACNT
- Highly dispersed Pt with particle sizes from 2 nm ~6 nm was observed
- Relatively uniform distribution through depth of ACNT layer was observed

TEM Study



RDE Study



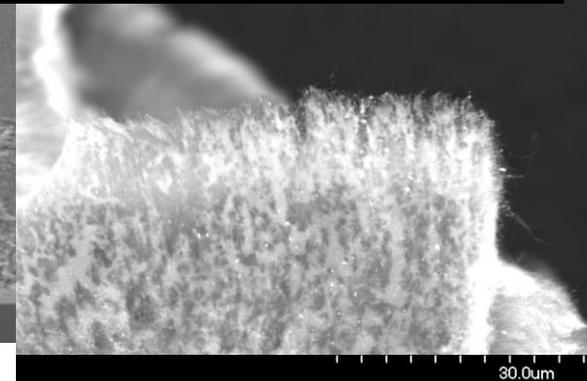
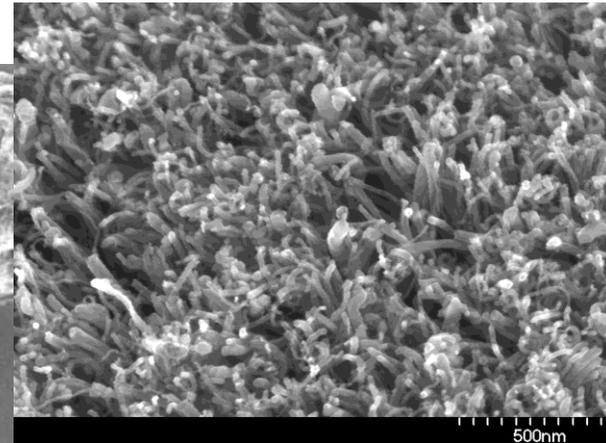
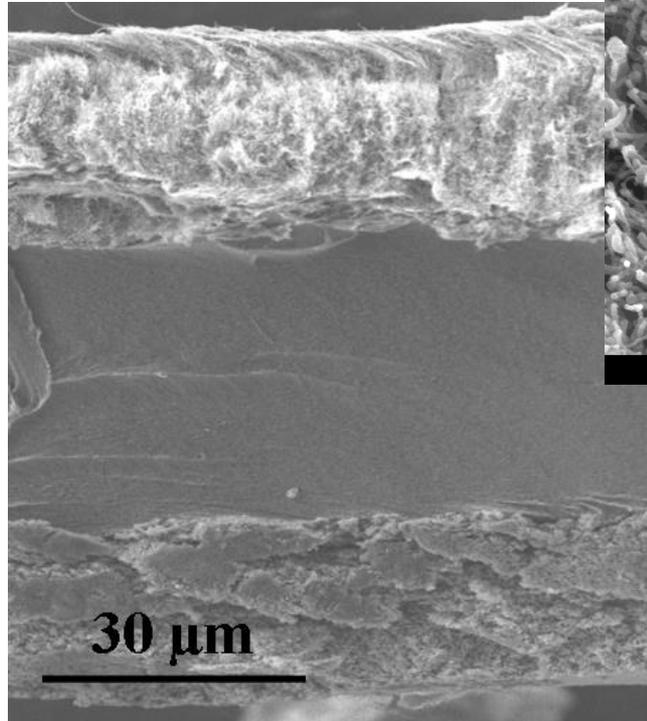
Pt/ACNT prepared through CVD process demonstrated very good electrochemical activity even with highly hydrophobic surface

