

Cummins-ORNL\FEERC Emissions CRADA: NO_x Control & Measurement Technology for Heavy-Duty Diesel Engines

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Overview

Timeline

- Start: FY1998
- Major Revisions: 2001, 03, 06, 10
- Current term: 2010-'12 revision
- Current end date: Sept. 2012
- ~80% Complete

Budget

- 1:1 DOE:Cummins cost share
- DOE Funding:
 - FY2010: \$400k
 - FY2011: \$450k
 - FY2012: \$450k

Barriers

- *Emissions controls*
 - Catalyst fundamentals,
 - Reactions & mechanistic insights
 - Catalyst models (design tools & imbedded)
 - Control strategies & OBD
- Combustion Efficiency
 - Shift emissions tradeoff to fuel efficiency
- *Durability*
 - Enhanced durability via knowledge-based controls
- *Cost*
 - Lower catalyst & sensor costs
 - Lower development costs

Partners

- **ORNL & Cummins Inc.**
- Chalmers Univ. of Technology
- Politecnico di Milano

Objectives & Relevance

- Quantify & correlate transient SCR performance distributions
- Improved methods & tools for enhanced analysis



Enabling &
Applications for:

- Better understanding of how catalyst operating & mechanistic insights
- Improved SS & dynamic catalyst simulations
- Better development tools
- Methods & ideas for improved control (OBD) & catalyst-state assessment
- Better vehicles for consumers:
 - **Higher Efficiency:** lower engineering margins via better design & control
 - **Lower Emissions:** better design tools, models, controls & OBD
 - **Improved Durability:** advanced controls for extended catalyst lifetime
 - **Lower Cost:** Analysis-led design, fewer & lower-\$ sensors, urea utilization

Milestones

2011 Milestone:

- ✓ ● Dynamic analysis of SCR-catalyst performance
 - NH₃ capacity distributions

2012 Milestones (on target for Sept. 2012 completion):

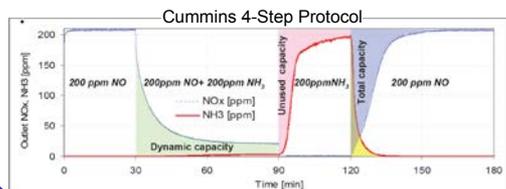
- Improve instrumental methods for transient analysis of catalyst state
 - Instantaneous NH₃ coverage & loading rate, instantaneous conversion
- Characterize spatiotemporal performance of Cummins Commercial SCR catalyst (SAPO-34)

