

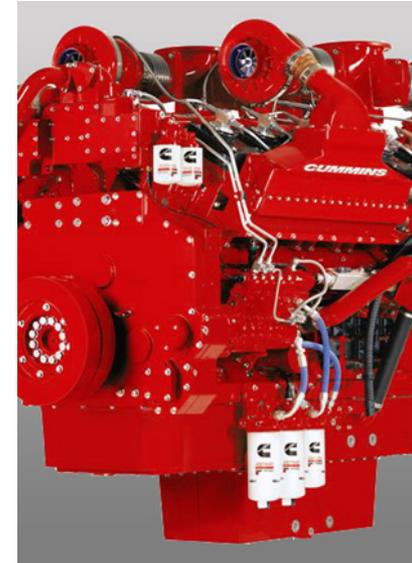
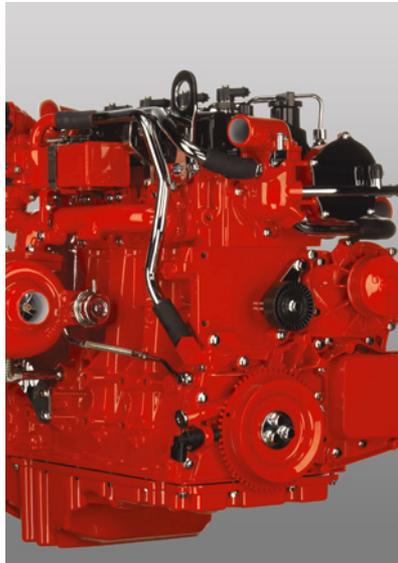
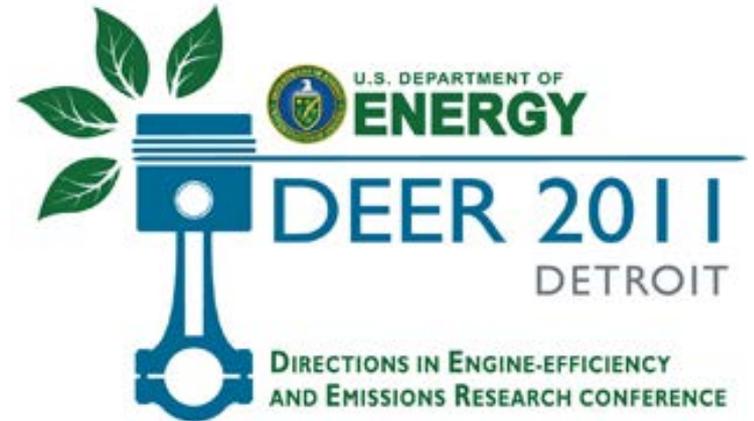
# N<sub>2</sub>O Emissions From 2010 SCR Systems



Krishna Kamasamudram

Cary Henry, Aleksey Yezerets

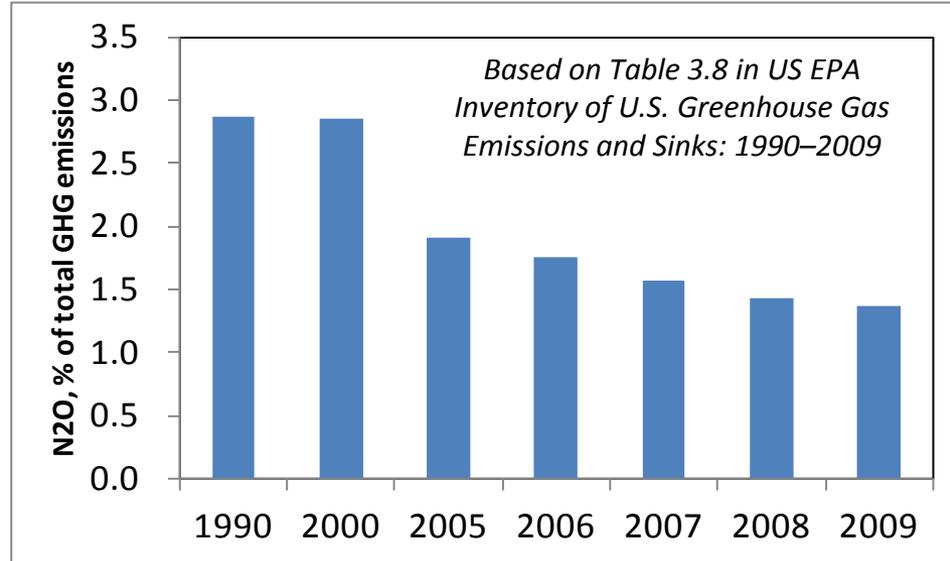
Cummins Corporate Research  
and Technology



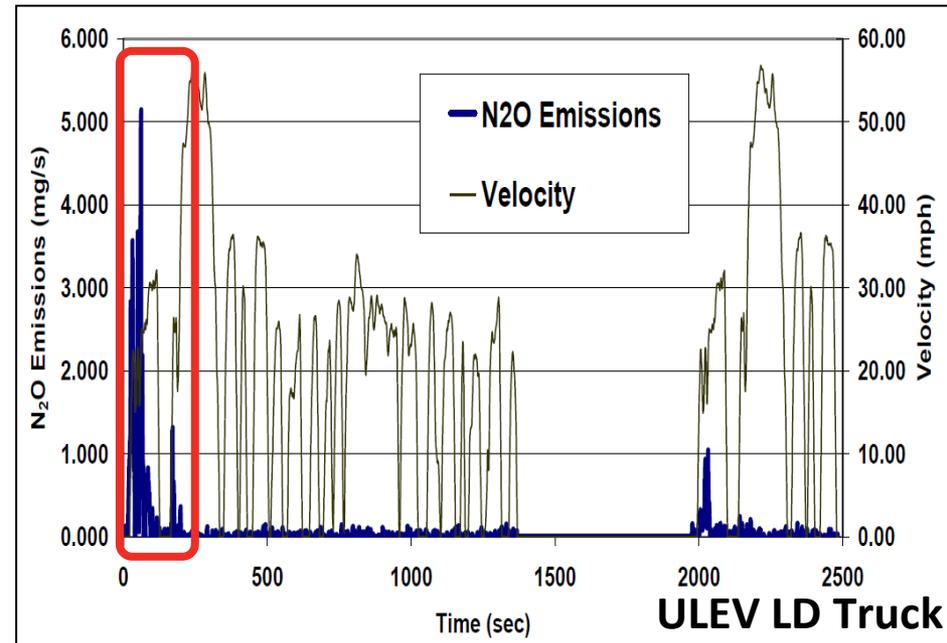
# Background

- Nitrous oxide ( $N_2O$ ) is produced in limited quantities by combustion processes and by all  $NO_x$  reduction catalysts
- $N_2O$  selectivity from TWC declined with years, due to improved catalyst formulations and operation strategies
- In three-way catalysts (TWC),  $N_2O$  forms mostly under cold-start conditions

