

Low-Cost Gas Heat Pump for Building Space Heating

2015 Building Technologies Office Peer Review



Project Summary

Timeline:

Start date: **March 01, 2013**

Planned end date: **August 31, 2015**

Key Milestones:

- 1. Cycle & System Design: 12/31/2014**
- 2. Breadboard Test Results: 12/31/2014**
- 3. Packaged Prototype Results: 04/01/2015**

Budget:

Total DOE \$ to date: **\$629,730**

Total future DOE \$: **\$273,140**

Target Market/Audience:

Residential & Light Commercial Space Heating

Light Commercial Potable Water Heating

Simultaneous Water Heating/Space Cooling

Key Partners:

A.O. Smith

Gas Technology Institute

Project Goal:

Develop and demonstrate a gas-fired absorption heat pump, with heating COP's greater than 1.0 at low ambients. Design simplicity and volume manufacturing requirements emphasized from conception. Achieving a projected 2-5 year economic payback to drive market penetration is a higher priority than ultra-high efficiency.

Purpose and Objectives

What We Use For Gas Heating Has Not Changed Much



Furnaces | Boilers | Water Heaters

Non-Condensing Models Are 75 – 83% Efficient

Condensing Models Are 90 – 98% Efficient

Direct Fired @ Maximum Efficiency
OEM Product Differentiation?
Efficiency Program Incentives?

Need COP >> 1.0

Must Work at Low Ambients

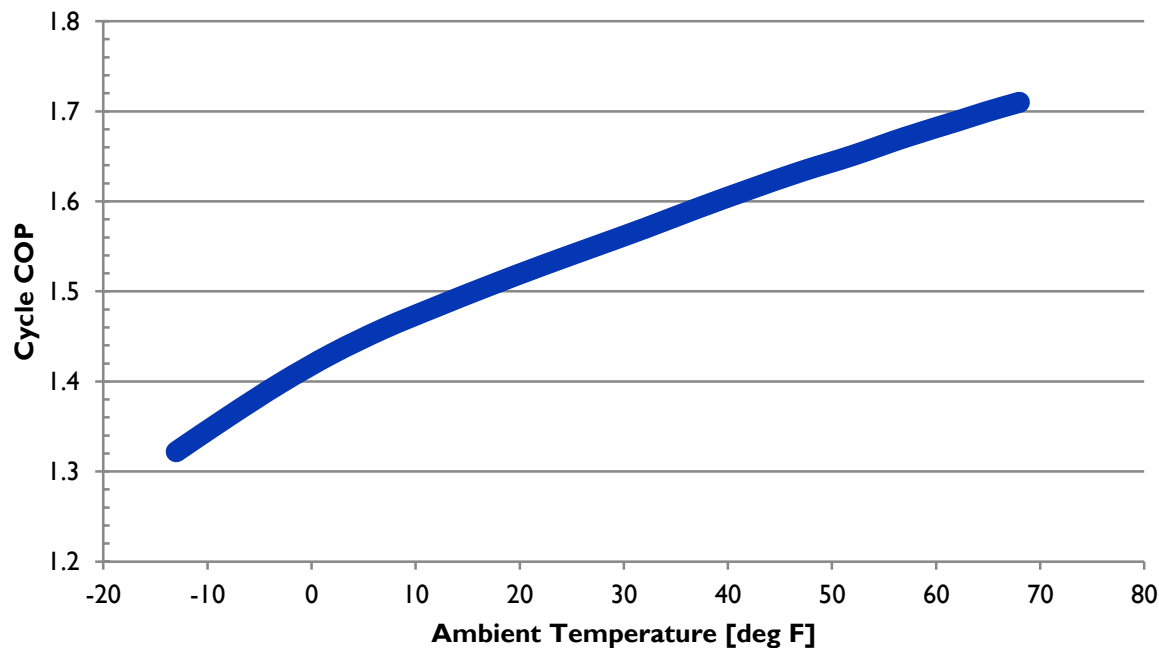
Must be Economically Viable

Purpose and Objectives

Gas Absorption Heat Pumps

Excellent Heating Efficiencies Even at Low Ambients

"Typical" Cycle COP vs Ambient
Single-Effect NH₃-H₂O Heat Pump
Producing 120 °F Water