Approach for addressing SCR Control Challenges

ORNL

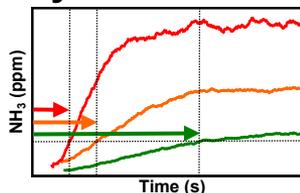
Catalyst Knowledge

Evaluate static & dynamic catalyst nature



Understand chemical & spatiotemporal relationships

Identify Control Measures



Improve models

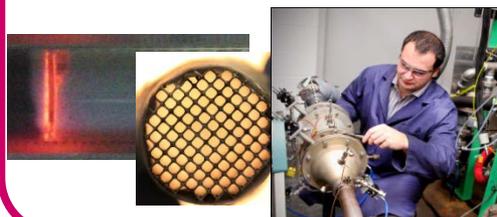
Diagnostic Tools

Develop diagnostics



Prioritize high-potential diagnostics

Bench & engine evaluation



Understanding + Diagnostics for Real-Time Catalyst Control

Improved Fuel Economy, emissions & catalyst durability

CUMMINS

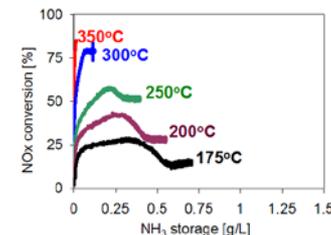
System Integration

Develop control strategies



Develop OBD strategies

Elucidate catalyst functional behavior



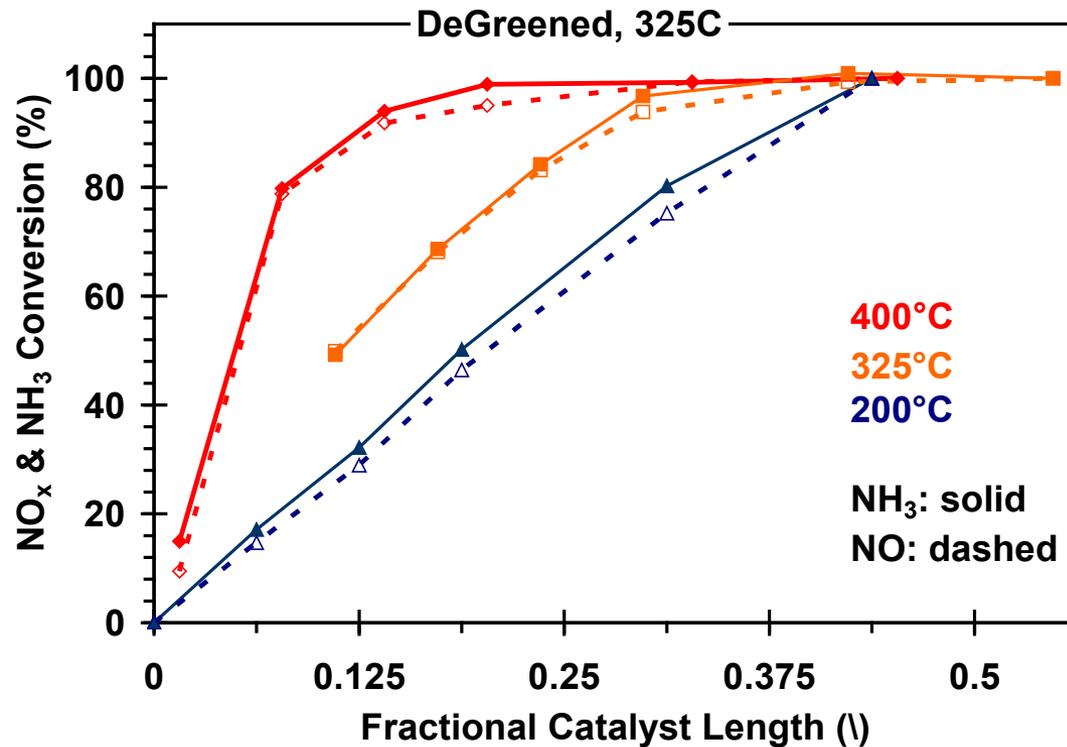
Improve models & designs

Technical Progress: Summary

- **Temperature impact on SCR performance**
 - SCR Zone
 - Parasitic NH_3 Oxidation
- **NH_3 Capacity Distributions** (*New Insights!*)
 - Correlation w/ SCR zone
 - Control implications
- **Hydrothermal Ageing**
 - Correlations w/ DeGreened results
 - Mechanistic implications
- **Dynamic & SS NH_3 Inhibition** (*New Insight for Cu Zeolite catalyst!*)
 - Location of Dynamic Inhibition
 - Mechanistic implications