$N_2O$  fraction in total GHG emissions from the transportation sector

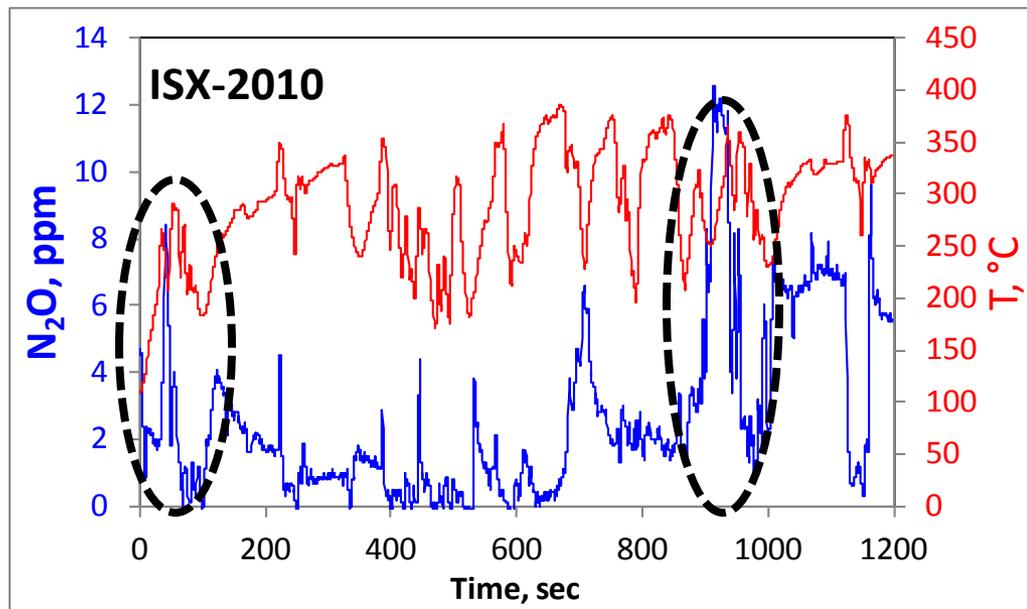


Durbin et al. CRC E-60 Final Report. 2003

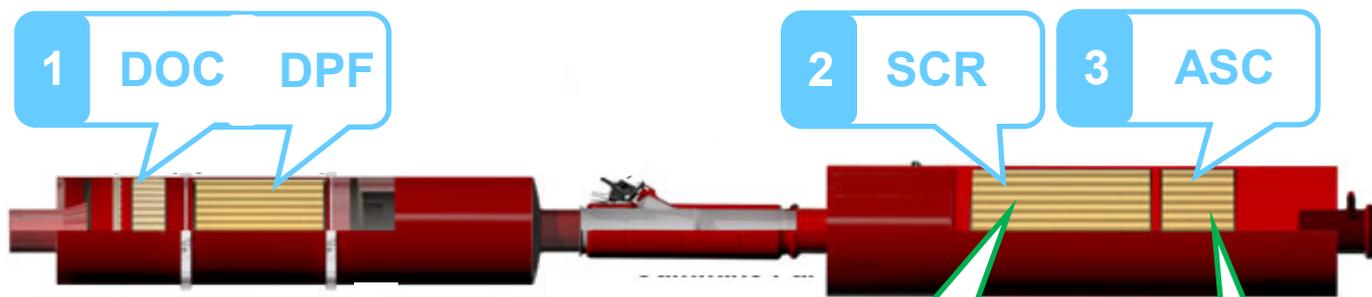


# N<sub>2</sub>O Emissions From SCR System

- In SCR system, N<sub>2</sub>O forms in different parts of the cycle, not just the cold start
- Various catalysts can contribute to N<sub>2</sub>O formation and mitigation



