



May 8th 2011
AMFC Workshop



2011 AMFC WORKSHOP

Electrolyte Materials for AMFCs and AMFC Performance

May 8th 2011
Tokuyama Corporation
Kenji Fukuta



Location of Tokuyama Corporation

Total area 1,910,000 m²

Policrystalline Silicon

Inorganics

Public Wharf

Undersea tunnel

Nanyo Plant (cement)

280,000 m²

610,000 m²

Tokuyama Plant (inorganic)

Organics & Polymers

AIN Ceramics High thermal conductivity

The image is an aerial photograph of the Tokuyama Corporation industrial complex, outlined in yellow. It features several callout boxes with images and text. The 'Policrystalline Silicon' callout shows circular silicon wafers. The 'Inorganics' callout shows a large industrial pipe and a bag of material. The 'Organics & Polymers' callout shows various plastic and polymer products. The 'AIN Ceramics' callout shows white ceramic rings and plates. The 'Tokuyama Plant (inorganic)' callout is a large area outlined in yellow. The 'Nanyo Plant (cement)' callout is another outlined area. The 'Public Wharf' and 'Undersea tunnel' callouts are also present. The total area of the complex is noted as 1,910,000 m². The 'AIN Ceramics' callout also notes 'High thermal conductivity'.



Application of Hydrocarbon IEM



Food And Pharmaceutical

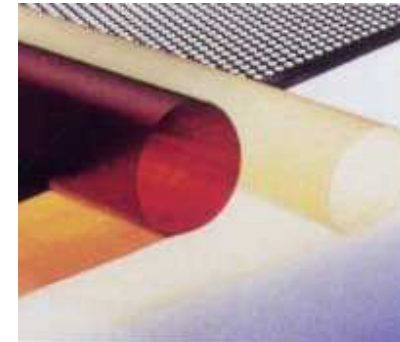
- * Demineralization of Cheese Whey
- * Demineralization of Organic Acids and Amino Acids
- * Desalination of Soy-Sauce
- * Stabilization of Wine
- * Demineralization and Purification of Pharmaceutical Intermediate



Electrodialyzers **ACILYZER**

Electronics

- * Production of High Purity Chemicals
- * Production of Ultra Pure Water
- * Battery Diaphragm



Ion exchange Membrane **NEOSEPTA**

NEOSEPTA®

EDCORE

NEOSEPTA®BIPOLAR

ACILYZER

Environmental Conservation

- * Desalination of Leachate
- * Removal of Nitrate from Under-Ground Water

Others

- * Production of Salt from Sea water
- * Production of Drinking Water from Brackish Water
- * Desalination of Deep Sea Water
- * Acid Recovery from Waste Acid



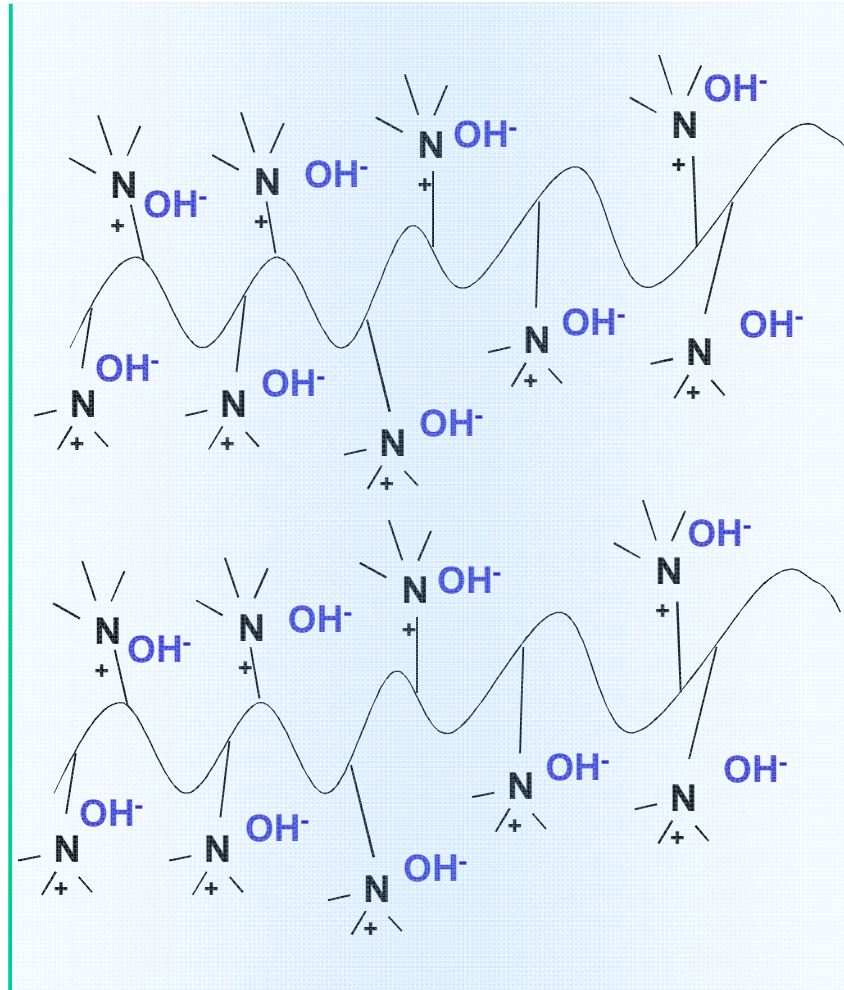
Outline

- 1 . Tokuyama's Electrolyte Materials for AMFCs**
 - **Anion exchange membrane**
 - **Alkaline Ionomer**
- 2 . Performance of AMFCs**
 - **Power density**
 - **Characteristic behavior in AMFC**
 - CO₂ problem**
 - Water transport**
 - **Durability**
- 3 . Summary**



Tokuyama Anion exchange Membrane

Structural image





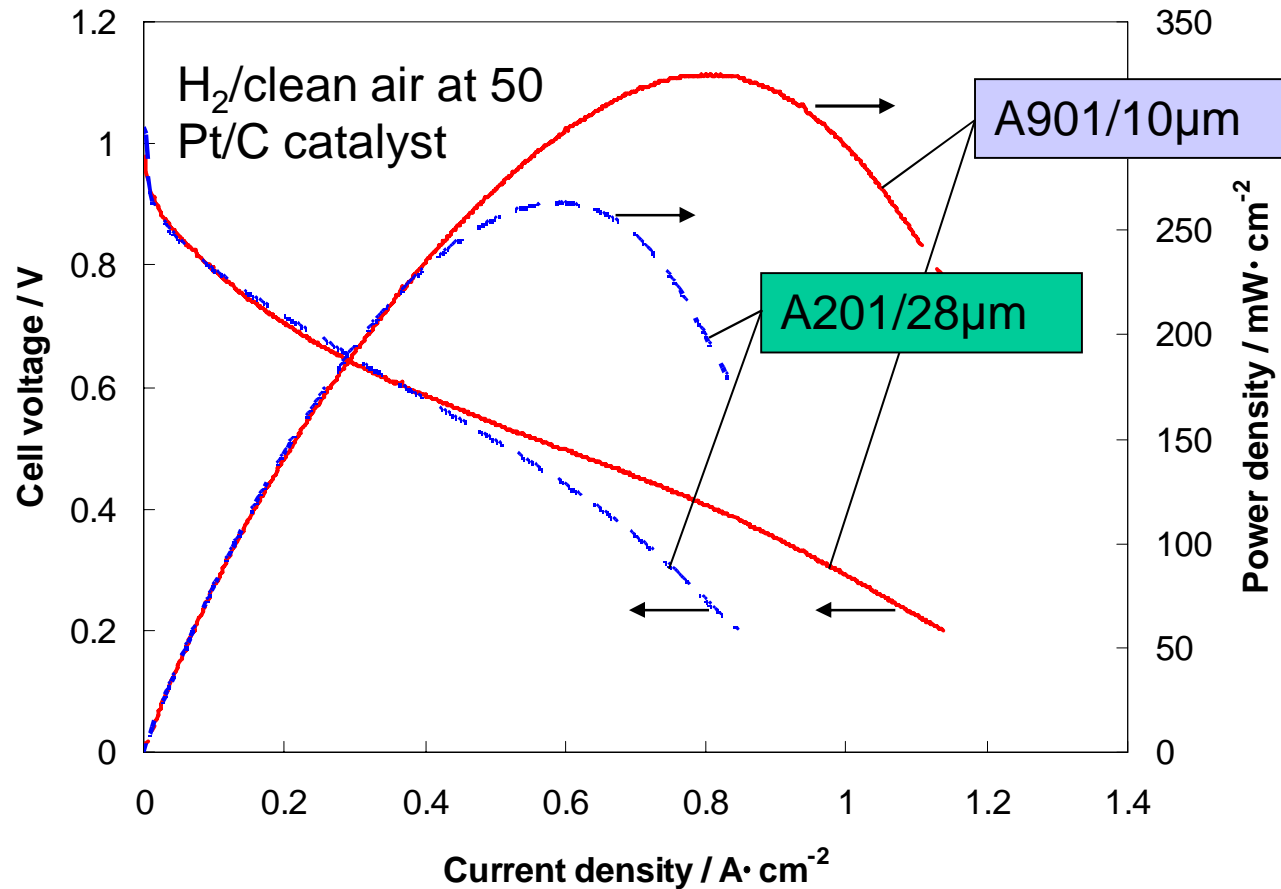
Properties of Anion Exchange Membranes

Properties		A201 (Tokuyama)	A901 (Tokuyama)	Fluorinated membrane (Cation Membrane)
Thickness	/ μm	28	10	180
Ion-exchange capacity	/ $\text{mmol}\cdot\text{g}^{-1}$	1.8	1.8	1.0
Water content	/ -	0.25	0.15	0.30
Ion conductance ¹⁾	/ $\text{mS}\cdot\text{cm}^{-2}$	11	29	4.2
Ion conductivity ¹⁾	/ $\text{mS}\cdot\text{cm}^{-1}$	42	38	84
Burst strength	/ MPa	0.4	0.2	0.5
Dimensional change	wet dry			
MD	/ %	2	1	10
TD	/ %	6	4	15

1) Two probe method for in plane conductivity measurement at 23 °C, 90%RH under N₂ atmosphere, at OH- form



AMFC Performance with Different Membrane



[MEA composition]

Membrane : A201 or A901

Ionomer : AS - 4

Pt amount : 0.5mg/cm²

[measurement condition]