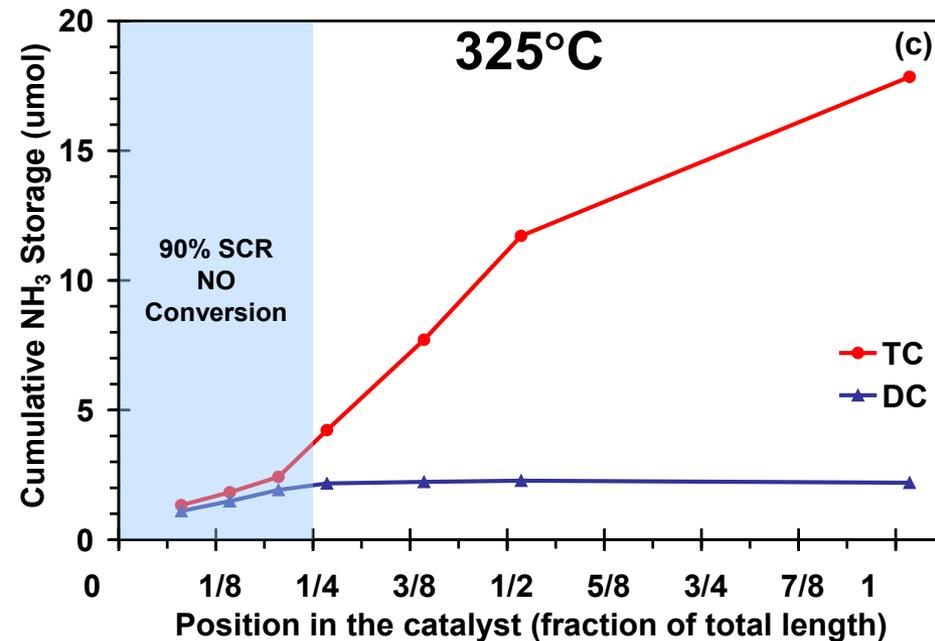
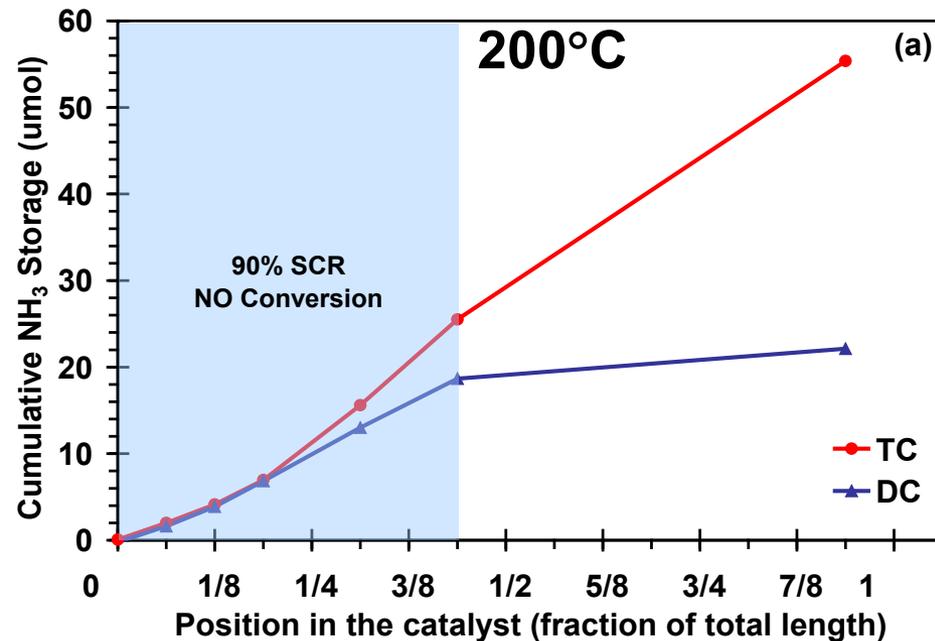


Technical Progress: Temperature-Induced SCR Shifts



- SCR zone shifts to catalyst front w/ increasing temperature
 - Major internal variations despite same 100% integral conversion
 - High NH₃ levels survive deeper into catalyst at lower T
- Negligible Parasitic NH₃ Oxidation
 - Despite significant NO_x-free NH₃ oxidation
 - i.e., SCR rate greater than O₂ + NH₃ rate

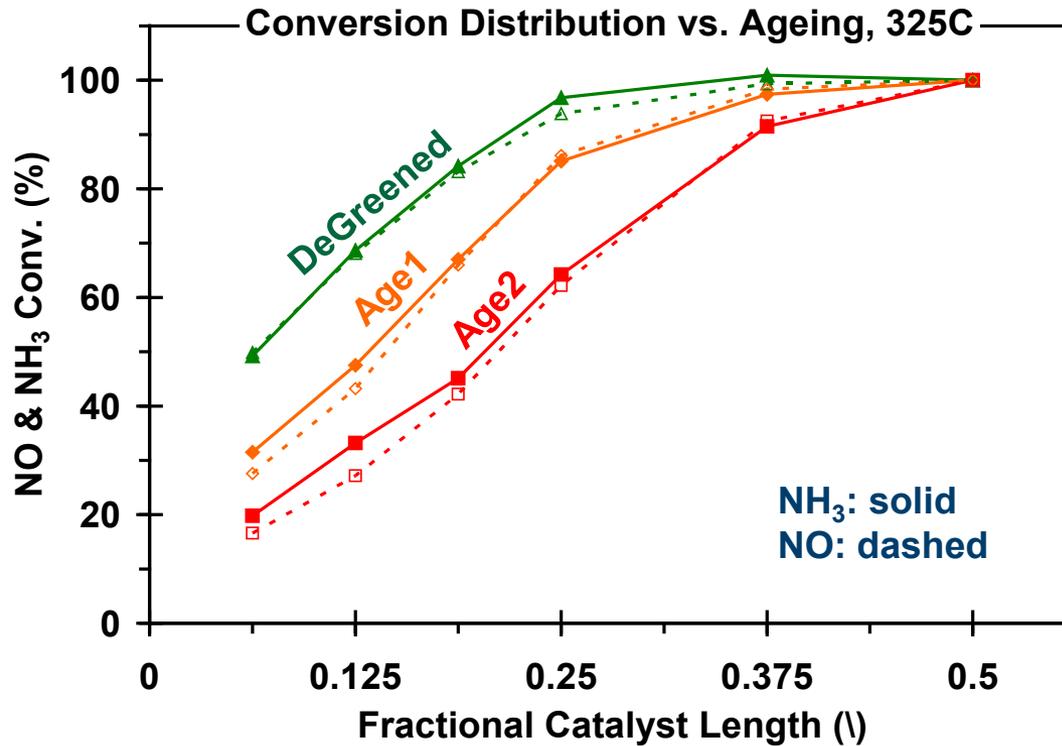
Technical Progress: 100% NH₃ Coverage in SCR Zone