Cross-section Characterization of ACNT-MEA

ACNT
Cathode
Layer

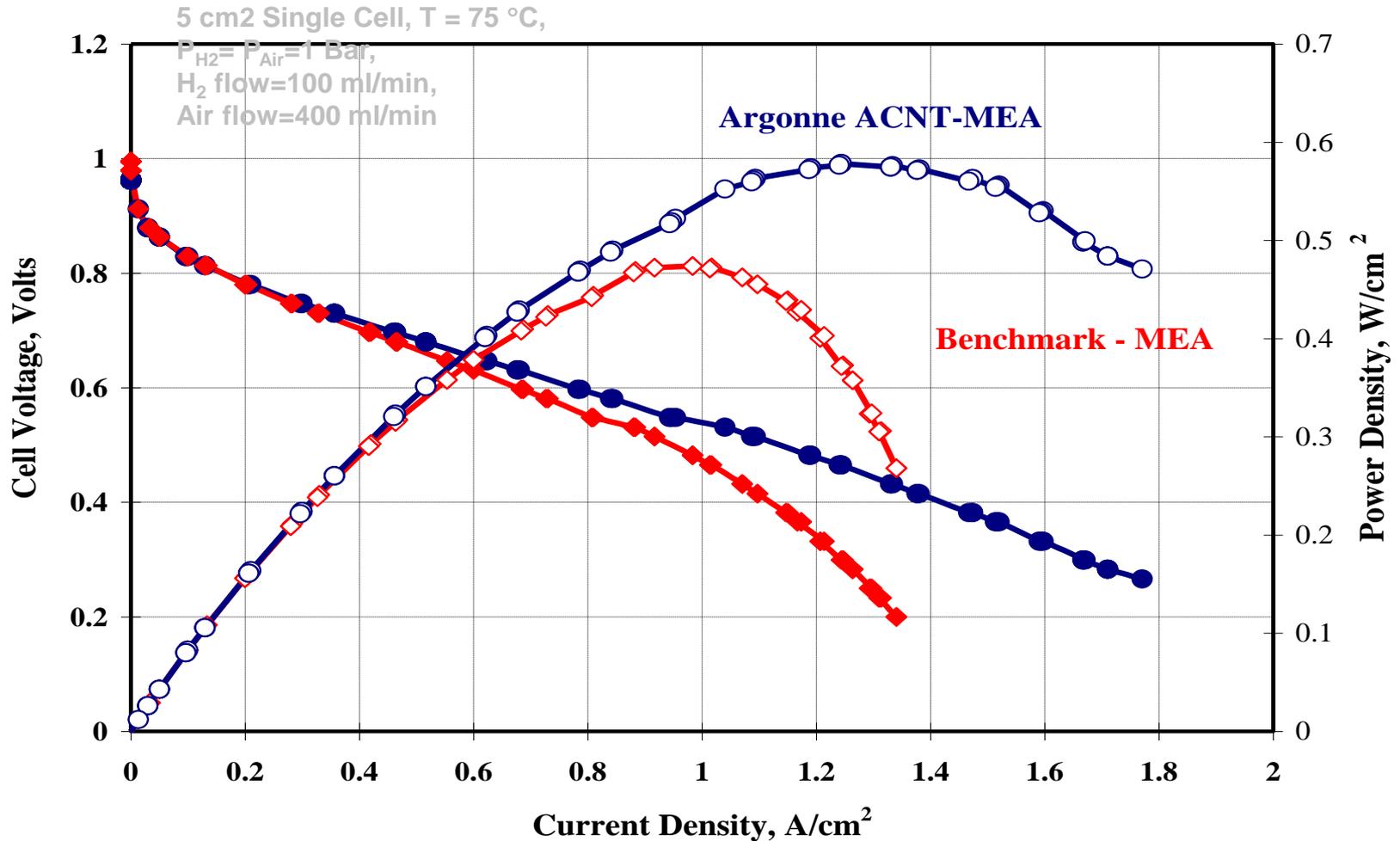
Nafion®
Membrane
Layer

Ink-based
Anode Layer



SEM Images of ACNT-MEA

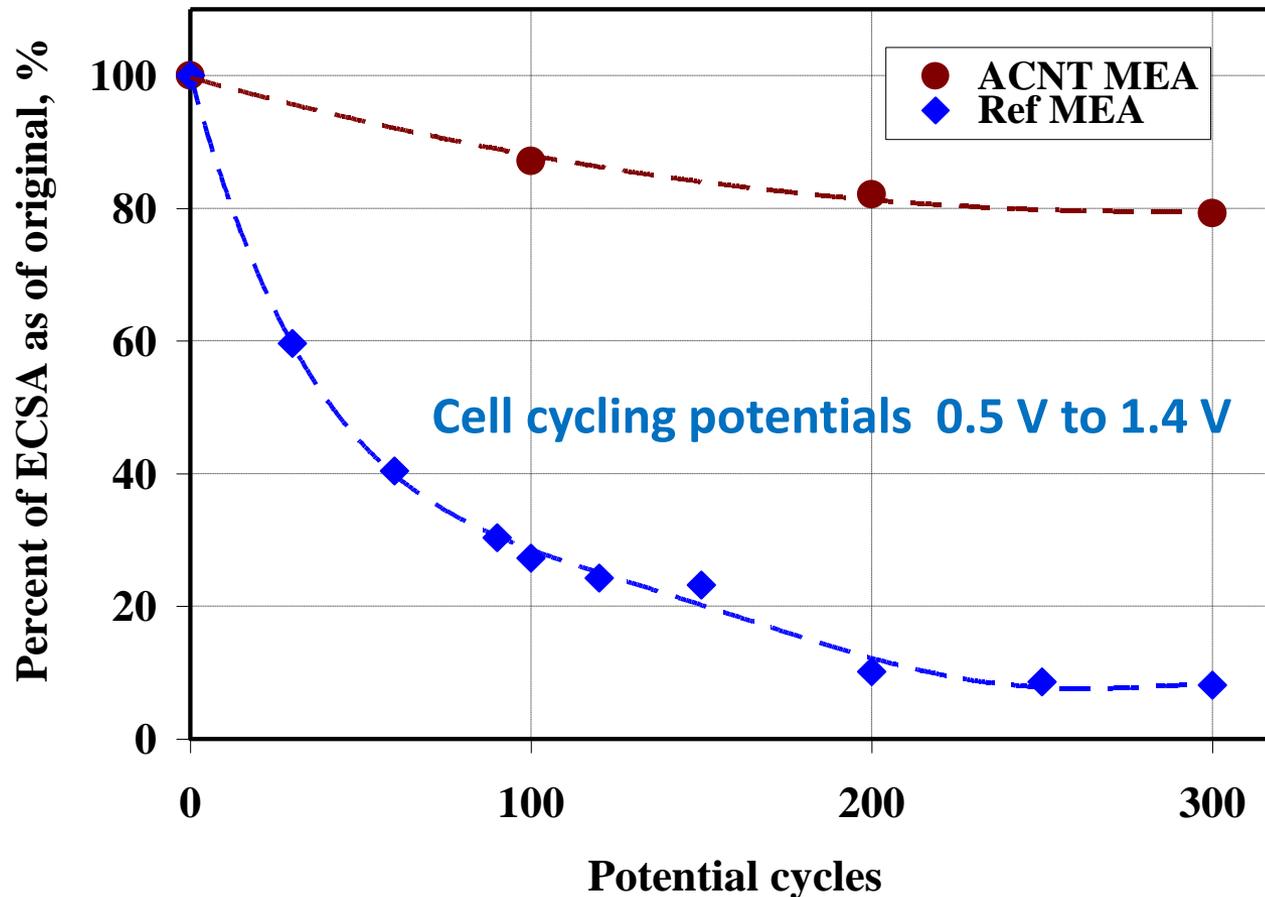
Single Cell Test



Single cell test demonstrated improved polarization using ACNT based MEA



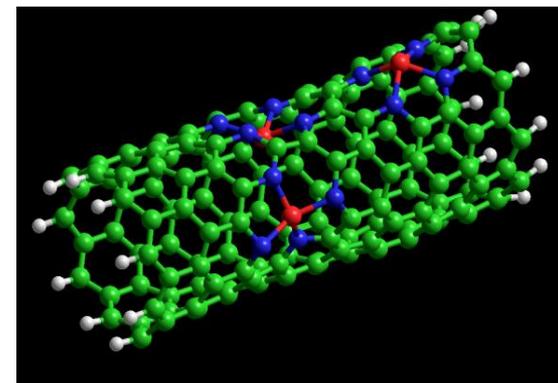
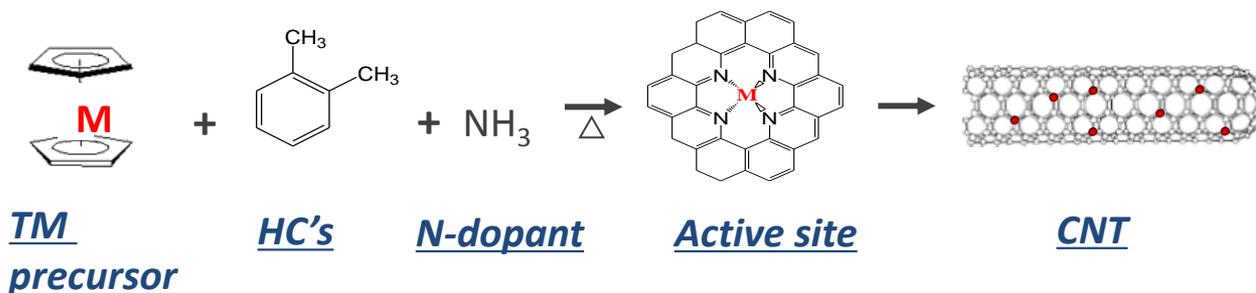
Support Stability Significantly Improved during Potential Cycling



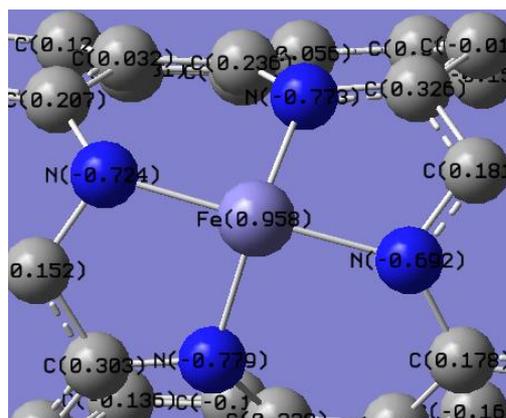
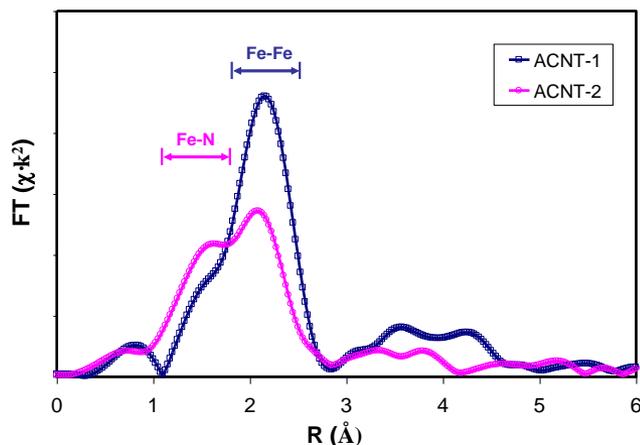
Improved electrocatalytic surface area retention is due to more stable graphitic ACNT