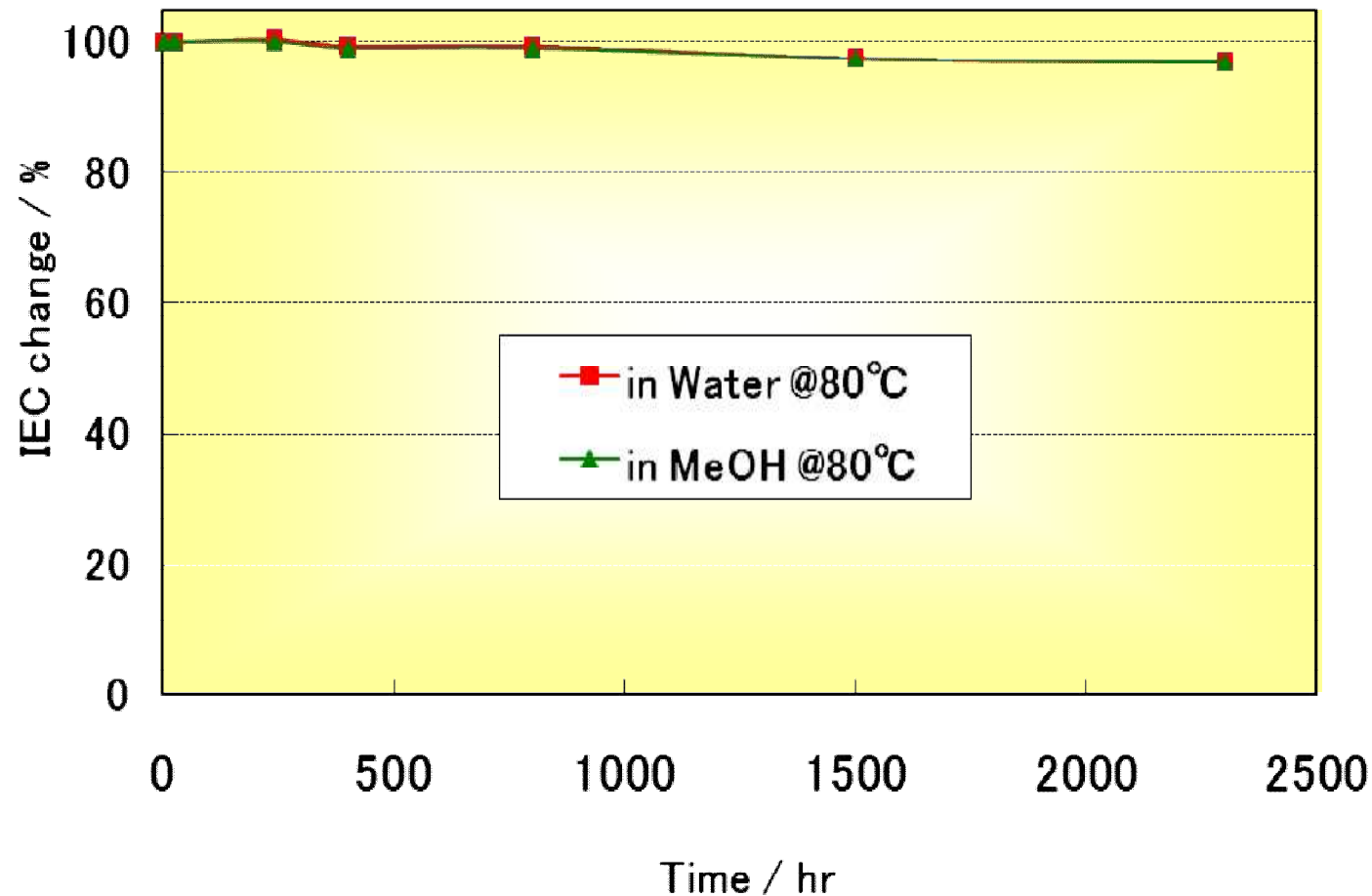
Cell temp. : 50

Anode : 95%RH H₂ 0.5L/min(A201), 1.0L/min(A901)

Cathode : 95%RH clean air 1.0L/min(A201), 2.0L/min(A901)



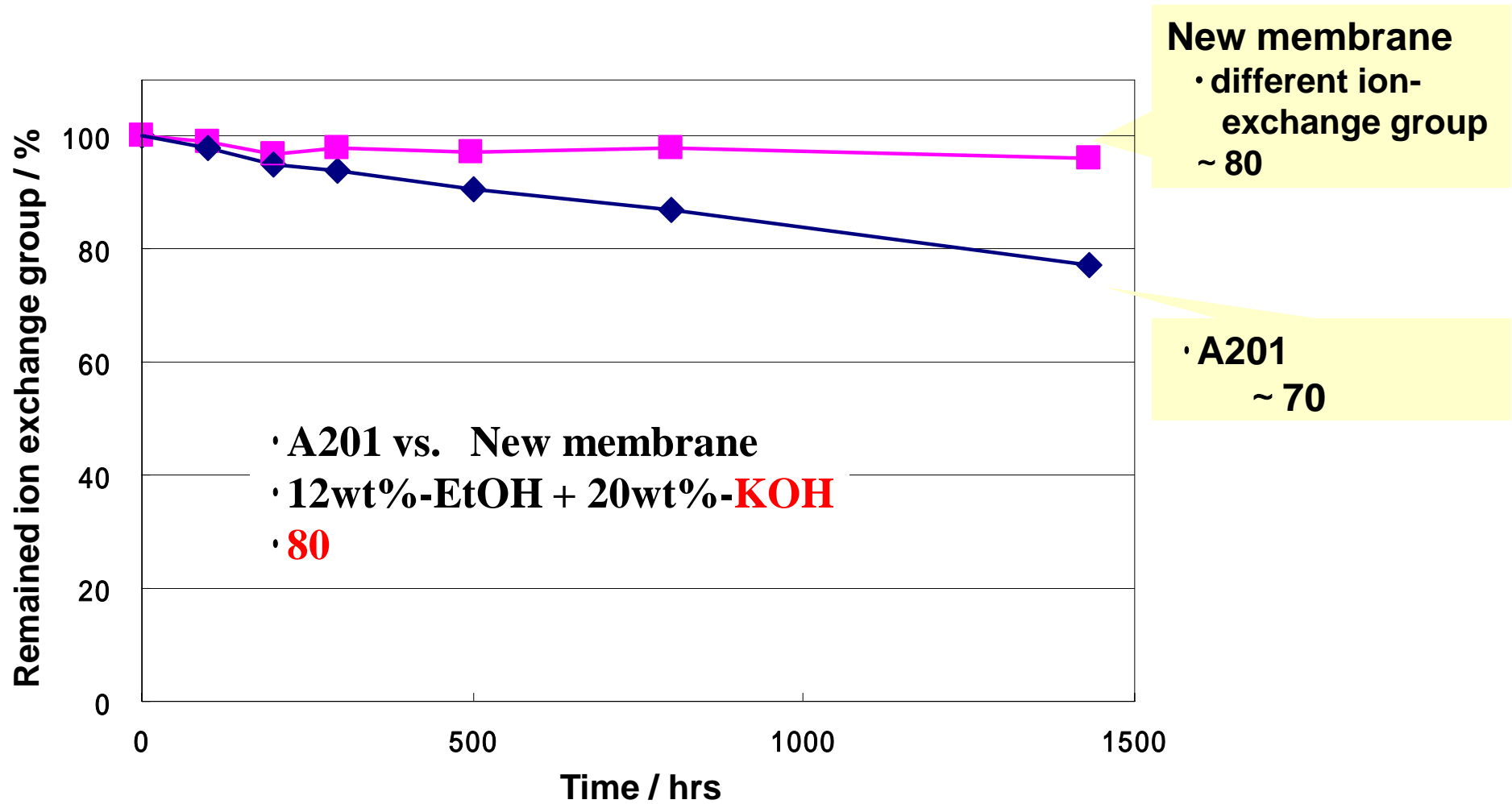
Stability Test of Membrane (A201)



Membrane was ion-exchanged to OH⁻ form and stored in the air before durability test.
(maybe converted to HCO₃⁻ form)



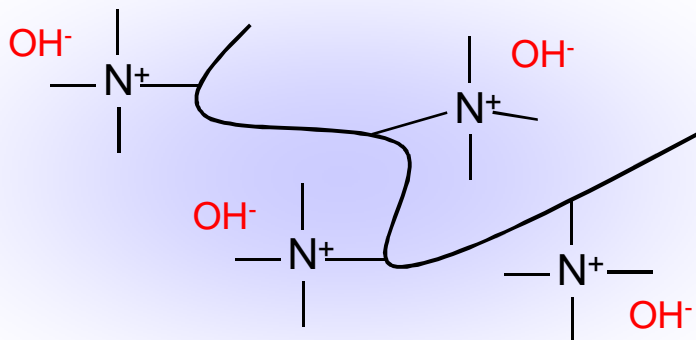
Accelerated Durability Test





Tokuyama Alkaline Ionomers

Structural image



**Linear hydrocarbon backbone
with
quaternary ammonium group**

Needs for ionomers

- High ion conductivity
- Solubility into solvent at preparation of catalyst ink
- Non-solubility after preparation of catalyst layer
- Dispersivity in catalyst ink
- Durability
- etc.



Properties of A-Ionomer Solution

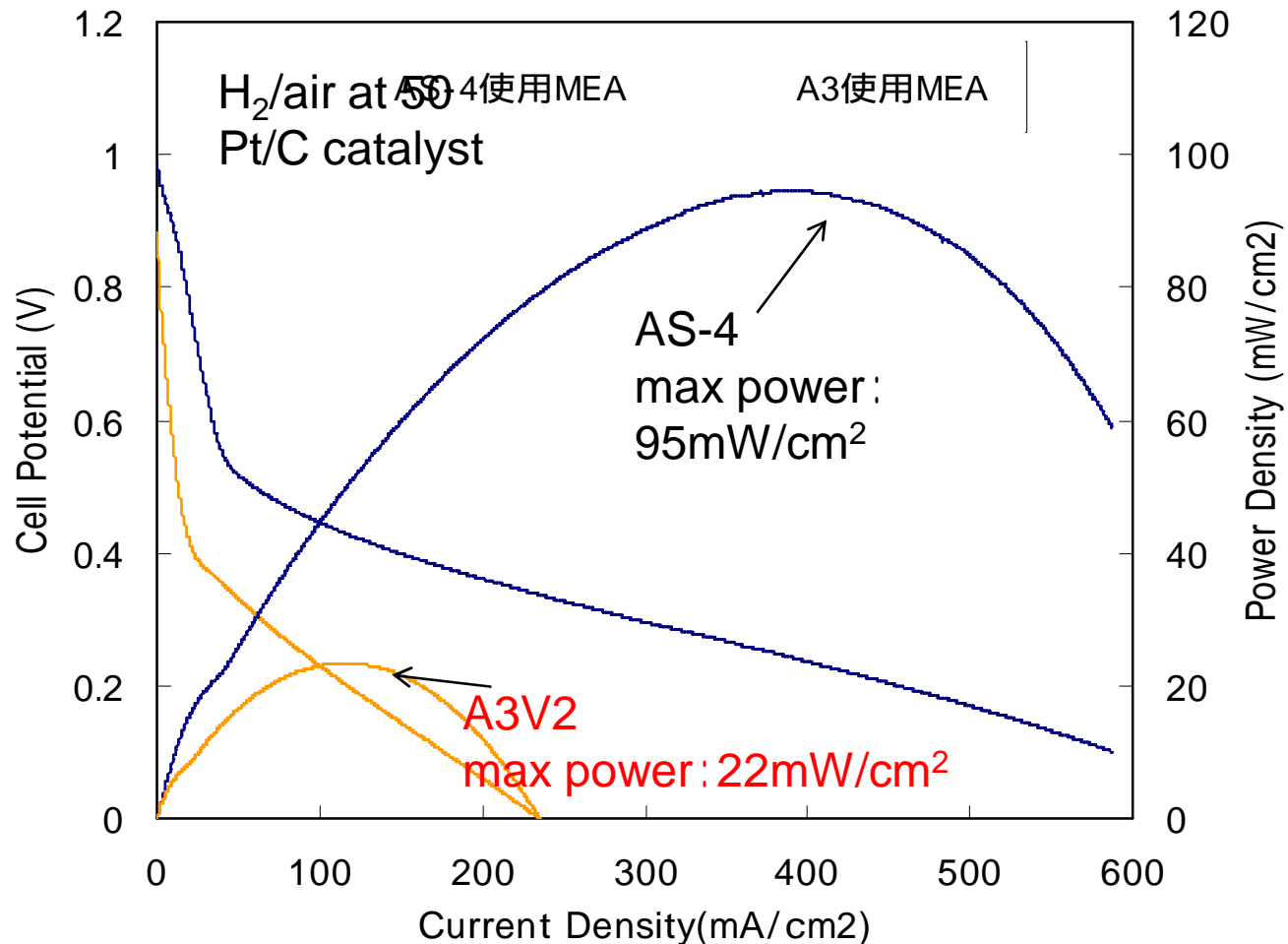
State	Features	A3 ver.2	AS-4
solution	Polymer concentration / wt%	5	5
	Solvent	Tetrahydrofuran & 1-Propanol	1-Propanol
membrane (cast film)	Ion-exchange capacity / mmol·g ⁻¹	0.7	1.4
	Ion conductivity / mS·cm ⁻¹ (HCO ₃ ⁻ form)	2.6	13
	Solubility to solvent		
	Water	not soluble	not soluble
	MeOH	not soluble	not soluble
EtOH	not soluble	not soluble	