N<sub>2</sub>O formation on

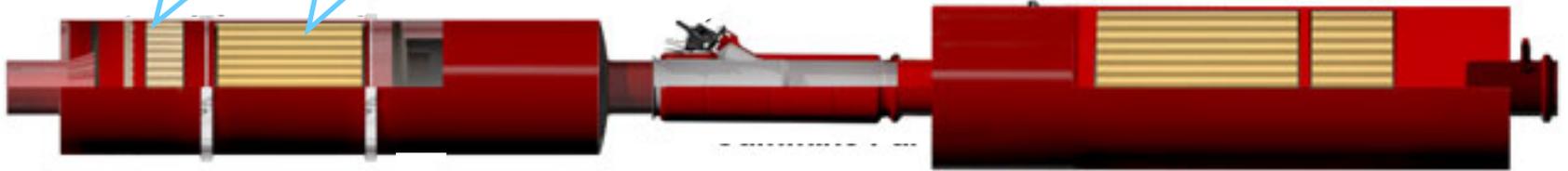


N<sub>2</sub>O mitigation on



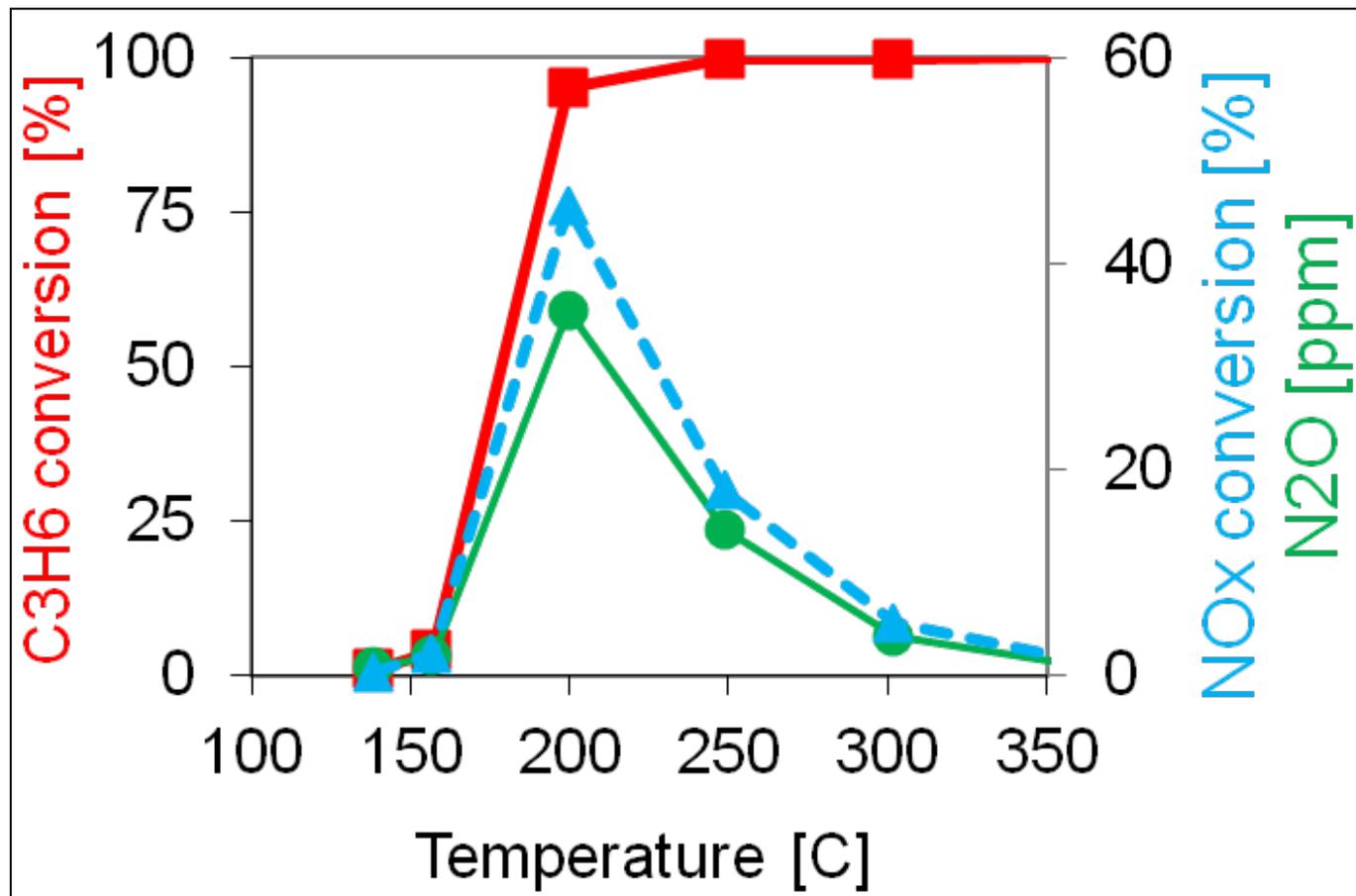
# N<sub>2</sub>O formation on

1 Oxidation catalysts  
DOC DPF



# N<sub>2</sub>O Formation on Oxidation Catalysts

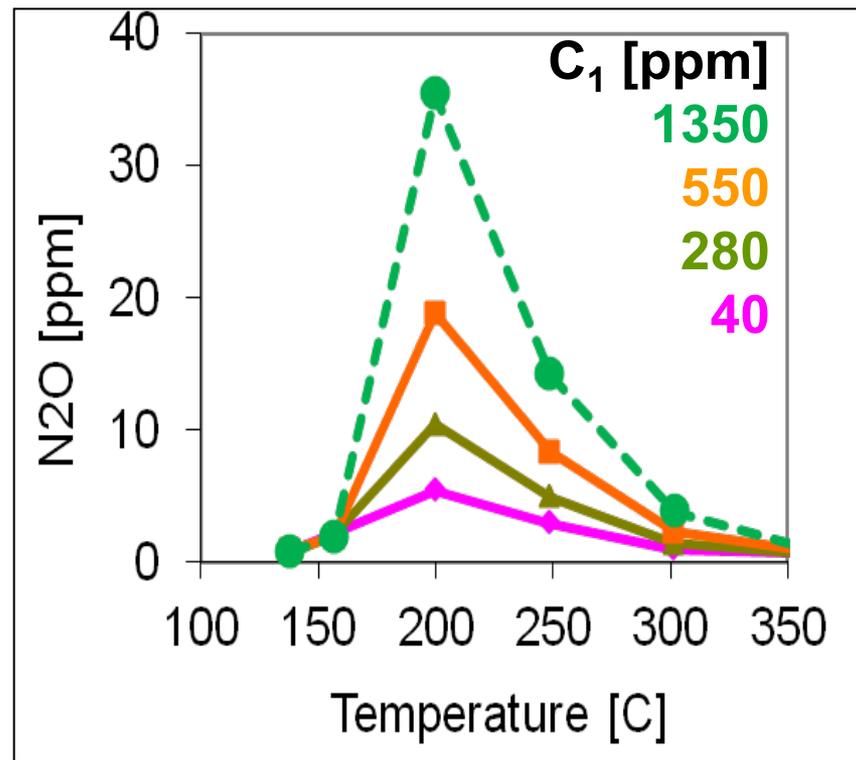
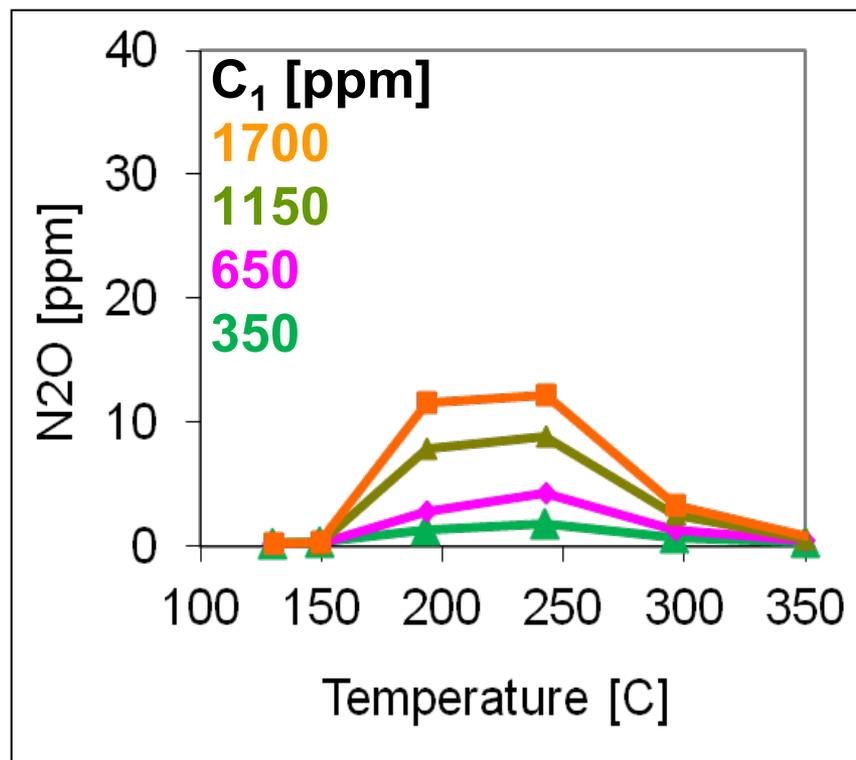
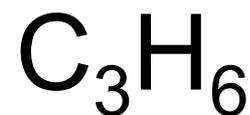
- Under certain conditions, NO<sub>x</sub> can be reduced over oxidation catalysts primarily to N<sub>2</sub>O and N<sub>2</sub> (lean-NO<sub>x</sub> catalysis or HC-SCR)



*NO<sub>x</sub> = 200 ppm, C<sub>3</sub>H<sub>6</sub> = 450 ppm, SV = 60kh<sup>-1</sup>*