ACNT as PGM-free Catalysts

Synthesize TM/N/C active site over carbon nanotubes



Study N-ligated TM active site structure by XAS and DFT calculation

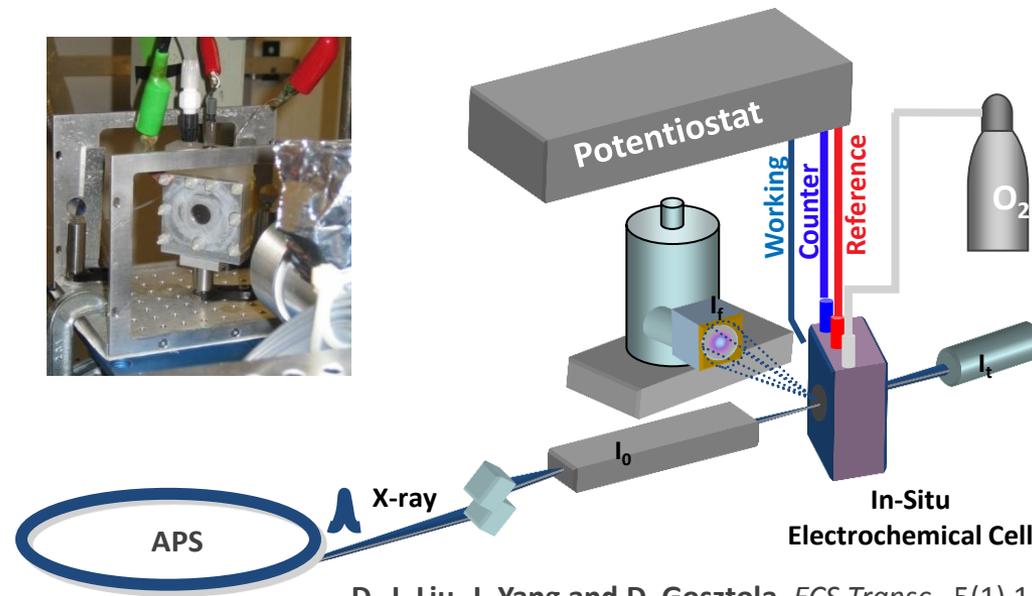
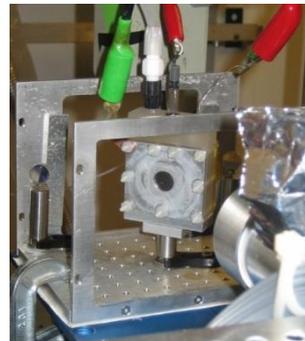
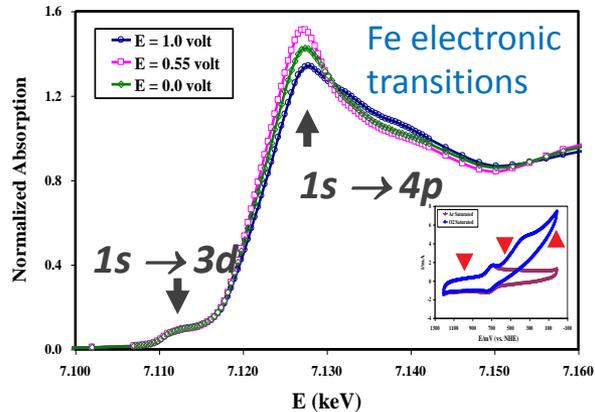


Shell	N	R (Å)
Fe-N	4.2	1.95

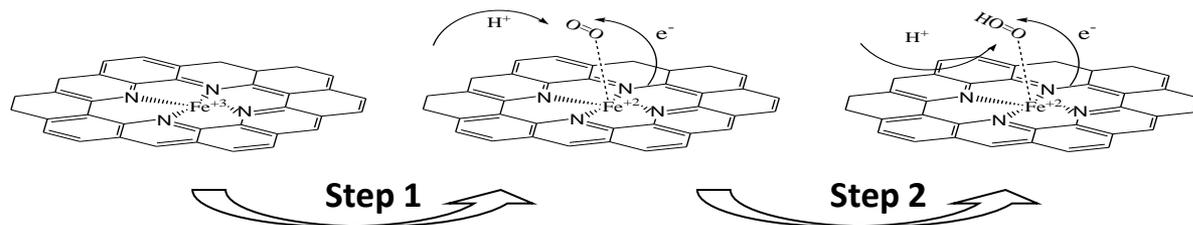
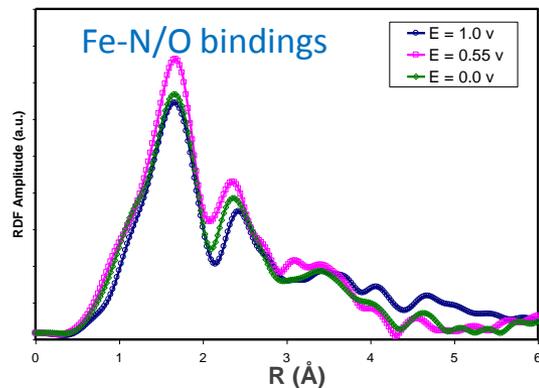
J. Yang, D.-J. Liu, N. Kariuki, L. Chen, *Chem. Comm.* **3**, 329 (2008)

A. Titov, P. Zapol, P. Kral, D.-J. Liu, & L. Curtiss, *J. Phys. Chem. C.* **113**, 21629 (2009)

Probing Active Site Redox Mechanism by *In Situ* X-ray Absorption Spectroscopy



D.-J. Liu, J. Yang and D. Gosztola, *ECS Transc.* 5(1) 147 (2007).



TM oxidation state and coordination structure under different polarization potentials revealed O_2 binding and conversion kinetics during ORR

Design Non-PGM Catalyst using “Support-free” Precursors

$$\text{Catalytic Activity} \propto \text{Turn-Over-Freq.} \times \text{Site Density}$$

- Different transition metals & organic ligands
- Different metal-ligand coordination

- Carbon “Support-free”
- High & uniformly distributed active site density

“Reality-check” on Non-PGM Activity

$$i \text{ (A/cm}^2\text{)} = 1.6 \times 10^{-19} \times \text{TOF (e}^-/\text{site}\cdot\text{s)} \times \text{SD (cm}^{-3}\text{)} \times \tau \text{ (cm)}^*$$

Achievable Current Density @ 0.8 V

(Cathode loading @ $4 \text{ mg}\cdot\text{cm}^{-2} / 1 \text{ bar O}_2$)

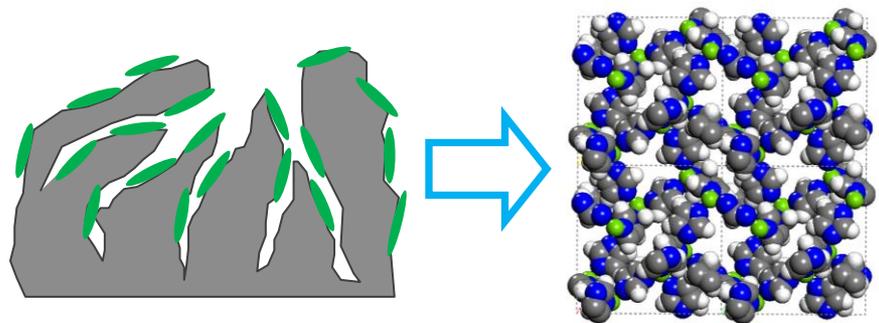
- 170 mA/cm² for 1% Fe, or
- 340 mA/cm² for 2% Fe loading

Critical assumption:

- TM site atomically dispersed & fully utilized
- TOF = 1/10 of Pt (2.5 e⁻/site.s)

* Gasteiger, *et al.* Applied Catalysis B: Environmental 56 (2005) 9

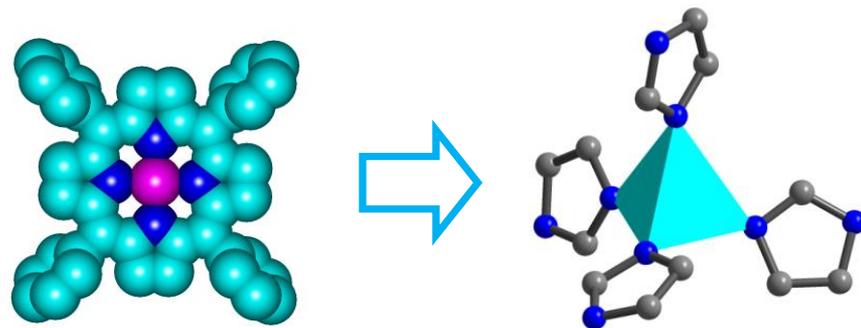
From carbon supported to “support-free” catalyst



