

Hydrogen and Biogas Production using Microbial Electrolysis Cells

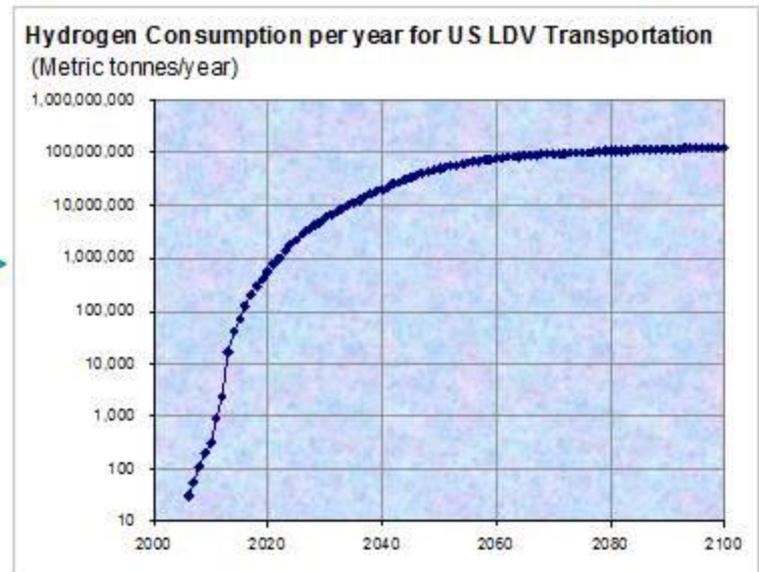
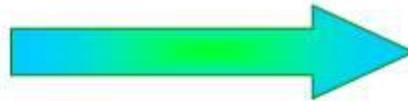
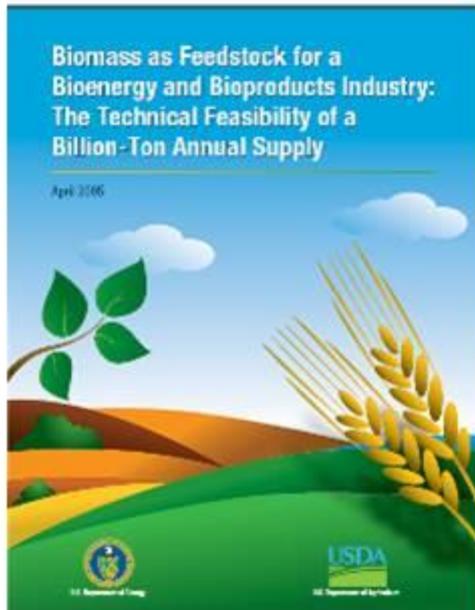
(Session 1-C) Biomass and Beyond:
Challenges and Opportunities for Advanced
Biofuels from Wet-Waste Feedstocks

Bruce E. Logan
Penn State University

Engineering Energy &
Environmental Institute

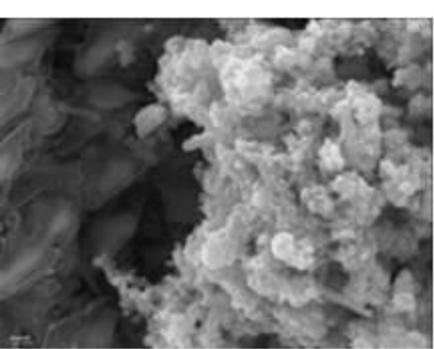


Cellulosic biomass → H_2

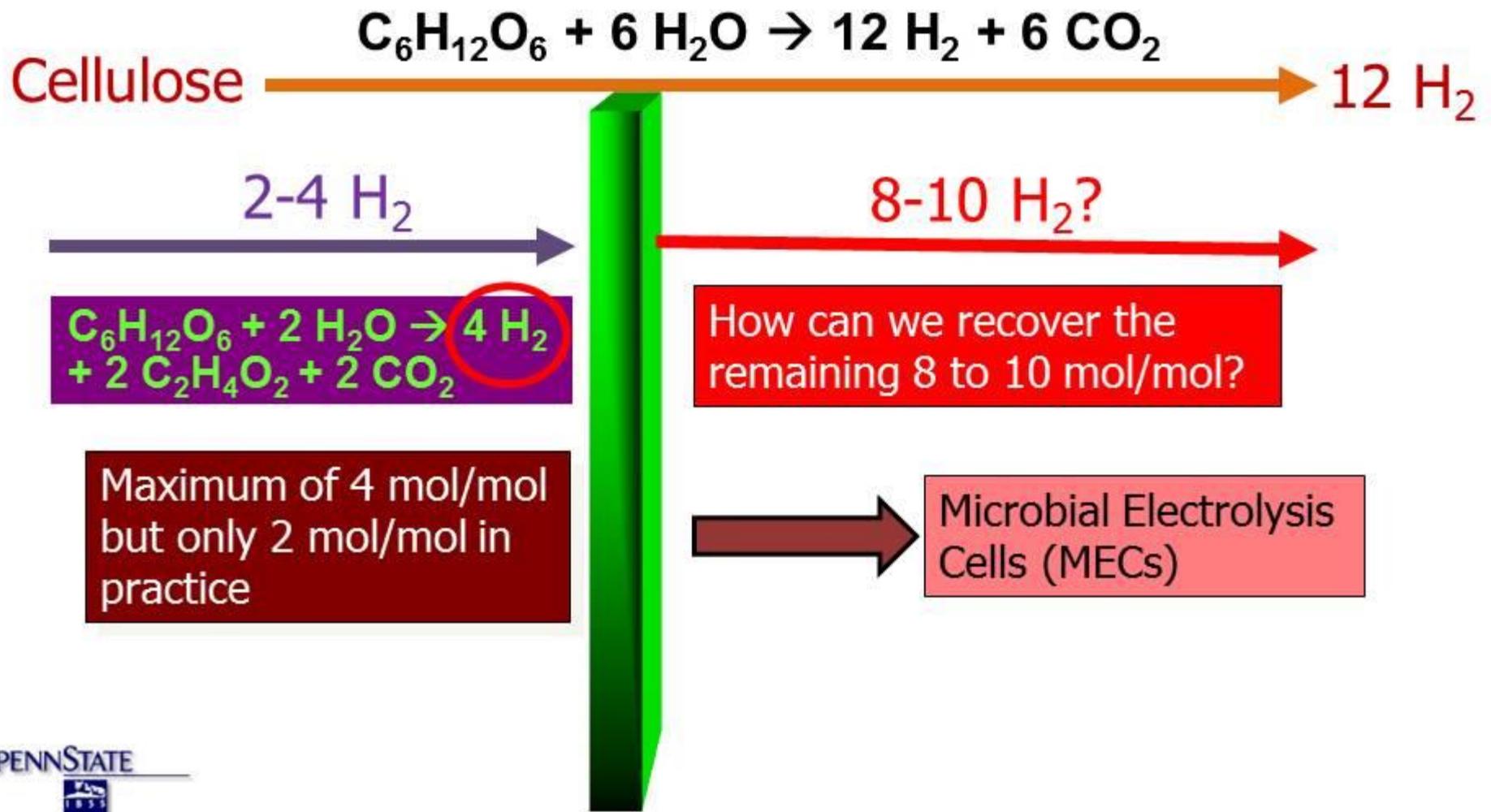


1.34 billion tons of cellulose/yr
= 2×10^{11} kg/yr H_2

Need 10^{11} kg/yr H_2
for transportation by
2060(light duty vehicles)



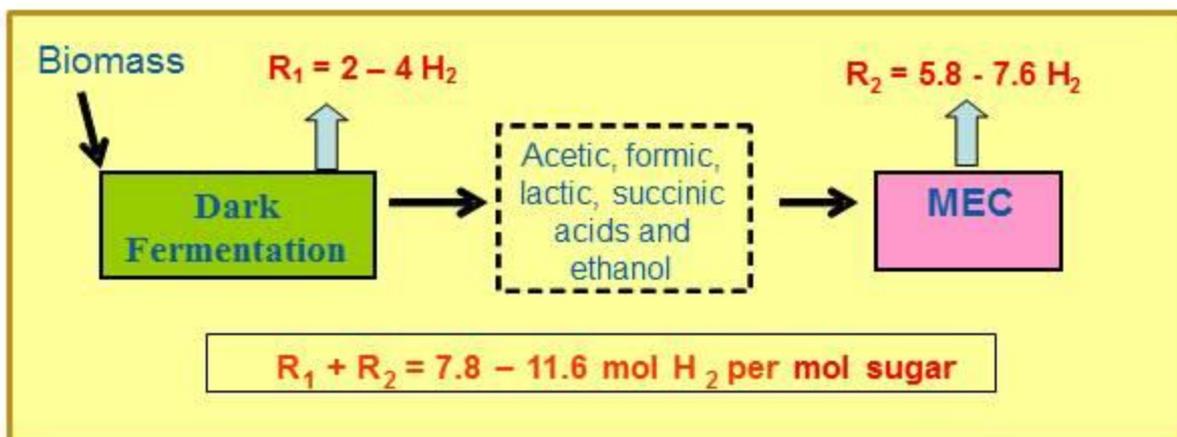
The cellulose "fermentation barrier"



Penn State project with NREL

2 stage process :

Convert renewable lignocellulosic biomass resources to H_2 using fermentation + MEC



Approach overcomes 2 key barriers to making H_2 from other biomass sources

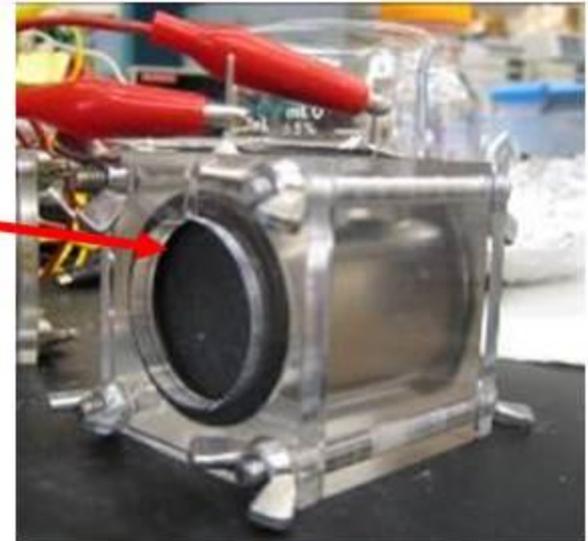
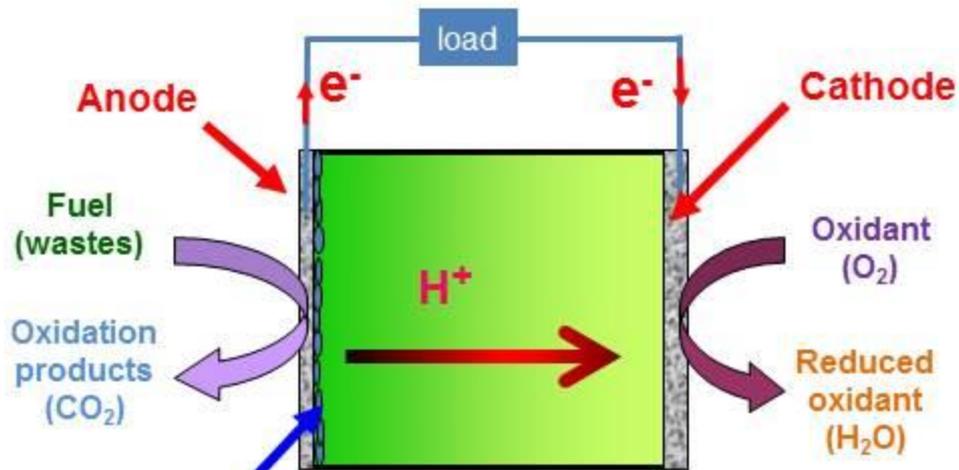
- Low feedstock cost of lignocellulose compared to corn/sugar
- Overcomes fermentation barrier:
 - Increases H_2 molar yield past 4 mol-hexose per mol- H_2 by using a microbial electrolysis cell (MEC)