1) ~ 3) Measured using cast film

2) Measured on alternative current(40 , wet) ,at HCO₃⁻ form



AMFC Performance - Ionomer Type

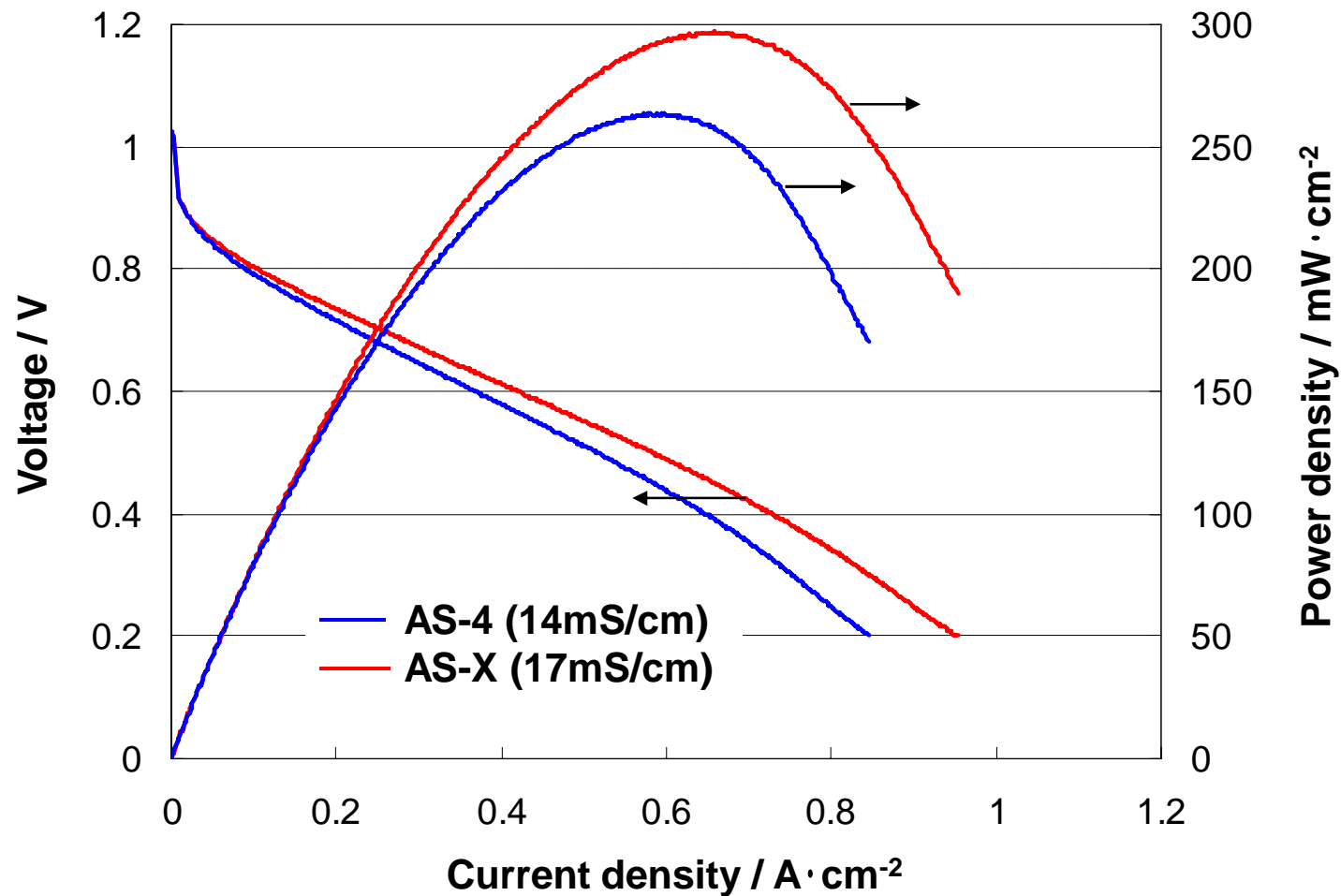


[MEA composition]		[measurement condition]	
Membrane	: A801	Cell temp.	: 50
Ionomer	: AS-4 or A3 ver.2	Anode	: 95% RH H ₂
Pt amount	: 0.5mg/cm ²	Cathode	: 95% RH air



Effect of improved ionomer

Ionomer	IEC (mmol/g)	Conductivity (mS/cm)
AS-4	1.4	14
AS-X	1.8	17





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2 . Performance of AMFCs

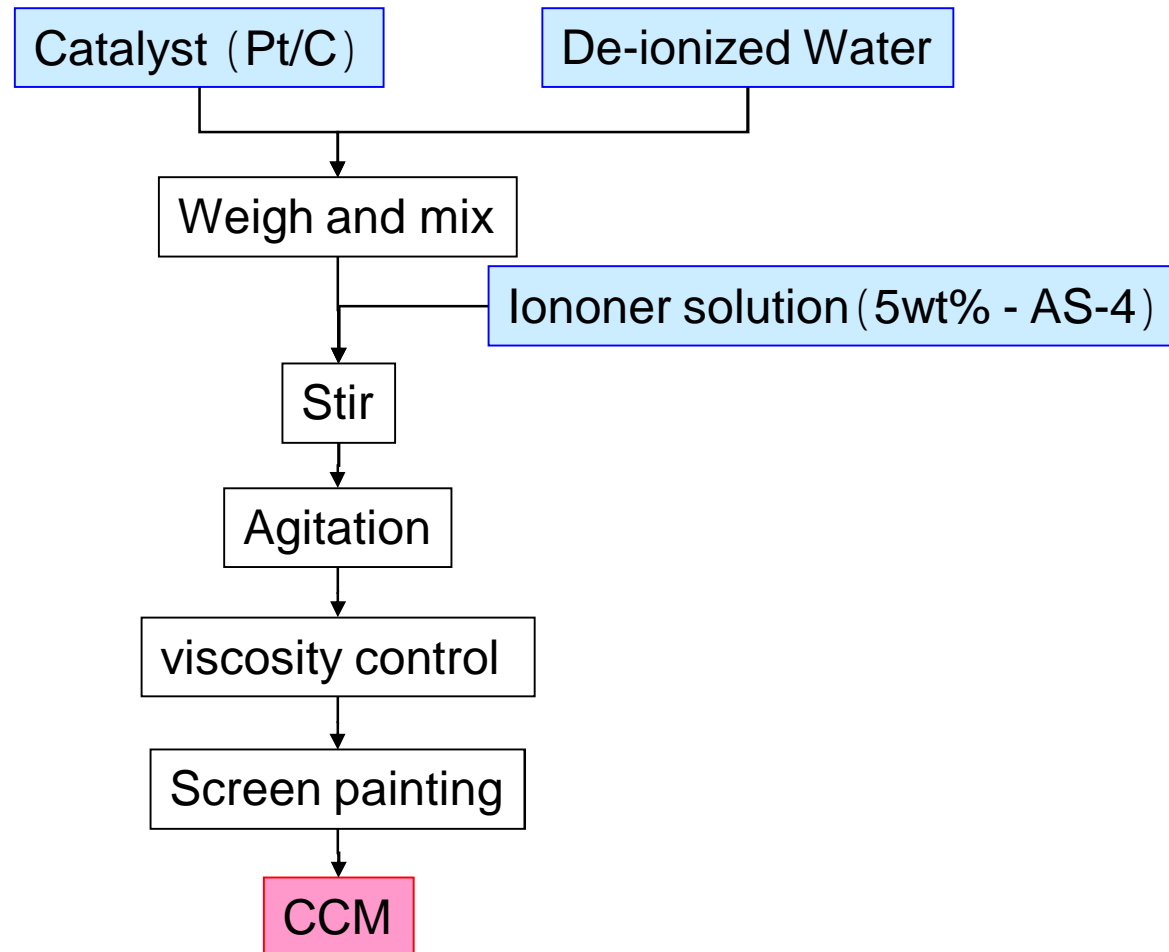
- **Power density**
- Characteristic behavior in AMFC
 - CO₂ problem
 - Water transport
- Durability

3 . Summary



Fabrication of CCM

Fabrication process (Catalyst : Iononer = 7:3)



Catalyst ink



CCM (5cm²)



Evaluation Procedure

Evaluation of I-V curves

- GDL : Toray TGP-H060 (without hydrophobic treatment)
- fuel : H₂ (95%RH, 1000mL/min)
- oxidant : clean-air (CO₂<0.1ppm, 95%RH, 2000mL/min)
or O₂ (95%RH, 1000mL/min)
- Temperature : 50
- evaluation step :
 - MEA set into cell → pre-operation at 0.1V for 15min (for activation)
 - measurement of I-V curves

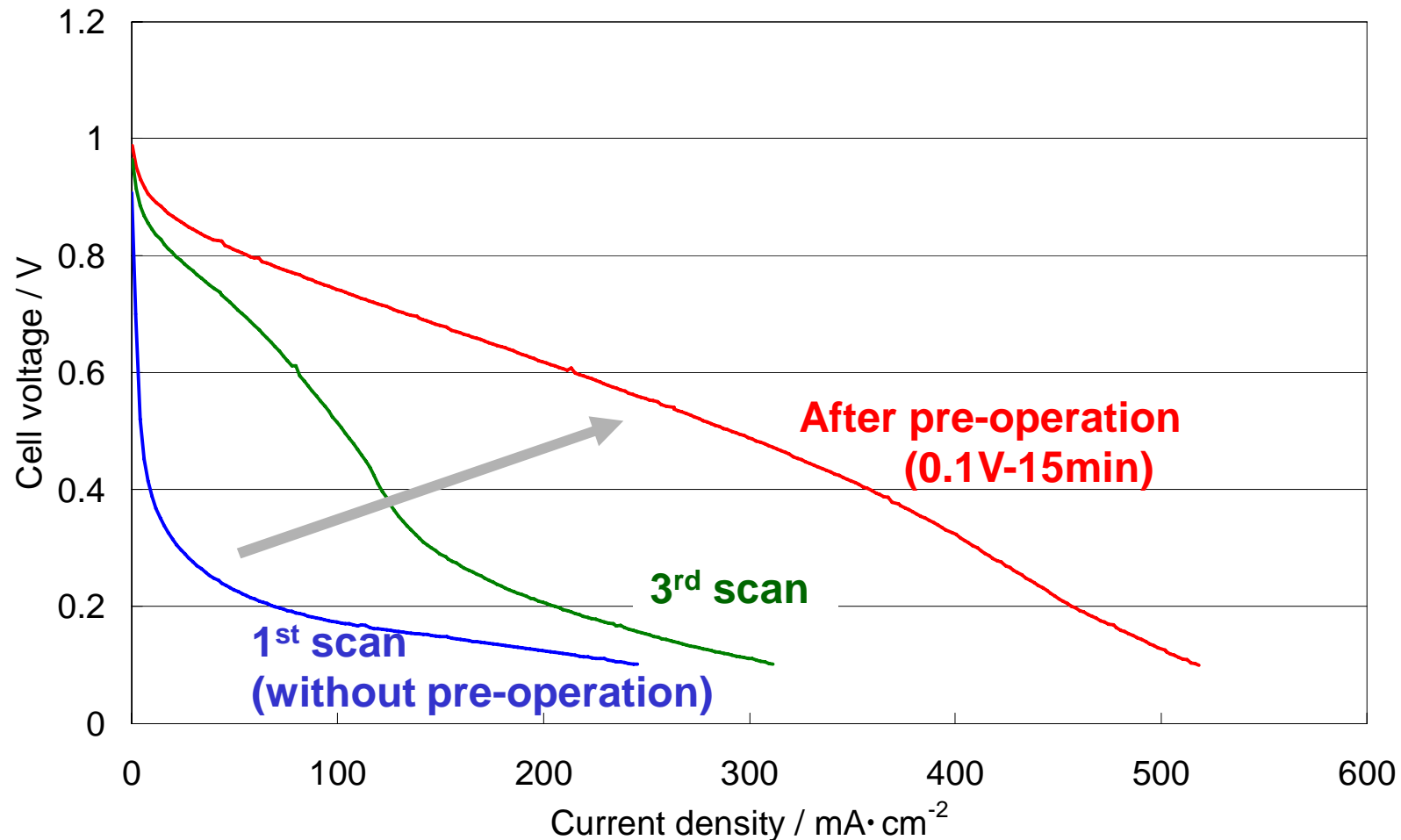
Optimized condition

- Pt/C:ionomer = 7:3 (in case of Pt/C(Pt;46wt%), at high flow rate)
- Maybe differ by catalyst and flow condition