Conventional

ANL's MOF/POP approach

From 2D to 3D - Breaking away from 50-year tradition of supported square-planar precursor

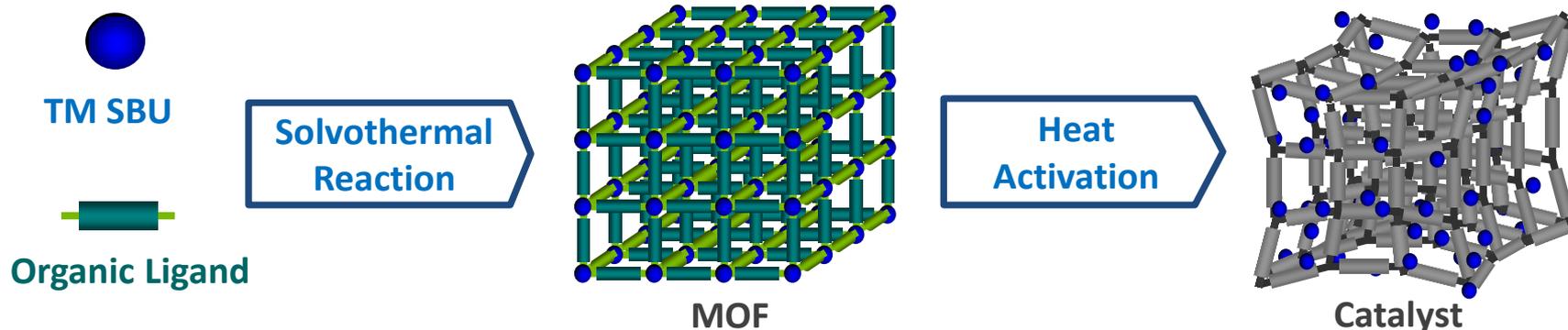


R. Jasinski, *Nature*, (1964)

Ma, Goenaga, Call and Liu, *Chemistry: A Euro. J* (2011)

MOFs as Precursors for non-PGM Catalysts

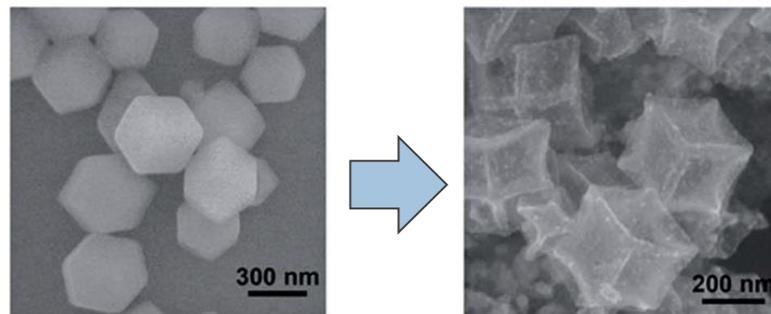
Synthesis of MOF-based non-PGM Catalyst (Why “burn a perfectly good crystal”?)



“Non-Platinum Group Metal Electrocatalysts Using Metal Organic Framework Materials and Method of Preparation”,
D.-J. Liu, S. Ma, G. Goenage, US Patent 8,835,343

Advantages of MOF based non-PGM Catalyst

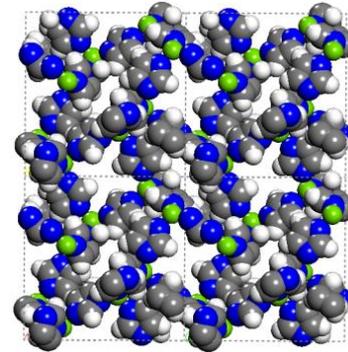
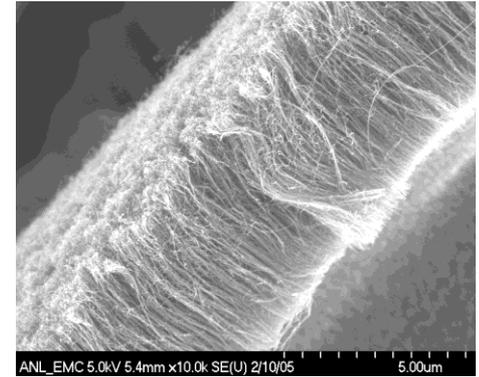
- Highest precursor density for active site conversion
- Well-defined coordination between metal (SBU) & ligand
- Porous 3-D structure with high SSA and uniform micropores
- Large selection of existing MOF compositions



ANL Non-PGM Catalyst IP Portfolio

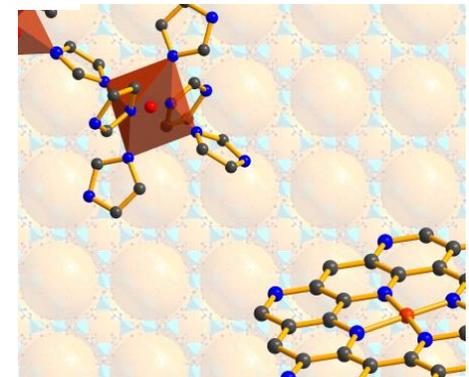
- Developed Fe/N/C decorated CNT catalyst for ORR and demonstrated FeN₄ active site structure
 - *Chem. Comm.* **3**, 329 (2008)
 - *US Patent* 7,927,748
 - *US Patent* 7767616
 - *US Patent* 8,137,858
 - *US Patent* 7,758,921
- Developed metal-organic framework (MOF) based non-PGM catalyst and started “support-free” approach
 - *Chemistry: A European Journal*, **17** 2063 (2011)
 - *US Patent* 8,835,343
 - *US Patent Application* 20150180045
- Developed binary MOF non-PGM catalyst, achieved measured volumetric current density and power density
 - *Chemical Science*, **3** (11), 3200 (2012)

Aligned
Carbon
Nanotube



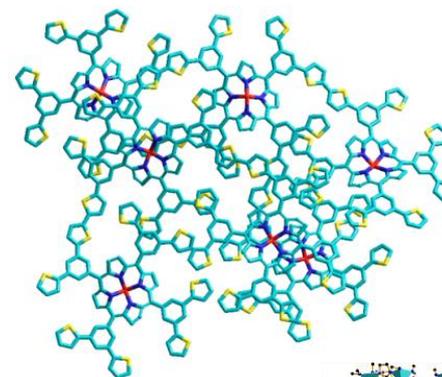
Co-Zeolitic
Imidazolate
Framework (ZIF)

Fe-ZIF/ZIF-8
binary MOF
System



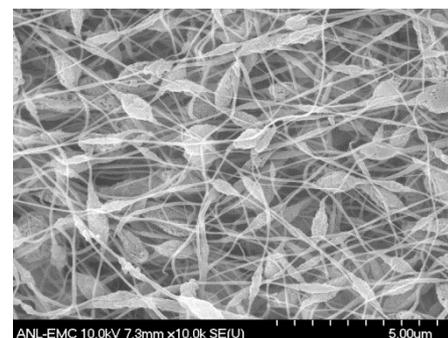
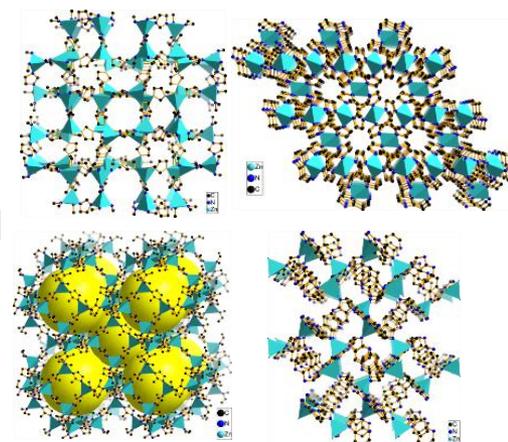
ANL Non-PGM Catalyst IPs (continued)