# N<sub>2</sub>O Formation on Oxidation Catalysts

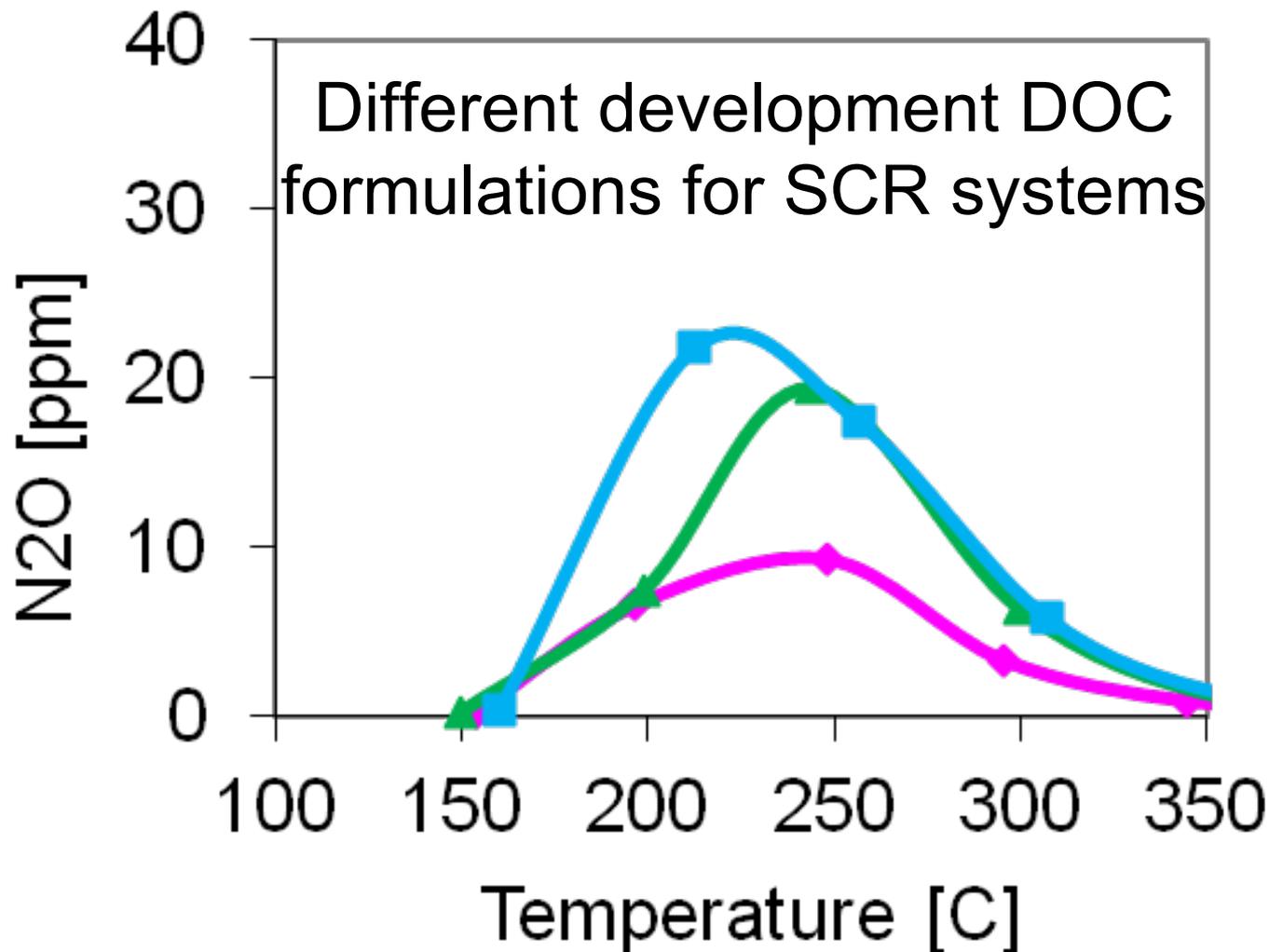
- N<sub>2</sub>O yield is affected by exhaust conditions, including temperature, concentration and nature of hydrocarbon species



NO<sub>x</sub> = 200 ppm, SV = 60kh<sup>-1</sup>

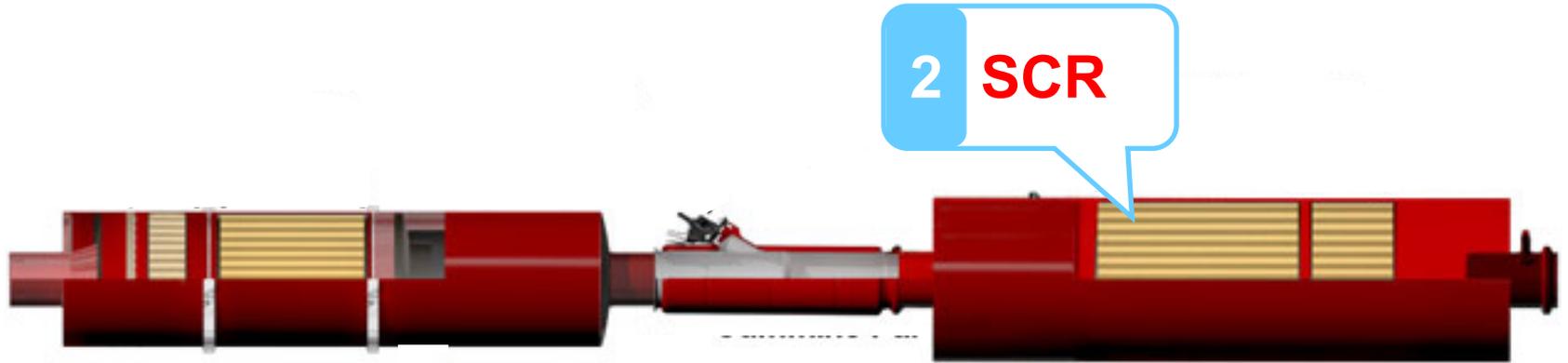
# N<sub>2</sub>O Formation on Oxidation Catalysts

- N<sub>2</sub>O selectivity is also affected by catalyst formulation details



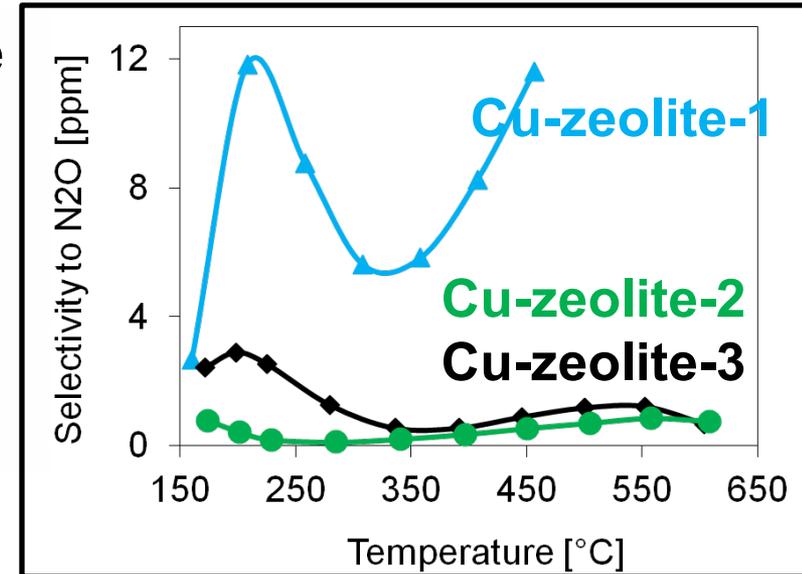
*NO<sub>x</sub> = 200 ppm, C<sub>3</sub>H<sub>6</sub> = 450 ppm, SV = 60kh<sup>-1</sup>*