Effect of Pre-Activation

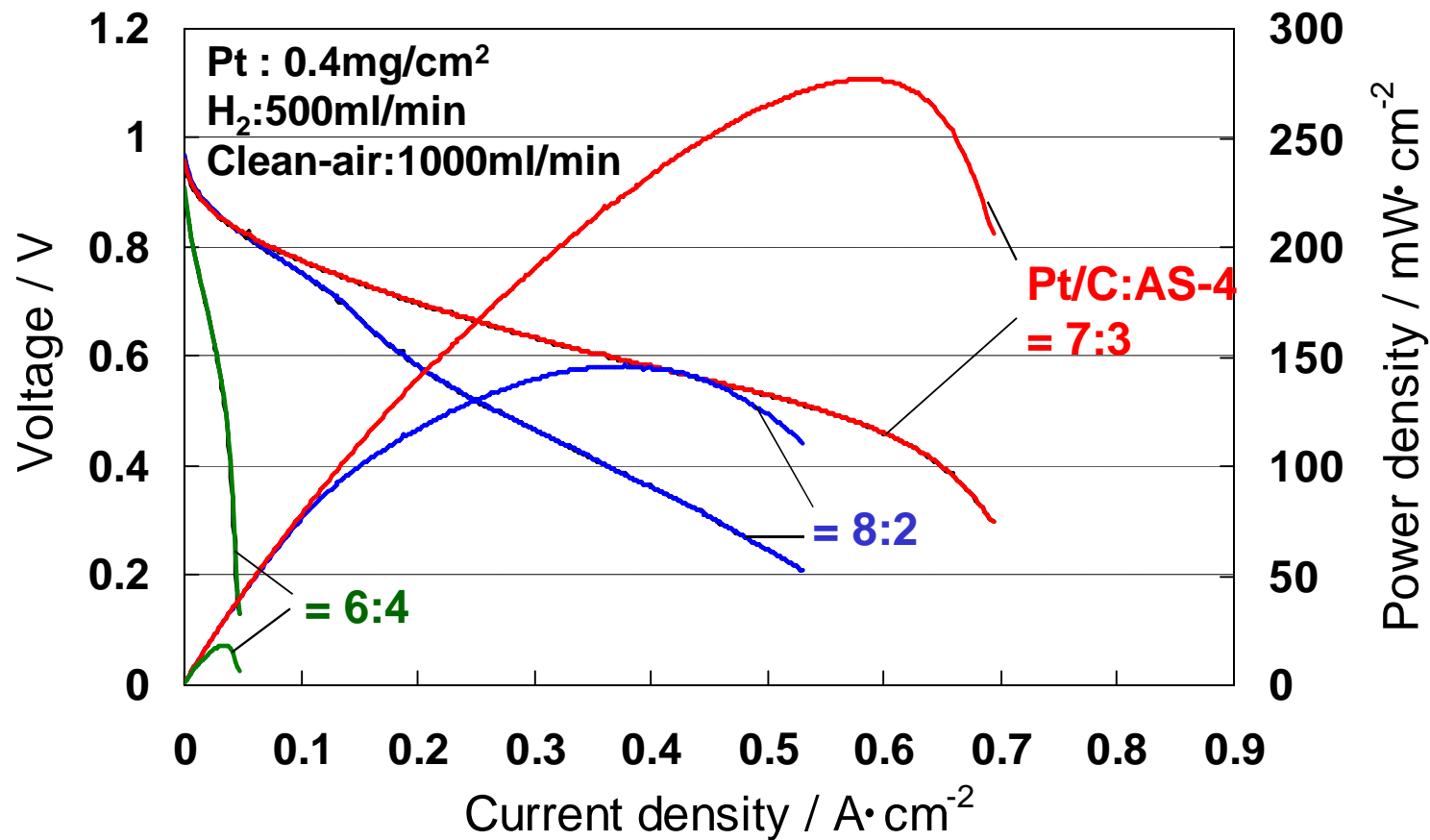
- HCO_3^- form membrane changes to OH^- form by the OH^- generated at cathode through pre-operation (self-purging), and it makes the performance higher.





Influence of Ionomer Content

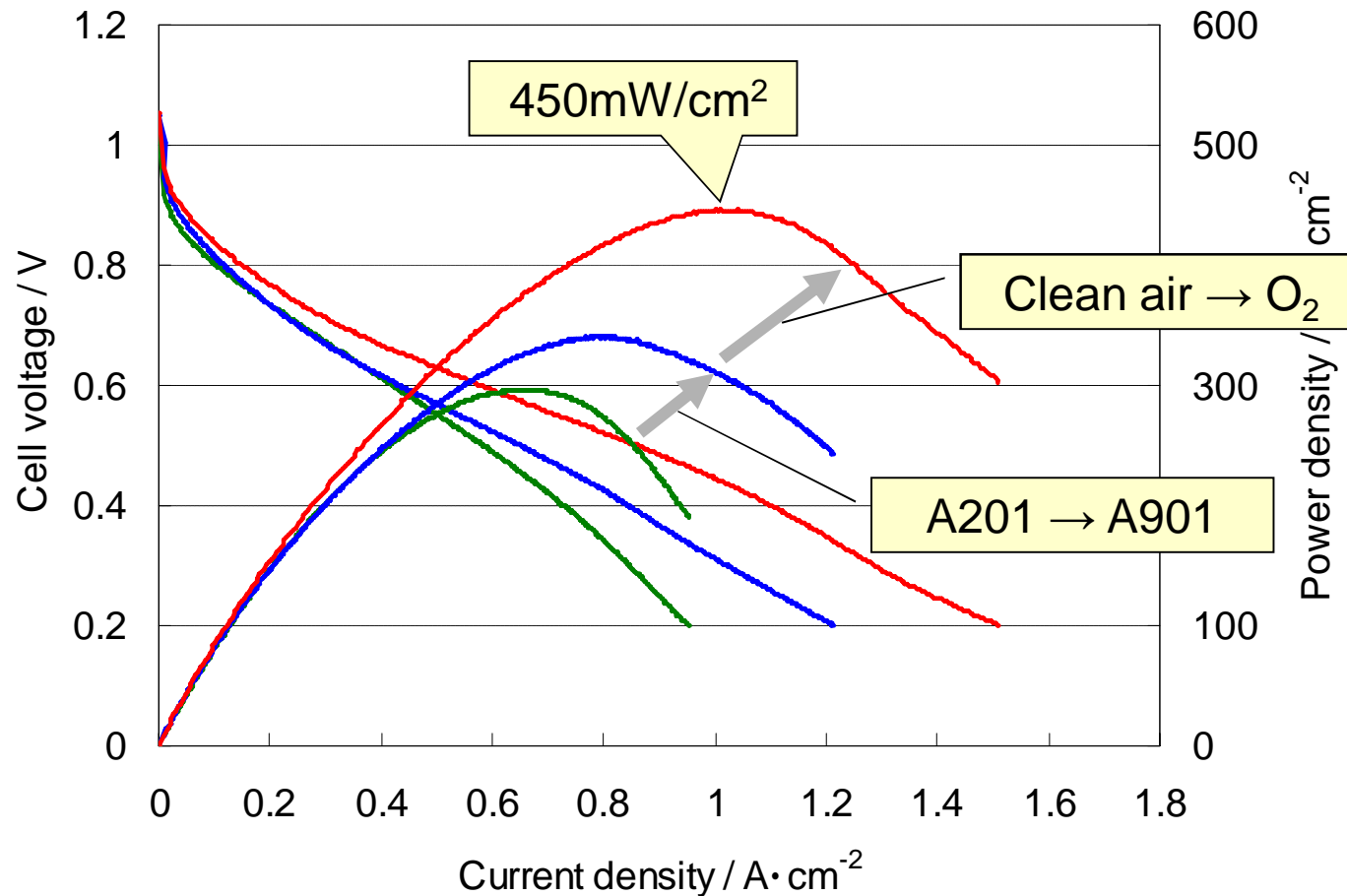
- Pt/C:AS-4 = 7:3 shows the best performance in this condition.
- Appropriate content should be differed by catalyst and operation condition.





Optimized Performance at Tokuyama

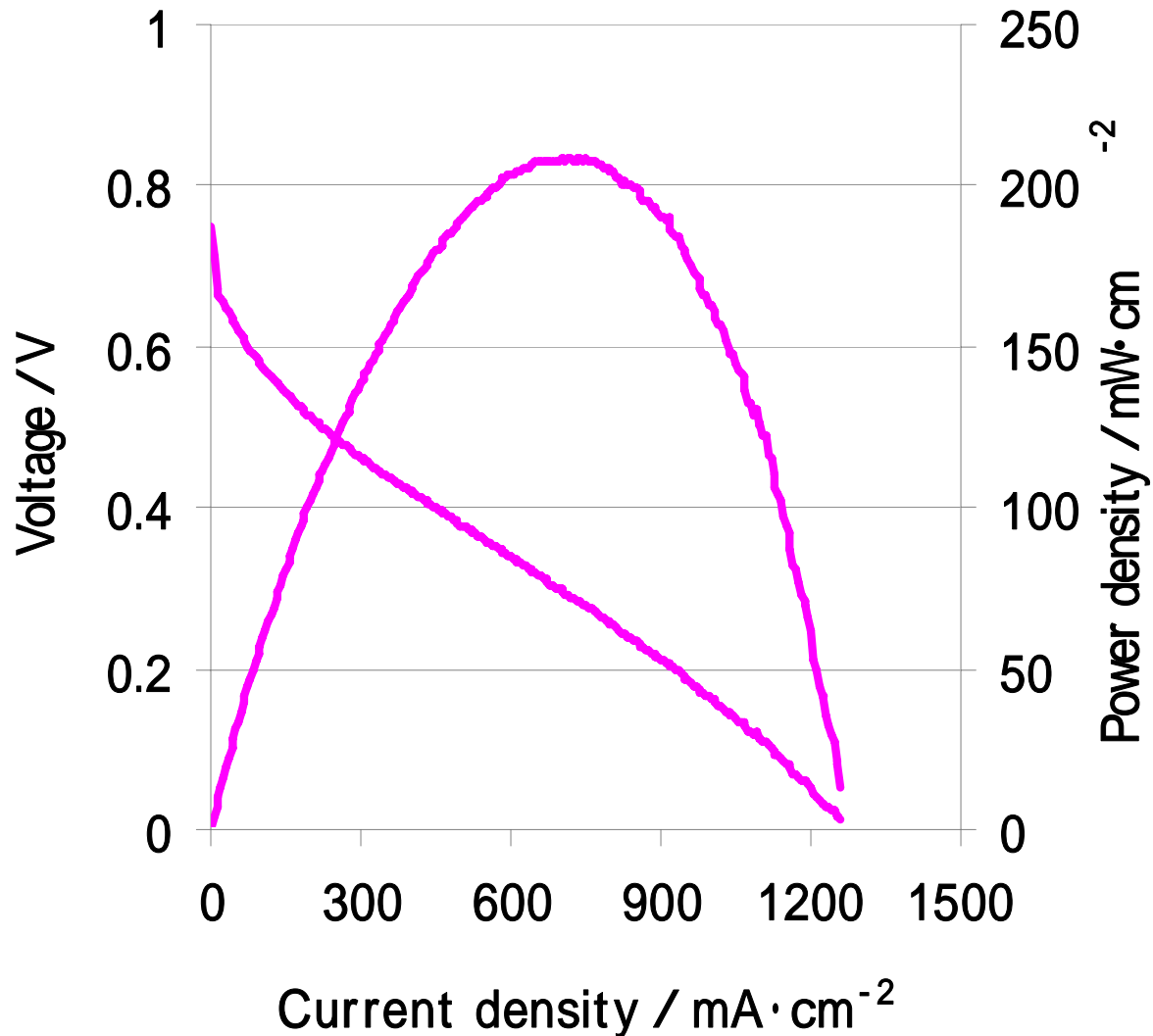
Membrane: A201 → A901, Ionomer: AS-4 → AS-X, Pt/C: AS-X=7/3, 0.5mg-Pt/cm²



