

# One Step Hydrogen Generation Through Sorption Enhanced Reforming

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Gas Technology Institute

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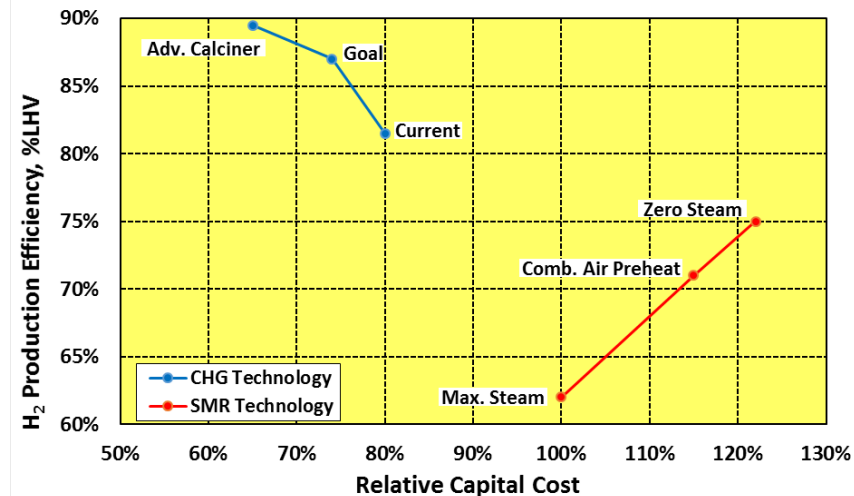
June 14-15, 2016

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# Project Objective

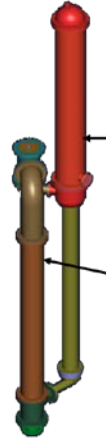
- Develop low-cost hydrogen production technology, utilizing Sorption Enhanced Reforming (SER), for large-scale commercial applications
  - Reducing cost of hydrogen by 15-20% vs. current technology
  - Reducing cost of carbon capture from natural gas feedstock
- Improve the Technology Readiness Level (TRL) from 4 to 6
- Develop a robust SER process and associated solids handling for fine, reacting sorbent particles

## Technology Comparison: CHG vs. SMR



# Technical Innovation

- Conventional hydrogen production uses Steam Methane Reforming (SMR)
- SER combines the reforming and water-gas shift processes into one-step (i.e., in the same vessel)
  - Sorbent balances heat necessary for reforming-eliminating costly SMR firebox and convective heat exchanger



### SER Chemistry

**Hydrogen Generation Reactions**

$$\text{CH}_4 + 2\text{H}_2\text{O} + \text{Heat} \rightarrow 4\text{H}_2 + \text{CO}_2$$

$$\text{CaO} + \text{CO}_2 \rightarrow \text{CaCO}_3 + \text{Heat}$$

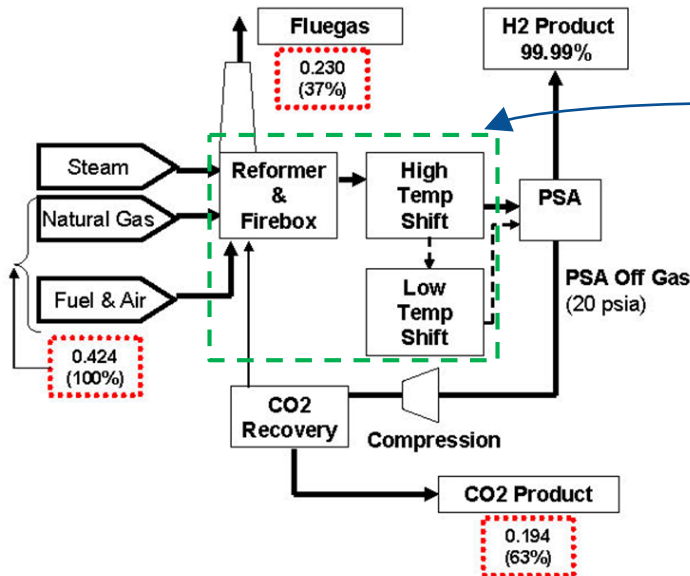

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$$\text{CH}_4 + 2\text{H}_2\text{O} + \text{CaO} \rightarrow 4\text{H}_2 + \text{CaCO}_3$$