- Various components to NH₃ capacity
 - Dynamic (DC): capacity used in SCR
 - Unused (UC) and Total (TC) capacity
 - TC = DC + UC
- **DC = TC in SCR zone**
 - Saturated surface NH₃ in SCR zone
 - Implies UC=0 in SCR zone
 - Corroborated by UC measurements

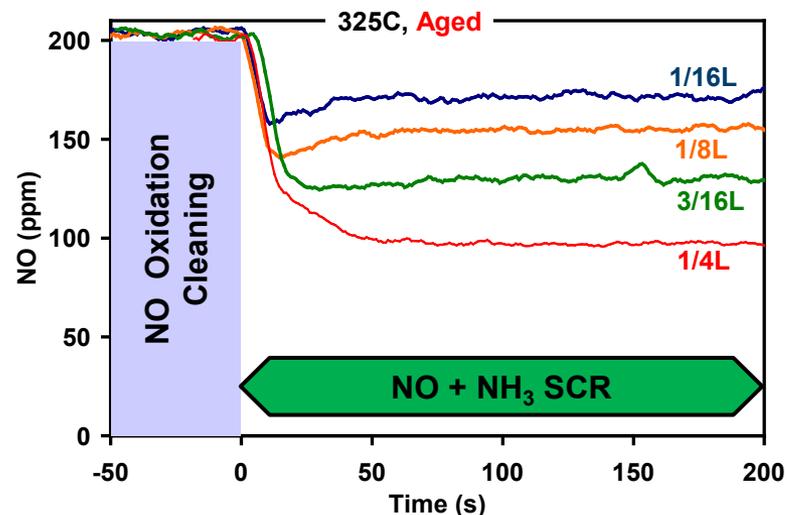
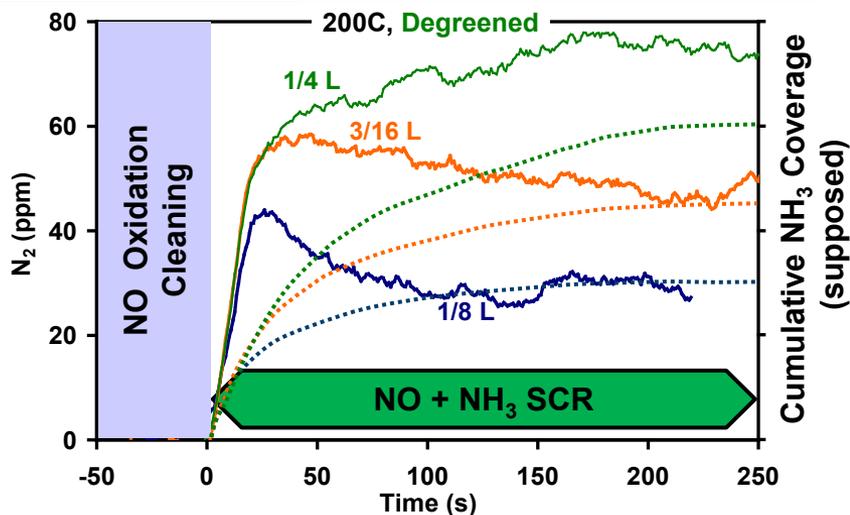
- DC plateaus after SCR zone
 - Because NH₃ is fully consumed
- DC & UC indicate catalyst use
 - DC/TC: fraction used for SCR
 - UC/TC: unused fraction of catalyst
 - **Can use for effluent analysis & catalyst control!**