- **Best power density : 340mW/cm² (using clean air)**
- **450mW/cm² (using O₂)**



AMFC Performance (MeOH/KOH-Air)



- Membrane : A201
- Catalyst : Anode Pt-Ru/C
1.1 mg/cm^2
Cathode Pt/C
0.5 mg/cm^2
- Ionomer : AS-4
- Fuel : 3wt%-MeOH
+ 5wt%-KOH
10 ml/min
- Oxidant : 95%RH Clean Air
4000 ml/min
- Temp. : 80



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- Durability

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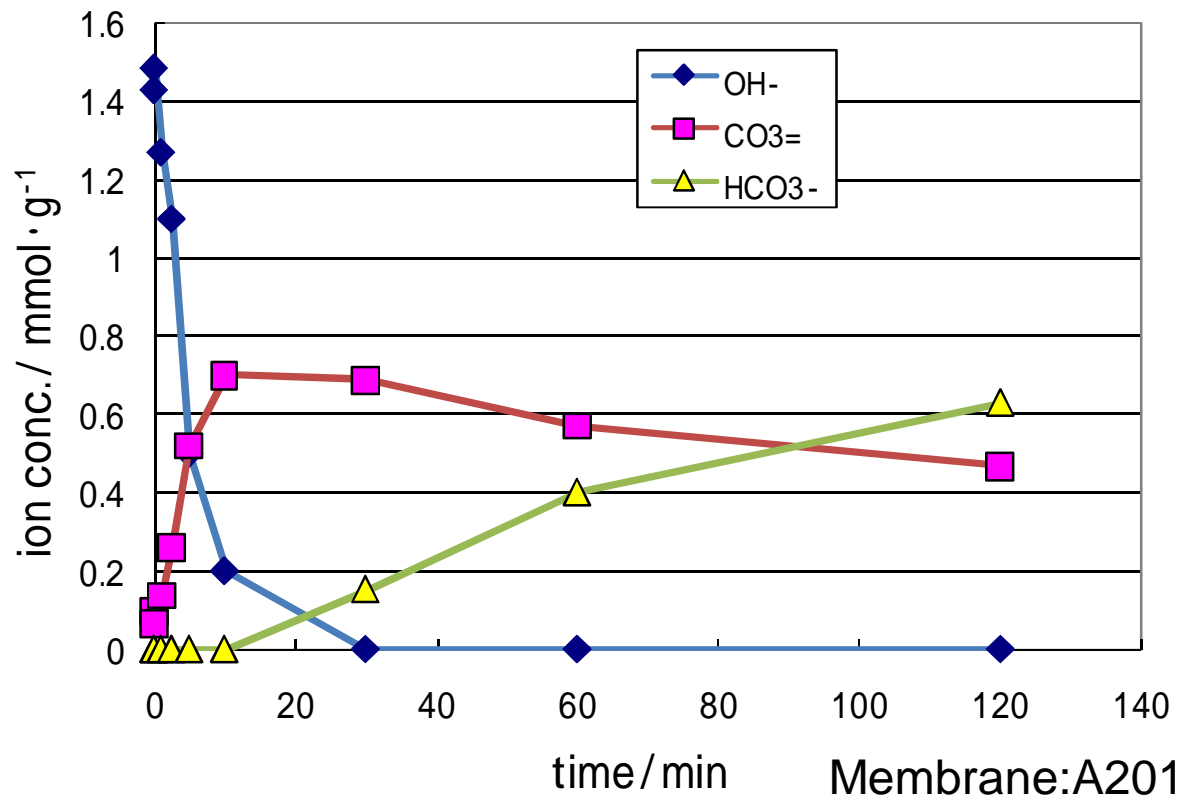


CO₂ Absorption into Alkaline Membrane

OH⁻ is changed to CO₃²⁻ in a few minutes, further to HCO₃⁻.



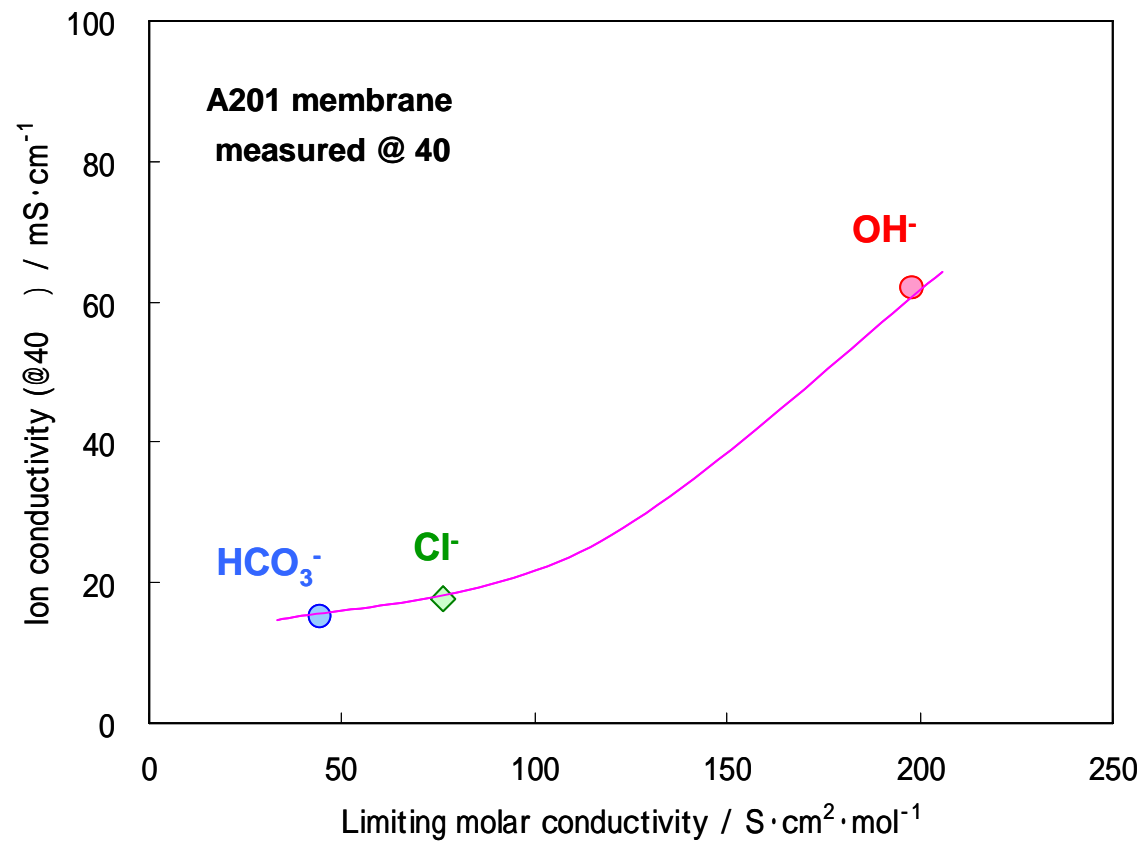
Needs to know the effect of counter ion on the conductivity





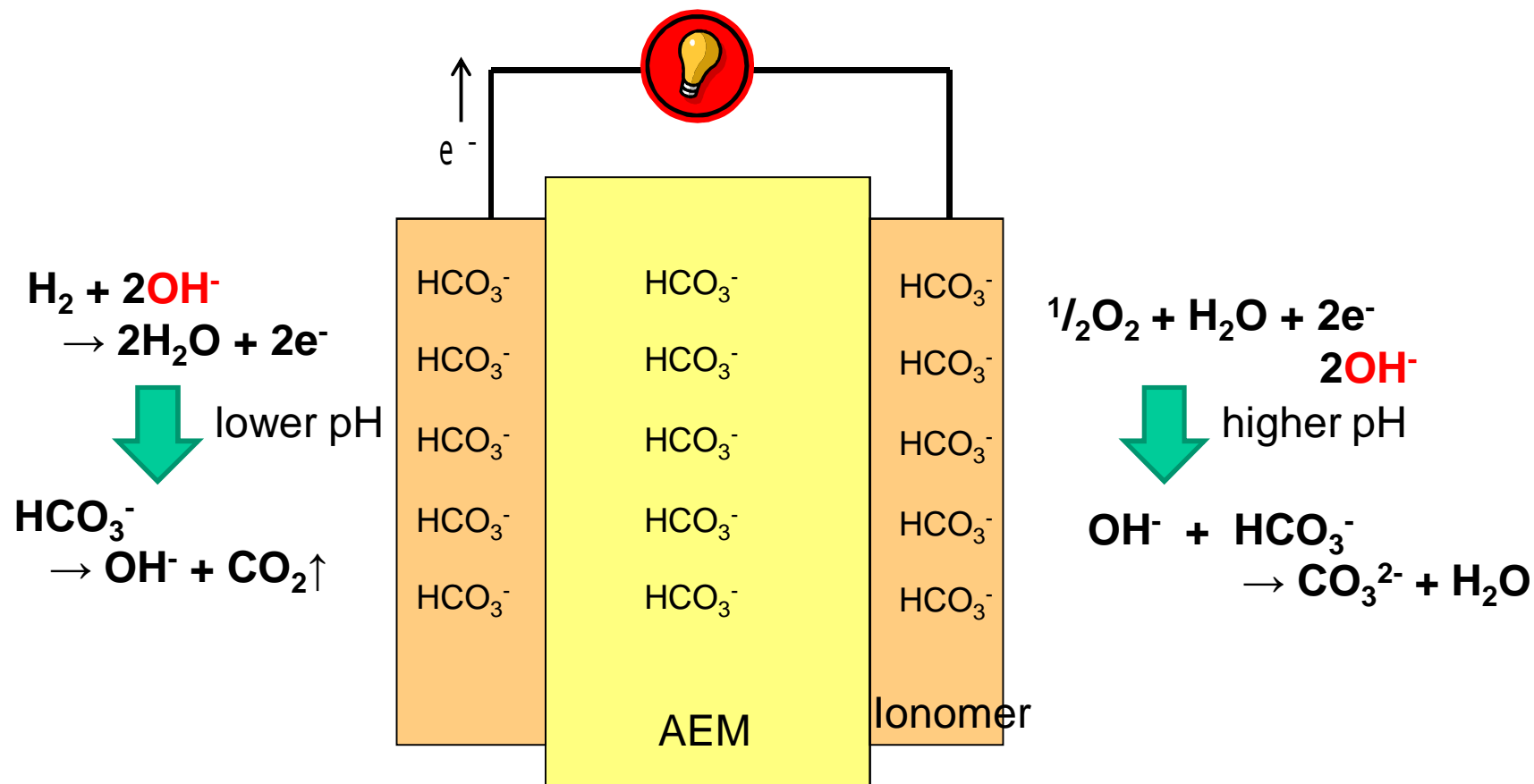
Effect of the counter anion

Membrane Conductivity depends on the mobility of counter anion .