# N<sub>2</sub>O formation on



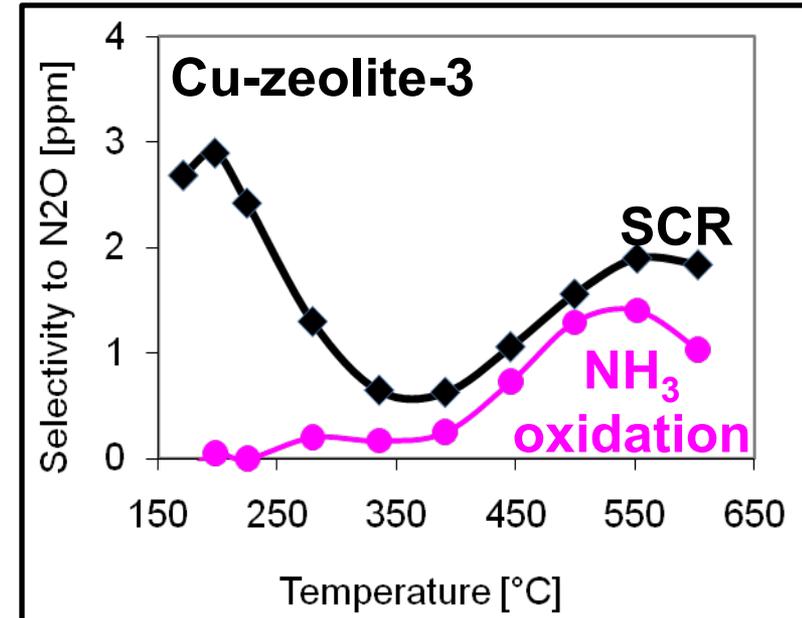
# Small amounts of $N_2O$ can be produced by all classes of SCR catalysts

- Vanadia-, Fe-zeolite and Cu-zeolite catalysts can all produce  $N_2O$
- Even within a given class of catalysts (e.g. Cu-zeolites),  $N_2O$  selectivity depends on catalyst formulation



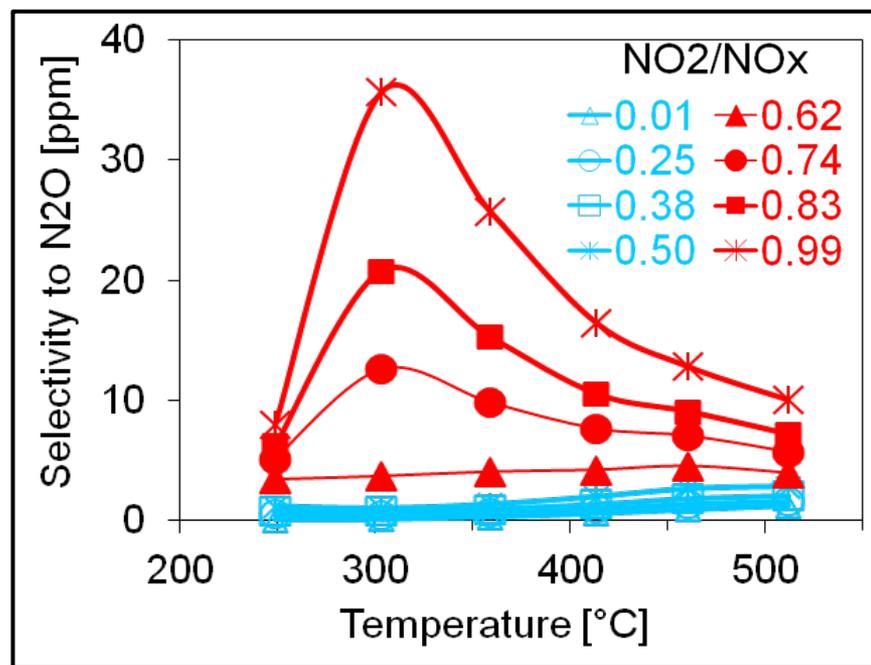
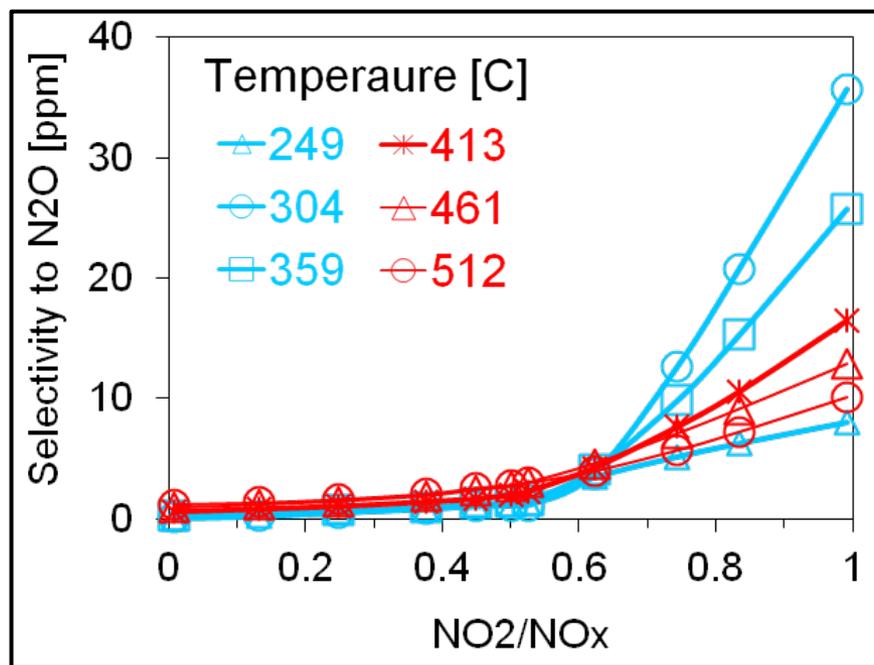
## Dual mode $N_2O$ formation mechanism:

- At higher T – mostly due to parasitic  $NH_3$  oxidation
- At lower T – primarily through the  $NH_4NO_3$  mechanism