- Developed non-PGM catalyst using porous organic polymer (POP), achieved peak power density of 730 mW/cm^2
 - *Angew. Chem. Int. Ed.* **52** (32), 8349 (2013)
 - *US Patent* 9012344
 - *US Patent Application* 20150194681
- Developed “one-pot” synthesis approach for low-cost production of a broader range of MOF-base non-PGM catalyst
 - *Advanced Materials*, **26**, 1093, (2014)
 - *US Patent Application* 20130273461
 - *US Patent Application* 20150056536
- Developed the first nano-network non-PGM catalyst, achieved peak power density of 870 mW/cm^2
 - *Proceedings of National Academy of Sciences*, **112**(34), 10629 (2015)
 - *US Patent* 9,350,026



Fe/Co-POP

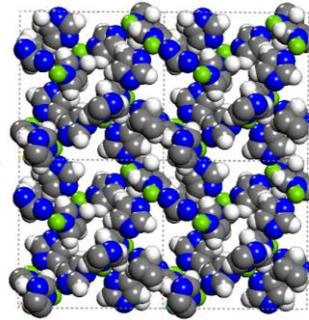
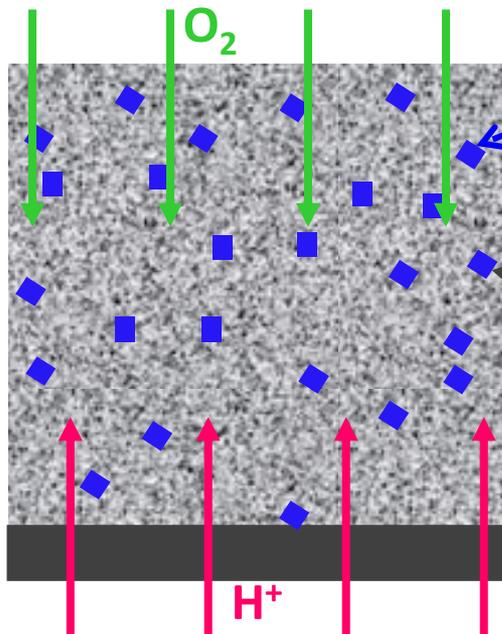
“One-pot”
Synthesized
ZIFs



Nanofibrous
Network

Catalytic Mass/Charge Transport Improvement in Graphitic Nanonetwork Architecture