Self-Purging (Initial Stage)

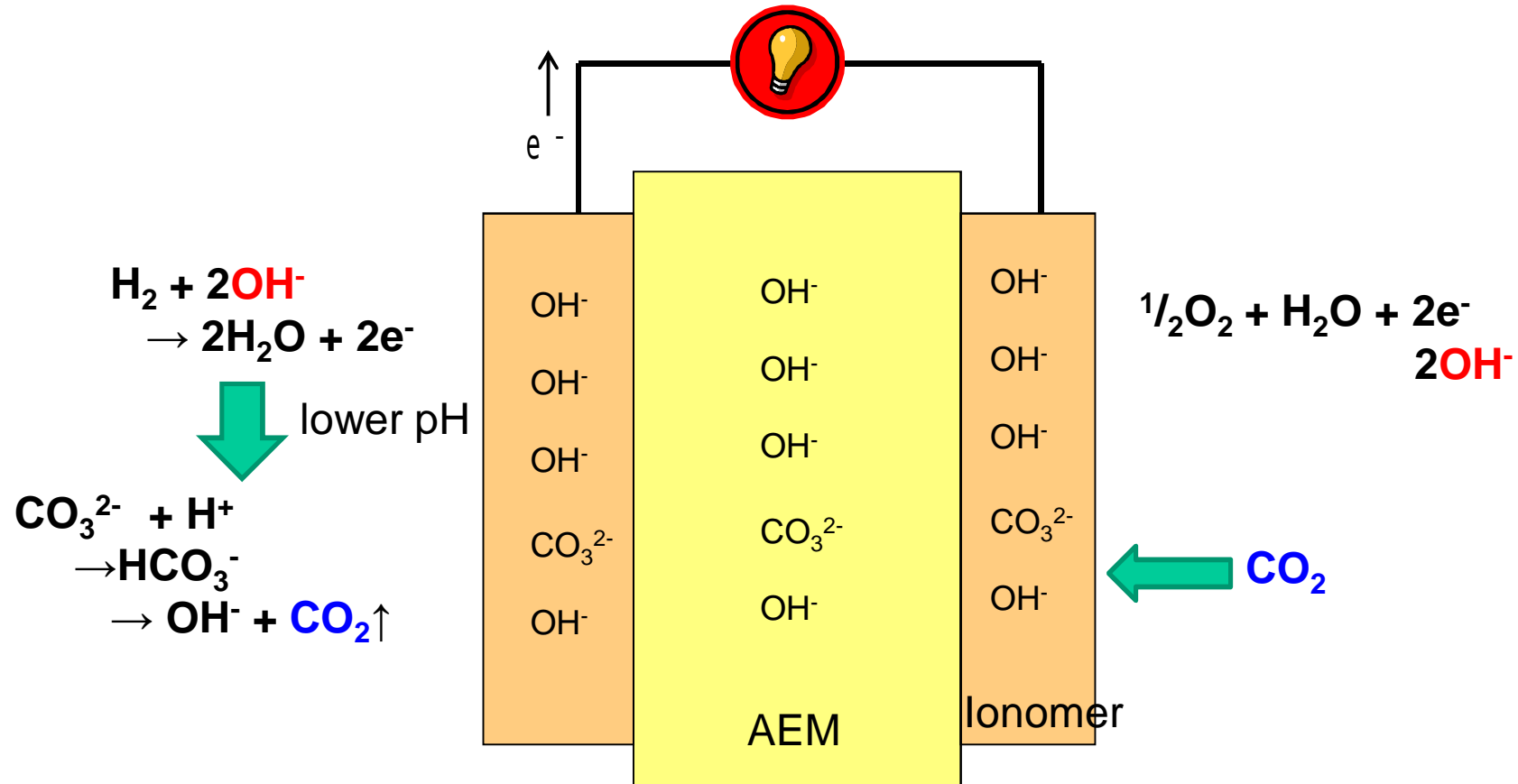


self-purge :

J.Varcoe et. al, ChemSusChem 2008, 1, 79–81

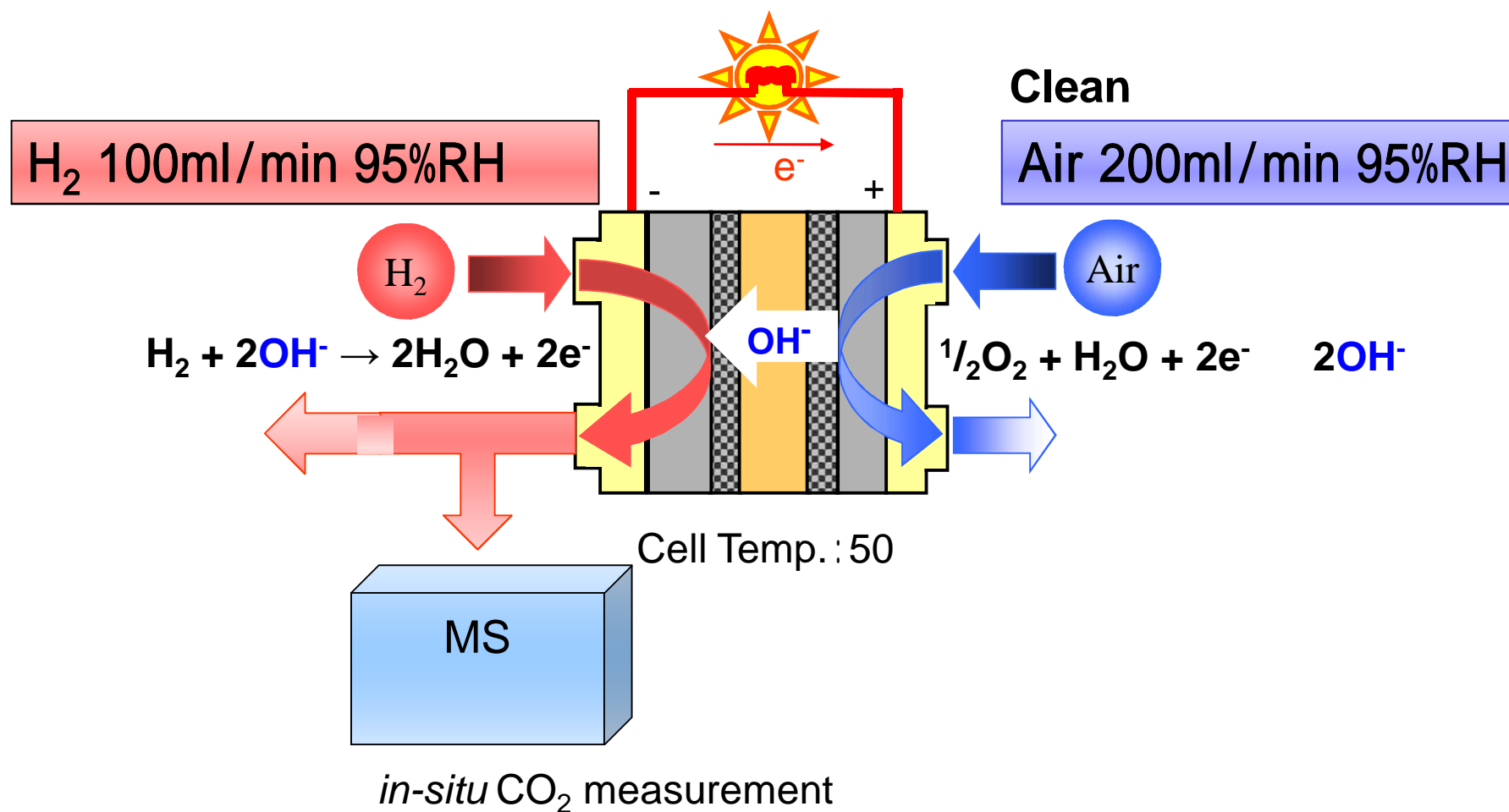


Self-Purging (Steady State)