Focus points

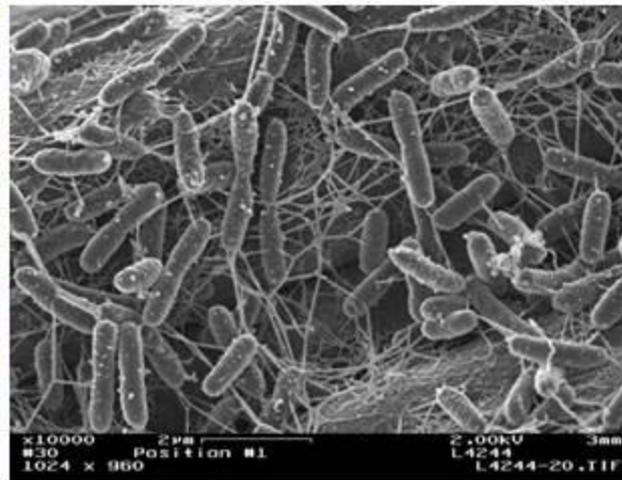
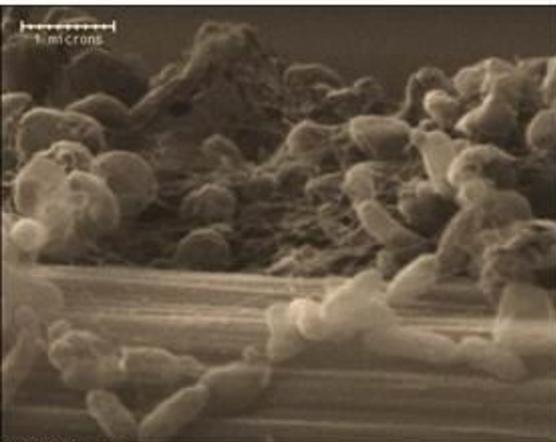
- Microbial electrolysis cells (MECs)
 - Electroactive microorganisms
- MECs for conversion of lignocellulose to H₂
- Avoiding the need for electricity in MECs

MFCs

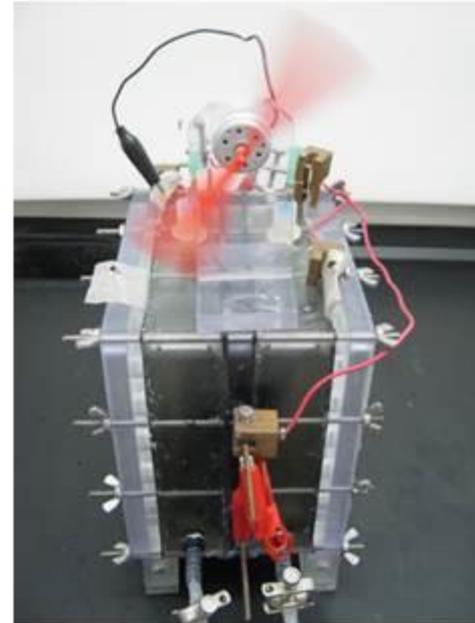
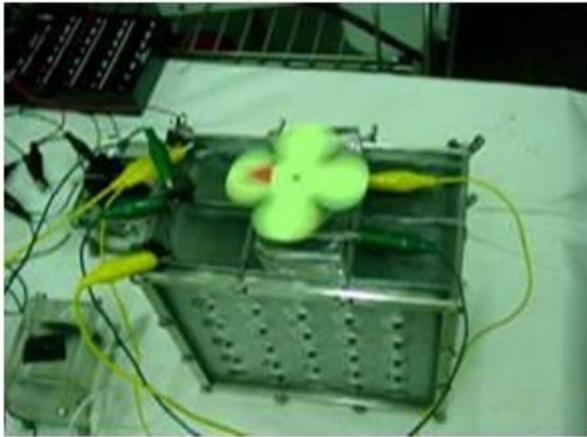
Electrical power generation in a **Microbial Fuel Cell (MFC)** using exoelectrogenic microorganisms



Bacteria that make electrical current



Demonstration of a Microbial Fuel Cell (MFC)

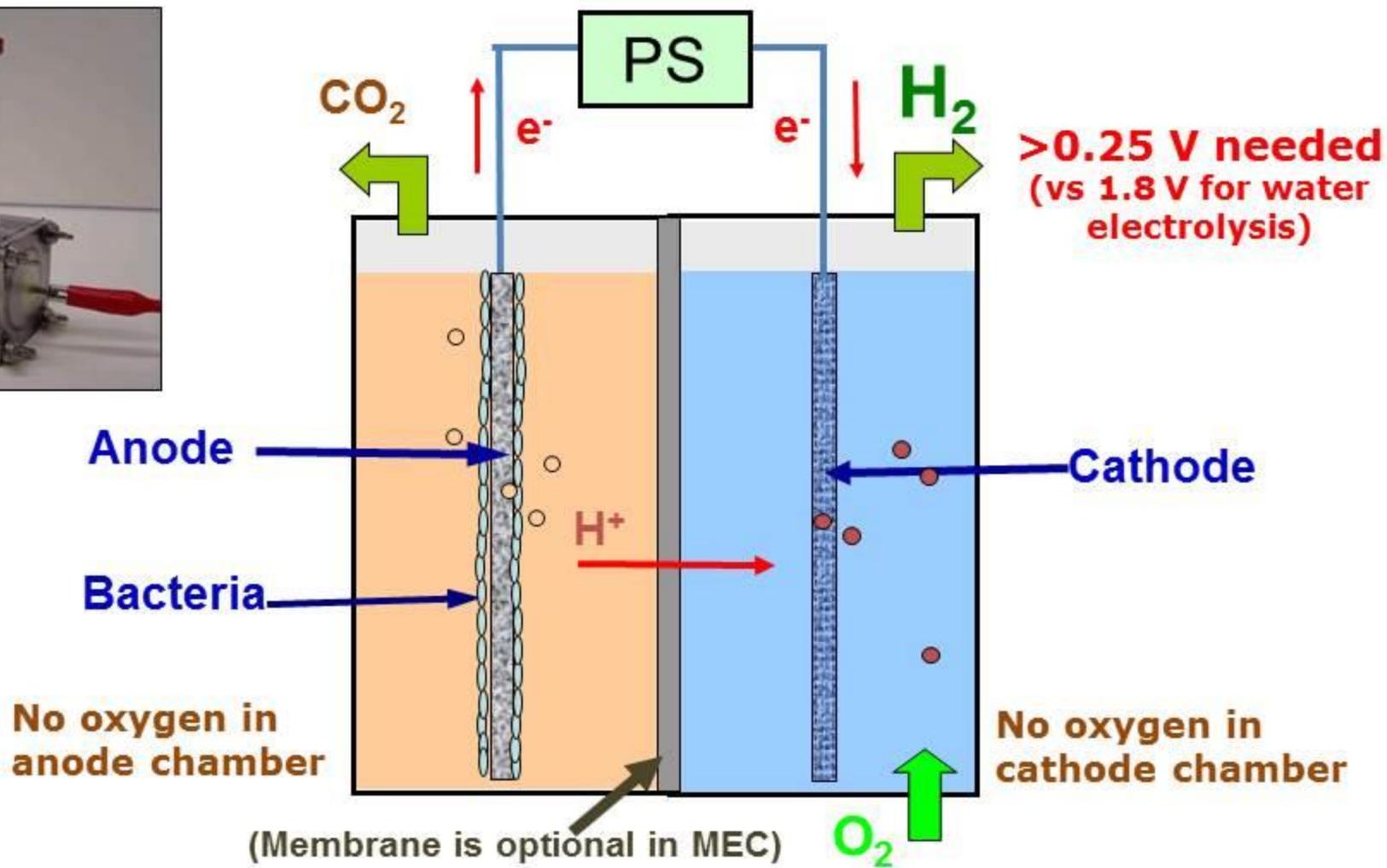


MFC webcam
(live video of an MFC running a fan)

www.engr.psu.edu/mfccam

MECs

H₂ Production at the cathode using microbes on the anode in **Microbial Electrolysis Cells**



H₂ production by MEC process:

Energy Yields

$$\eta_W = \frac{W_{H_2}}{W_{in}}$$

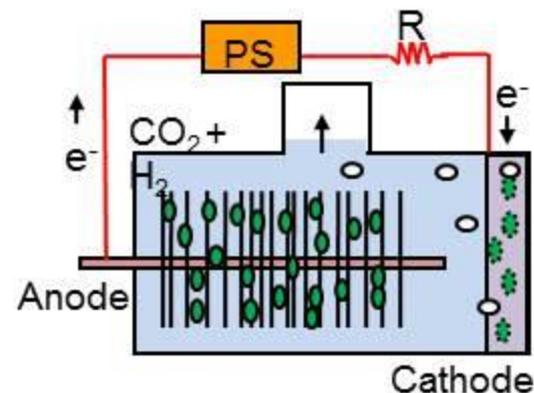
Energy in H₂ produced
—————
Energy in electricity required

200 – 400%

$$\eta_{W+S} = \frac{W_{H_2}}{W_{in} + W_s}$$

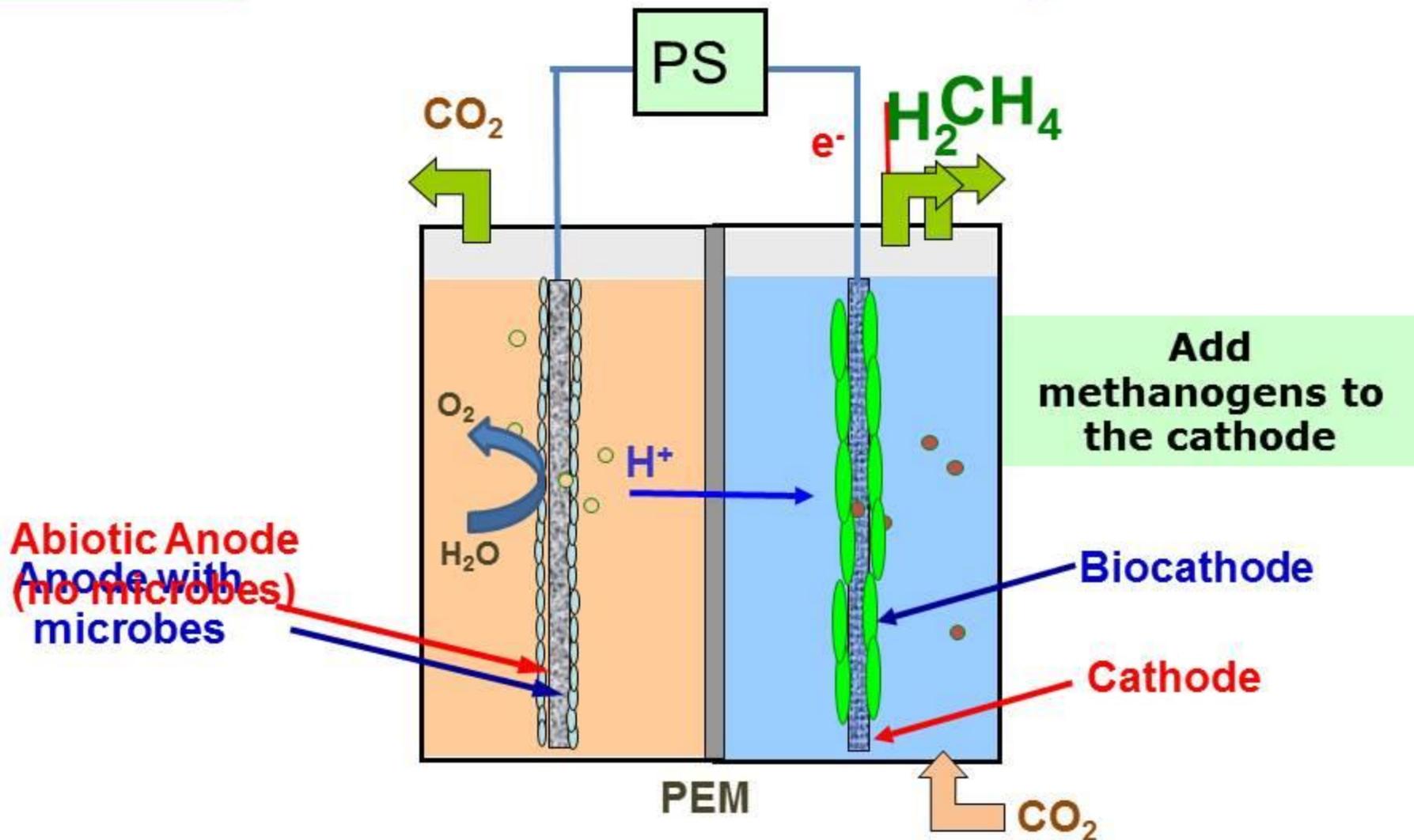
Energy in H₂ produced
—————
Energy in electricity + substrate