Technical Progress: Hydrothermal Ageing Spreads SCR



- Same integral 100% conversion
- Negligible Parasitic NH₃ oxidation
- TC decreases w/ Hydrothermal Ageing
- Similar NH₃ capacity observation
 - **DC=TC in SCR zone**
- Slower SCR w/ ageing
 - More catalyst required
 - Consistent w/ active site loss
 - **Generally follows TC degradation**
 - **Suggests SCR dominated by available NH₃ coverage**

Technical Progress: Dynamic Inhibition when NH_3 is High



- Dynamic inhibition indicates threshold NH_3 coverage for inhibition onset
 - Conversion inflection indicates SCR slowing w/ continued NH_3 coverage buildup
 - NH_3 coverage continues to grow beyond inflection point
 - Occurs when coverage buildup is fast
 - i.e., when NH_3 (gas) concentration is high
 - Observable when at these points (usually within the catalyst)
- Can get to SS inhibited condition w/o passing through dynamic
 - Because low [NO] & slow (low) NH_3 coverage buildup
- Important for catalyst model & controls development
- Need improved temporal resolution of analytical methods

Collaborations & Coordination

- **Cummins**

- CRADA Partner, Neal Currier (Co-PI)



- **Prof. Louise Olsson,
Chalmers**

- SCR measurements & analysis (Xavier Auvray)
- Modeling steady state distributed SCR performance (Filipa Coelho)



- **Prof. Enrico Tronconi & Isabella Nova
Politecnico di Milano**

- Mechanistic investigation of selected SCR reactions
- Plan for 6-month ORNL visit in CY2012 (Maria Pia Ruggeri)



- **CLEERS**

- Diagnostics, analysis & modeling coordination



- **Prof Milos Marek & Dr. Petr Kočí,
Prague Institute of Chemical Technology**

- LNT modeling N₂O chemistry
- KONTAKT II Grant from Czech Republic Government
- Petr to ORNL April 17-20



- **Dissemination via Publications, Presentations and Patents**

- 10 Presentations & 1 Major Award in 2011

Future Work

2012 Work:

- Model instrument response for improved transient analysis
- Characterize spatiotemporal performance of Cummins commercial catalyst
 - NH_3 capacity utilization, Parasitic oxidation, inhibition, transient analysis
- Transient analysis of model & commercial catalyst
 - Evolution & instantaneous SCR conversion, NH_3 coverage (w/ Chalmers)
- Modeling steady state SCR conversion distributions (w/ Chalmers)
- Investigate mechanistic aspects of selected SCR reactions
 - Experimental & numerical, reported to CLEERS (w/ Politecnico di Milano)

2013 Work:

- Impact of conditions on spatiotemporal SCR performance
 - $\text{NH}_3:\text{NO}_x$, $\text{NO}:\text{NO}_2$, HC
- Extend SS distributed SCR model to include transient performance
- Demonstrate diagnostics for SCR-state characterization
- Correlate control relationships w/ performance parameters
 - Identify strategies for SCR-catalyst control & diagnostics

Summary

- CRADA approach effectively addresses major DOE & Cummins goals
 - Insights for better SCR understanding, models & control
 - Advanced diagnostics to elucidate the same
 - Enabling improved SCR **efficiency, cost and durability**
- Analytical methods improved to allow transient analysis (DC, TC & UC)
 - Further improvements planned for 2012
- New CRADA insights improve understanding of SCR performance & control
 - NH_3 coverage is saturated over SCR zone
 - DC & UC indicate portion of the catalyst Used & Unused for SCR
 - Dynamic NH_3 inhibition occurs at the catalyst front
 - Due to high NH_3 (gas) causing fast NH_3 coverage buildup rate
- Leveraging collaborations to strengthen CRADA & enhance value
 - Modeling distributed steady state SCR performance w/ Chalmers
 - Studying SCR reaction mechanisms w/ Politecnico di Milano (*cf. 2011 Review feedback*)
 - Improving analytical methods w/ CLEERS
- Future work focuses on:
 - Commercial Cummins SCR catalyst
 - Better transient analysis to elucidate dynamic performance of realistic drive cycles
 - Modeling transient SCR performance
 - Insights & diagnostics to demonstrate and enable advanced control strategies