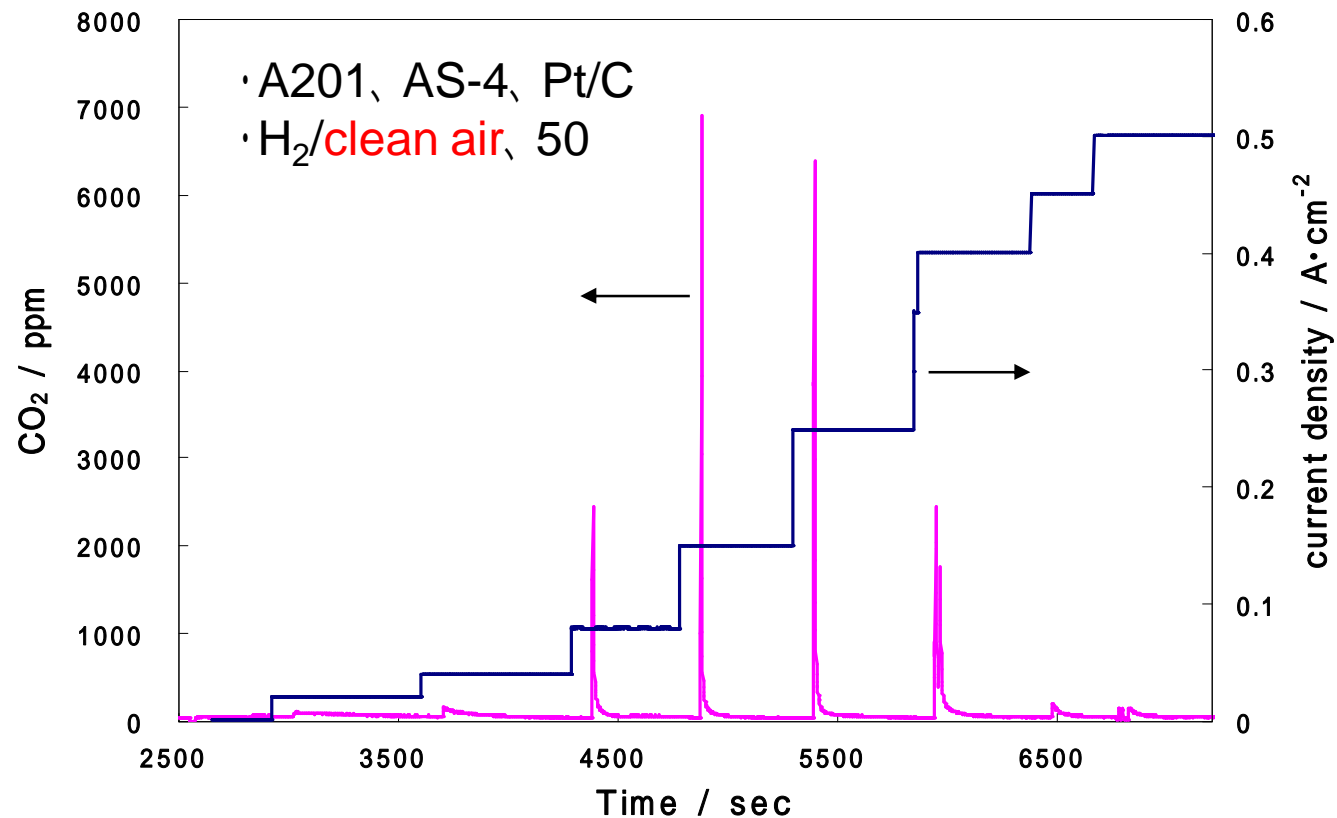


in-situ Analysis of CO₂





Observation of CO₂ Release from Anode

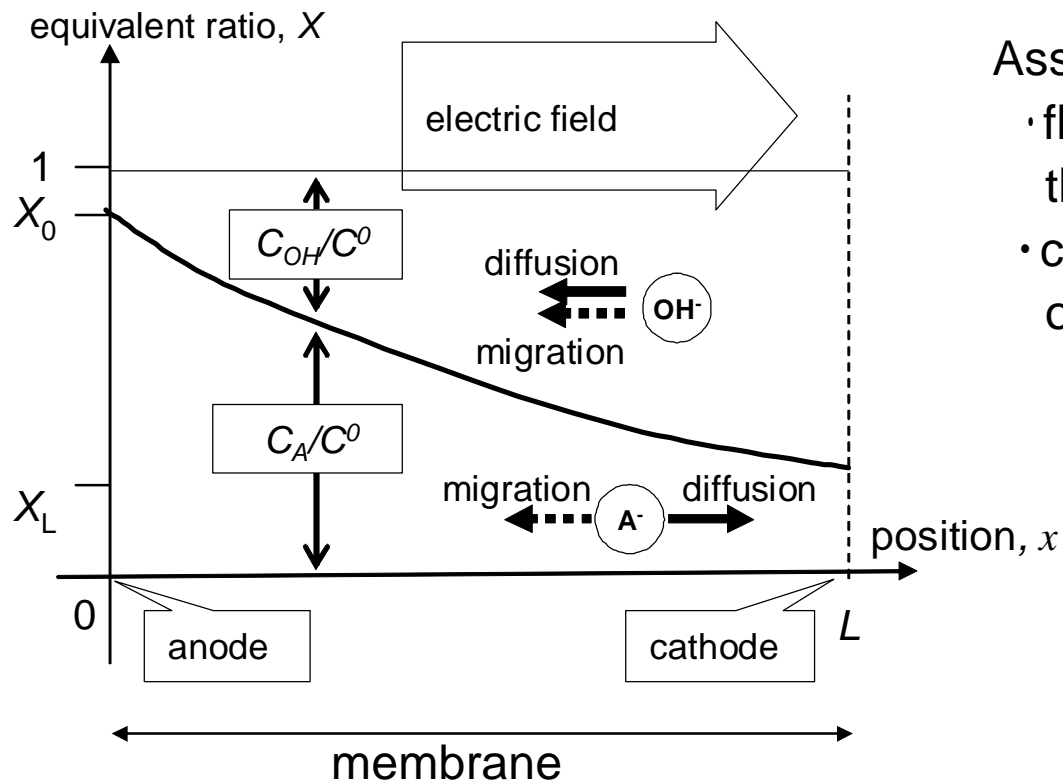


CO₂ is released quickly after increasing current density.
Released amount seems to depend on the current density.

Ref. Z. Siroma, et. al., *J. ElectroChem. Soc.*, 158, B682 (2011).



Modeling of CO₂ concentration profile

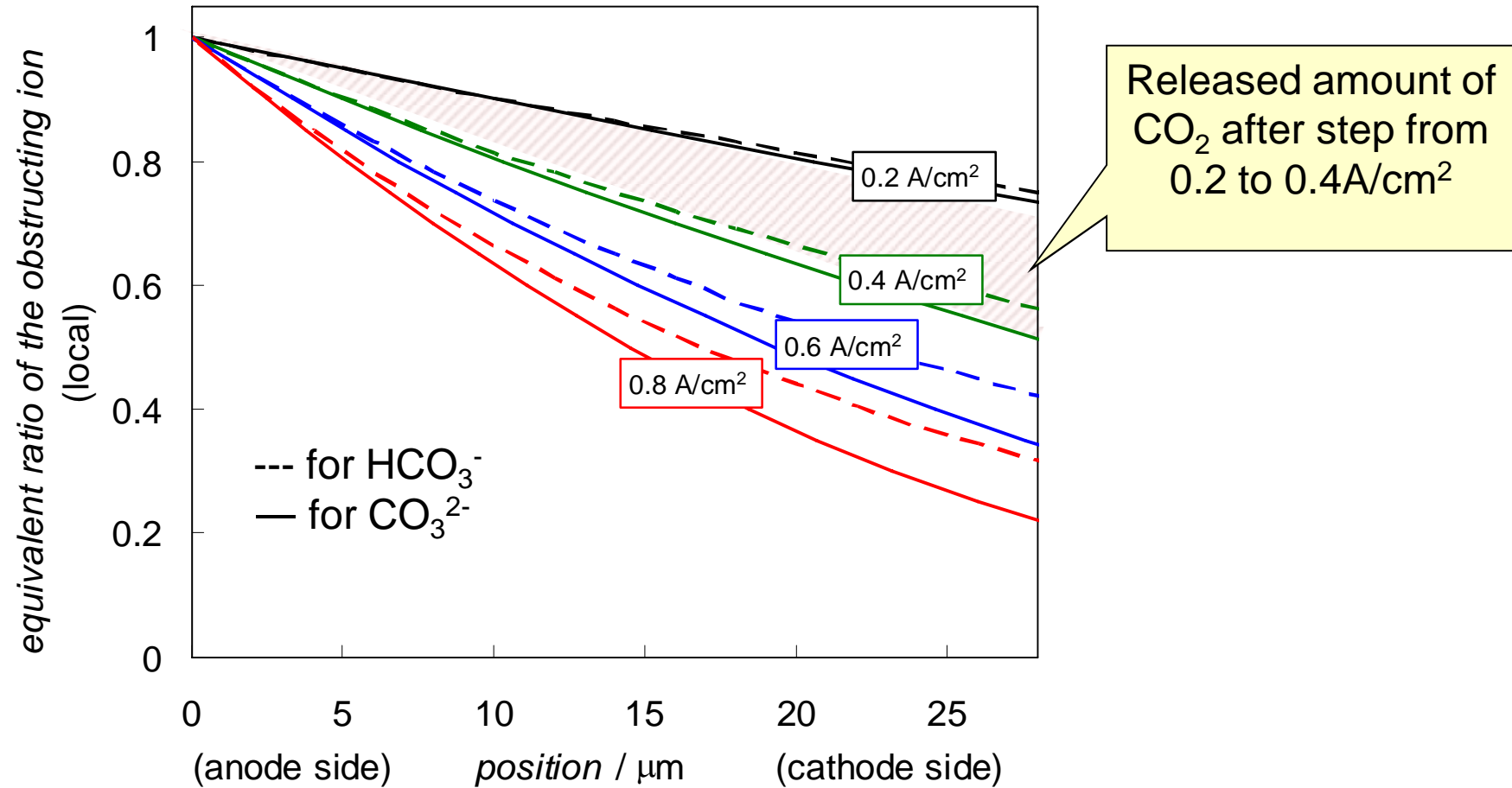


Assumption

- flux of carbonate ion is zero throughout the membrane
- concentration of OH⁻ at the end of anode is fixed to zero



Calculated CO₂ concentration profile





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Water Transport Measurement

PENNSTATE

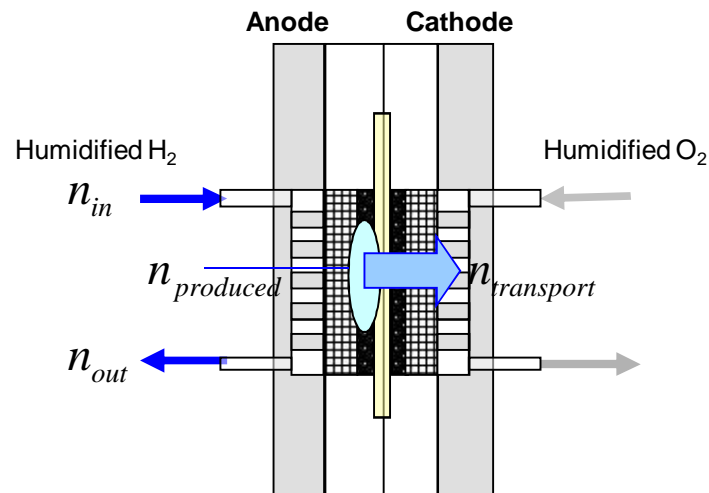


Electrochemical Engine Center

- ✓ To learn how the water for ORR is supplied in AMFC
- ✓ To test the operation under the dry gas feeding condition

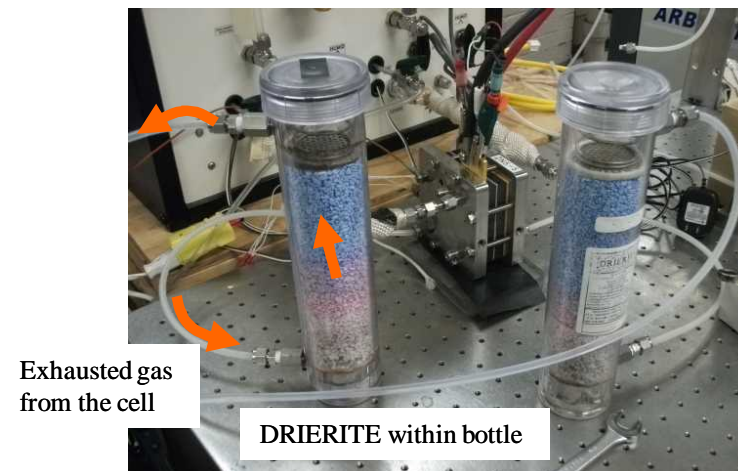
Net Water Flux from anode to cathode; $n_{transport}$

$$n_{transport} = n_{out} - n_{in} - n_{produced}$$



The Conditions for humidification in this study

Anode (H ₂)	Cathode (O ₂)
100	100
100	0 (dry gas)
0 (dry gas)	0(dry gas)



From the presentation at 219th ECS meeting (Montreal)

AMFC Performance with Dry Feed Conditions

- ✓ AMFC performance decreased with lowered humidity.
- ✓ The effect of cathode humidity was quite small.

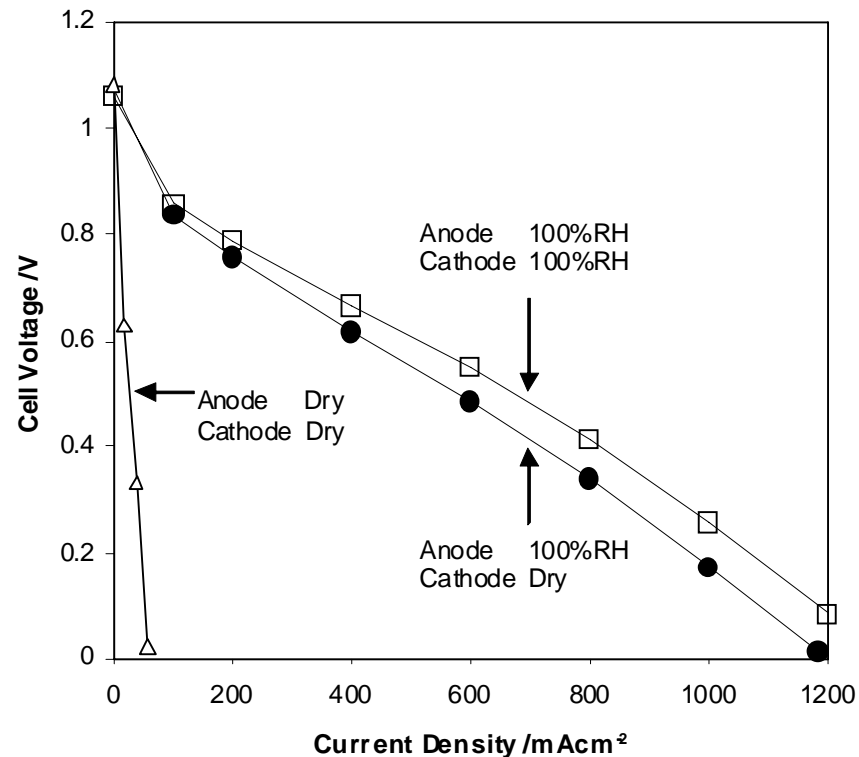


Fig.1 Polarization Curves under various humidified conditions
Anode feed: H₂ 200mLmin⁻¹, Cathode feed: O₂ 200mLmin⁻¹ Cell
Temperature 50°C



Net Water Flux from Anode to Cathode

- ✓ At 100%RH/100%RH, net water flux from anode to cathode was same as the theoretical amount of water required for ORR.
- ✓ It suggested that all the water required for ORR was supplied from anode.