65 – 89%



MMCs

CH₄ Production at the cathode using microbes on the cathode in **Microbial Methanogenesis Cells**



MECs used to harvest methane from renewable forms of electricity generation

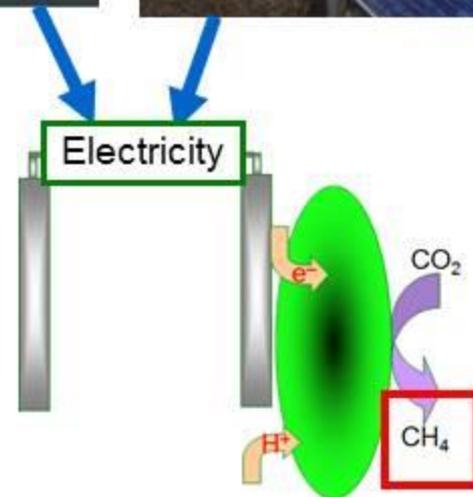
Anaerobic digesters

(methane from organic matter)



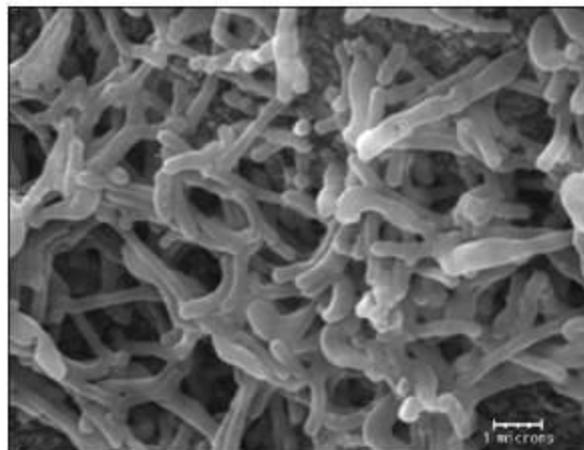
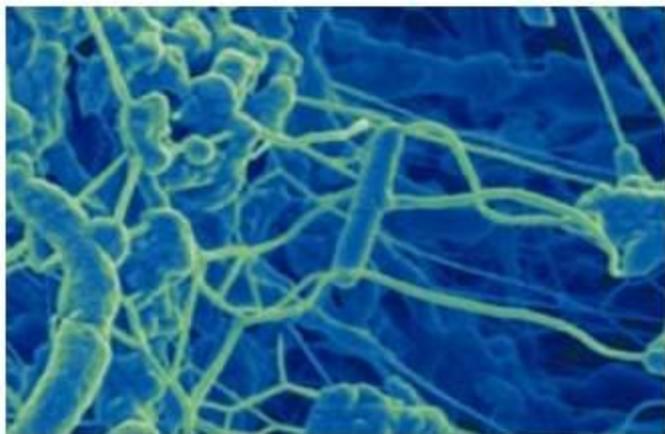
MMCs

Methane from renewable electricity



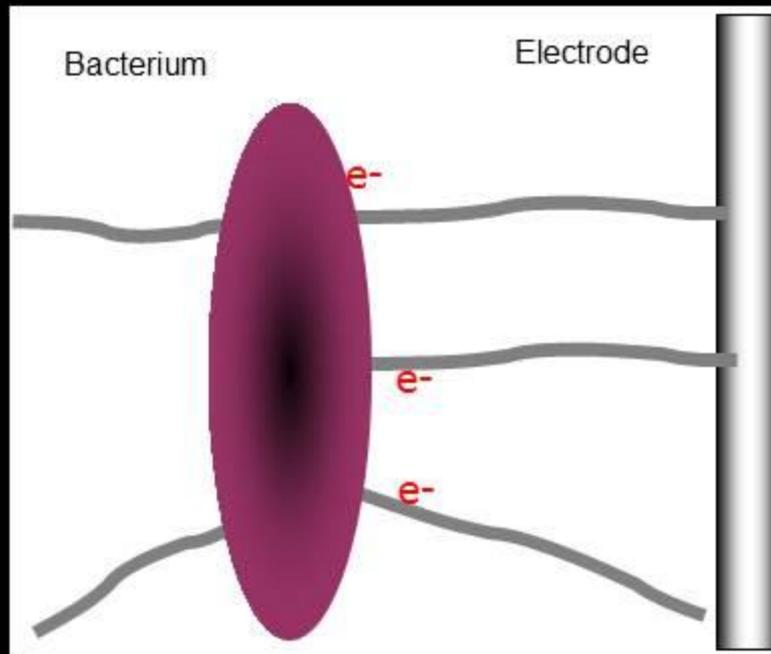
Electro-active Microorganisms

- Electromicrobiology
 - New sub-discipline of microbiology examining exocellular electron transfer



Mechanisms of electron transfer in the biofilm:

Nanowires produced by bacteria !



Gorby & 23 co-authors (2010) *PNAS*

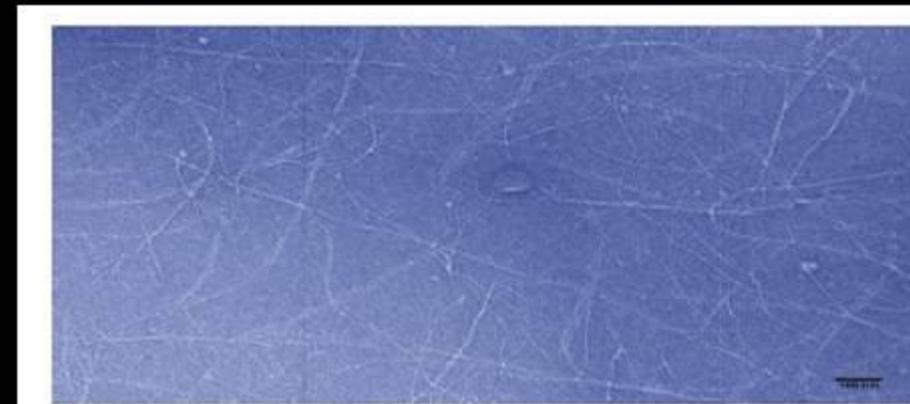
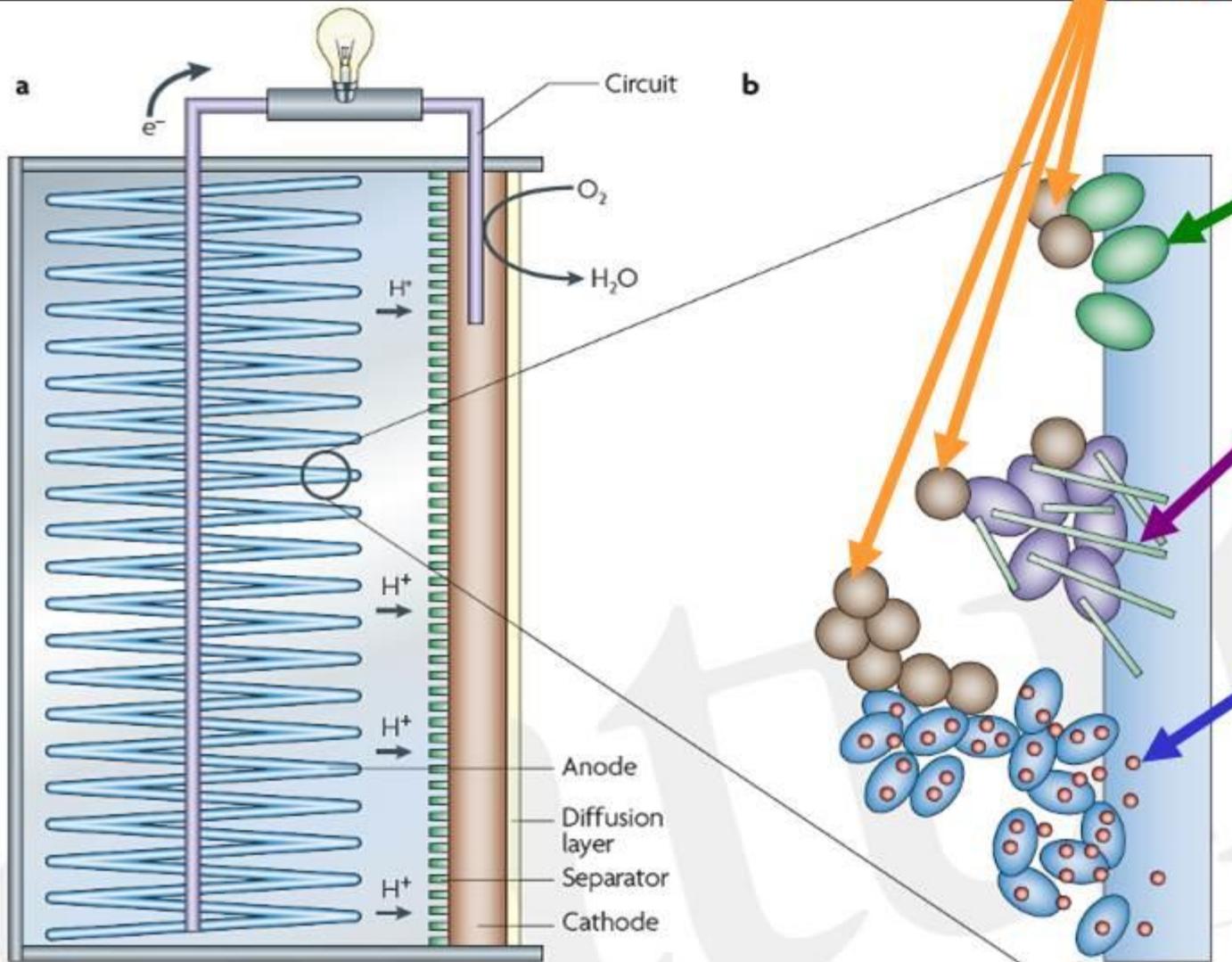


Figure 1. Colorized transmission electron micrograph of microbial nanowire networks secreted by *Geobacter sulfurreducens*. Scale bar, 100 nm.