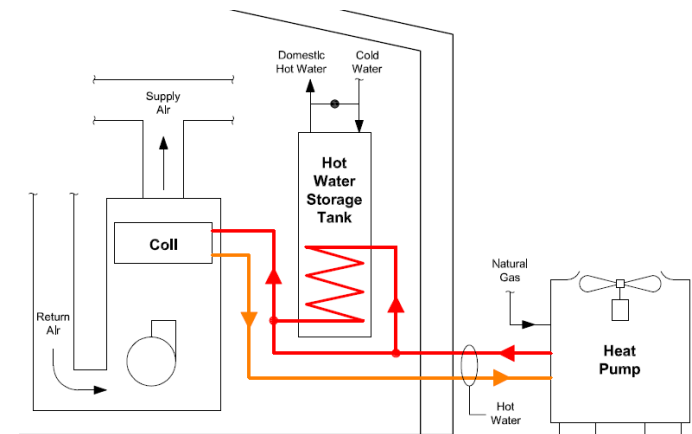
Problem: Historically Complex Cycles and High Cost

Purpose and Objectives

80,000 Btu/hr (23 kW) @ 47°F

COP = 1.40	47°F (8.3°C)
COP = 1.35	32°F (0°C)
COP = 1.30	17°F (-8.3°C)
COP = 1.20	-13°F (-25°C)

- ❖ *COP @ HHV, including Parasitic Power*
- ❖ *Parasitic Power < 750 watts*
- ❖ *Condensing Combustion Efficiencies*
- ❖ *At least 3:1 Modulation*
- ❖ *20°F (11.1°C) Hydronic Differential*
- ❖ *Consumer Price ~\$4,500*