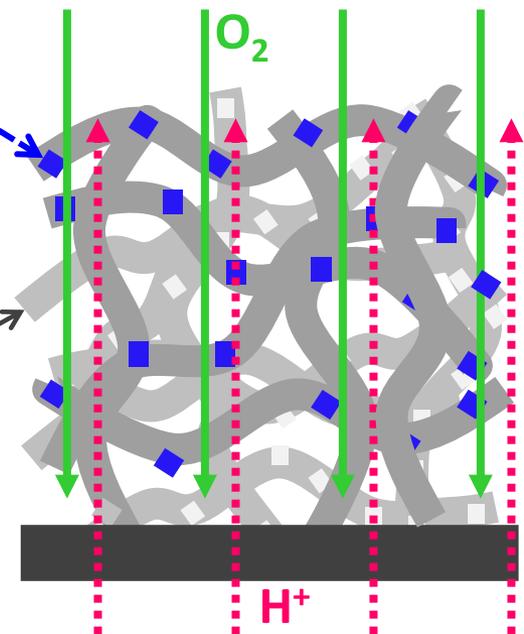
Conventional Support



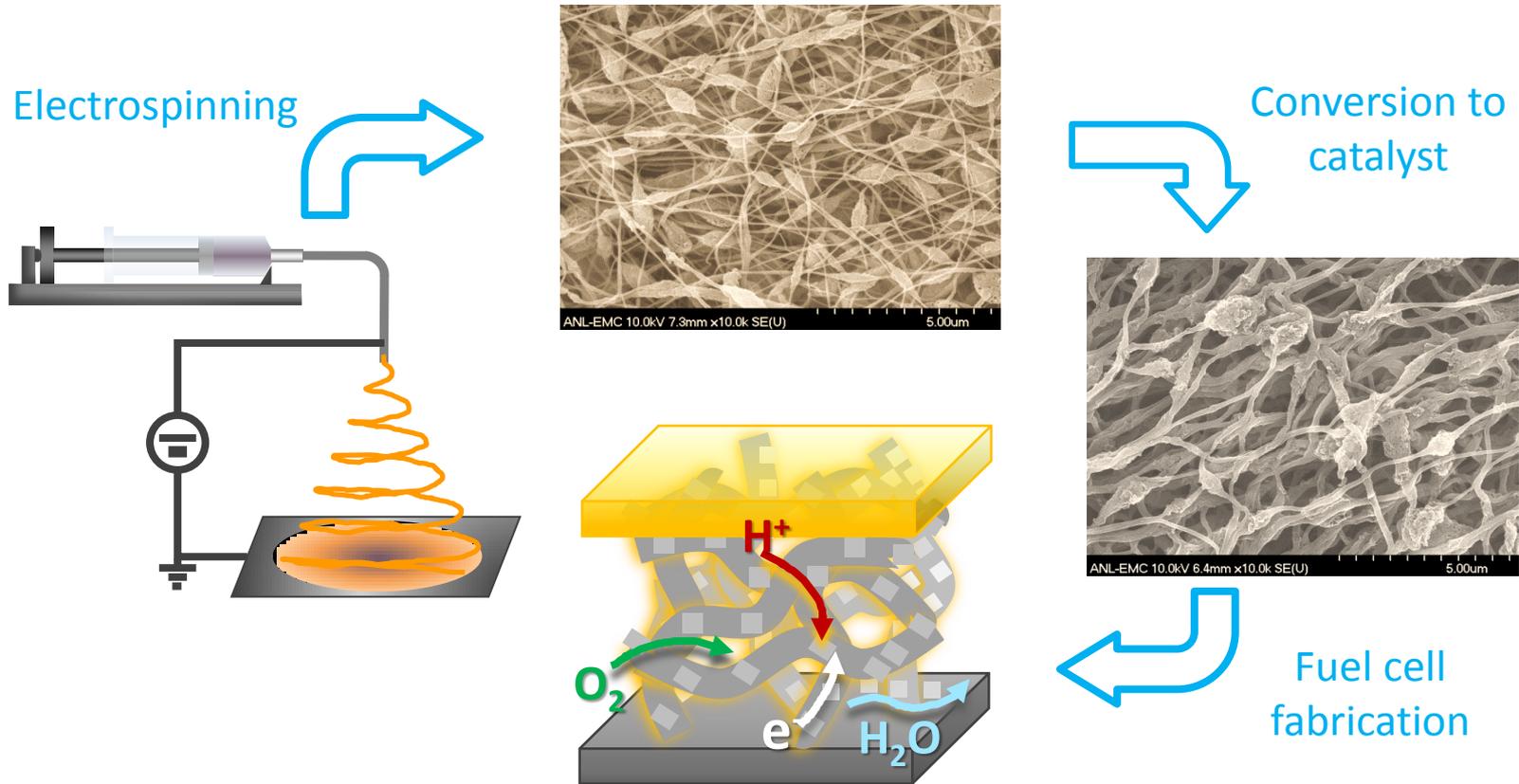
MOF Catalyst

Nano-network

Nanofibrous Support



Process of Preparing PGM-free Catalyst with Porous Nano-network Architecture

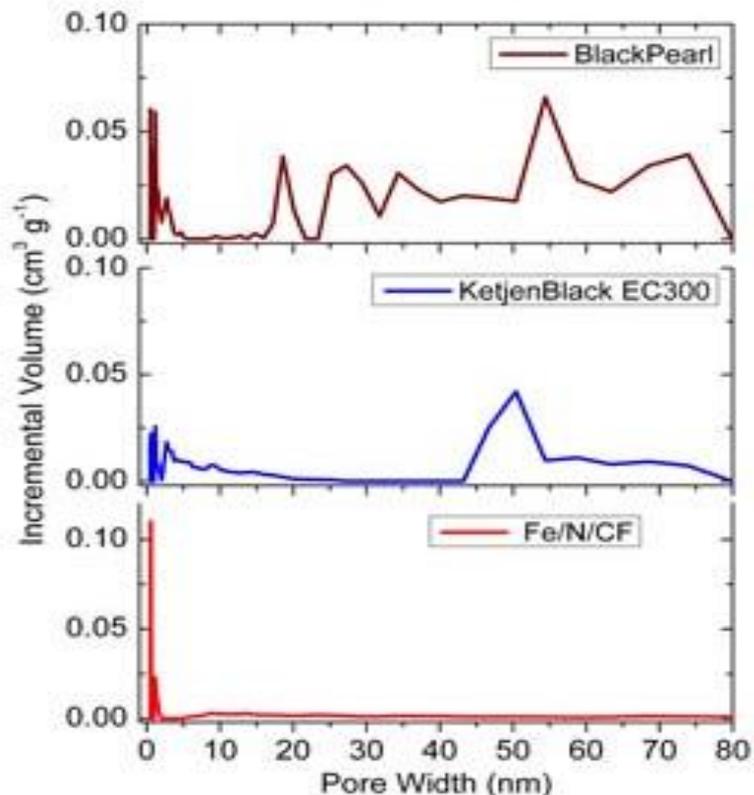


J. Shui, C. Chen, L. R. Grabstanowicz, D. Zhao and D.-J. Liu, *Proceedings of National Academy of Sciences*, U. S. A. **2015**, vol. 112, no. 34, 10629

D.-J. Liu, J. Shui, C. Chen, "Nanofibrous electrocatalysts", **US Patent 9,350,026**



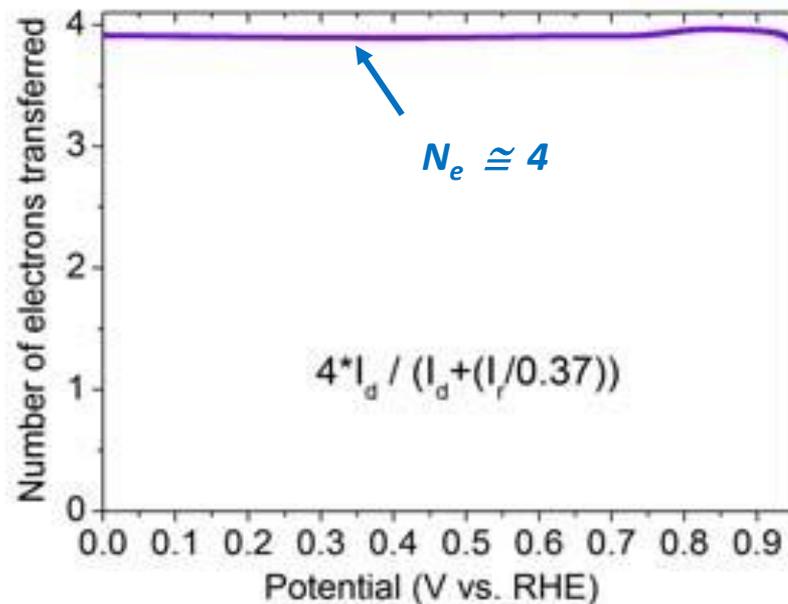
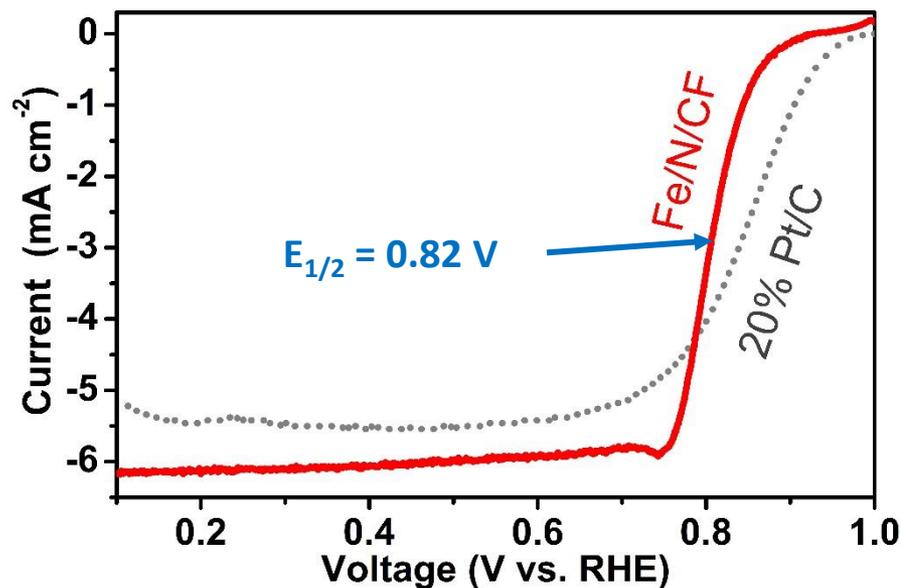
Unique Nanofiber Morphology - High Surface Area Nearly Exclusively Distributed in Micropore Region



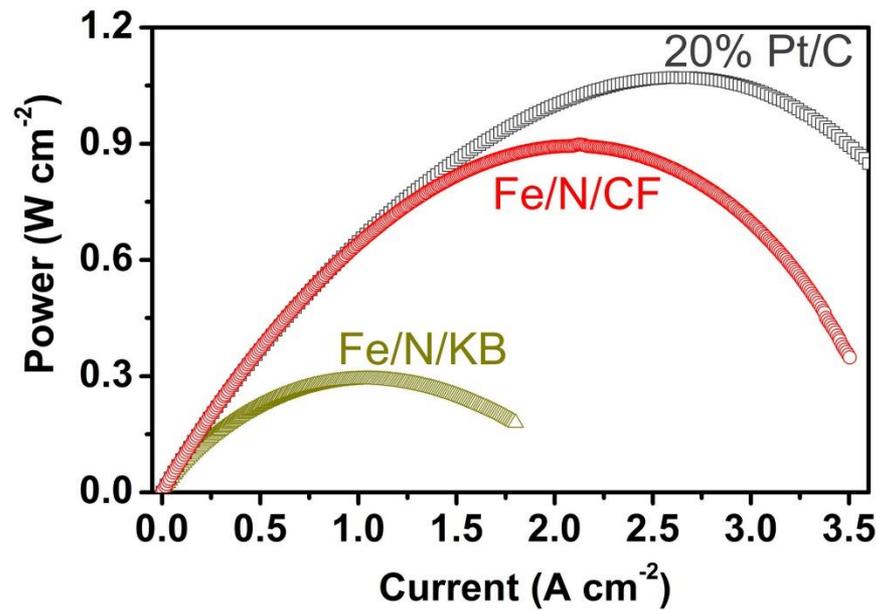
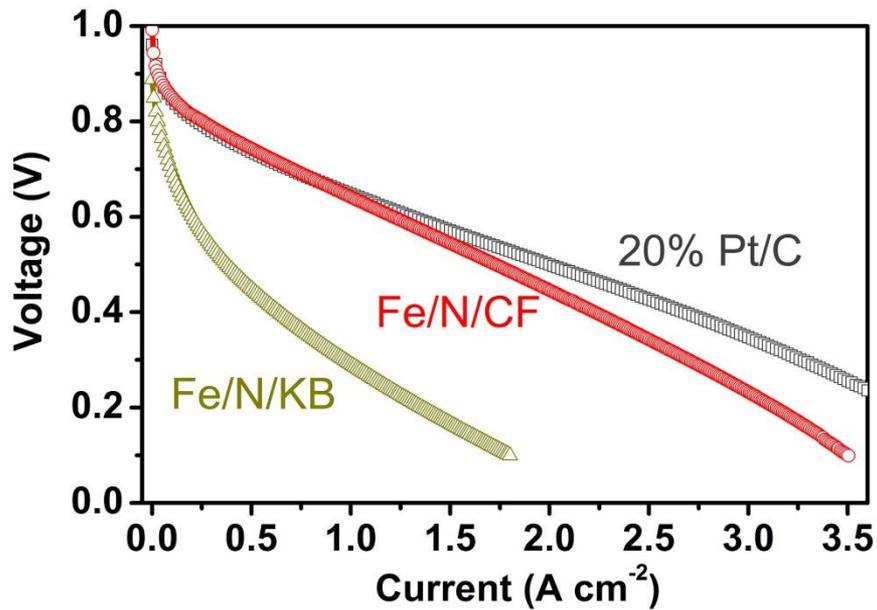
	Black Pearl	Ketjen Black	Fe/N/CF
BET (m ² g ⁻¹)	1432	798	809
Surface Area of Pores ≤ 2nm (m ² g ⁻¹)	867	398	780
Surface Area of Pores ≤ 50nm (m ² g ⁻¹)	960	507	788
$S_{\leq 2\text{nm}}/S_{\leq 50\text{nm}}$	90%	78%	99%
Total Volume in Pores ≤ 80 nm (cm ³ g ⁻¹)	0.955	0.508	0.330
Volume of Pores ≤ 2nm (cm ³ g ⁻¹)	0.371	0.167	0.271
Volume of Pores ≤ 50nm (cm ³ g ⁻¹)	0.766	0.463	0.323
$V_{\leq 2\text{nm}}/V_{\leq 50\text{nm}}$	48%	36%	84%