Malvankar & Lovley (2012) *ChemSusChem*

Electrogenic biofilm ecology

Bacteria living off exoelectrogens



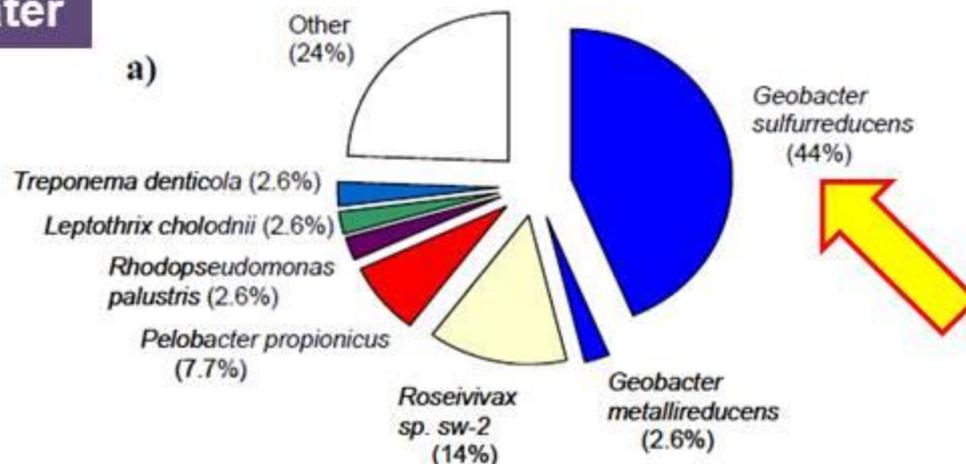
Direct contact

Produce nanowires (wired)

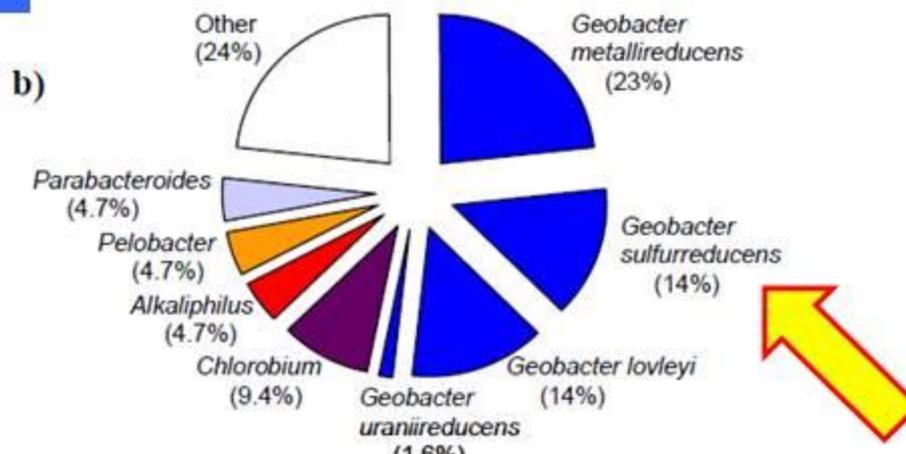
Produce mediators (wireless)

Bacteria on the anodes

Winery Wastewater

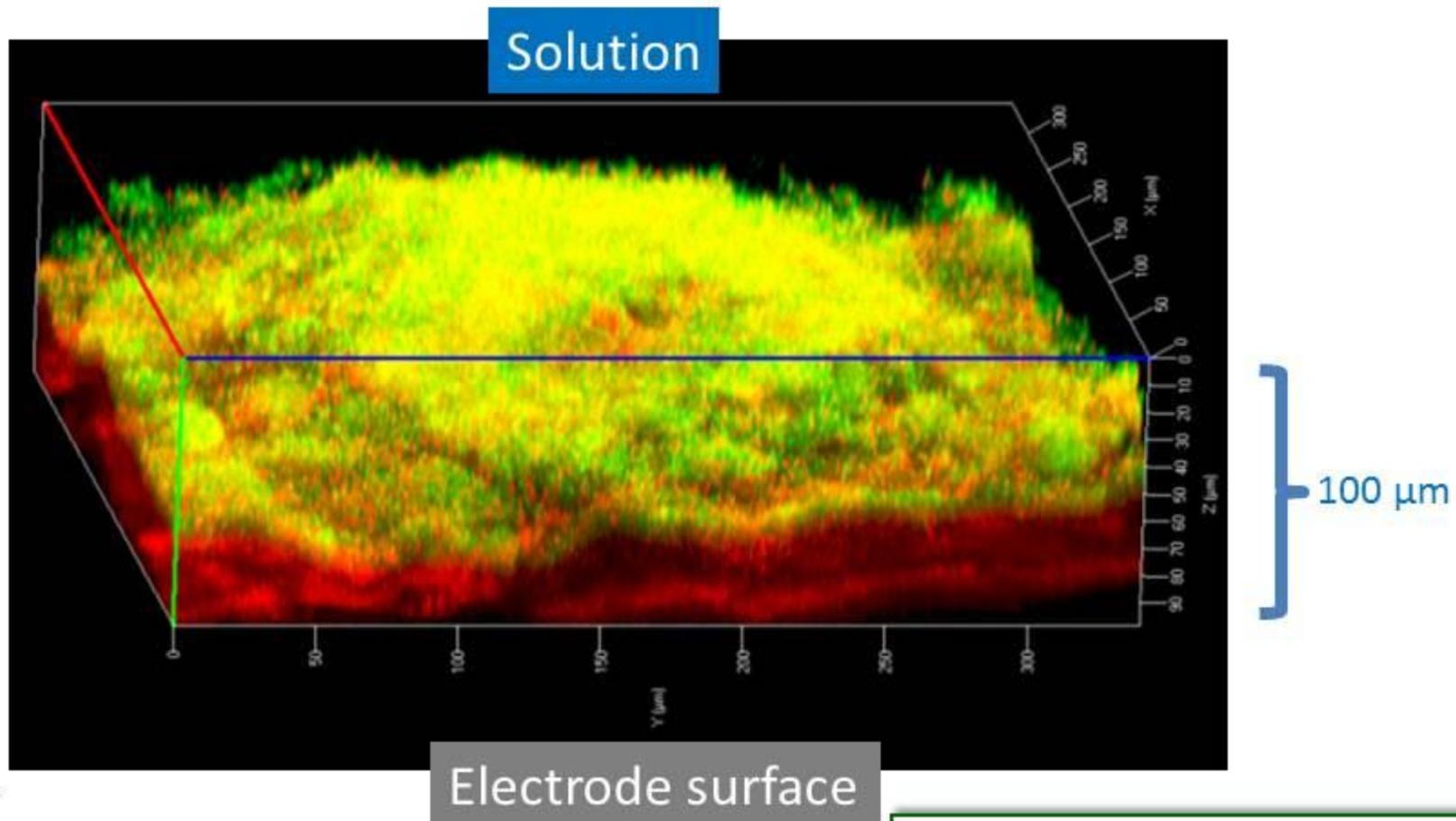


Domestic Wastewater



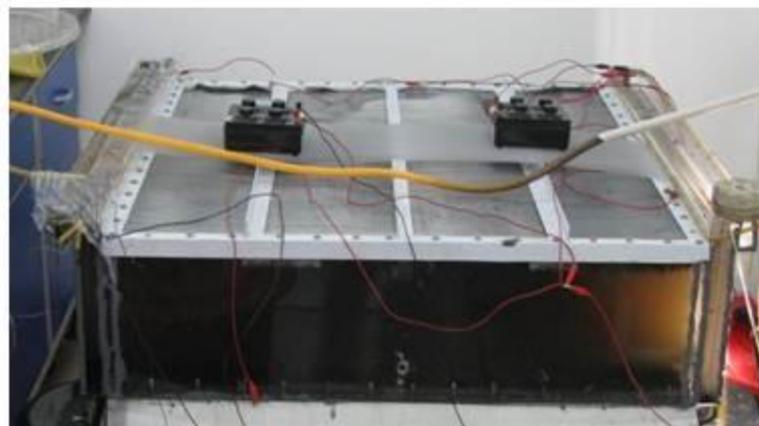
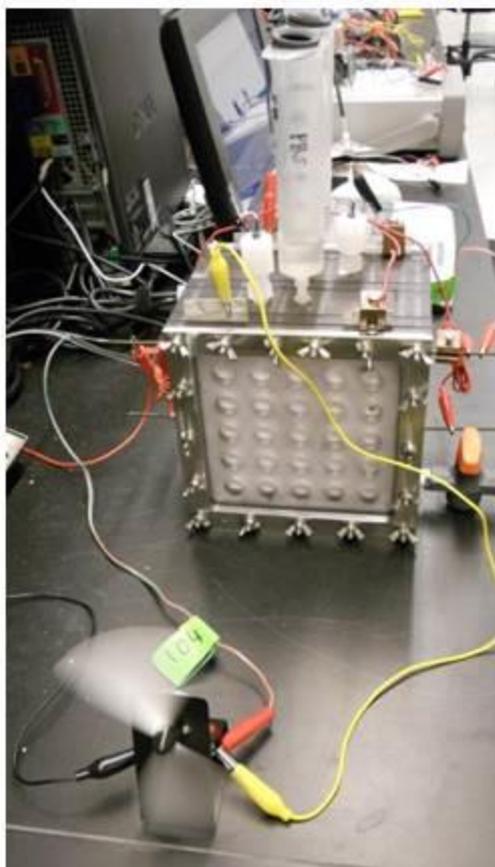
Electrogenic Biofilms

- **Dead biofilm (red)** remains electrically conductive for **active biofilm (yellow/green)**



Scaling up MFCs & MECs

MFCs= fuel cells, make electricity
MECs= electrolysis cells, make H₂



MxC Architecture

CHEMSUSCHEM



DOI: 10.1002/cssc.201100732

Bioelectrochemical Systems: An Outlook for Practical Applications

Tom H. J. A. Sleutels,^[a] Annemiek Ter Heijne,^{*[b]} Cees J. N. Buisman,^[a, b] and Hubertus V. M. Hamelers^[a, b]

Bioelectrochemical systems (BESs) hold great promise for sustainable production of energy and chemicals. This review addresses the factors that are essential for practical application of BESs. First, we compare benefits (value of products and cleaning of wastewater) with costs (capital and operational costs). Based on this, we analyze the maximum internal resistance (in $m\Omega m^2$) and current density that is required to make microbial fuel cells (MFCs) and hydrogen-producing microbial electrolysis cells (MECs) cost effective. We compare these maximum resis-

tances to reported internal resistances and current densities with special focus on cathodic resistances. Whereas the current densities of MFCs still need to be increased considerably (i.e., internal resistance needs to be decreased), MECs are closer to application as their current densities can be increased by increasing the applied voltage. For MFCs, the production of high-value products in combination with electricity production and wastewater treatment is a promising route.