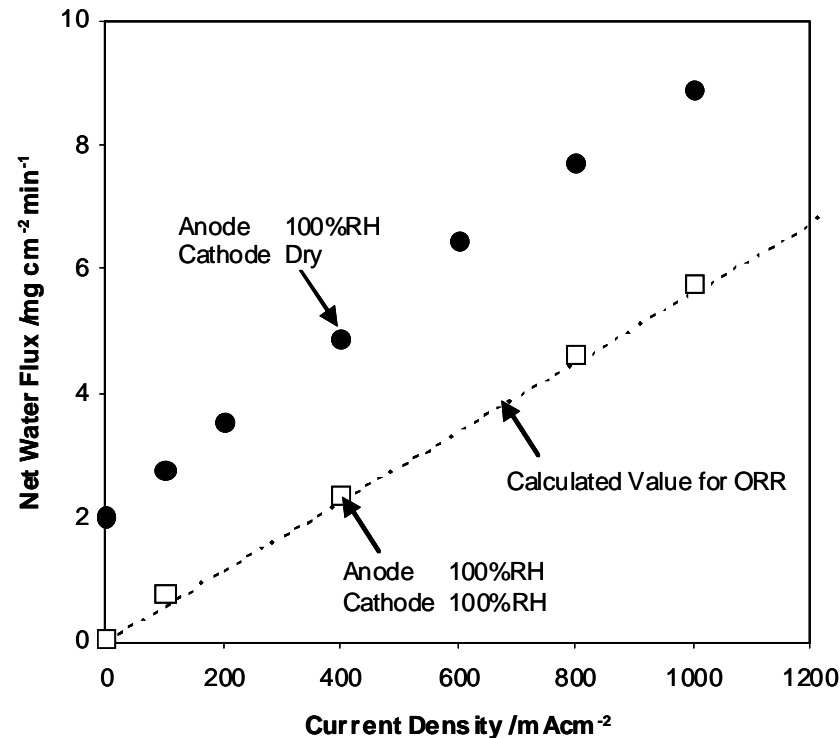


Fig.2 Net Water Flux from anode to cathode under various humidified conditions Dotted line shows calculated amount of water for ORR at cathode, Anode feed: H₂ 200mL.min⁻¹, Cathode feed: O₂ 200mL.min⁻¹ Cell Temperature 50°C



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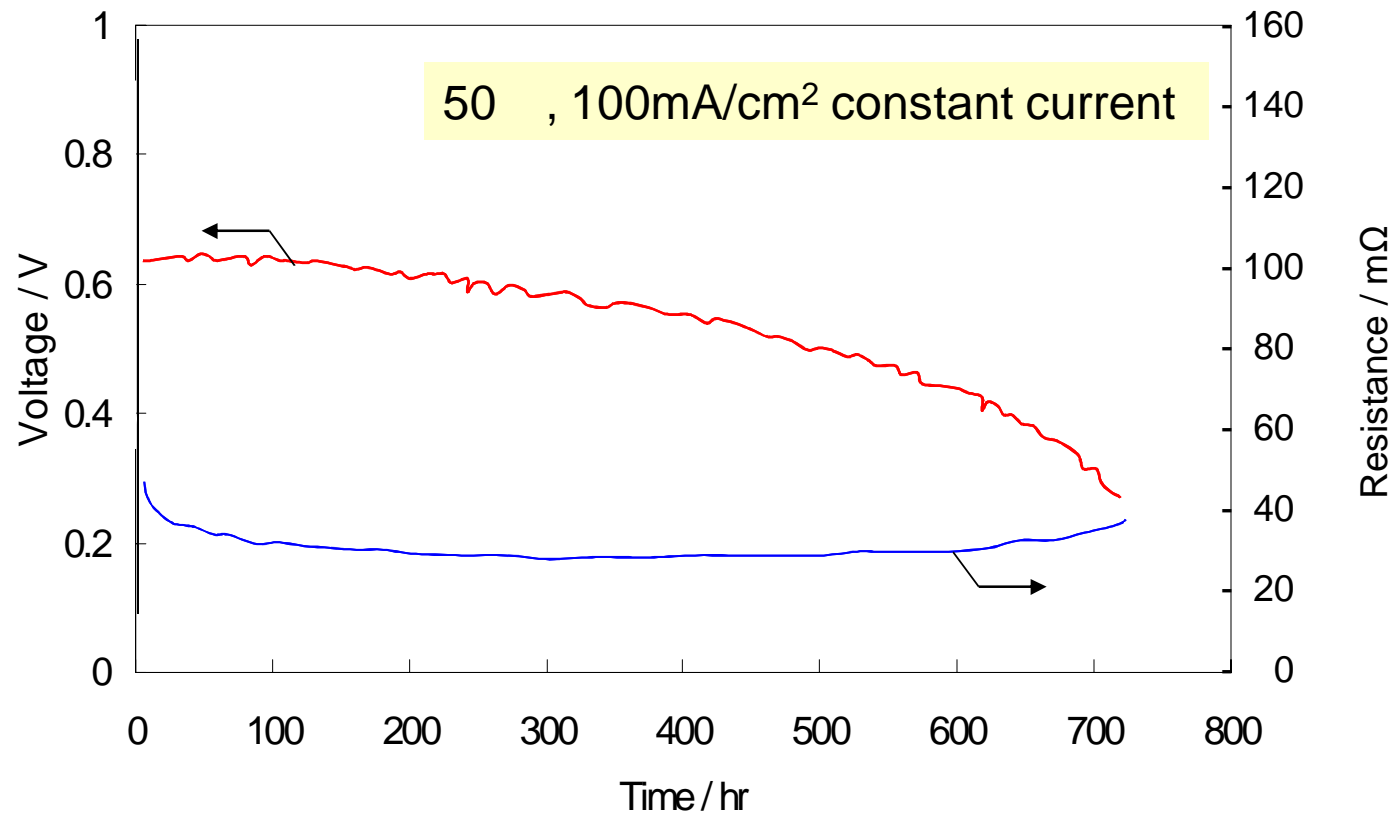
3 . Summary



Durability Test

With improved adhesion between membrane and catalyst layer, higher Pt loading seems to lead to better durability.

Even after long-term operation, IEC of membrane has not changed.



[MEA composition]

Membrane : A201

Ionomer : AS - 4

Pt amount : 0.8mg/cm²

[measurement condition]

Cell temp. : 50

Anode : 95%RH H₂ 100ml/min

Cathode : 95%RH clean air 200ml/min (A201)



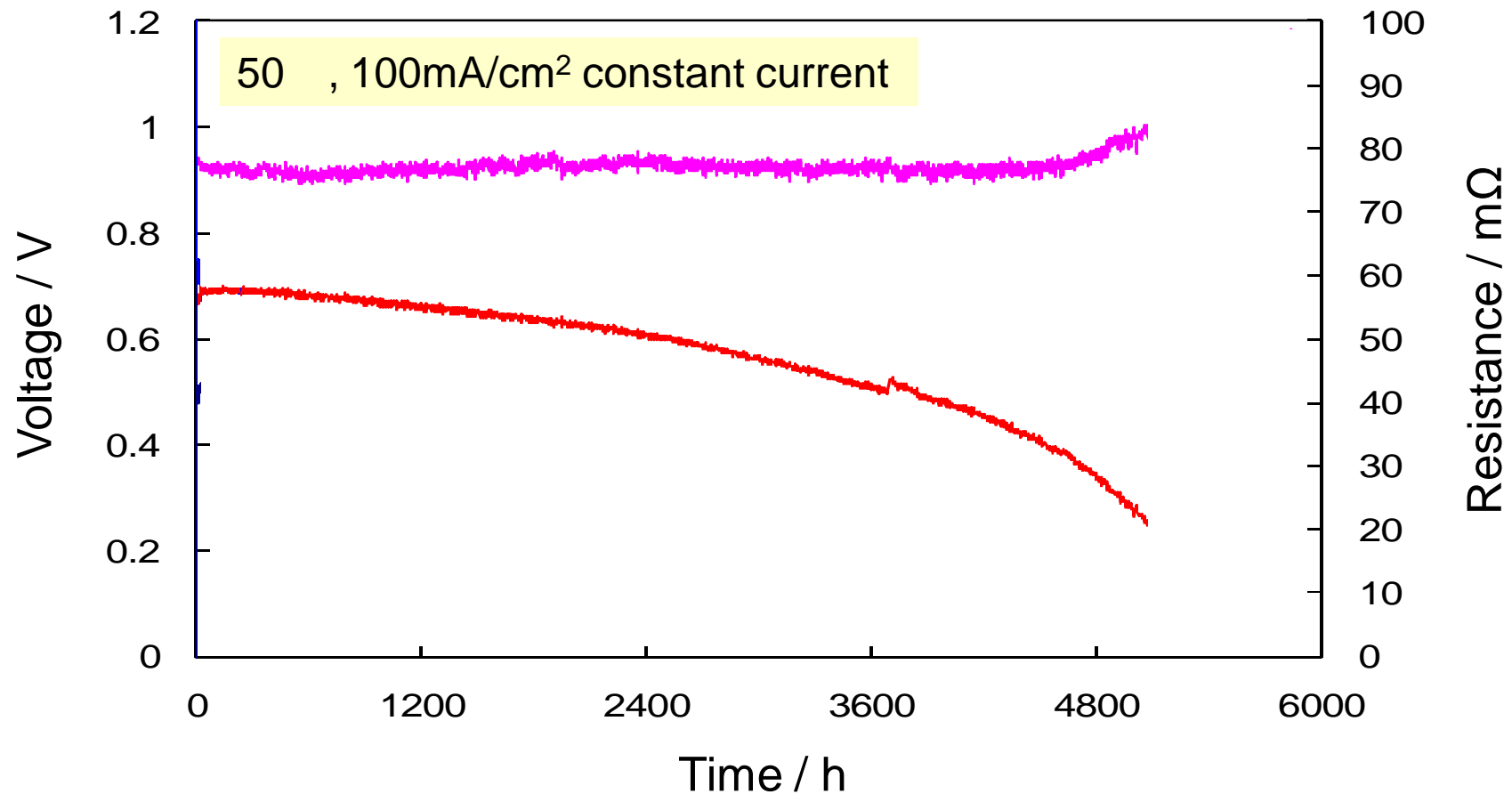
Improved Durability with Cross-Linked Ionomer

PENNSTATE



Electrochemical Engine Center

With cross-linked Ionomer, which also has higher IEC, shows better durability.





Summary

By improving properties of electrolyte materials, optimizing MEA construction and operating conditions, maximum power density was increased.

- around 500mW/cm² (H₂/O₂)
- around 350mW/cm² (H₂/clean air)

CO₂ in the air has large influence on the AMFC performance. To decrease the influence, AMFC operation at elevated temperature is effective, though it needs improved ionomer like cross-linked one.

- around 300mW/cm² (at 80 °C, H₂/normal air) *... not shown, unpublished date of PSU*

Durability at state of the art

- 700hrs at standard materials
- with cross-linked GDE : > 4000hrs (50 °C)
> 1200hrs (80 °C) *... not shown, unpublished date of PSU*

Issues for better performance

Materials improvement : ion conductivity, thermal stability

Decrease CO₂ influence : new concepts other than high temp. operation

MEA fabrication in relation with operating conditions



Thank you !