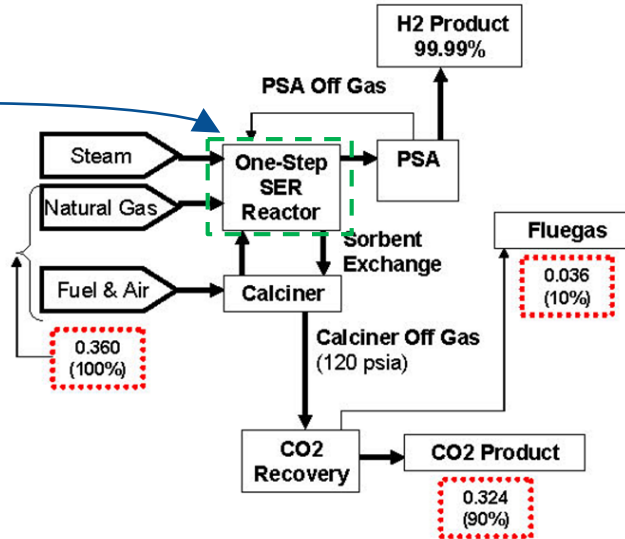
**Calcination Reaction**

$$\text{CaCO}_3 + \text{Heat} \rightarrow \text{CaO} + \text{CO}_2$$

**Conventional Steam Methane Reformer (SMR)**



**One-Step Sorption Enhanced Reformer (SER)**



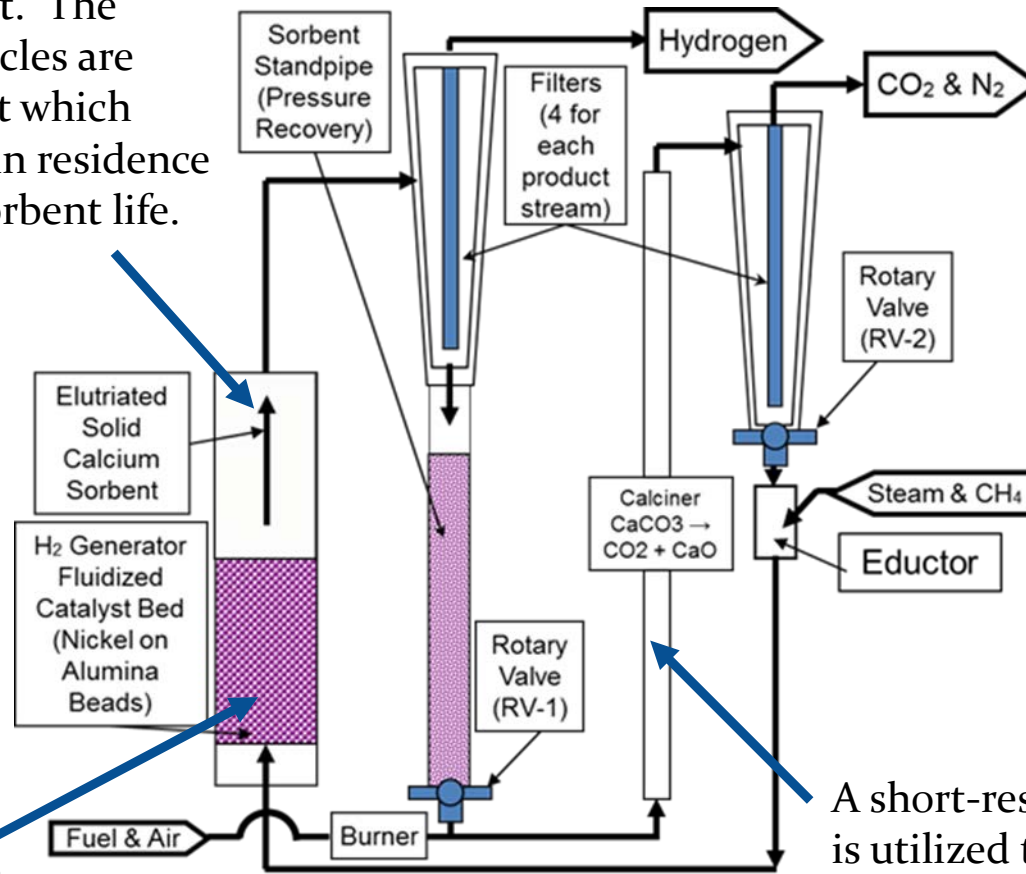
## Benefits

Lower capital cost and higher efficiency result in lower cost of hydrogen

Separate CO<sub>2</sub> stream arising from calcination reduces CO<sub>2</sub> capture costs

# Technical Innovation

A process which enables the sorbent to flow through a bubbling fluidized bed of catalyst. The elutriated sorbent particles are hindered by the catalyst which provides ~10x increase in residence time, thus extending sorbent life.