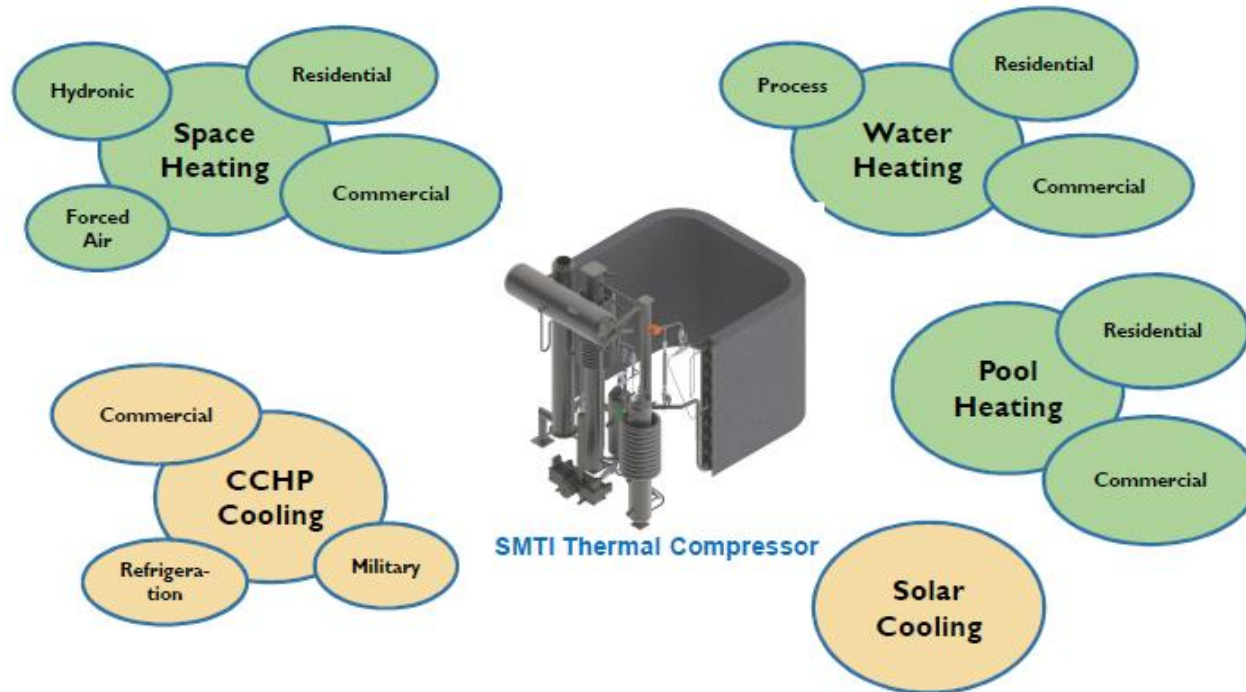
TARGET APPLICATIONS

- ❖ Residential Space & Water Heating (cool/cold climates)
 - ❖ *3.5 Quads (185.5 Million Metric Ton CO₂) (65% Cool Climate Zones)*
- ❖ Commercial Space & Water Heating (all climates)
- ❖ Commercial Simultaneous Water Heating & Space Cooling (all climates)
- ❖ Pool Heating
- ❖ New Construction & Retrofit

Purpose and Objectives

Target Customers for SMTI Thermal Compressor:

HVAC & Water Heating OEMs That Want to Offer Gas Heat Pump Products



U.S. based manufacturing, family of Thermal Compressor products

Winter 2015: Controlled Field Testing, Reliability
2016: Customer Agreement(s) in Place, Large Field Test, DFM, Vendor Qualifications
2017: Certification and Production Start

Approach

- Simple Cycle, optimized for cost and reliability.
- Commonality of raw material, processes, and scalability.
- Total Cost Focus from beginning.
- Optimization of evaporator coil (highest cost component).
- Breadboard development, then packaged prototype.
- Parallel development of controls and design for modulation.
- 3rd Party validation of Packaged Prototype performance.
- OEM and Natural Gas Industry Partners to Ensure Market Acceptance & Education

Key Issues:

- **Evaporator Coil Design:** Validation of design model to ensure we arrive at optimized design for packaged prototype (achieve target cost and performance).
- **Rectifier Performance:** Achieving target ammonia purity using simple, low-cost design.
- **Scalability of Low-Cost Solution Pump**
- **System Behavior:** Understanding system behavior, especially at start-up and reduced load conditions (controls development for modulation, important for real-life seasonal energy efficiency and customer satisfaction).

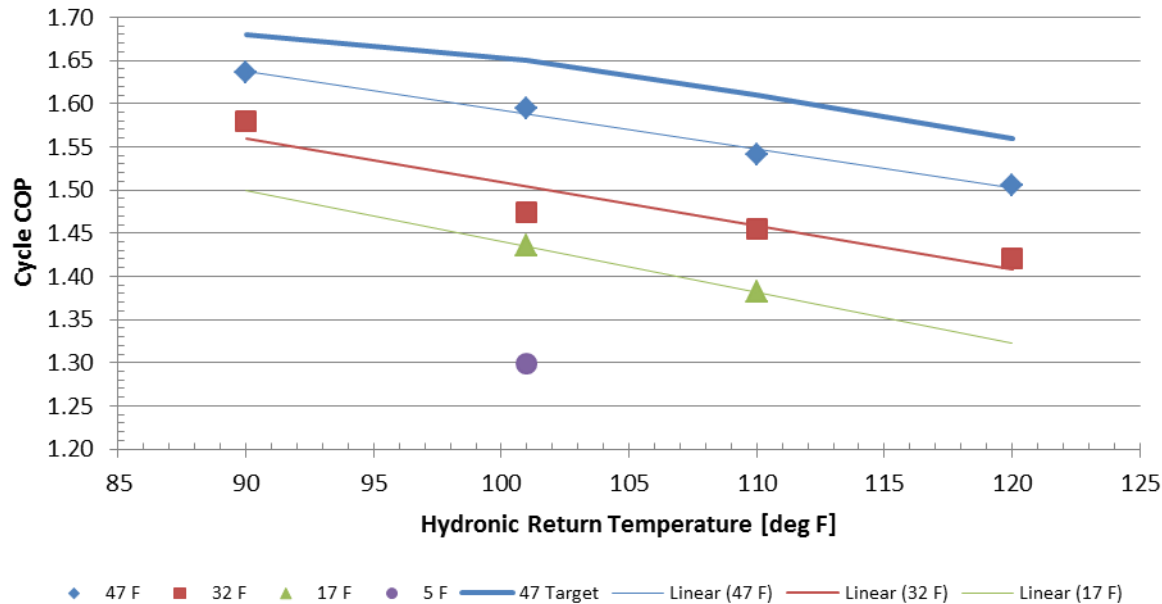
Progress and Accomplishments

Accomplishments:

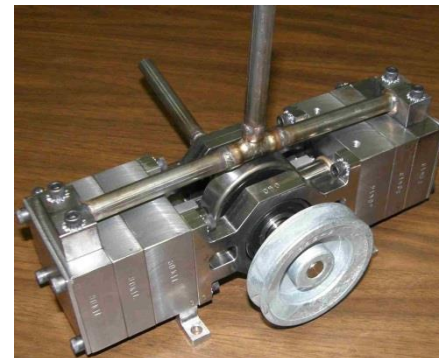
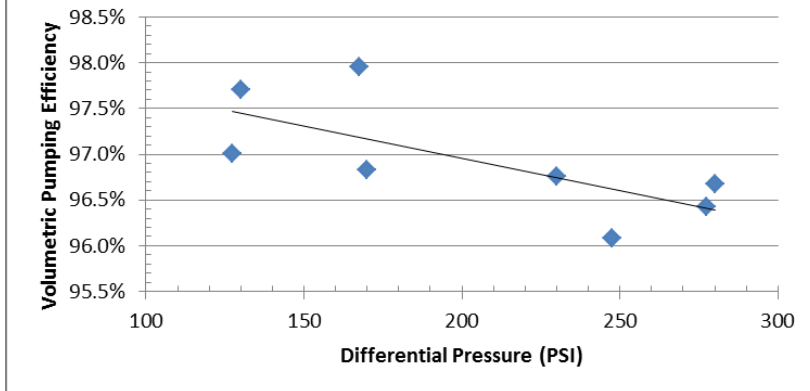
- ✓ **Optimized Simple Single-Effect Cycle That Predicts Target Performance.**
- ✓ **Breadboard Testing Complete**
 - ❖ 95% of Performance Target at design condition
 - ❖ 4:1 Modulation Achieved
- ✓ **Evaporator Design Model Developed and Verified w/Experimental Data**
 - ❖ 3 Coils Tested
 - ❖ Optimized coil ~25% cost reduction from original design
- ✓ **Low-Cost Solution Pump Successfully Scaled Up Factor of 10.**
- ✓ **Alpha Packaged Prototype Fabricated & Lab Tested**
- ✓ **Preliminary manufacturing cost estimate is within our target range.**

Progress and Accomplishments

Breadboard: Cycle COP vs Ambient & Hydronic Return Temperature



Alpha Solution Pump Bench Test Performance
Inlet Pressure 70 psig



Progress and Accomplishments

Alpha Prototype



Nominal Output : 80,000 Btu/hr (23.4 kW)

Gas Input: 54,000 Btu/hr (15.8 kW)

Max Supply: 145°F (63°C)

Size: 36 x 40 x 42" (91 x 112 x 117 cm)

Weight: ~500 lbm (227 kg)