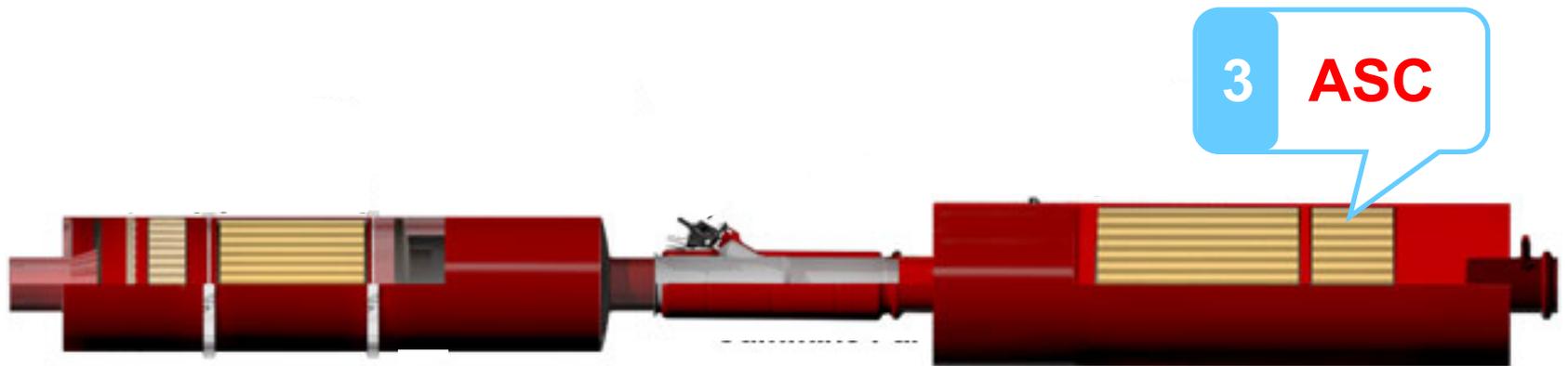
# N<sub>2</sub>O Formation on SCR

- Selectivity to N<sub>2</sub>O is strongly affected by the NO<sub>2</sub>/NO<sub>x</sub> ratio, especially above 0.5
- Upstream DOC/DPF influence N<sub>2</sub>O production over SCR catalyst



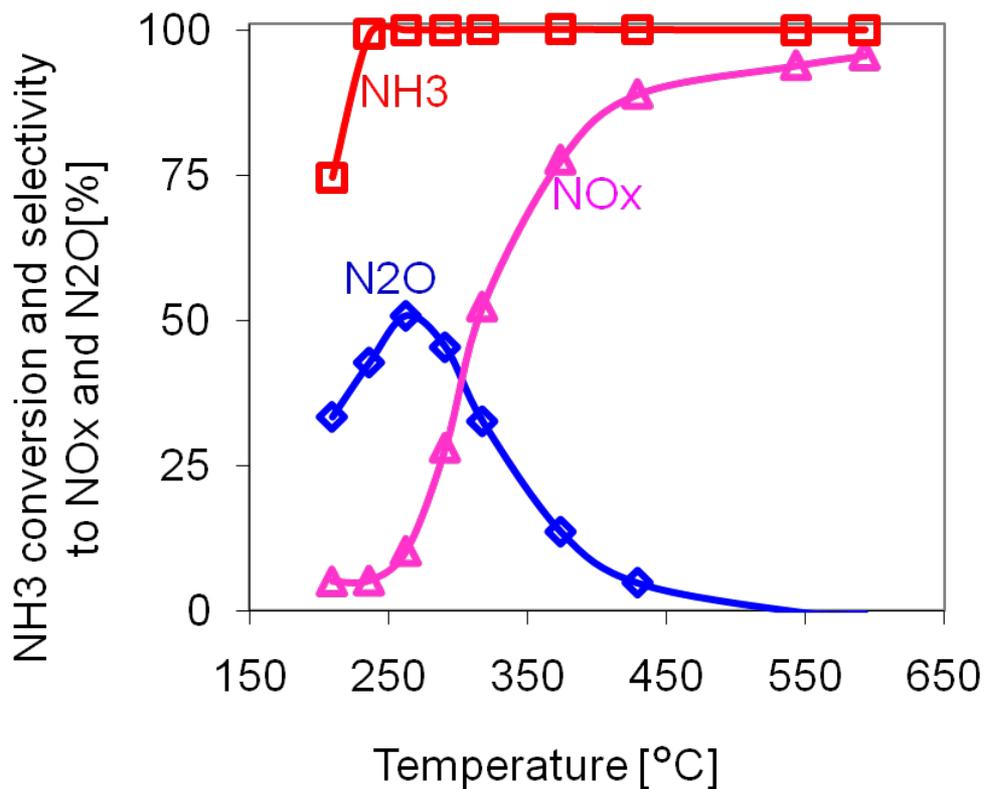
NO<sub>x</sub> = 200 ppm, NH<sub>3</sub> = 200 ppm, SV = 20kh<sup>-1</sup>

# N<sub>2</sub>O formation on



# Conventional oxidation catalysts have poor selectivity in the NH<sub>3</sub> oxidation process

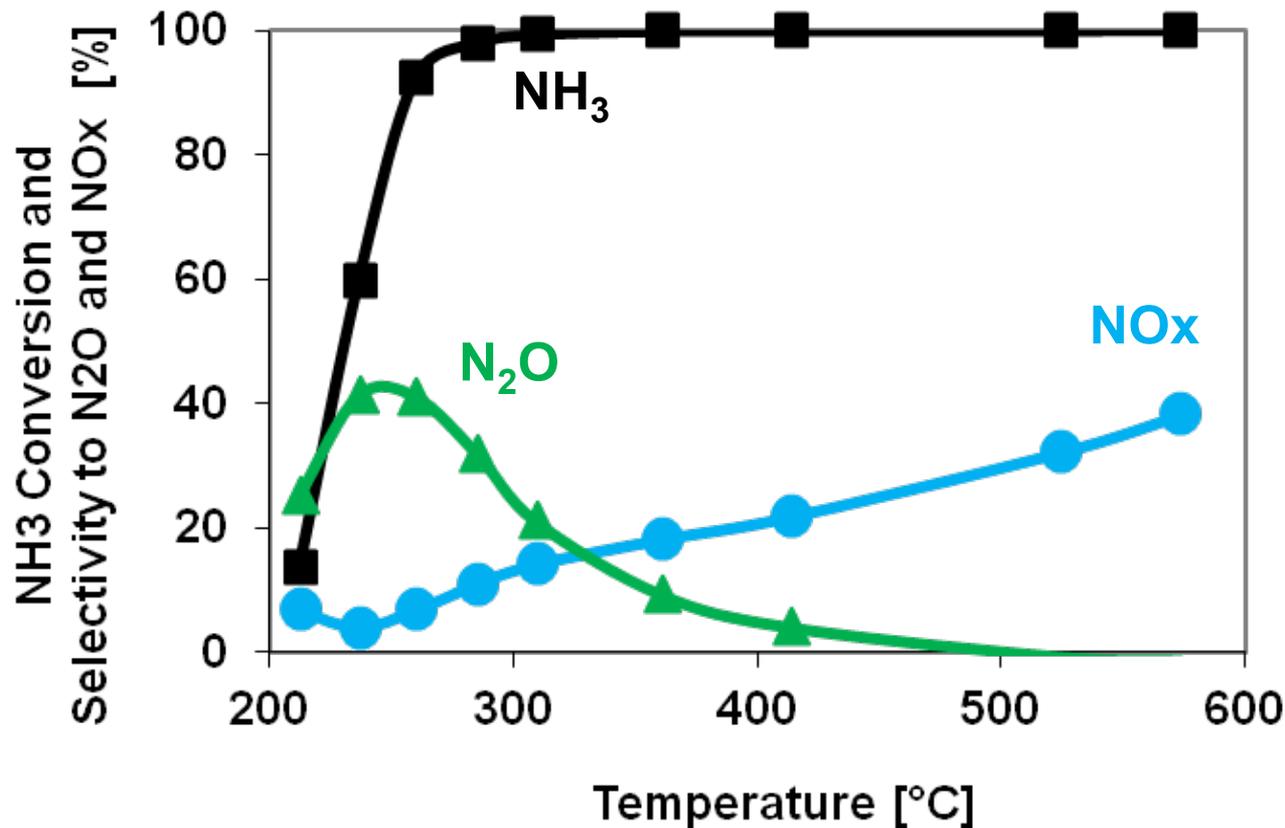
- Precious metal-based oxidation catalysts are highly active in NH<sub>3</sub> oxidation, but produce high yields of NO<sub>x</sub>, N<sub>2</sub>O