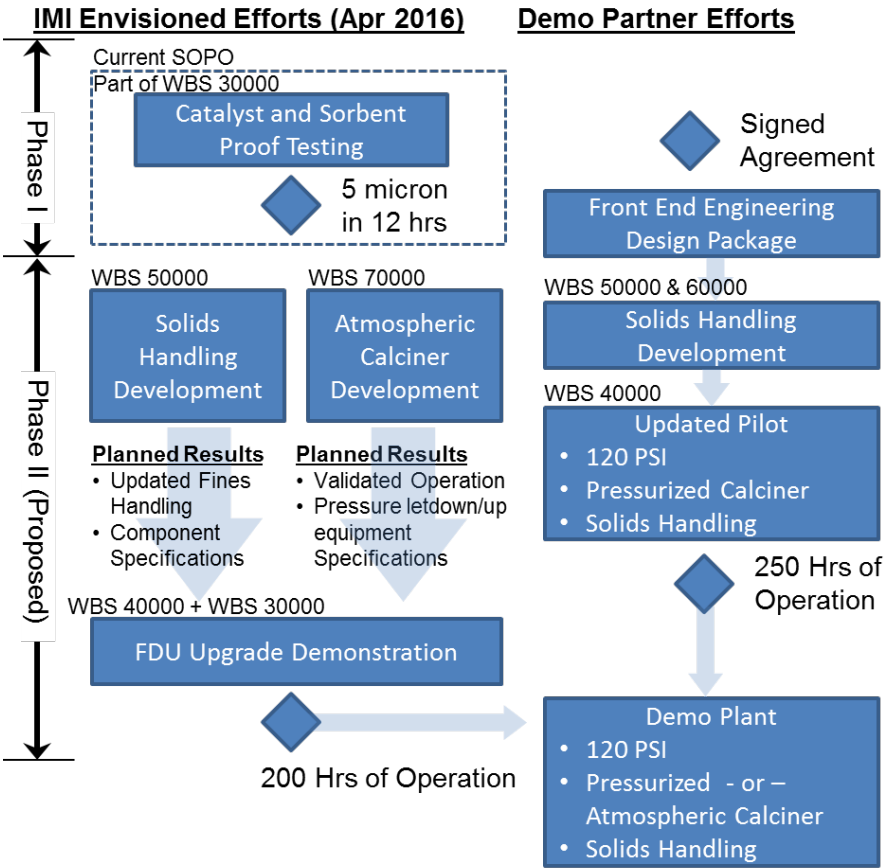
A high aspect ratio bubbling-bed, which increases the overall reactivity of the reactor

A short-residence time calciner is utilized to minimize “time at temperature” of the sorbent, and extends its reactivity (seconds vs. minutes)

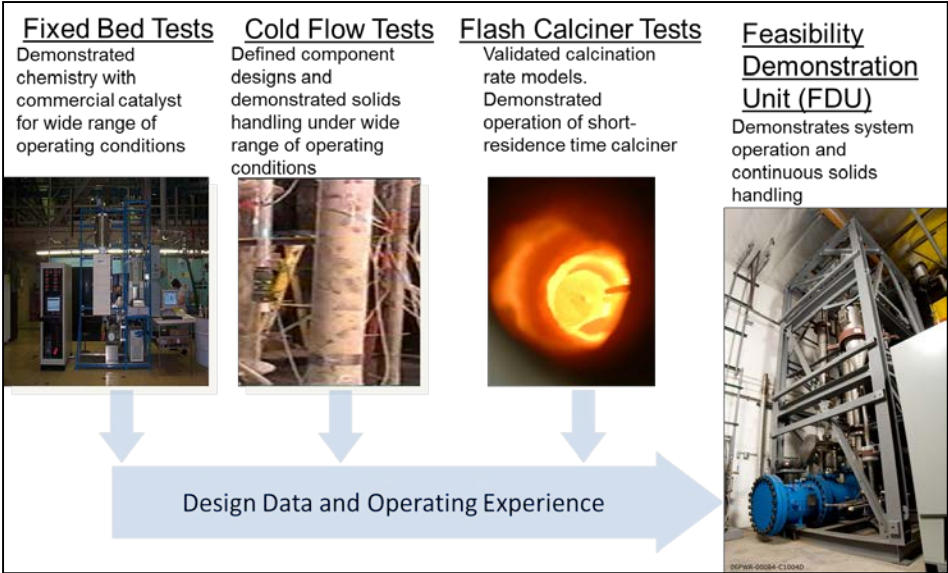
# Technical Approach

- Actively pursue input from industrial gas suppliers and EPC's to validate the technology
- Leverage existing development assets and partners to develop and commercialize product