Review



Towards practical implementation of bioelectrochemical wastewater treatment

René A. Rozendal^{1,2,3}, Hubertus V.M. Hamelers², Korneel Rabaey¹, Jurg Keller¹ and Cees J.N. Buisman^{2,3}

¹ Advanced Water Management Centre, The University of Queensland, St. Lucia, QLD 4072, Australia

² Sub-department of Environmental Technology, Wageningen University, Bomenweg 2, P.O. Box 8129, 6700 EV Wageningen, The Netherlands

³ Wetsus, Centre for Sustainable Water Technology, Agora 1, P.O. Box 1113, 8900 CC Leeuwarden, The Netherlands

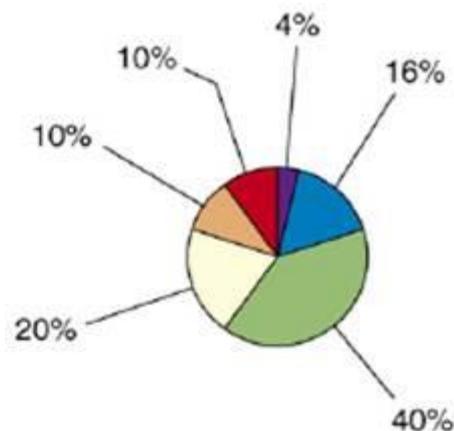
Estimates for MFCs

- 100 €/m² or \$130/m²

Estimates for MECs

- 100 €/m² or \$130/m²

(b) Future
(-0.4 €/kg COD)



Key:

- Anode
- Cathode
- Membrane
- Current collectors
- Reactor
- Other costs

MxC Materials

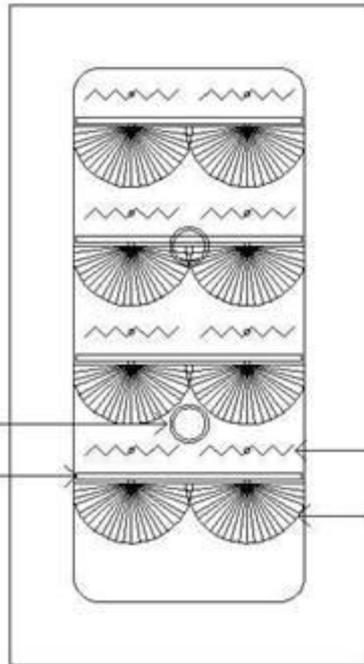
Anode: Graphite brush electrode

- Graphite fibers commercially available (used in tennis rackets, airplanes, etc.)
- Easy to manufacture
- Fiber diameter- 6-10 μm a good match to bacteria ($\sim 1 \mu\text{m}$)
- High surface area per volume-
Up to $15,000 \text{ m}^2/\text{m}^3$



MEC components (2.5 L reactor)

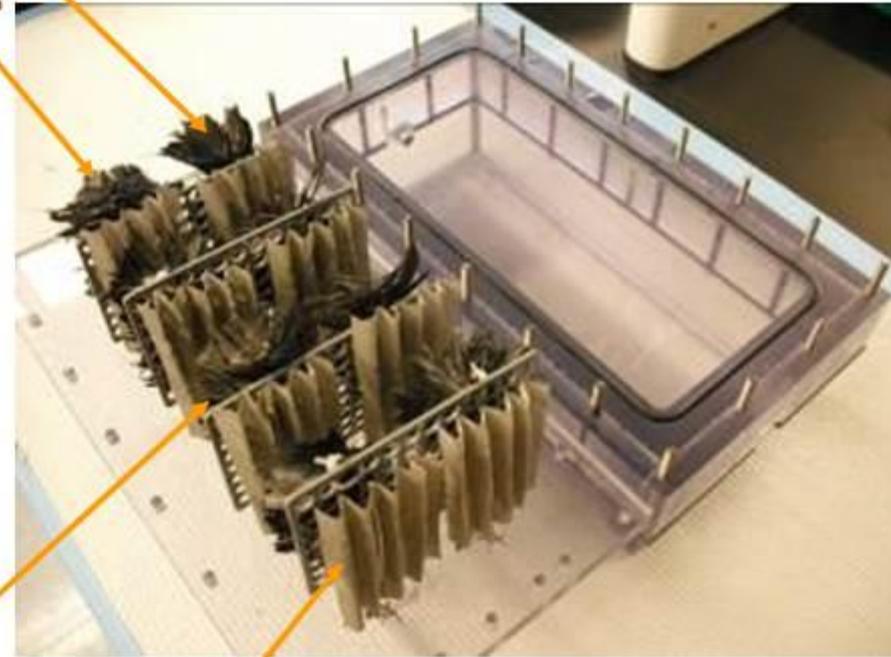
Schematic



anaerobic gas
collection tube
plastic
separator

stainless steel
mesh cathode
half graphite fiber
brush anode

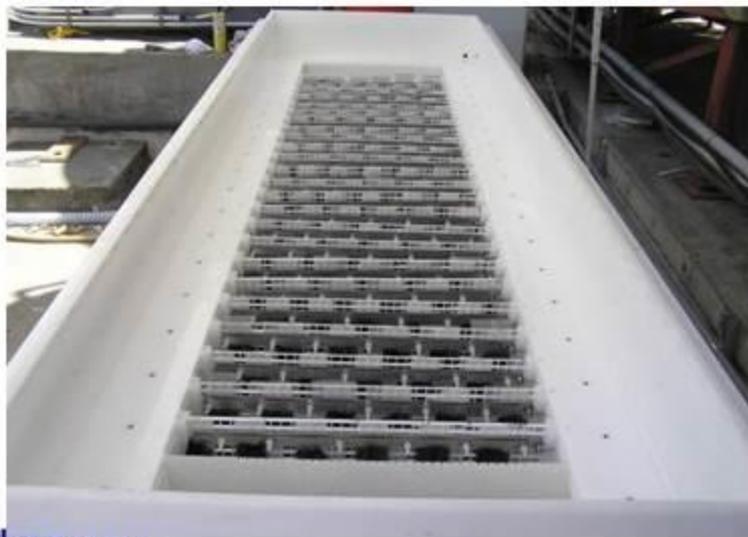
Half Graphite
Fiber Brush
Anodes



Plastic
Separator

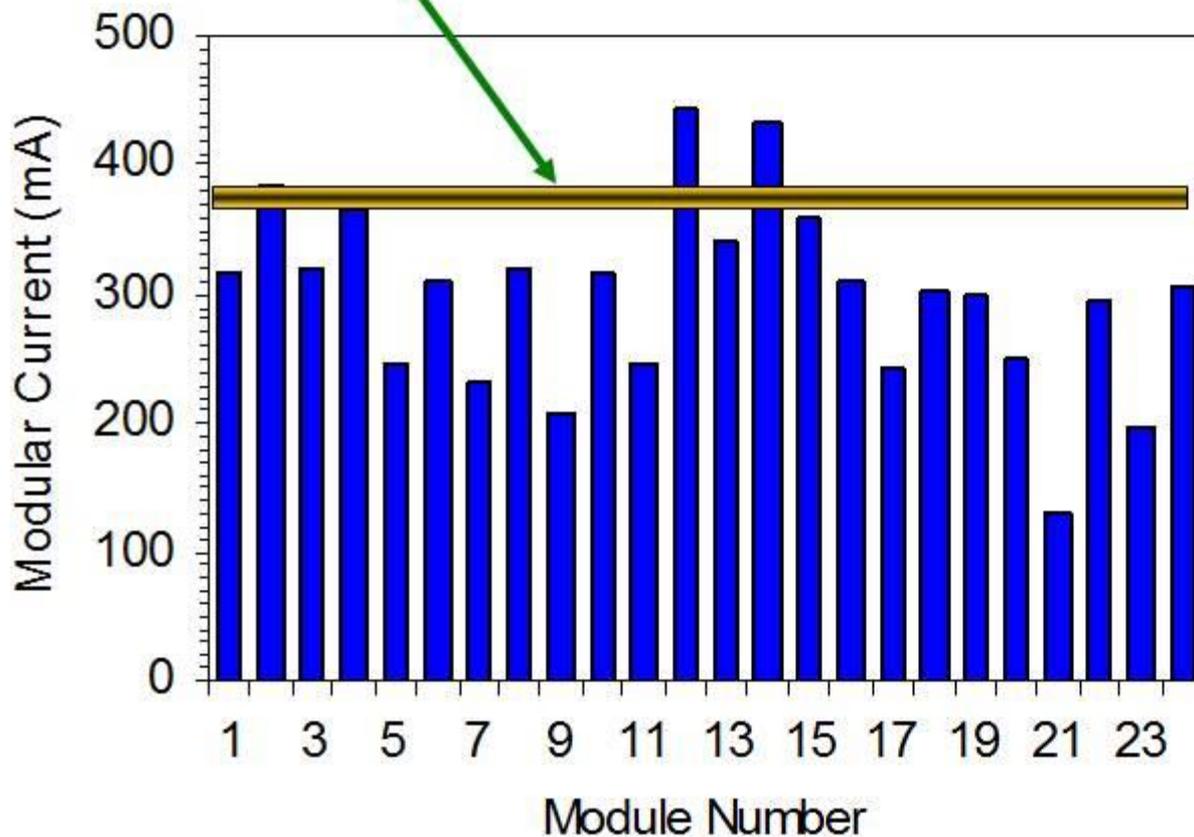
Stainless Steel
Mesh Cathodes

MEC Reactor that has 24 modules with a total of 144 electrode pairs (1000 L)



Individual module performance of the MEC treating Wastewater

Predicted: 380 mA/module (total of 9.2 A)

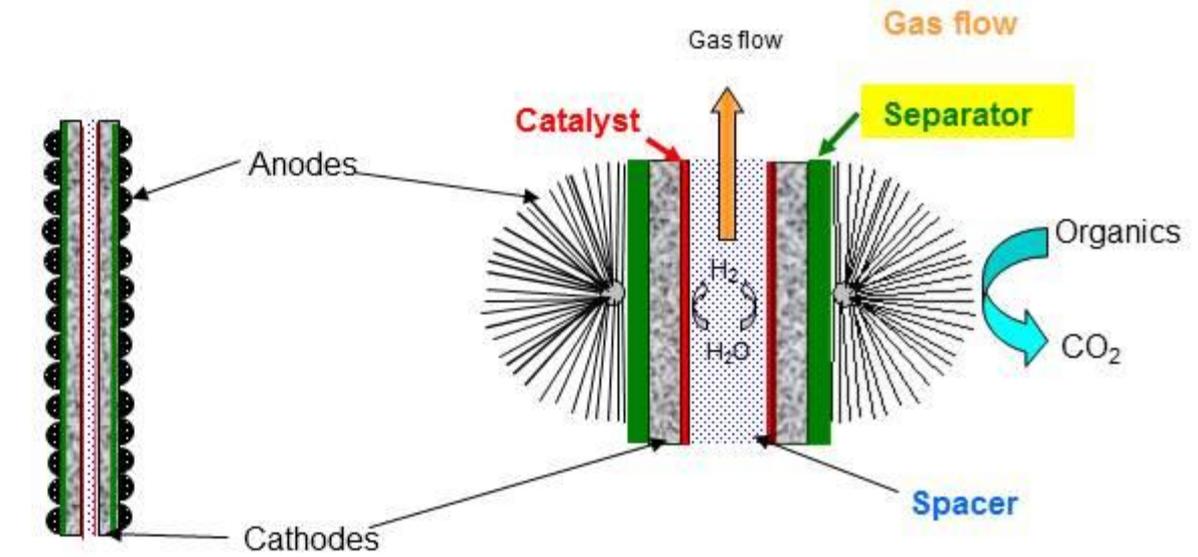
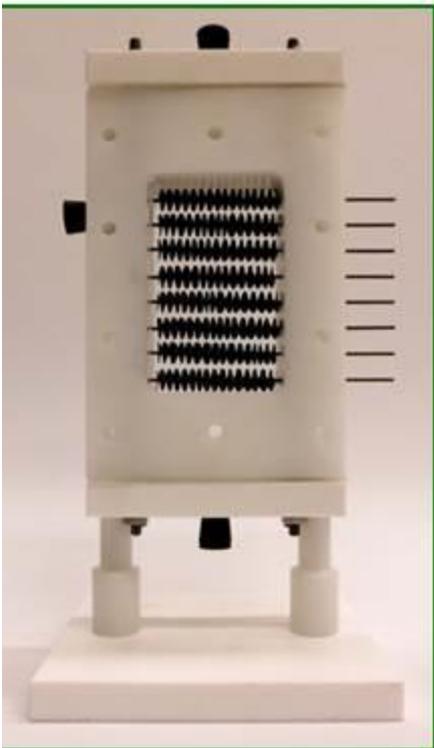
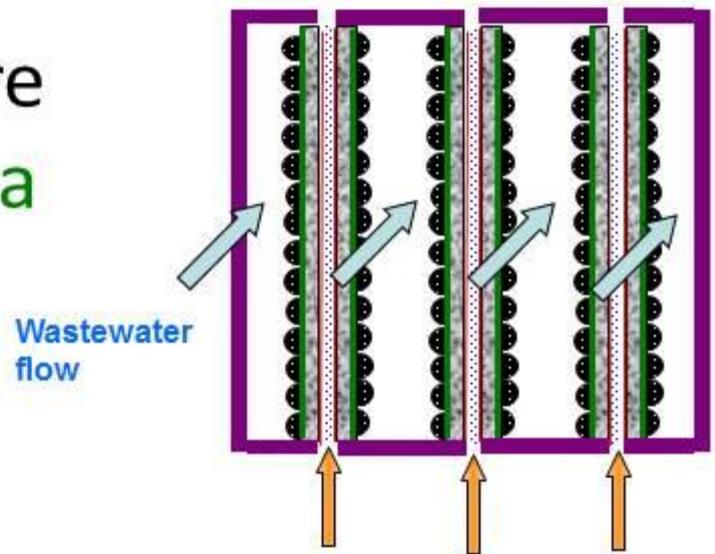