NH<sub>3</sub> = 100 ppm, SV = 100 kh<sup>-1</sup>

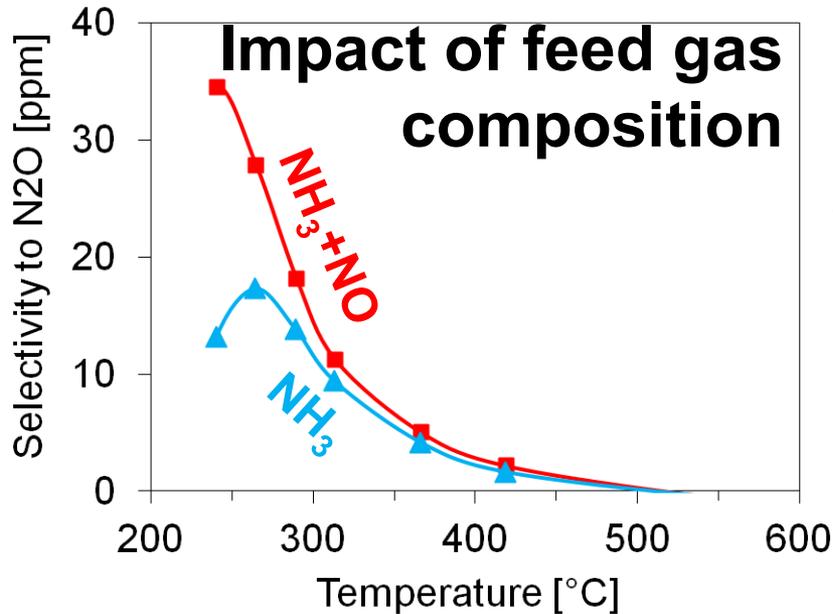
# Use of dedicated ASC reduces N<sub>2</sub>O formation in the NH<sub>3</sub> oxidation process

- ASC can be formulated to maximize selectivity to N<sub>2</sub>, while maintaining high NH<sub>3</sub> conversion



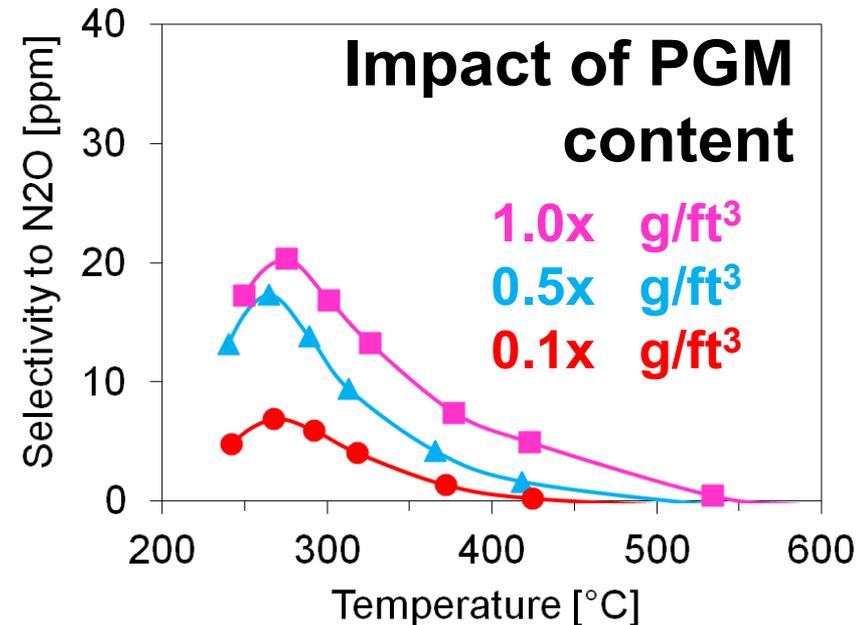
*NH<sub>3</sub> = 100 ppm, SV = 100 kh<sup>-1</sup>*

# N<sub>2</sub>O formation depends on reaction conditions and ASC formulation

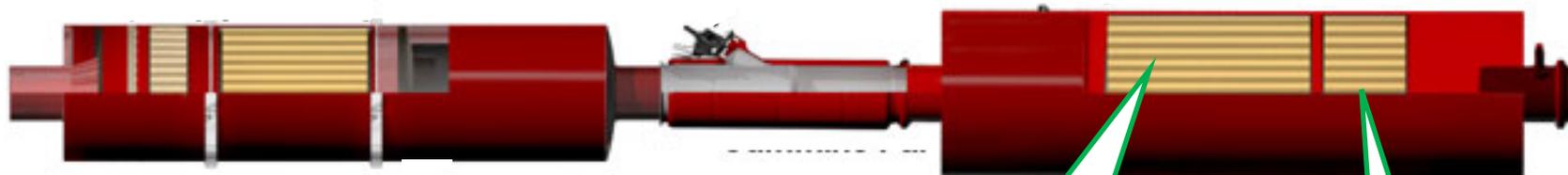


Presence of NO<sub>x</sub> along with NH<sub>3</sub> leads to an increase in selectivity to N<sub>2</sub>O