## Go-Forward Approach

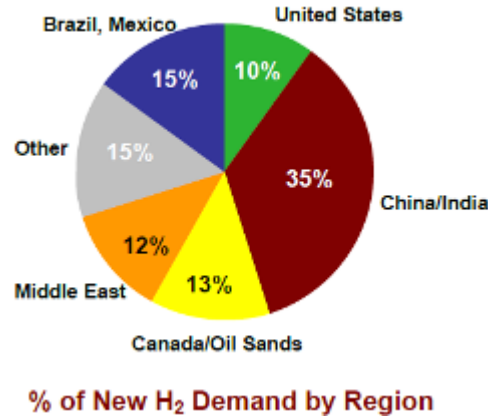
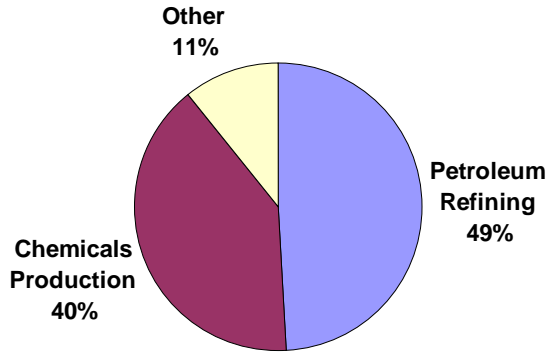


## Technology Development History



# Transition and Deployment

## Hydrogen Demand<sup>3</sup>



- Overall hydrogen market size is between \$60B - \$90B<sup>1</sup>
- Hydrogen equipment market size is between \$3B-\$4.5B
- Annual market growth ranges from 7%-15%<sup>2</sup>

<sup>1</sup> Based on a average value of \$2.00 - \$3.00 Mscfd, where M represents thousands

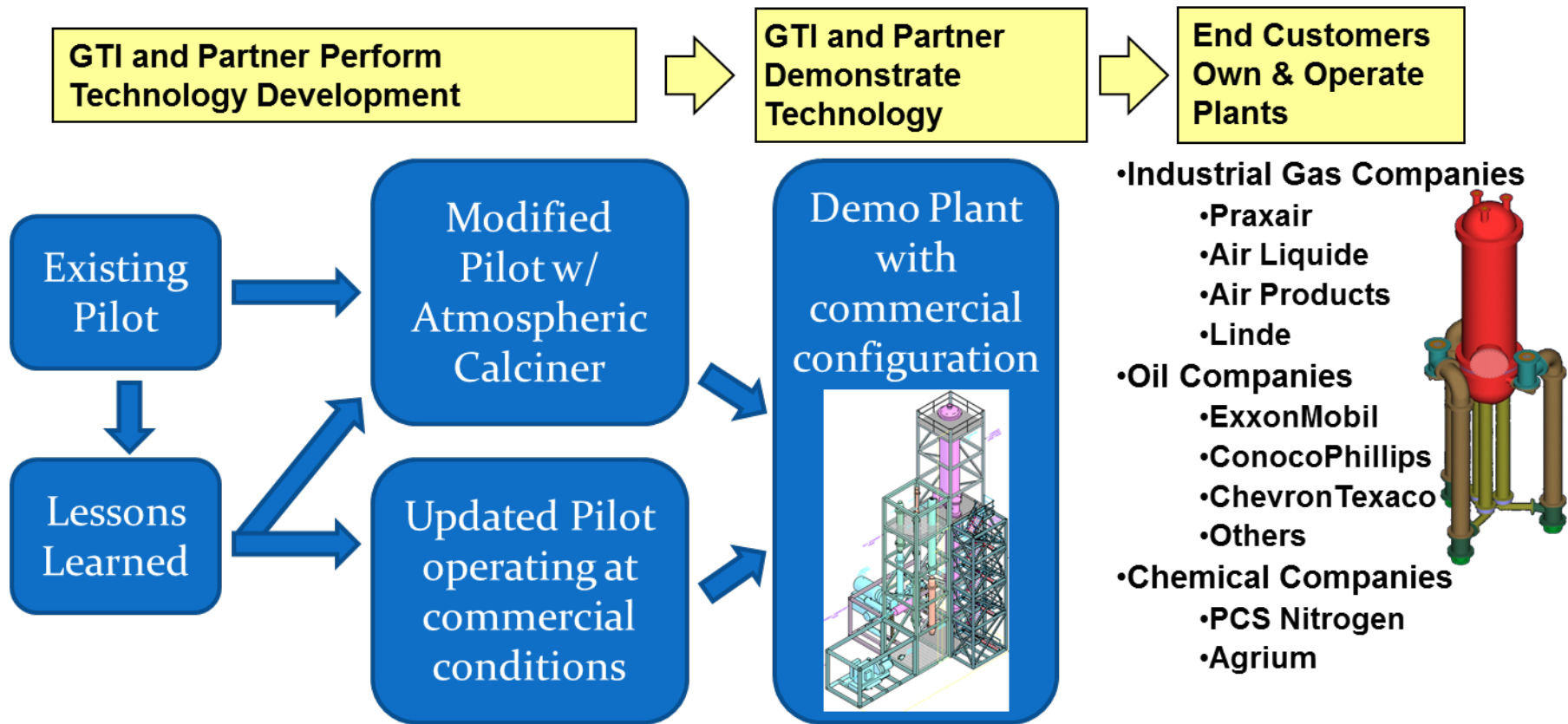
<sup>2</sup> March 2010 Praxair CFO Presentation