H₂ initially produced, but it all was converted to CH₄

Elec. Energy input = 6 W/m³
Energy Out = 99 W/m³

16× more energy recovered than electrical energy put into the process

NEW Module Design to capture H_2 from the cathode \rightarrow Needs a separator or membrane



Side View

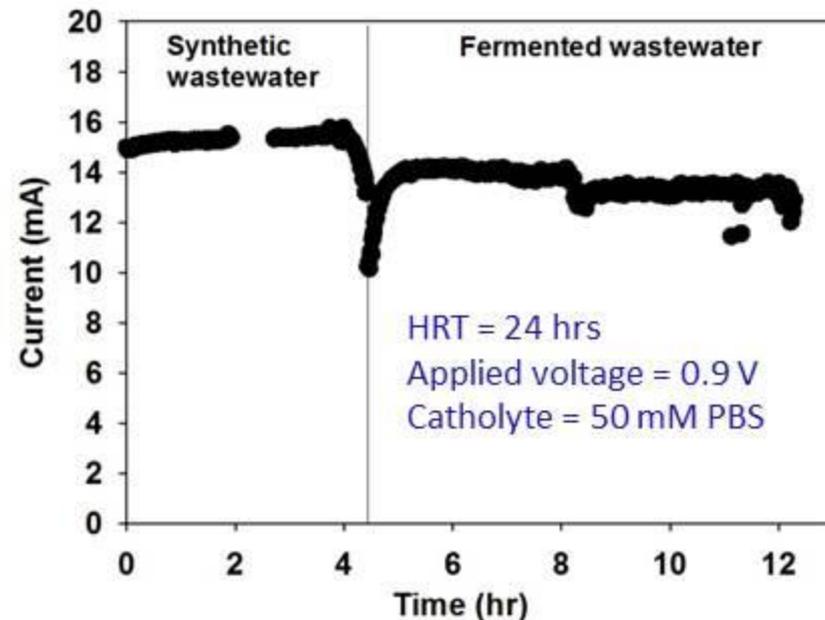
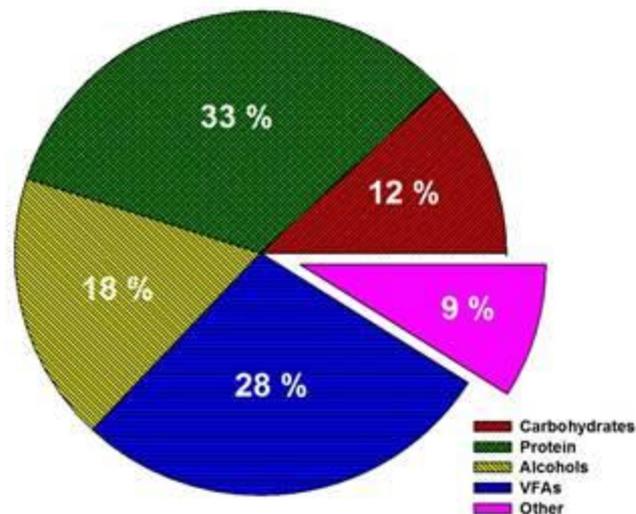
Close up view

Task 3.1 – Technical Accomplishments

Hydrogen Generation from Fermentation Wastewater



Fermentation Effluent Composition

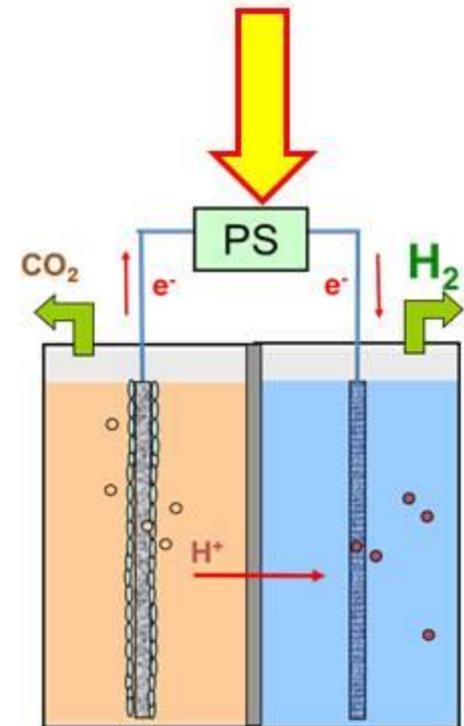


- **Current:** Synthetic ww = 51 A/m³; Fermented ww = 44 A/m³ (no protein in synthetic ww).
- **Gas production rates:** Synthetic, 0.6 L-H₂ L⁻¹ d⁻¹ ; Fermented, 0.5 L-H₂ L⁻¹ d⁻¹.
- **COD (chemical oxygen demand) removal:** Synthetic ww = 87%; Fermented ww = 73%.
 - Removals in fermented ww: Alcohols and VFAs >90%; Carbohydrates= 89 %, Protein= 48%.

Avoiding the need for electricity (PS)

Use waste heat as an “energy source” for MECs rather than a power source (PS). *Two options being examined*

- **1: Thermal regenerative ammonia batteries** (new, not tested)
 - Waste heat used to produce ammonia, which is the “fuel” in a metal-salt solution battery
- **2: Reverse electrodialysis (RED) stacks incorporated into the MEC** (works!)
 - RED stacks can produce electricity from salinity gradient energy (SGE)
 - Both natural and engineered salinity gradients can be used.

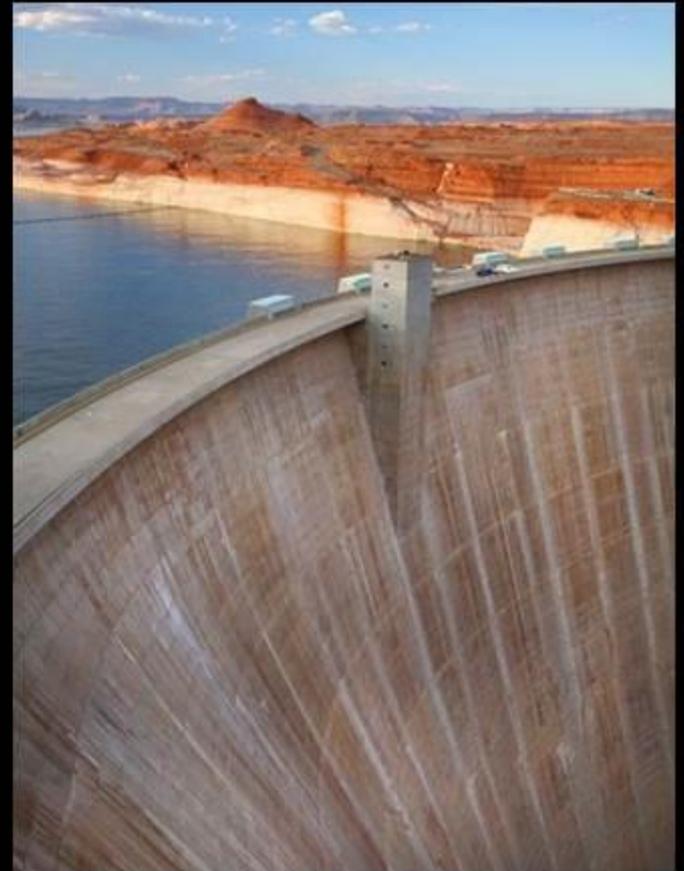


Natural Salinity Gradient Energy (SGE)