As of end of March: 58 Steady-State Tests

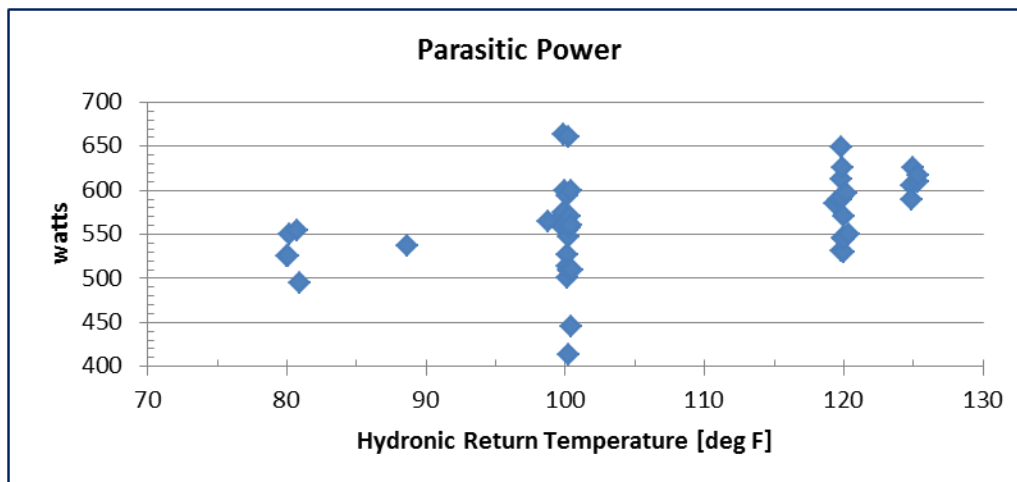
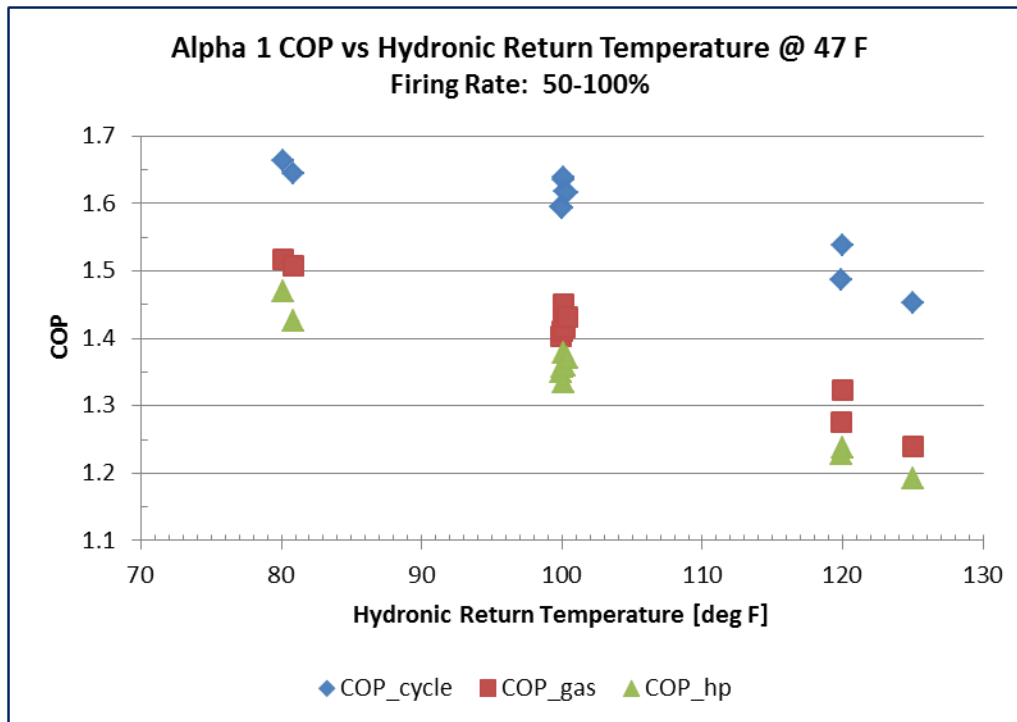
Ambient: -1 to 56°F (-18.3 to 13.3°C)

Hyd Return: 80 to 125°F (26.7 to 51.7°C)

Hyd Supply: 92 to 142°F (33.3 to 61.1°C)