Decrease in PGM content of ASC decreases selectivity to N<sub>2</sub>O



# N<sub>2</sub>O mitigation on



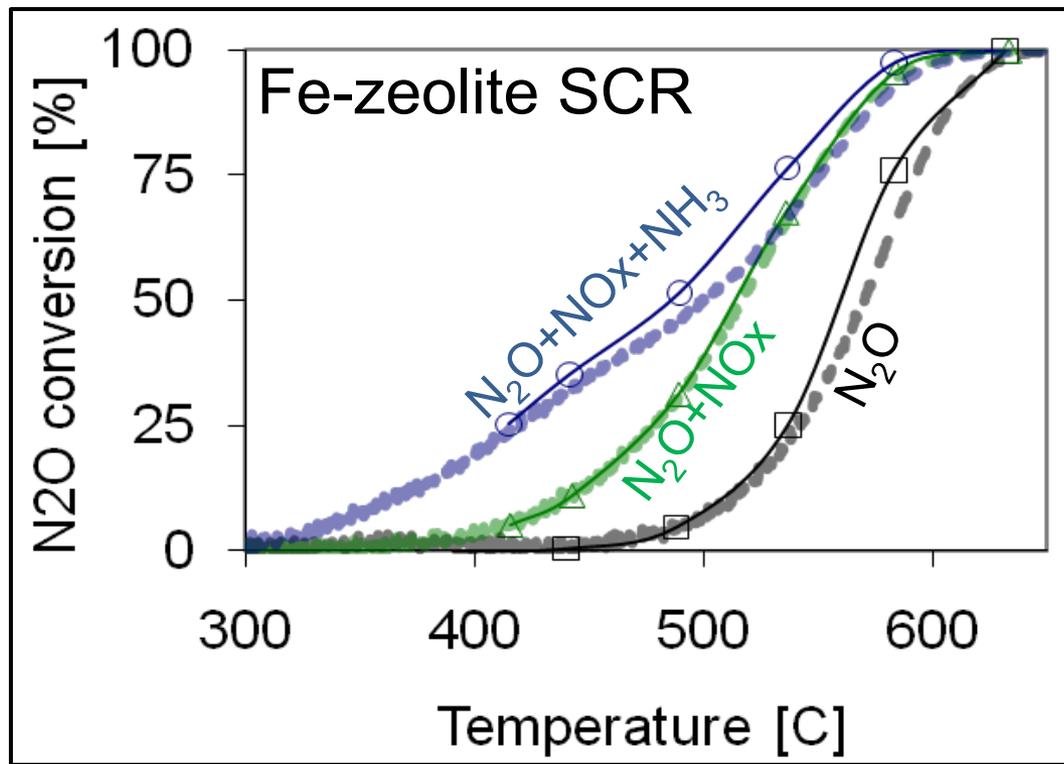
4

Cu- & Fe-  
zeolite SCR

5

ASC

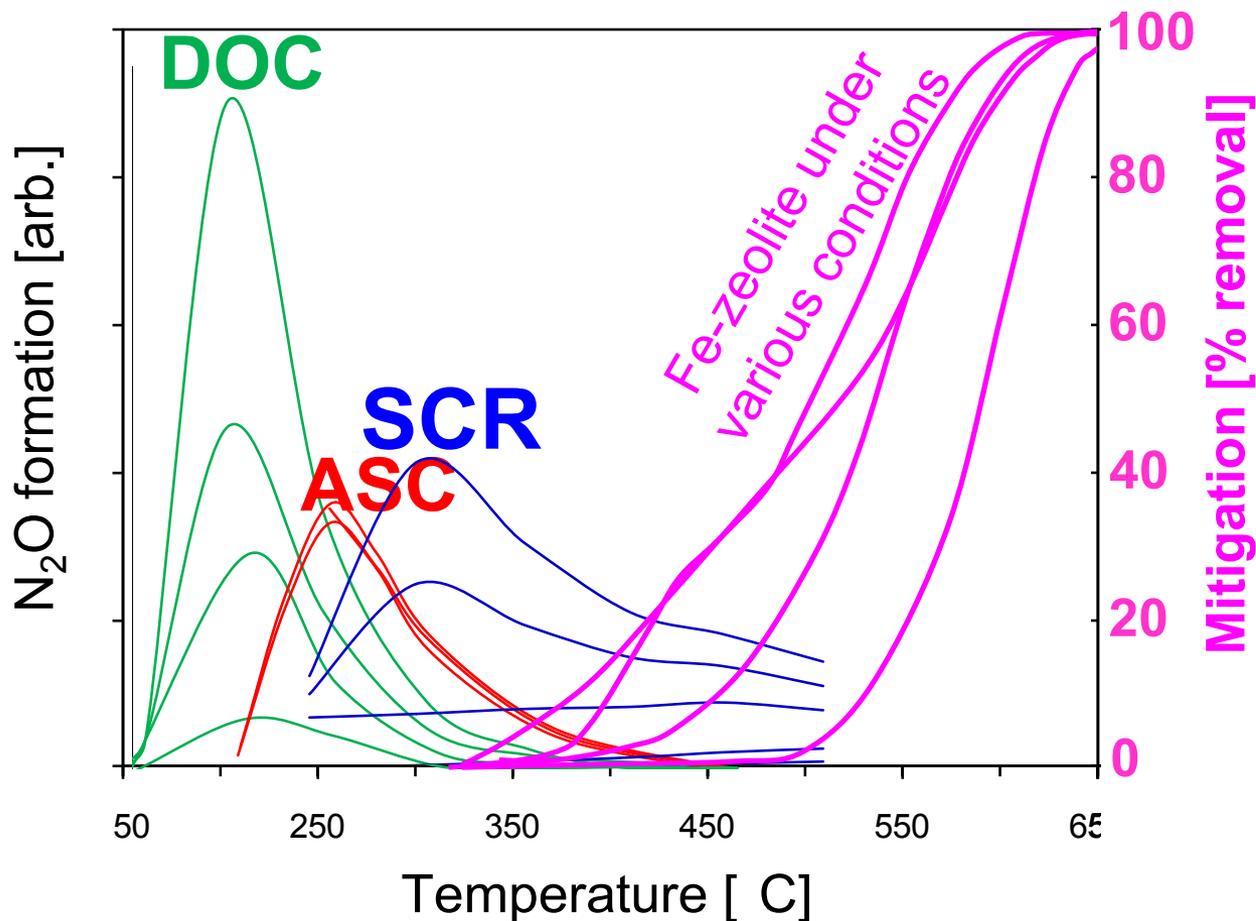
# N<sub>2</sub>O conversion on SCR and ASC is very limited under practically relevant conditions



- Each color corresponds to a particular set of feed gas composition
- Symbols – steady-state points
- Dotted curves – continuous temperature-programmed experiments

- Very little N<sub>2</sub>O reduction activity below ~400 C
  - Fe-zeolites are known to be among the most active catalysts
- N<sub>2</sub>O does not store on the catalyst
  - Similar steady-state and transient profiles indicate this

# N<sub>2</sub>O formation and reduction/decomposition temperature windows have limited overlap



Focus: Minimize N<sub>2</sub>O *formation*

# Conclusions

- $\text{N}_2\text{O}$  is a common byproduct of fossil fuel combustion, with or without  $\text{NO}_x$  aftertreatment
  - No direct health impact, hence unregulated until the recent advent of GHG regulations
- Various elements of SCR system can contribute to  $\text{N}_2\text{O}$  emissions, depending on the conditions
- Minimization of  $\text{N}_2\text{O}$  involves catalyst formulations, system architecture, operation strategy and controls
- With proper understanding of the underlying chemical processes, new EPA standards for  $\text{N}_2\text{O}$  emissions can be met by SCR systems
  - Test data indicate that Cummins 2010 SCR systems are below the adopted  $\text{N}_2\text{O}$  threshold

# Acknowledgements

Randy Jines      For assistance with data collection

Neal Currier      For valuable discussions

Shirish Shimpi      For advice and examples of engine data