+

=



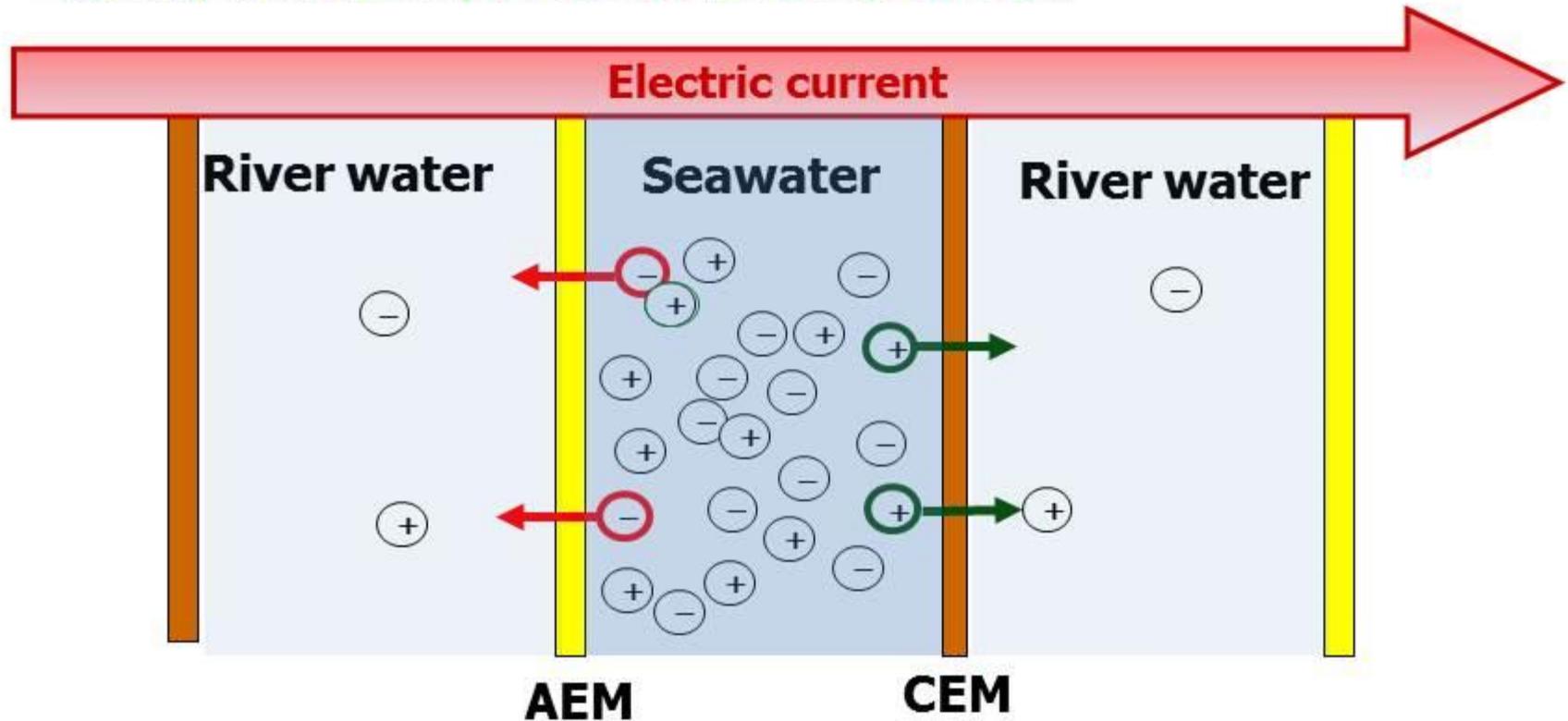
270 m of
Hydraulic Head



Oceanside WWTPs and
Rivers could produce
980 GW

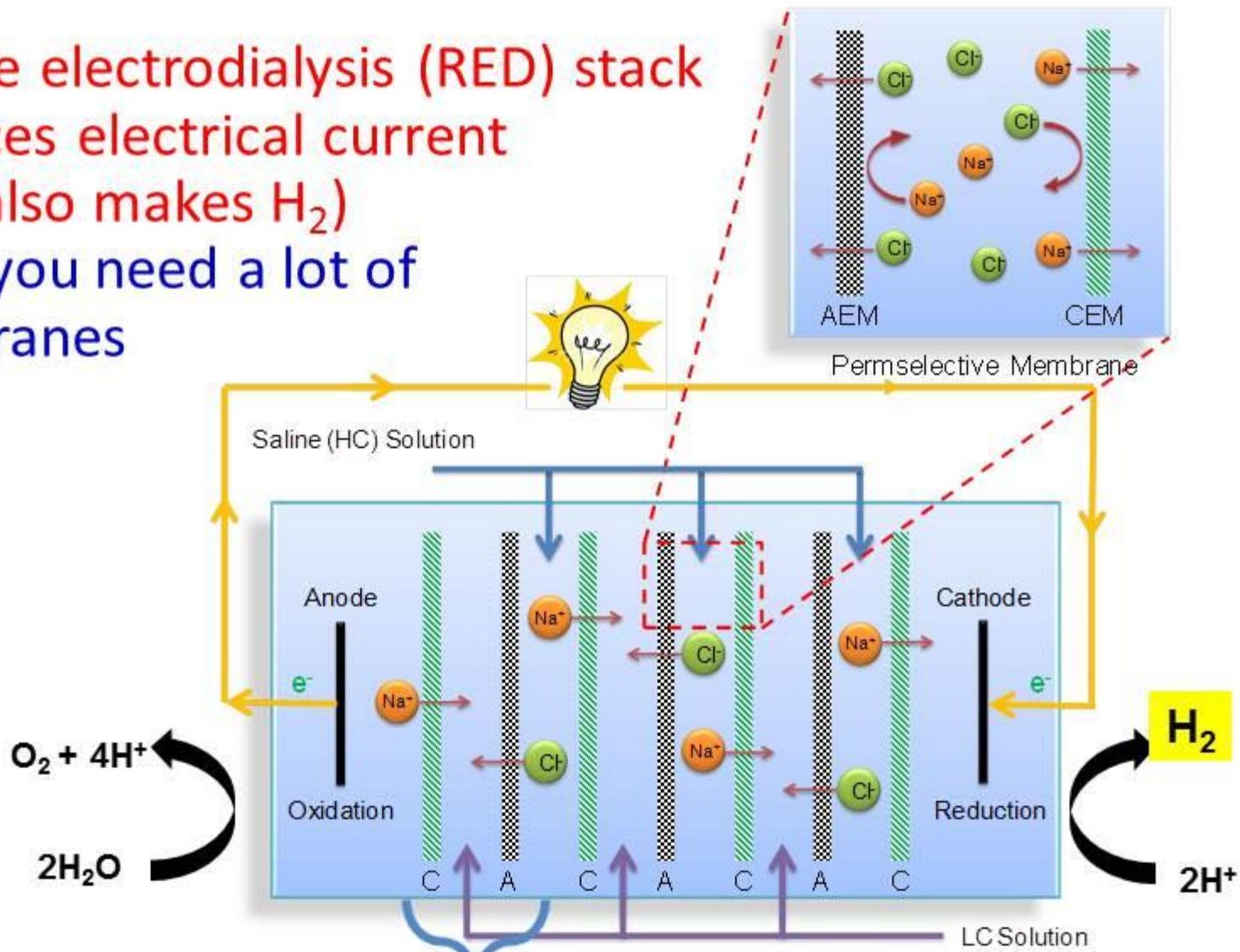
Reverse electrodialysis (RED)

Salinity difference **produces** electrical current



Each pair of seawater + river water cells \rightarrow **$\sim 0.1 - 0.2$ V**

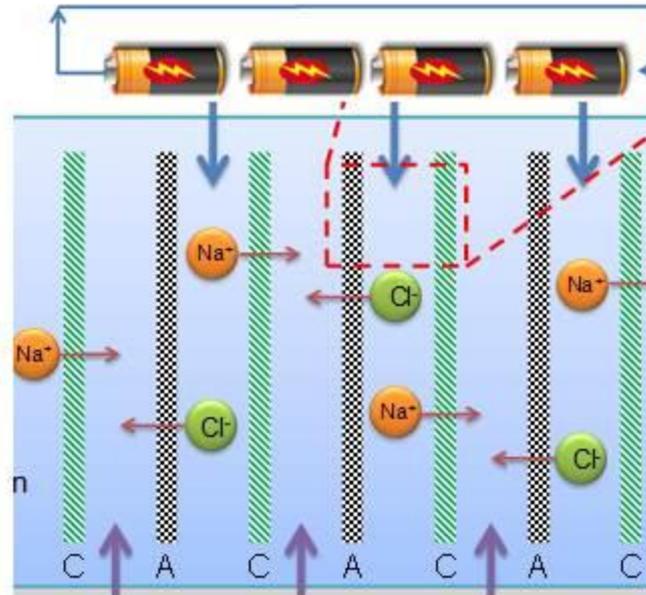
Reverse electrodialysis (RED) stack produces electrical current (here also makes H₂)
 ... but you need a lot of membranes



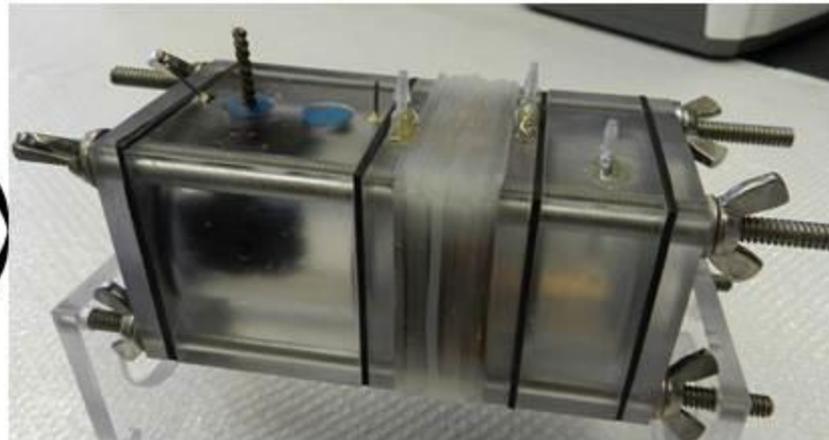
Each pair of high salt (HC) + low salt (LC) cells = **~0.1 – 0.2 V**



What if we move the RED stack into an MFC?

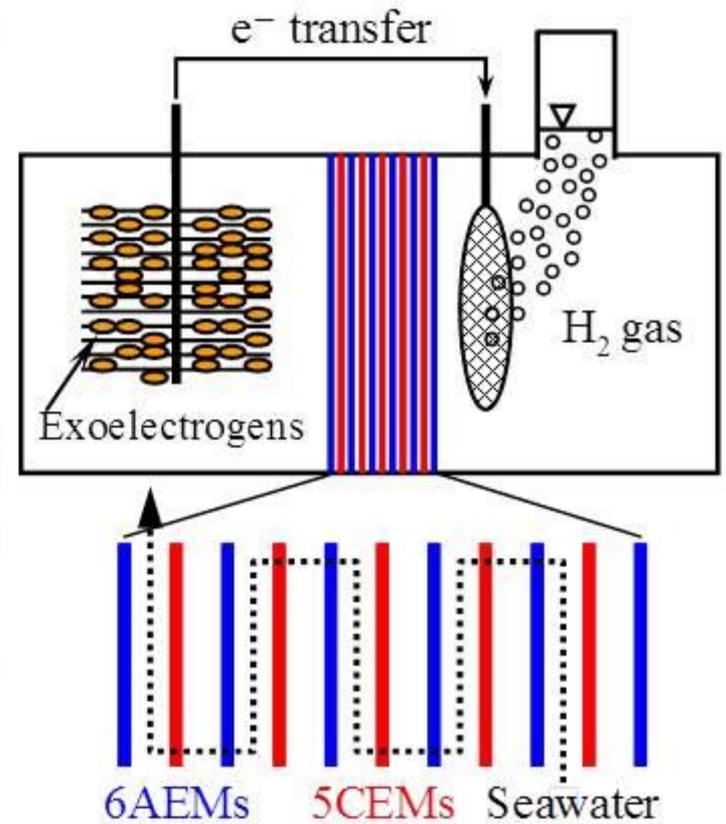
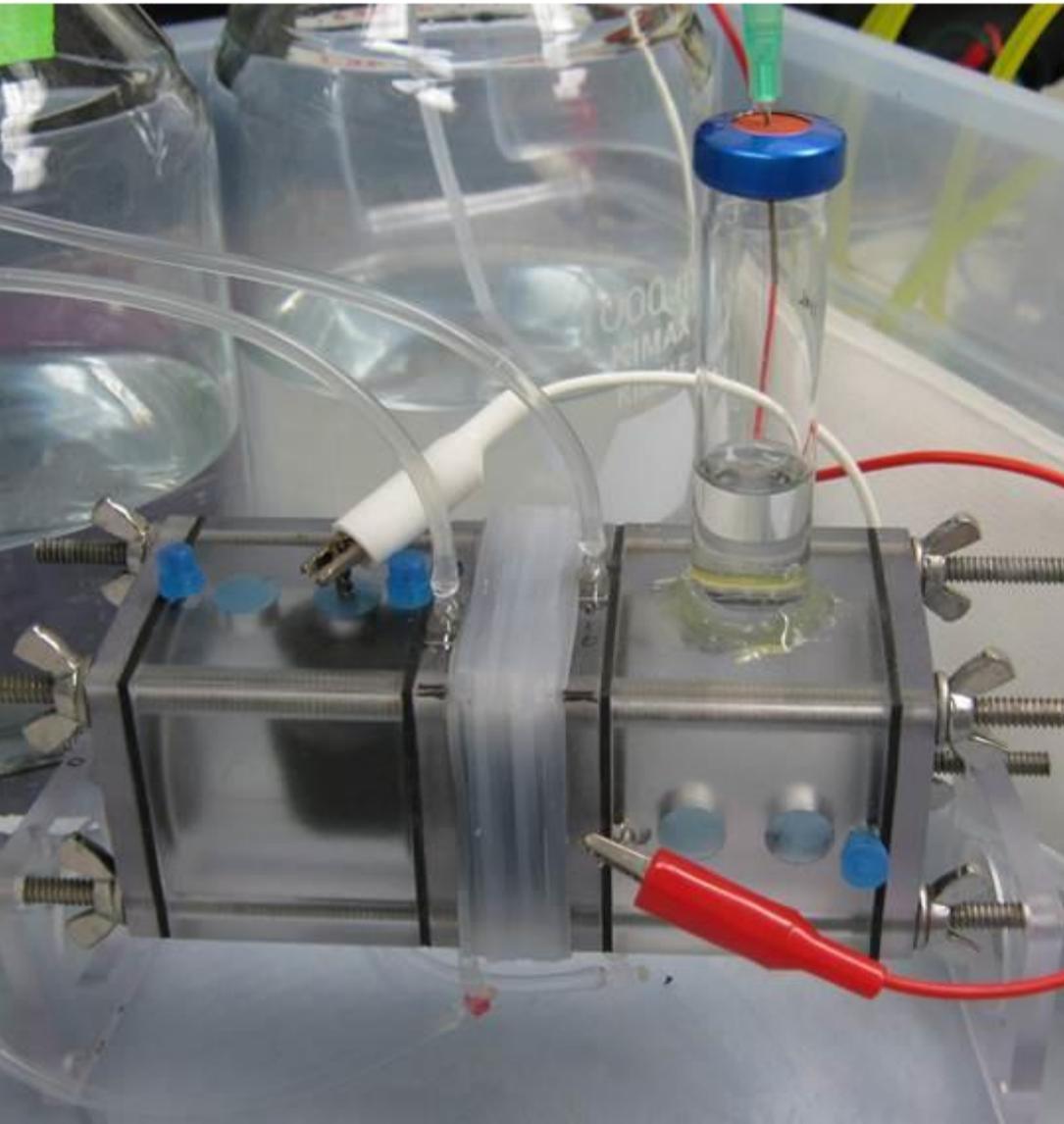