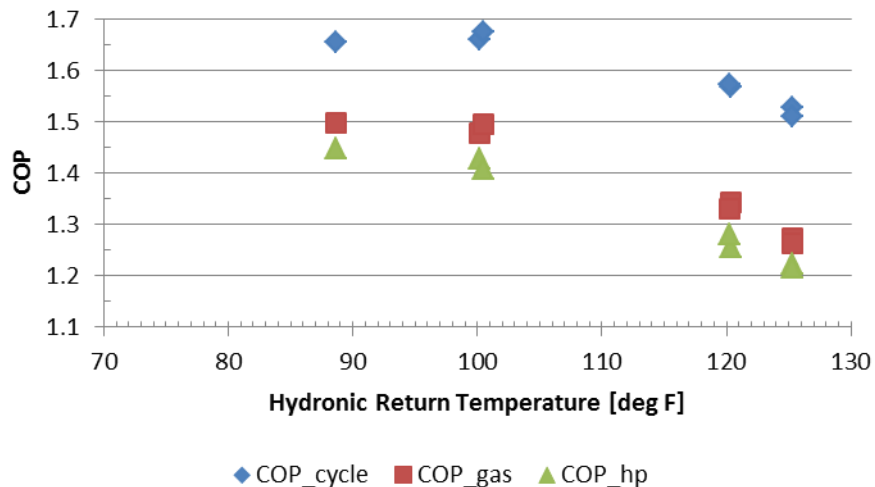
Modulation: 4:1

Progress and Accomplishments

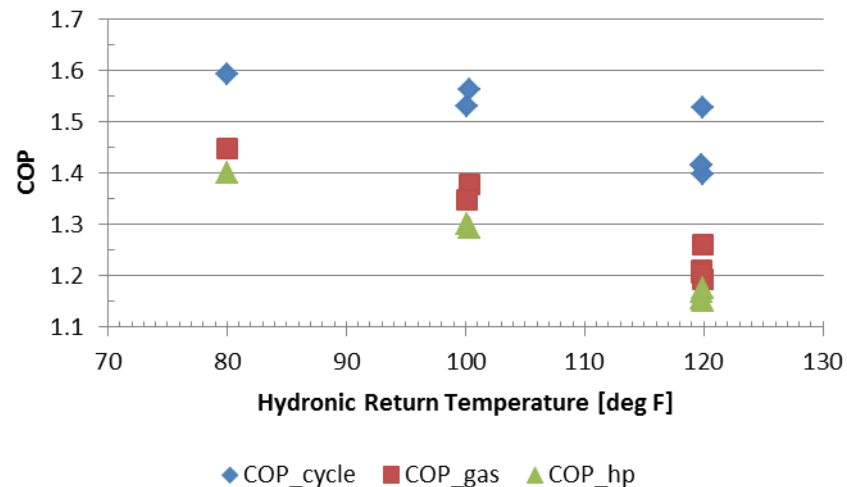


Progress and Accomplishments

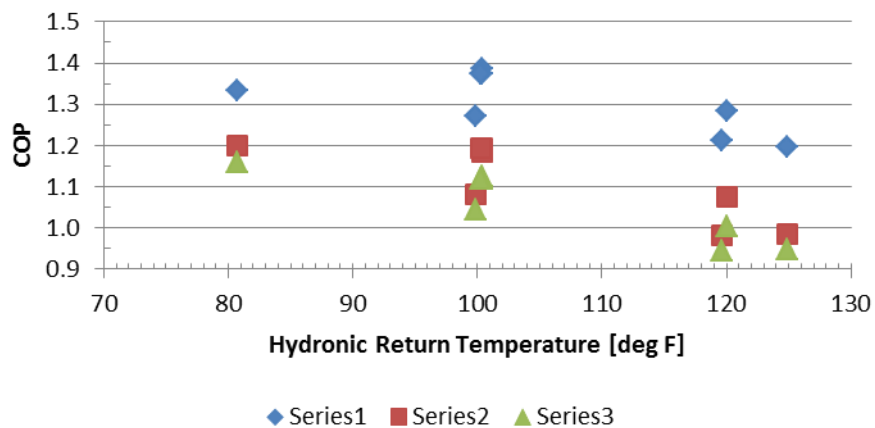
Alpha 1 COP vs Hydronic Return Temperature @ 55 F
Firing Rate: 50-100%



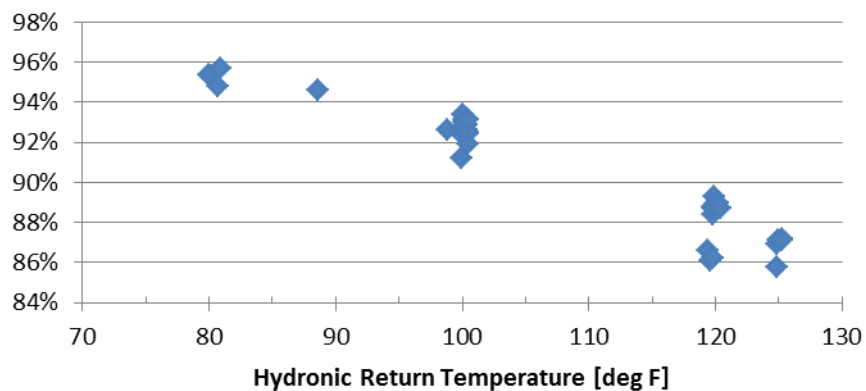
Alpha 1 COP vs Hydronic Return Temperature @ 32 F
Firing Rate: 50-100%