<sup>3</sup> Hydrogen and Synthesis Gas, SFA Pacific, Inc., 1998 and March 2010 Praxair CFO Presentation

- Hydrogen end-users benefit from process intensification
  - Reduced hydrogen cost through:
    - Lower capital cost
    - Improved efficiency
    - Smaller Footprint

*Large market, growing at steady rate*

# Transition and Deployment



- Utilize continuous improvement process for technology sustainment
  - Separate technology improvement budget will be jointly funded with licensing revenues

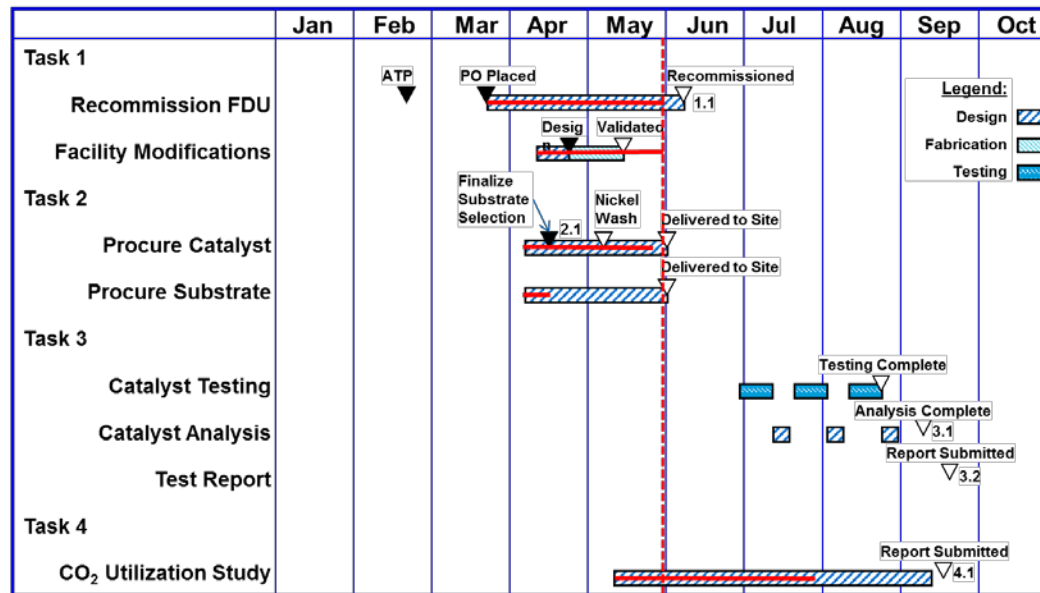
- Successful deployment of CHG technology will reduce cost of hydrogen, provide lower cost CO<sub>2</sub> capture, and lead to additional market penetration due to compactness (e.g., debottlenecking, oil sands in-field upgrading)
- Success will be measured through an increase in market share against SMR's (projected to be 26% share in 10 years)
  - Equates to energy savings of 43.6 Trillion BTU/year
- Increased global marketshare results in more U.S. jobs in engineering and manufacturing of special equipment



# Project Management & Budget



- Project Duration = 9 Months
- Project Performance: Schedule = 96% (behind), Cost = 105% (under budget)



Total Project Budget	
DOE Investment	\$630,868
Cost Share	\$651,377
<b>Project Total</b>	<b>\$1,282,245</b>

- Only 3 months into the project, major progress:
  - Pilot Plant recommissioning 95% complete
  - 2 of 3 catalyst candidates procured
  - CO<sub>2</sub> co-production discussed with Oil Sands companies
- Work to be completed:
  - Complete recommissioning effort
  - Demonstrate catalyst performance
  - Evaluate Urea production applicability for CO<sub>2</sub> co-production study