Organic matter
 CO_2 & H^+

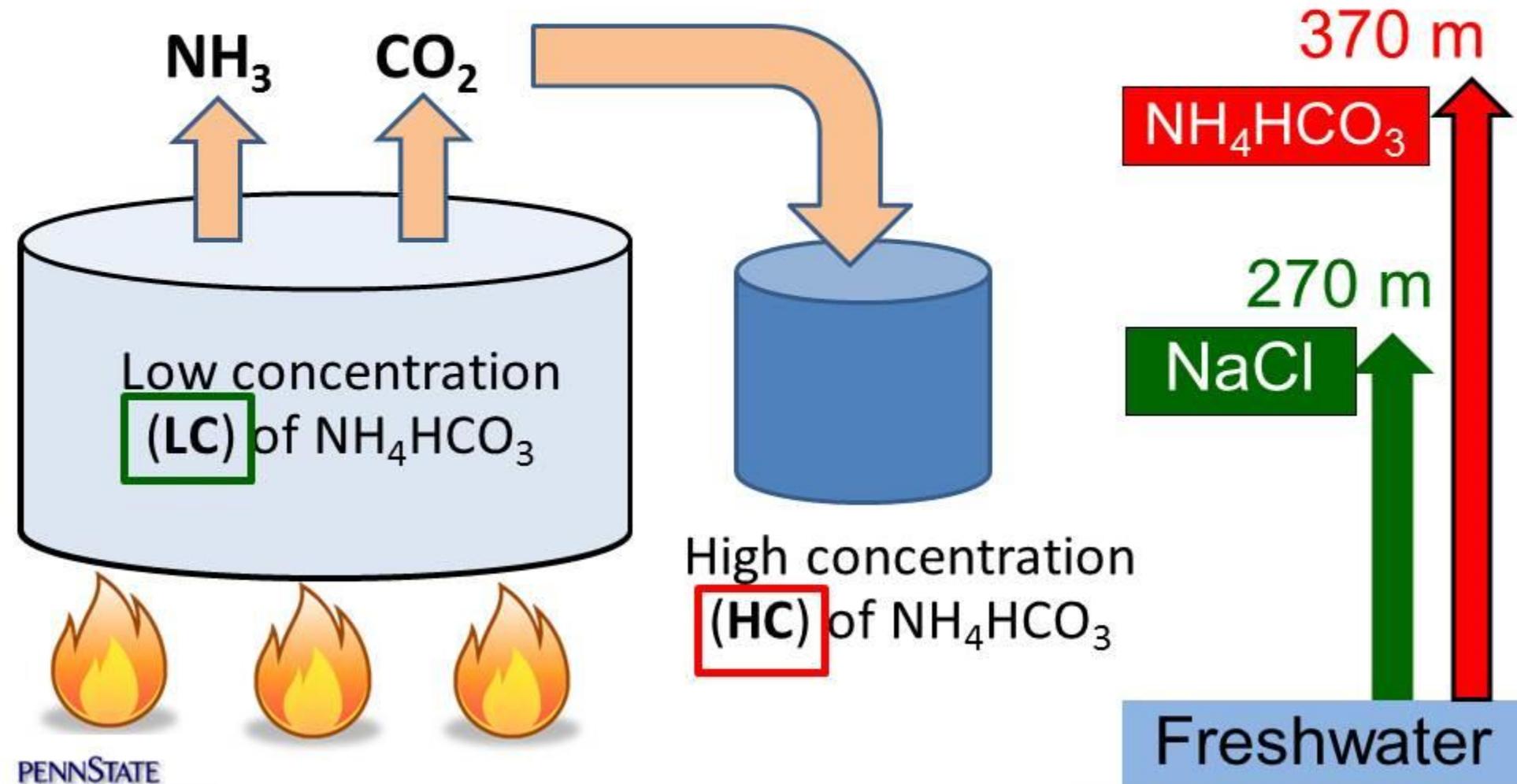


$\text{O}_2 + 4\text{H}^+$
 $2\text{H}_2\text{O}$

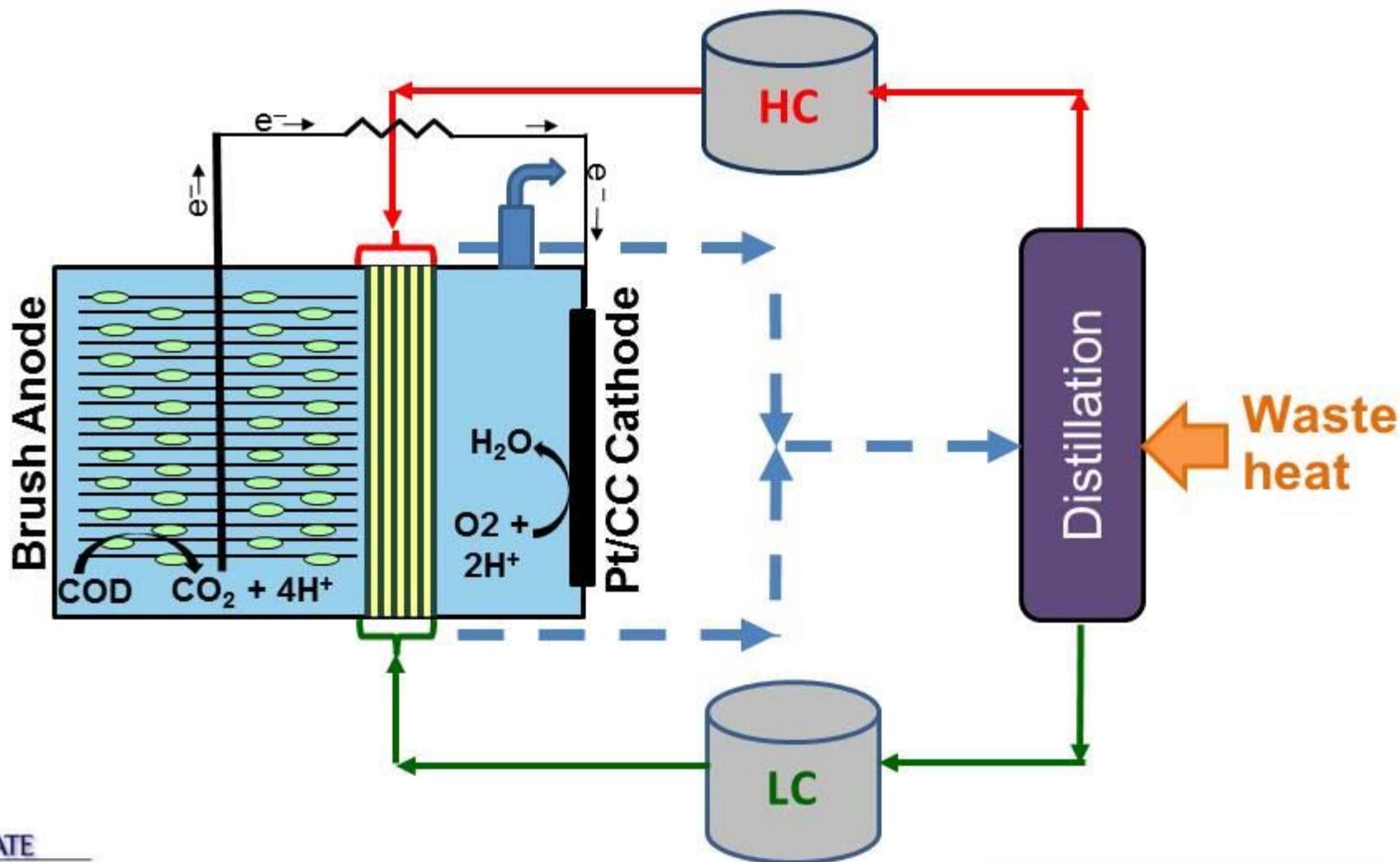
MEC + RED = MREC (Microbial RED Elec. Cell)



Engineered SGE: Use waste heat to create artificial “salinity gradient” energy using ammonium bicarbonate



MRFC Using Ammonium Bicarbonate



Challenges & Opportunities

- Challenges- Big picture

- Renewable H₂ production at high yields possible from lignocellulose
- Microbial electrolysis cells have not been widely recognized as a method for H₂ production

- Challenges-Technical

- Reactions at electrodes/materials/kinetics need to be improved (but without use of any precious metals)
- Rates of H₂ production need to be increased
- Cost of membranes will be a key factor in overall economics
- Use of osmotic/heat energy systems needs to be further explored

- Opportunities

- H₂ production is carbon neutral (CO₂ in plants is fixed and not fossil)
- Incentives for “green” H₂ production could speed development and applications.

Conclusions

- New **green/renewable** energy technologies can be created using electro-active microorganisms in different microbial electrochemical technologies:
 - MFCs= Electrical power
 - MECs= H₂ or CH₄ gases
- MECs can be combined with **Blue energy** technologies based on salinity gradient and waste heat energy sources
 - TRABs- thermal regenerable ammonia batteries using waste heat
 - MRECs = RED stacks incorporated into MECs

Thanks to students and researchers
in the MxC team at Penn State!



Current research sponsors

SERDP/DOD (2012-2015); GCEP/Stanford (2012-2015); NREL/DOE (2014-2017); NSF SusChem-EAGER (2015-2016)

International Collaborations



جامعة الملك عبد الله
للعلوم والتقنية
King Abdullah University of
Science and Technology

Water Desalination and
Reuse Center



STANFORD
UNIVERSITY



DeTao Masters Academy