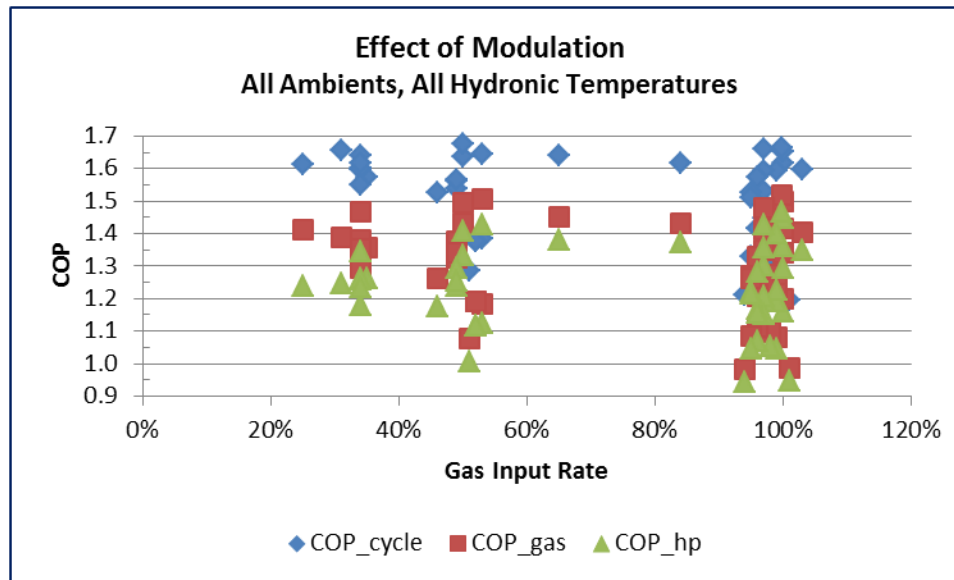
Alpha 1 COP vs Hydronic Return Temperature @ -1 to 9 F
Firing Rate: 50-100%



Combustion Efficiency

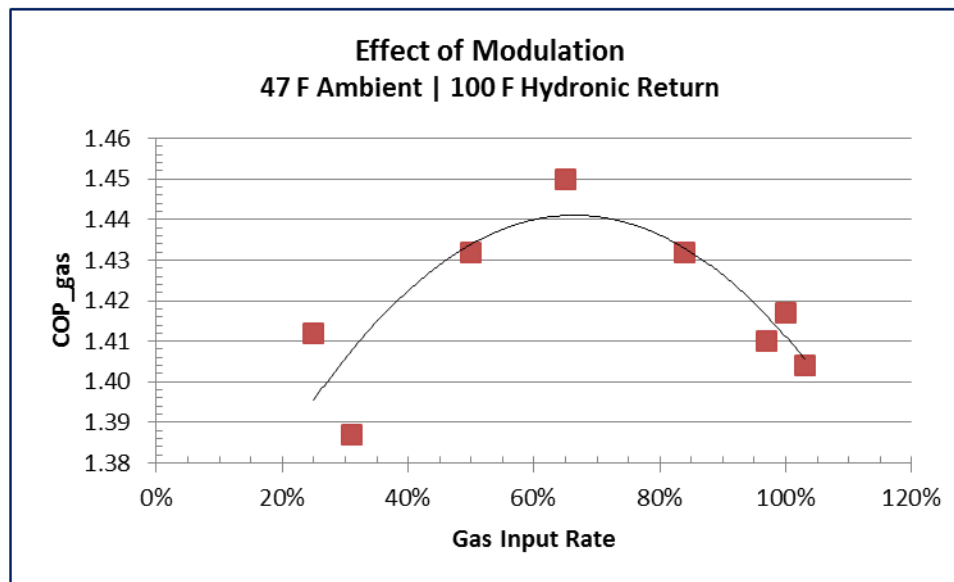


Progress and Accomplishments



Considering all data, effect of modulation is minor.

Stability good all the way down to 4:1 modulation.



At single ambient and return hydronic temperature, performance maximized between 50 and 80% target gas input rate.