- High specific surface area (BET = 700 ~ 1251 m²/g)
- High micro-porosity (Micro-pore vol./Total pore vol. > 80%)

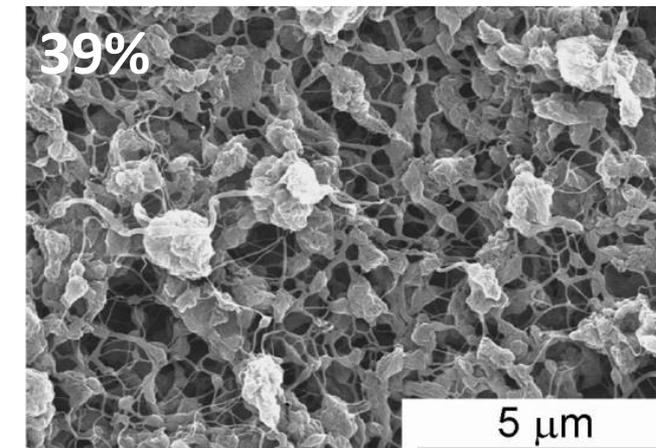
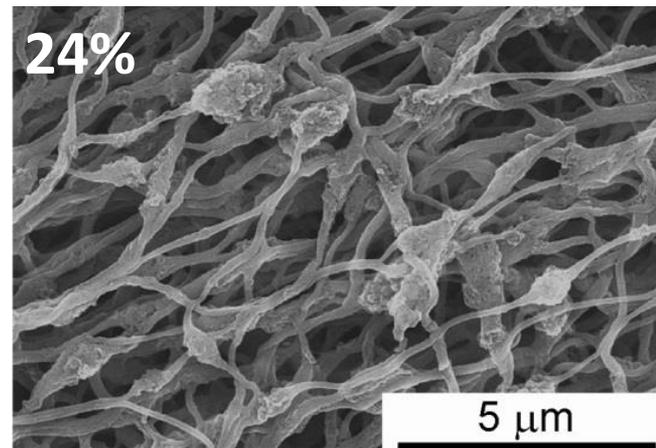
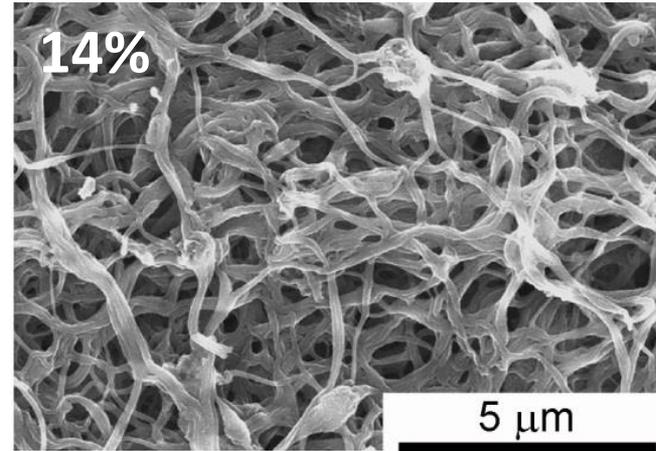
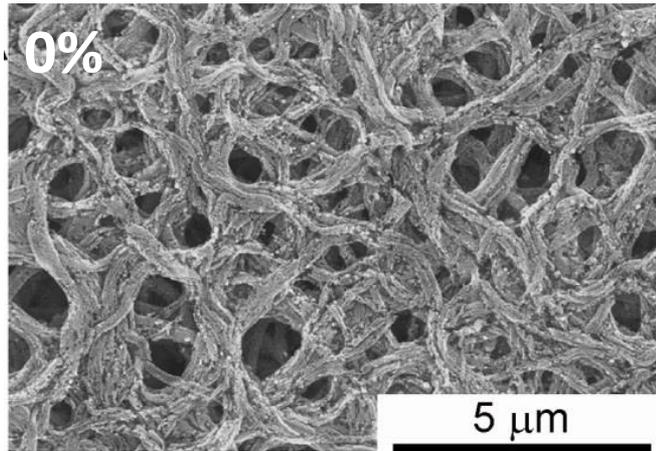
Excellent PGM-free Catalytic Activity Measured by RDE