Progress and Accomplishments

Lessons, Issues & Opportunities:

- ❖ Performance 96% target at design conditions. 90% at cold ambients.
- ❖ Ammonia purity 99.2 – 99.4% at design conditions, down slightly from breadboard and less than 99.7% target. Primary cause of remaining performance gap and impact is greater at low ambients / high return temperatures.
- ❖ Solution Heat Exchanger effectiveness above target , but increases Rectifier load.
- ❖ Rectifier size to be increased 10% for Alpha 2 packaged prototype.

Market Impact:

- ❖ Field test and reliability units planned for 2015/2016 winter heating season.
- ❖ Business model to partner with leading OEMs for each market application. Leverages existing distribution/service channels, maximizes marketing efforts and consumer education, and minimizes time and money required by SMTI to launch product line.

Project Integration and Collaboration

Project Integration:

- Market-leading OEM is a sub-contractor and providing cost-share.
- Gas Technology Institute is a sub-contractor and providing cost-share through contributions from gas utilities.
- Both are in constant communication with SMTI via conference calls, emails, and quarterly project reports (going both directions).
- GTI keeps gas utility sponsors updated via bi-annual meetings and informal communications.

Partners, Subcontractors, and Collaborators:

- **AO Smith (OEM):** Provides component design, fabrication, testing support, market research, and cost share to the project.
- **GTI:** Provides combustion system design and testing, system performance testing, cost share and gas utility communication.

Communications:

ACEEE Hot Water Forum, Energy Solutions Center Annual Meeting, CEE member conference call presentation, GTI bi-annual meetings with gas utility research sponsors, International Sorption Heat Pump Conference.

Next Steps and Future Plans

Next Steps and Future Plans:

- ❖ **3rd Party Testing & Verification of Alpha 1 by GTI (April – June, 2015)**
 - ❖ Steady-state and home/DHW simulation testing
 - ❖ Energy/Cost savings modeling for several regions
- ❖ **Fabrication & Testing of Alpha 2 prototype at SMTI**
 - ❖ Target incremental performance improvements
 - ❖ Controls optimization (modulation, combo systems, ambient set-back, etc).
 - ❖ Study coil defrost requirement and evaluate options
 - ❖ Test under commercial water heating conditions
- ❖ **Installation of Alpha 1 on SMTI lab as primary heating system**
- ❖ **Sponsored field test/reliability units, Winter 2015/2016**
- ❖ **Expansion of Product Family (larger and smaller capacities)**

Project Budget

Project Budget: \$902,870 (Fed) + \$232,294 (CS) = \$1,135,164

Variances: Currently Under-Budget. Six month no-cost extension approved.

Cost to Date: **Federal:** \$629,730 of \$902,870 (70%)
Cost Share: \$181,880 of \$260,508 (70%)

Budget History

03/01/13 – FY2014 (past)		FY2015 (current)		FY2016 (planned)	
DOE	Cost-share	DOE	Cost-share	DOE	Cost-share
\$458,385	\$142,586	\$444,485	\$117,922		

Project Plan and Schedule

Project Schedule												
Project Start: 03/01/2013	Completed Work											
Projected End: 08/31/2015	Active Task (in progress work)											
	◆ Milestone/Deliverable (Originally Planned) use for missed											
	◆ Milestone/Deliverable (Actual) use when met on time											
	FY2013				FY2014				FY2015			
Task	Q1 (Oct-Dec)	Q2 (Jan-Mar)	Q3 (Apr-Jun)	Q4 (Jul-Sep)	Q1 (Oct-Dec)	Q2 (Jan-Mar)	Q3 (Apr-Jun)	Q4 (Jul-Sep)	Q1 (Oct-Dec)	Q2 (Jan-Mar)	Q3 (Apr-Jun)	Q4 (Jul-Sep)
Past Work												
M1: Cycle Modeling			◆									
M2: Cycle Heat HX and Combustion Design				◆								
M3: Solution Pump Design and Testing					◆							
M4: Breadboard Fabrication					◆							
M5: Breadboard Testing								◆				
M6: Condensing HX Prototype Testing							◆					
M7: Packaged Prototype Fab & Assy								◆				
Current/Future Work												
M8: Packaged Prototype Preliminary Testing									◆			
M9: Packaged Prototype 1 Final Testing										◆		
M9: Packaged Prototype 2 Final Testing											◆	
M10: Packaged Prototype 3rd Party Testing										◆		