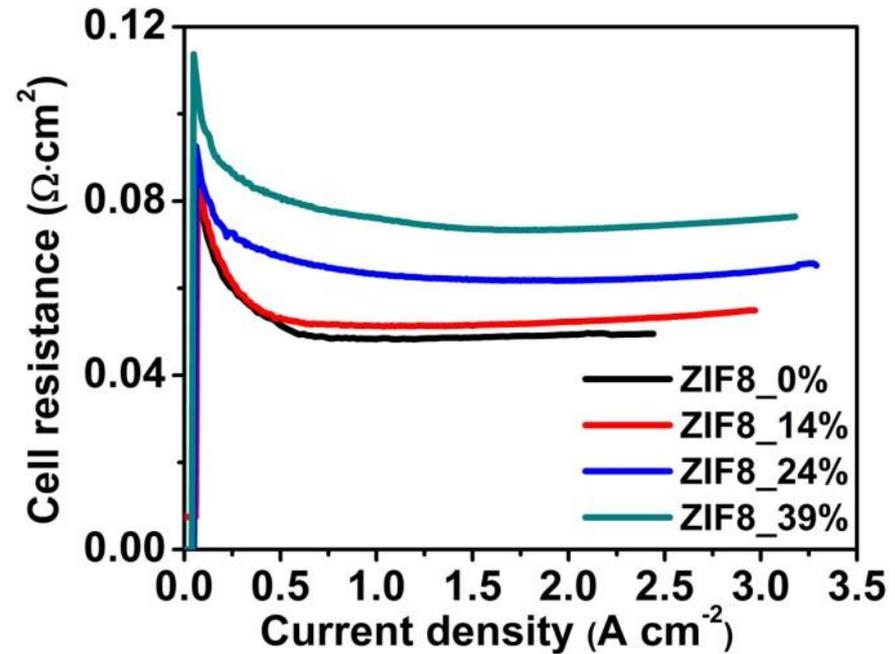
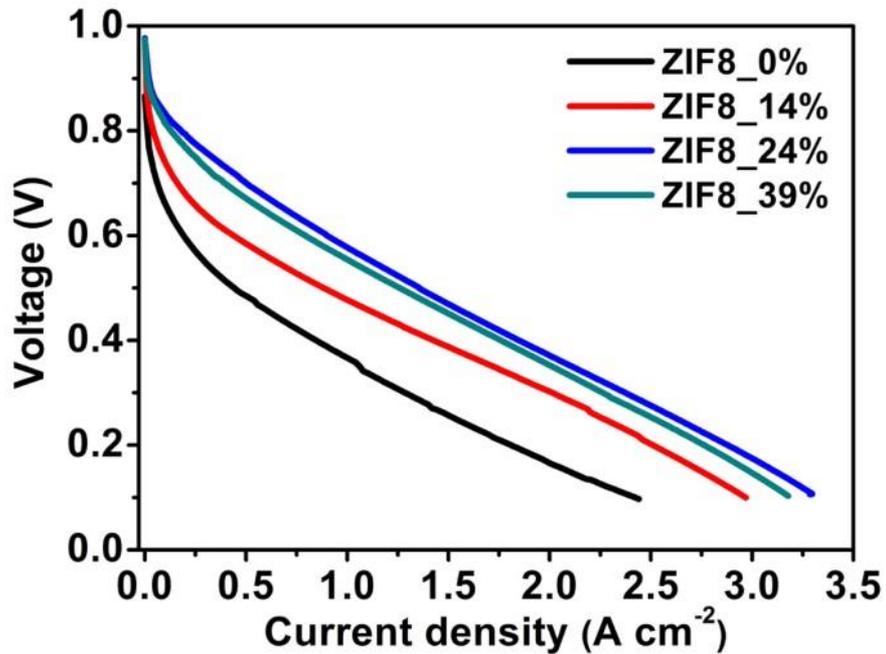
New Electrode Architecture Led to Very Good Performance at Single Cell Levels



Nanofibrous Network Morphology is Sensitive to Composition of Electro-spin Mixture

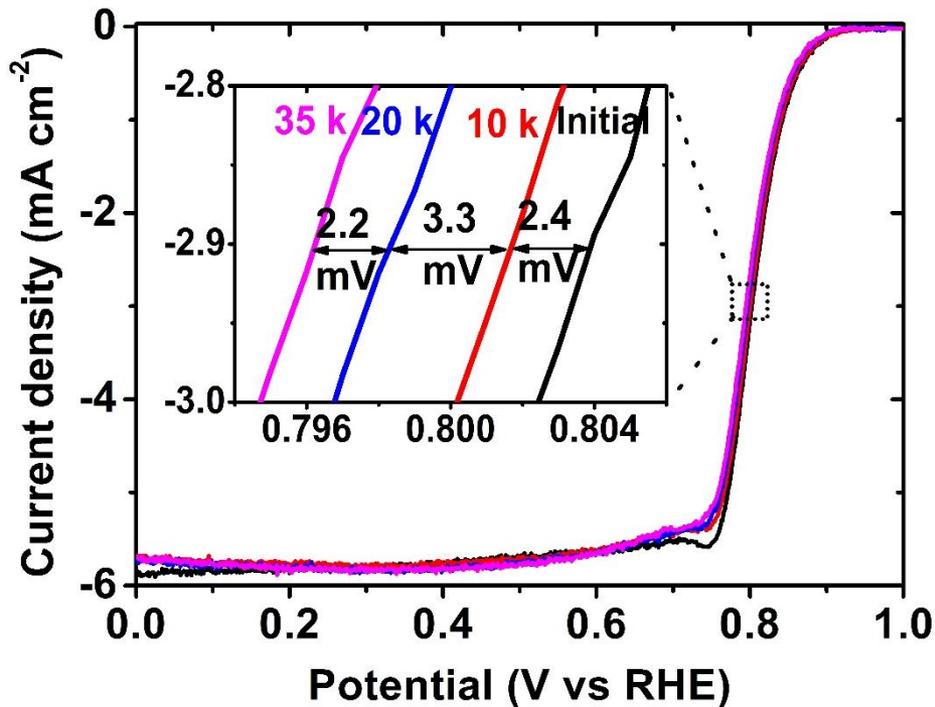


Morphology Impacts Electrode Architecture and Fuel Cell Performance

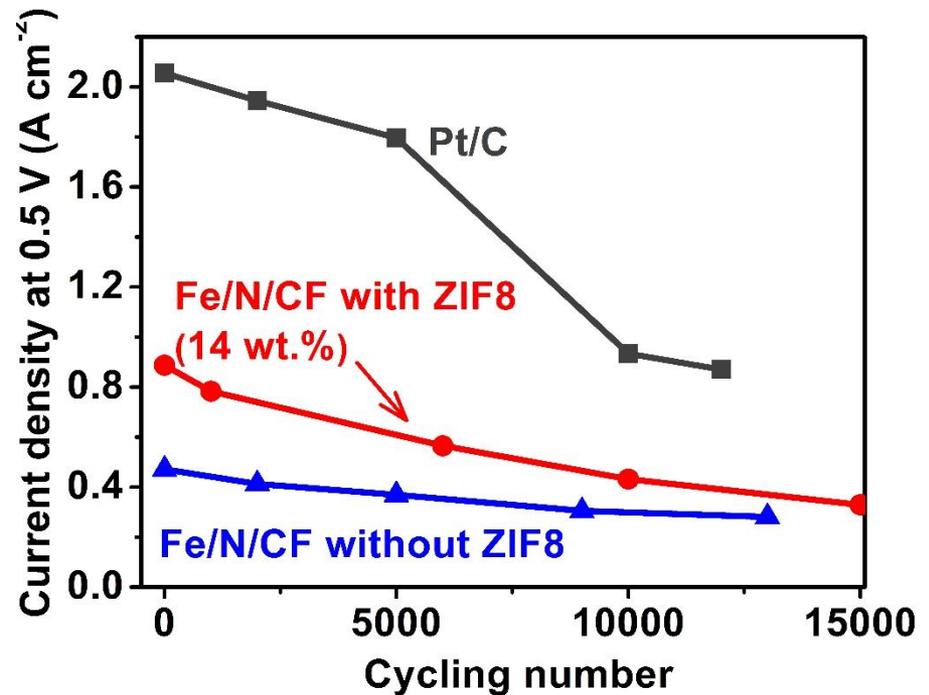


New Nanofibrous Network Showed Promise for Durability Improvement

RDE shows excellent activity retention under multi-potential (0.6 to 1.0 V) cycling in acidic media



Fuel cell accelerated stress test (AST) shows similar decay rate to that of commercial Pt/C MEA



Prospects of Porous Nanonetwork as New Support for PGM Catalyst

- Efficient mass transport
- Better thermal/electronic conductivity
- Stable graphitic network backbone
- High specific surface area
- Tailored surface compositions to promote catalyst-support interaction



Acknowledgement

- **Fuel Cell Research - Shengqian Ma, Dan Zhao, Shengwen Yuan, Jianglan Shui, Gabriel Goenaga, Junbing Yang, Chen Chen, Heather Barkholtz, Lina Chong, Lauran Grabstanowicz, Alex Mason, Brianna Reprogle, Sean Comment, Zachary Kaiser, Debbie Myers**
- **US DOE, US DOE Office of Fuel Cell Technologies and Office of Science. The use of Advanced Photon Source and Electron Microscopy Center are supported by Office of Science, U. S. Department of Energy under Contract DE-AC02-06CH11357.**

